

# Fundamentals of Radium and Uranium Removal from Drinking Water Supplies

Dennis Clifford  
University of Houston

# Important Radium Isotopes

Radium Isotope	Half Life	Primary Emission	Decay Series
$^{226}\text{Ra}$	1600 y	Alpha	Uranium
$^{228}\text{Ra}$	5.7 y	Beta	Thorium
$^{224}\text{Ra}$	3.64 d	Alpha	Thorium

# Important Uranium Isotopes

<b>Isotope, Emission</b>	<b>Natural Abundance %</b>	<b>Half Life yr</b>	<b>Specific Activity pCi/μg</b>	<b>Relative Activity %</b>
$^{238}\text{U}, \alpha$	<b>99.276</b>	<b><math>4.51 \times 10^9</math></b>	<b>0.333</b>	<b>47.33</b>
$^{235}\text{U}, \alpha/\gamma$	<b>0.7196</b>	<b><math>7.1 \times 10^8</math></b>	<b>2.144</b>	<b>2.21</b>
$^{234}\text{U}, \alpha$	<b>0.0057</b>	<b><math>2.47 \times 10^5</math></b>	<b>6189.0</b>	<b>50.51</b>

Natural abundance and half life from Lange's Handbook, 1973, p. 3-108

Specific activity and relative activity calculated from isotope mass, half life and natural abundance.

If present at natural abundance  $1\mu\text{g U} = 0.67 \text{ pCi}$

# Chemical and Physical-Chemical Behavior of Isotopes

---

---

- Although possessing differing decay rates and modes of decay, the chemical and physical-chemical behavior of all isotopes is the same.
- 95% removal of  $^{226}\text{Ra}$  is also 95% removal of  $^{228}\text{Ra}$  when they are present together regardless of the ratio of their initial activities.
- 95% removal of  $^{238}\text{U}$  is also 95% removal of  $^{235}\text{U}$  when they are present together regardless of the ratio of their activities.

# Radium and Uranium Speciation in Ground Water as a Function of pH

<b>pH Range</b>	<b>Predominant Species</b>	<b>Predominant Species Charge</b>
<i>All</i>	$Ra^{2+}$	<i>a divalent cation</i>
<b>&lt; 5</b>	$UO_2^{2+}$	<b>a divalent cation</b>
<b>5 to 6.5</b>	$UO_2CO_3^0$	<b>a neutral molecule</b>
<b>6.5 to 7.6</b>	$UO_2(CO_3)_2^{2-}$	<b>a divalent anion</b>
<b>➤ 7.6</b>	$UO_2(CO_3)_3^{4-}$	<i>a tetravalent anion</i>

$$pCO_2 = 10^{-2} \text{ atm}, C_{T,U} = 2.38 \text{ mg/L}, 25 \text{ }^\circ\text{C}$$

*Above pH 10.5, positively charged uranyl hydroxide complexes are dominant.*

# Radium-Removal Methods

---

---

- **Cation Exchange Softening (BAT)**  
$$2 RNa + Ra^{2+} \rightarrow R_2Ra + 2 Na^+$$
- **Lime Softening (BAT)**
- **Reverse Osmosis (BAT)**
- **Sorption onto MnO<sub>2</sub> (HMO)**
- **Precipitation with BaSO<sub>4</sub> (by adding BaCl<sub>2</sub>)**
  - (Excess)Ba<sup>2+</sup> + (Trace)Ra + SO<sub>4</sub><sup>2-</sup> = Ba(Ra)SO<sub>4</sub>
- **Sorption onto BaSO<sub>4</sub>-Impregnated Media**
  - Media•BaSO<sub>4</sub> + Ra<sup>2+</sup> = Media•Ba(Ra)SO<sub>4</sub> + Ba<sup>2+</sup>
- **Electrodialysis**

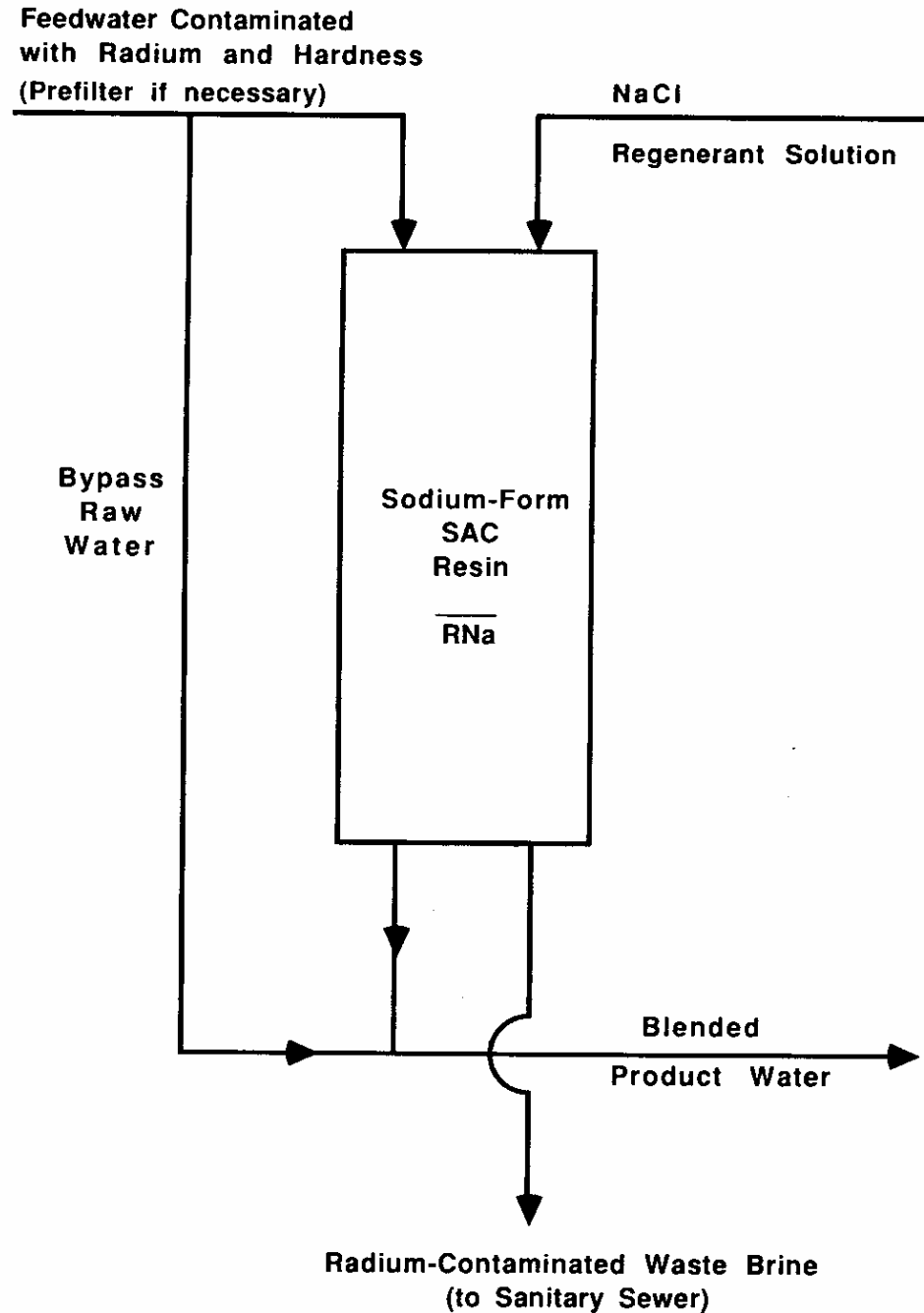
# POU Radium-Removal Methods

---

---

- **Reverse Osmosis (BAT)**
- **Cation Exchange Softening**  
$$2 RNa + Ra^{2+} \leftrightarrow R_2Ra + 2 Na^+$$
- **Sorption onto MnO<sub>2</sub>-impregnated fibers or filters, e.g., DE or granular media.**
- **Sorption onto BaSO<sub>4</sub>-Impregnated Resin or Activated Alumina**

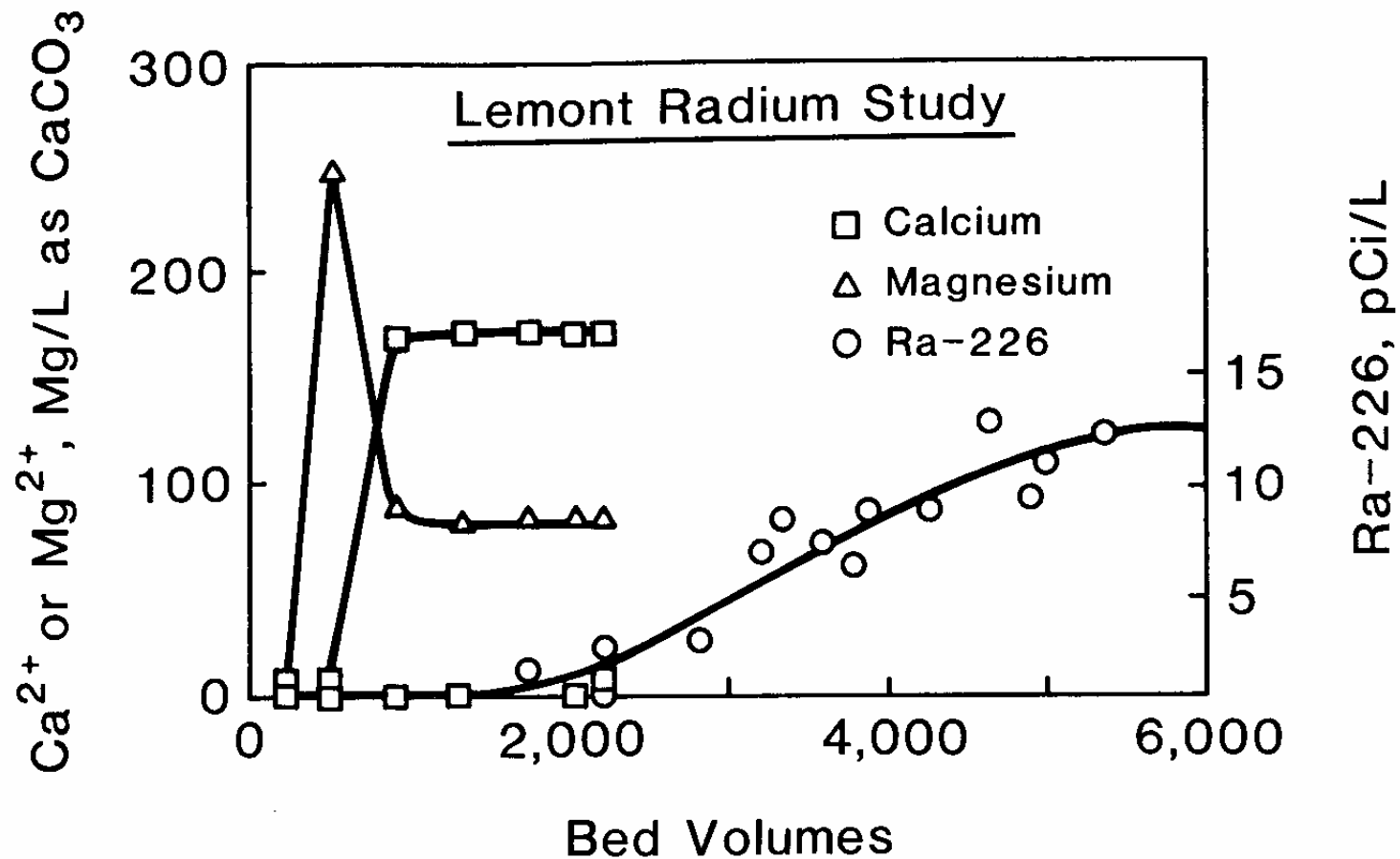
Radium  
removal by  
ion-  
exchange  
softening  
with  
bypass  
blending of  
raw water.





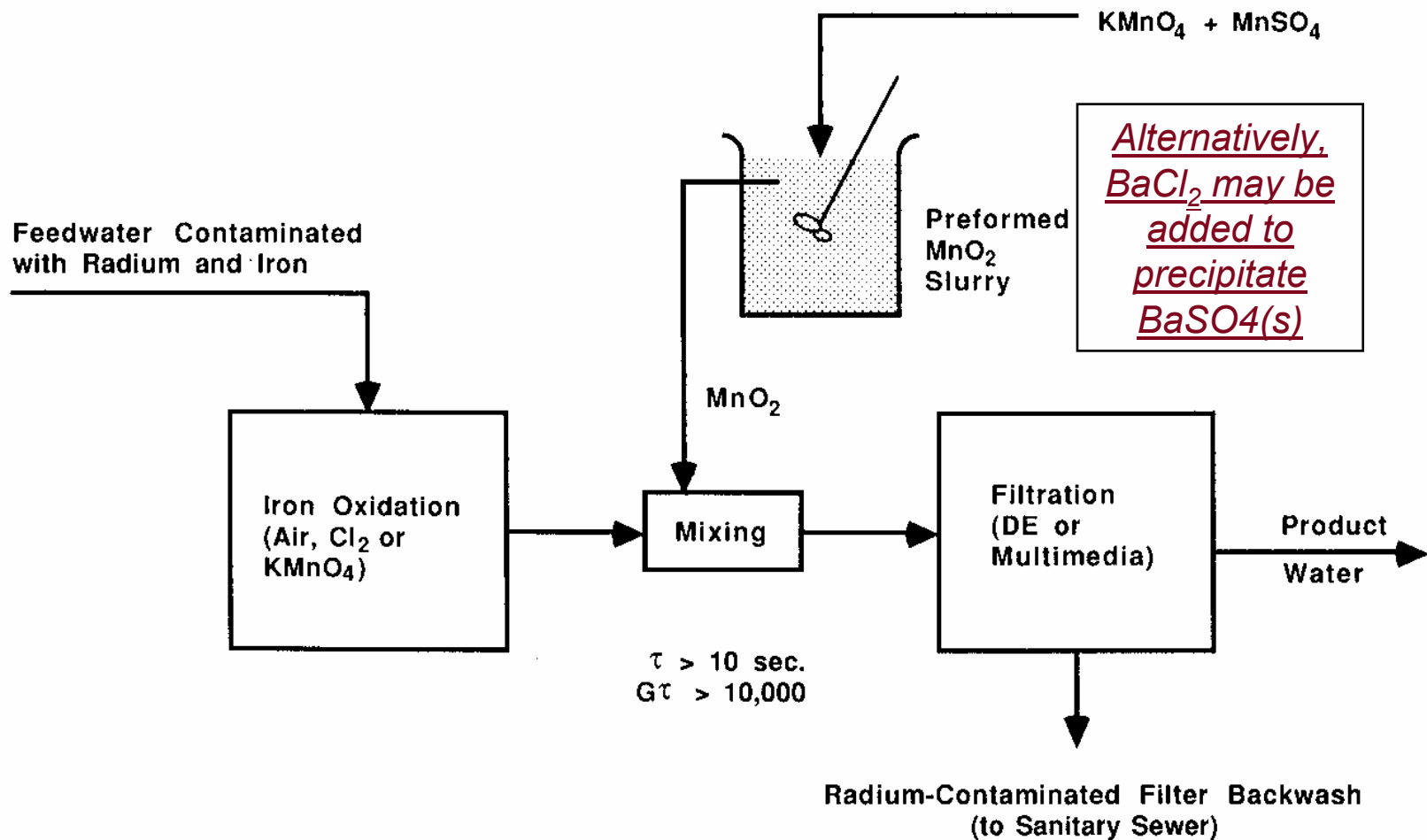
# Ion Exchange Resins for Radium Removal

<b>Designation</b>	<b>Resin Description</b>	<b>Ionic Form</b>	<b>Capacity meq/mL</b>
<b>Strong Acid Cation exchange resin for radium removal: Amberlite IR-120+, Duolite C20, Purolite C100, Dowex HCR-S</b>	<b>Standard gel SAC resin, polystyrene-DVB matrix, —SO<sub>3</sub><sup>-</sup> exchange groups</b>	<b>Na<sup>+</sup></b>	<b>1.9</b>

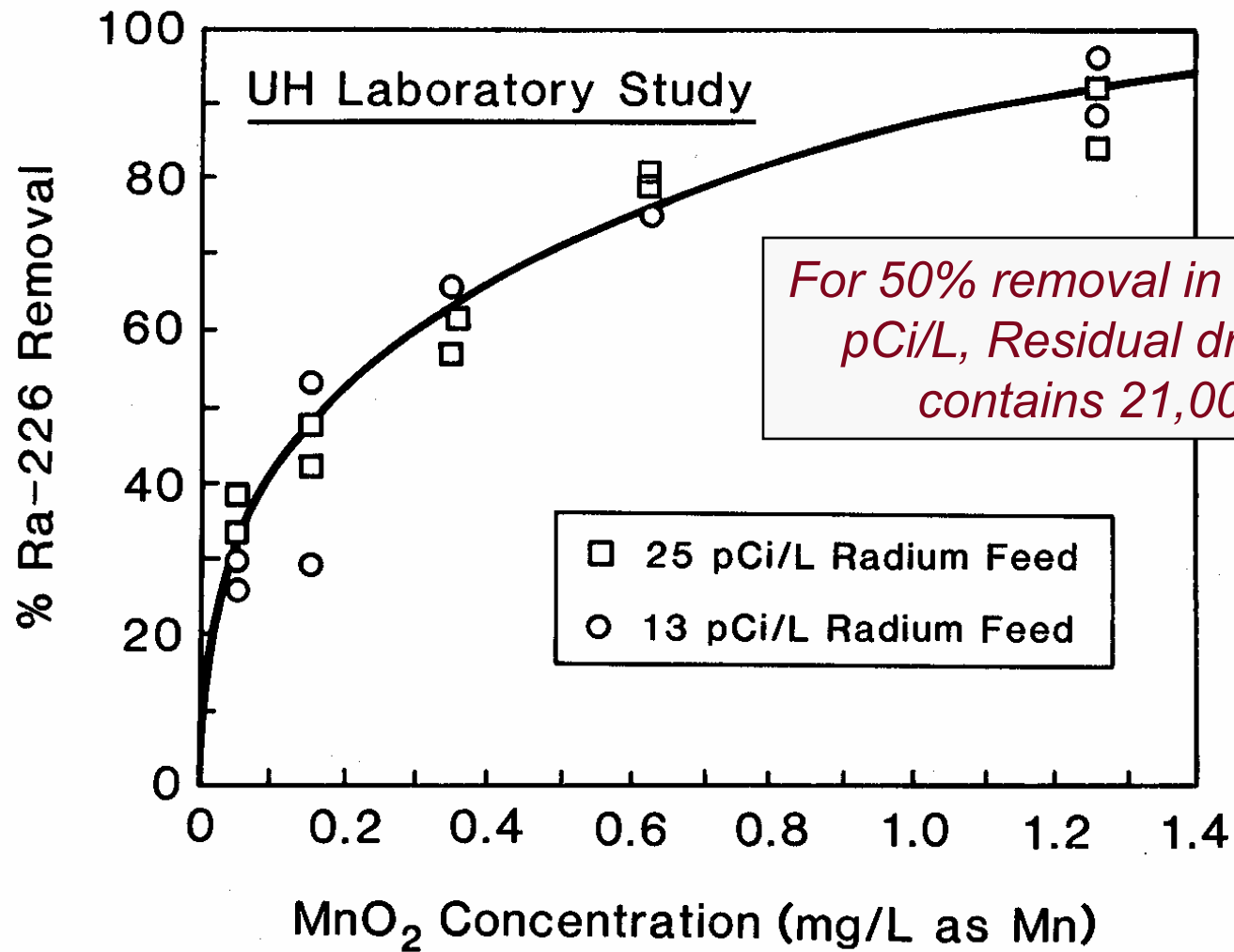


Magnesium, calcium and radium breakthrough curves for ion-exchange softening.

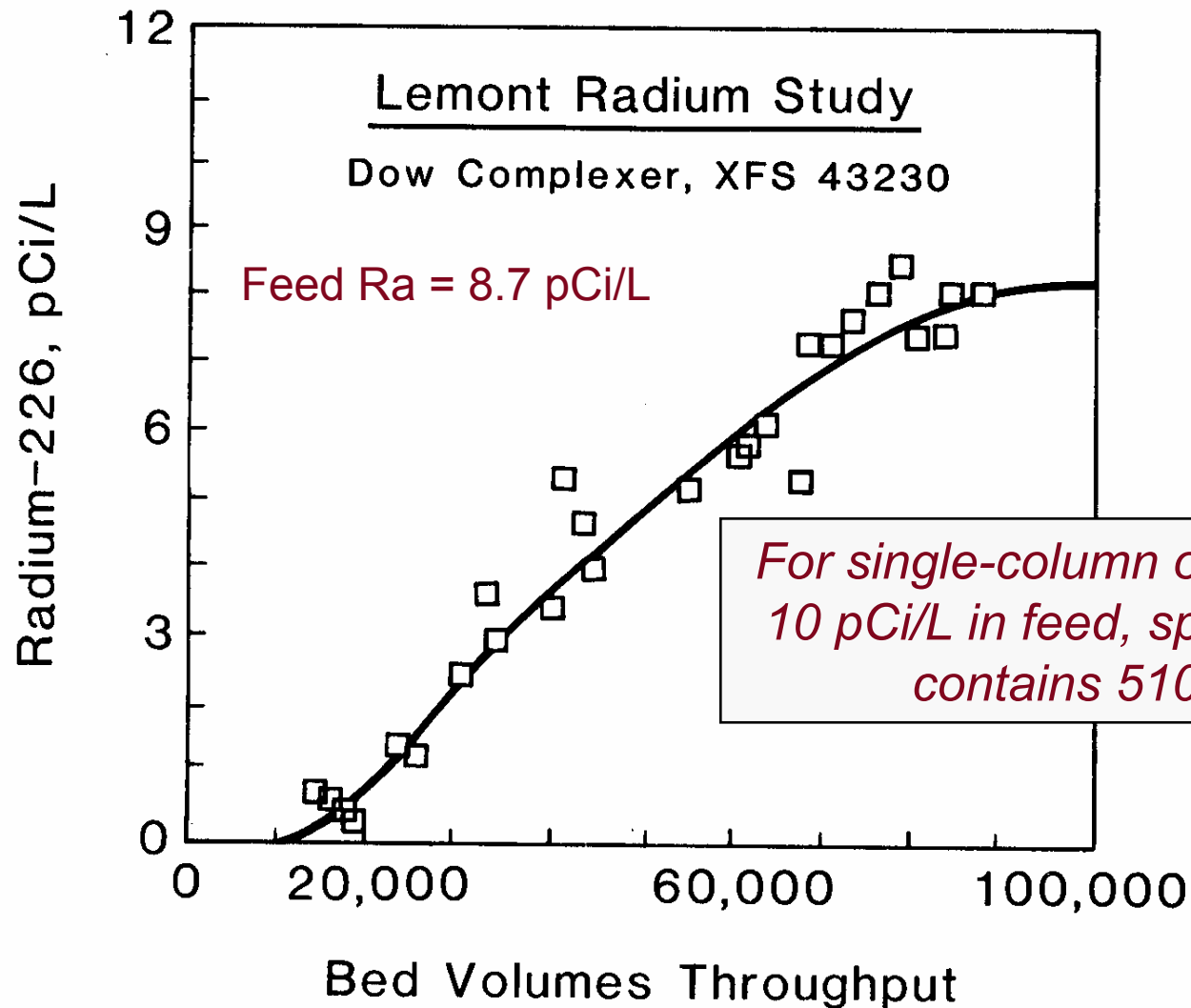
*If feed water contains 10 pCi/L, the resin contains ~20 pCi/g at steady state operation. Waste brine contains ~600 pCi/L*



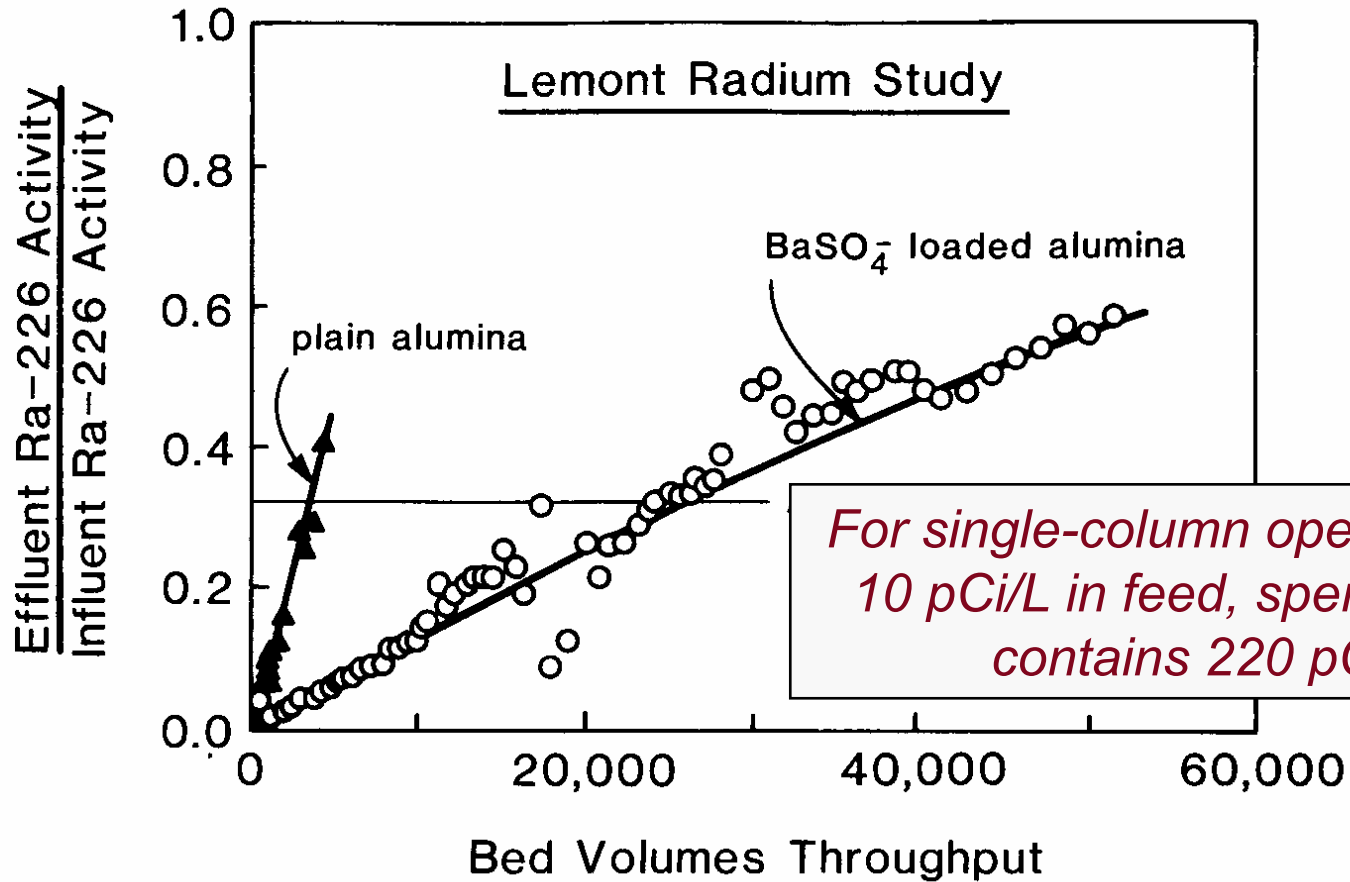
Process flow schematic for radium removal by adsorption onto preformed  $\text{MnO}_2$



Radium Removal as a function of  $\text{MnO}_2$  dose.  
Houston GW with 120 mg/L hardness and pH = 7.5



Radium breakthrough curve for Dow Radium Selective Complexer (RSC), a BaSO<sub>4</sub>(s) loaded cation resin.



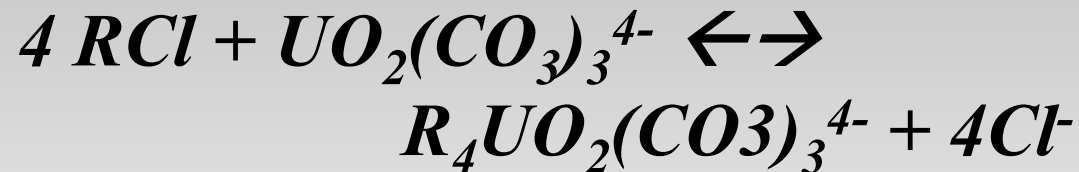
Radium breakthrough curves for plain and BaSO<sub>4</sub>-loaded activated alumina. EBCT = 3 min. Feed Ra = 8.7-11.3 pCi/L

# Uranium-Removal Methods

---

---

- **Anion Exchange (BAT)**



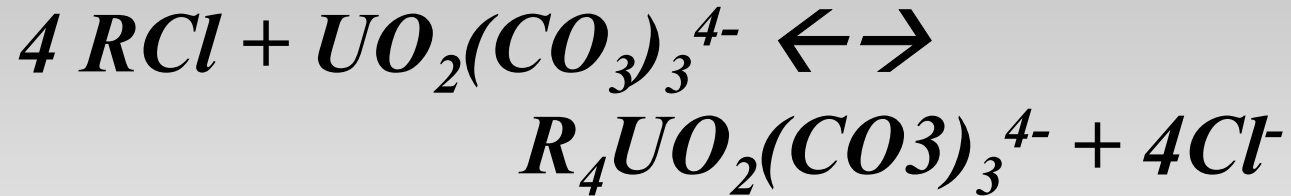
- **Lime Softening (BAT)**
- **Enhanced Coagulation /Filtration (BAT)**
- **Reverse Osmosis (BAT)**
- **Activated Alumina Adsorption**
- **Electrodialysis**

# POU Uranium-Removal Methods

---

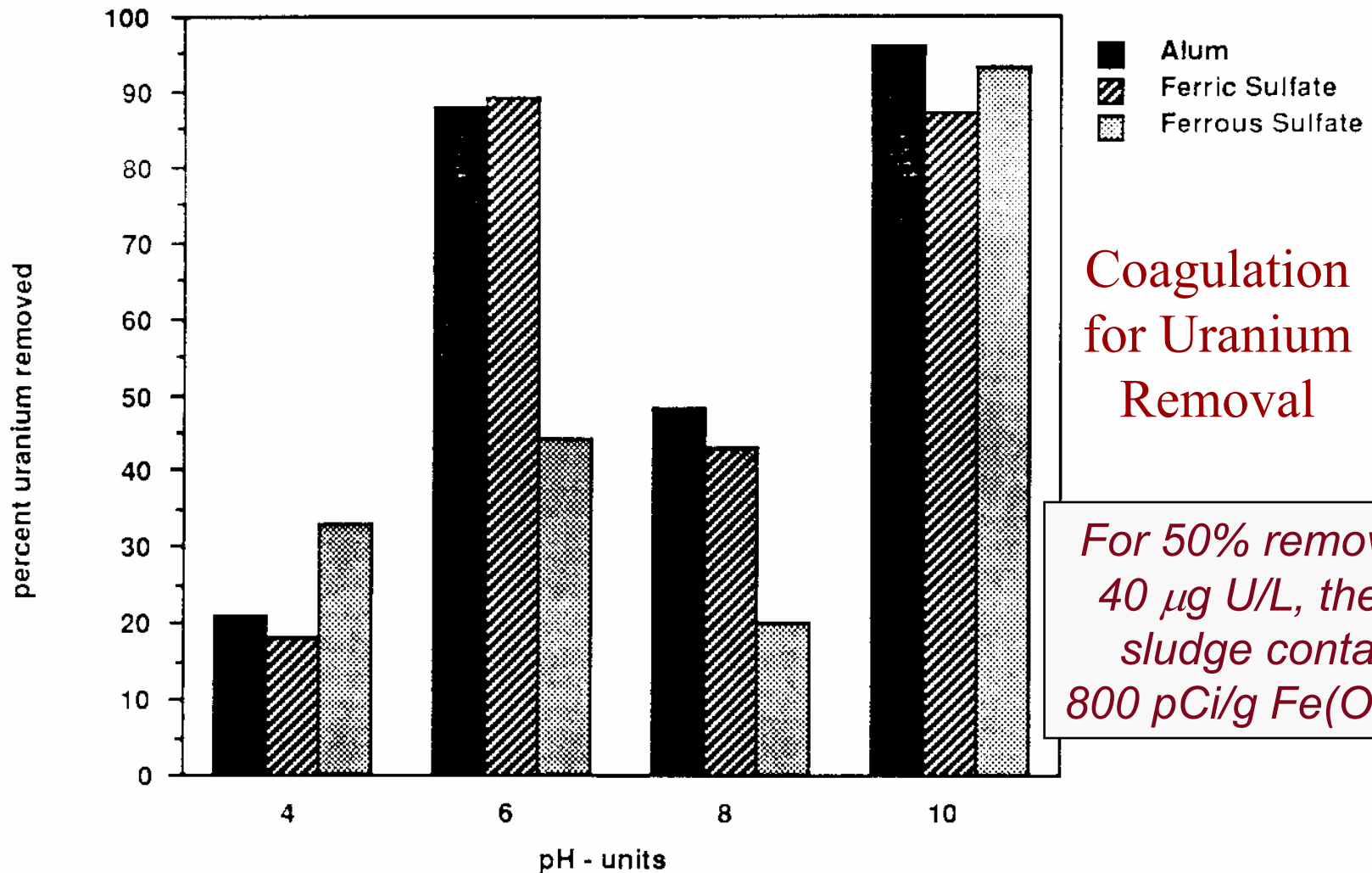
---

- **Anion Exchange**



- **Reverse Osmosis**
- **Activated Alumina Adsorption**



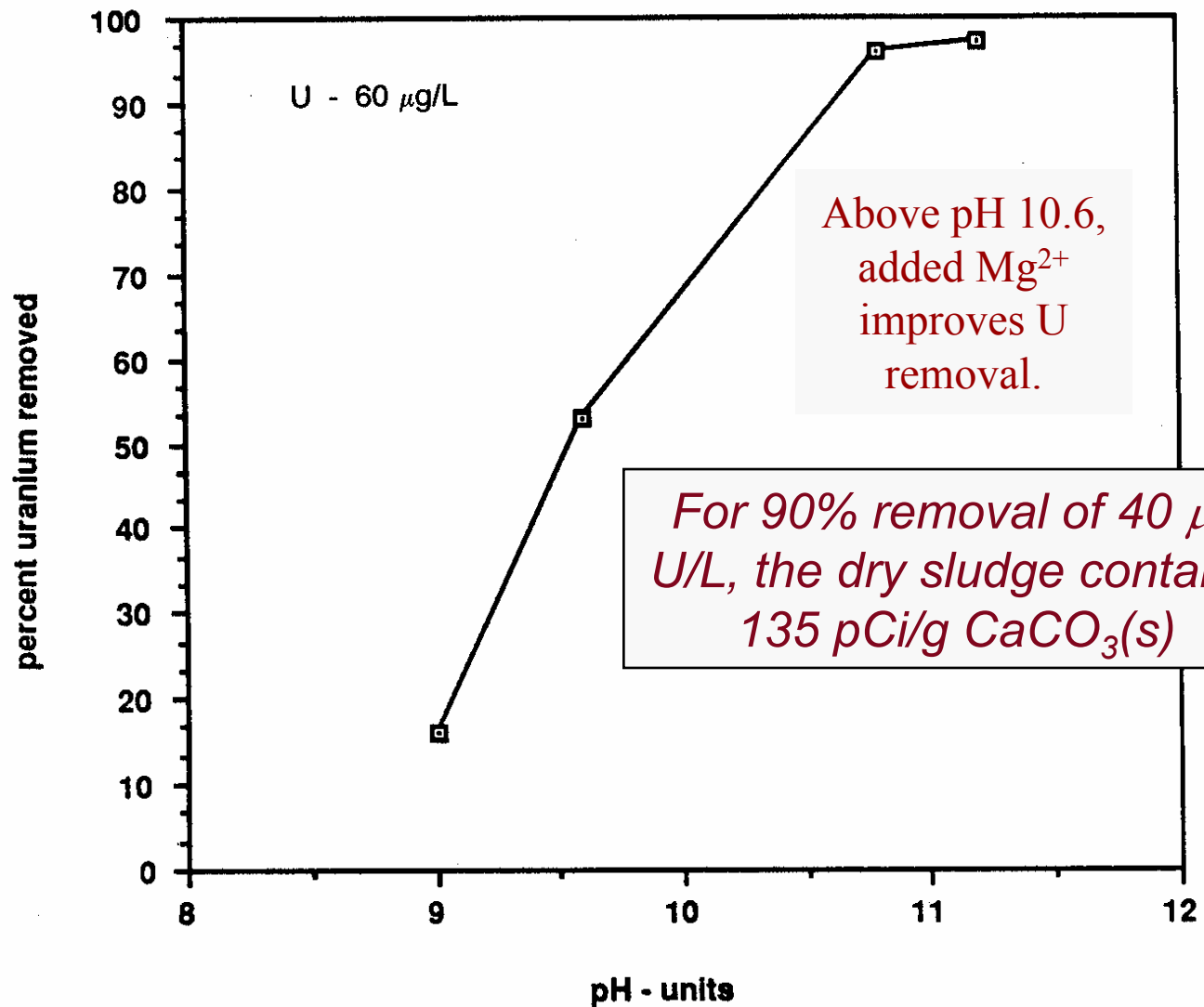


Coagulation  
for Uranium  
Removal

*For 50% removal of  
40  $\mu\text{g U/L}$ , the dry  
sludge contains  
800  $\text{pCi/g Fe(OH)}_3(\text{s})$*

Effect of pH and coagulant on uranium removal by  
coagulation with 25 mg/L dose.  
(Sorg 1990; Lee & Bondietti, 1983)

# Lime Softening for Uranium Removal

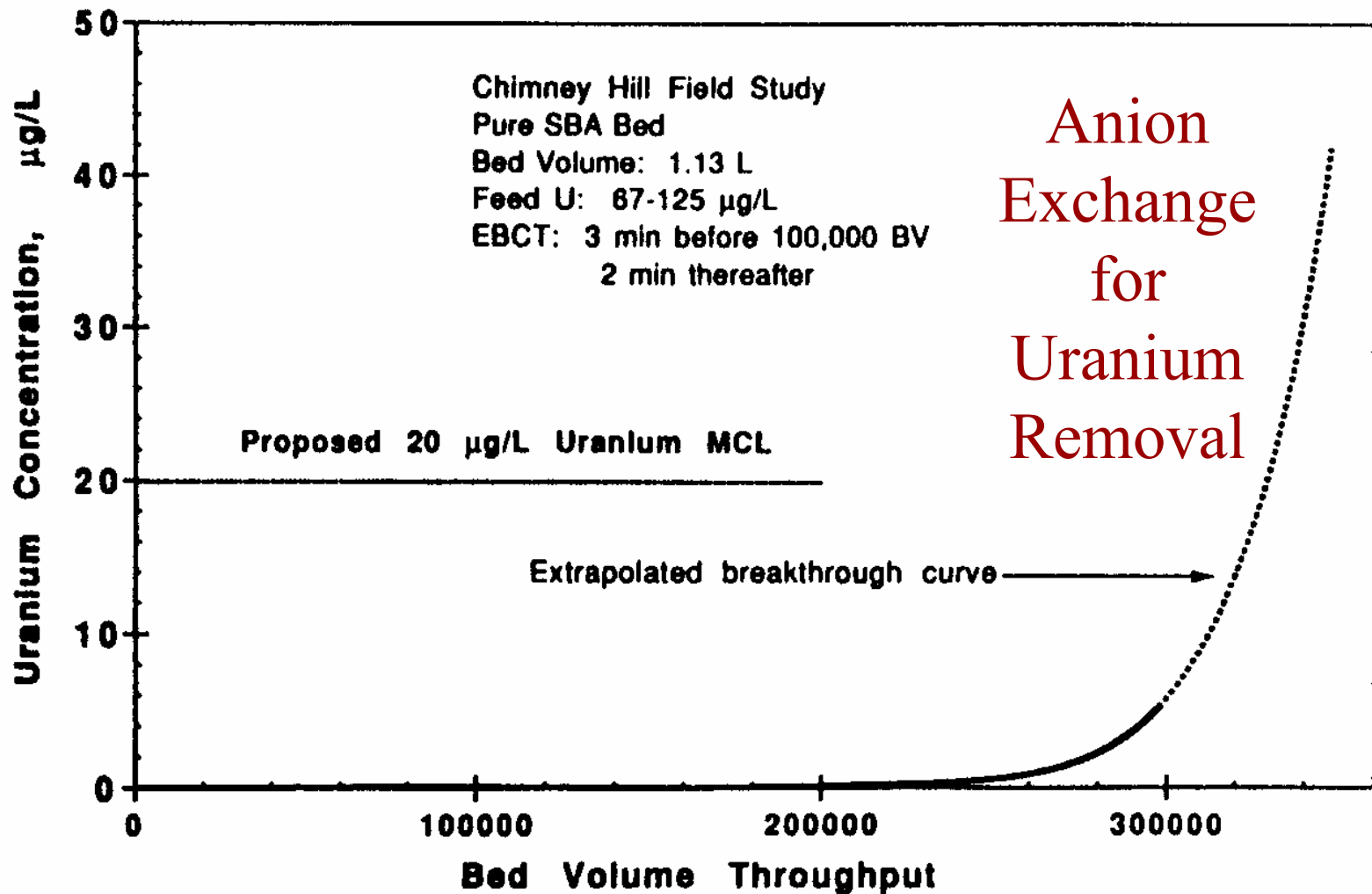


Effect of pH (and lime dose) on uranium removal by lime softening.

(Sorg 1990; Lee & Bondiotti, 1983)

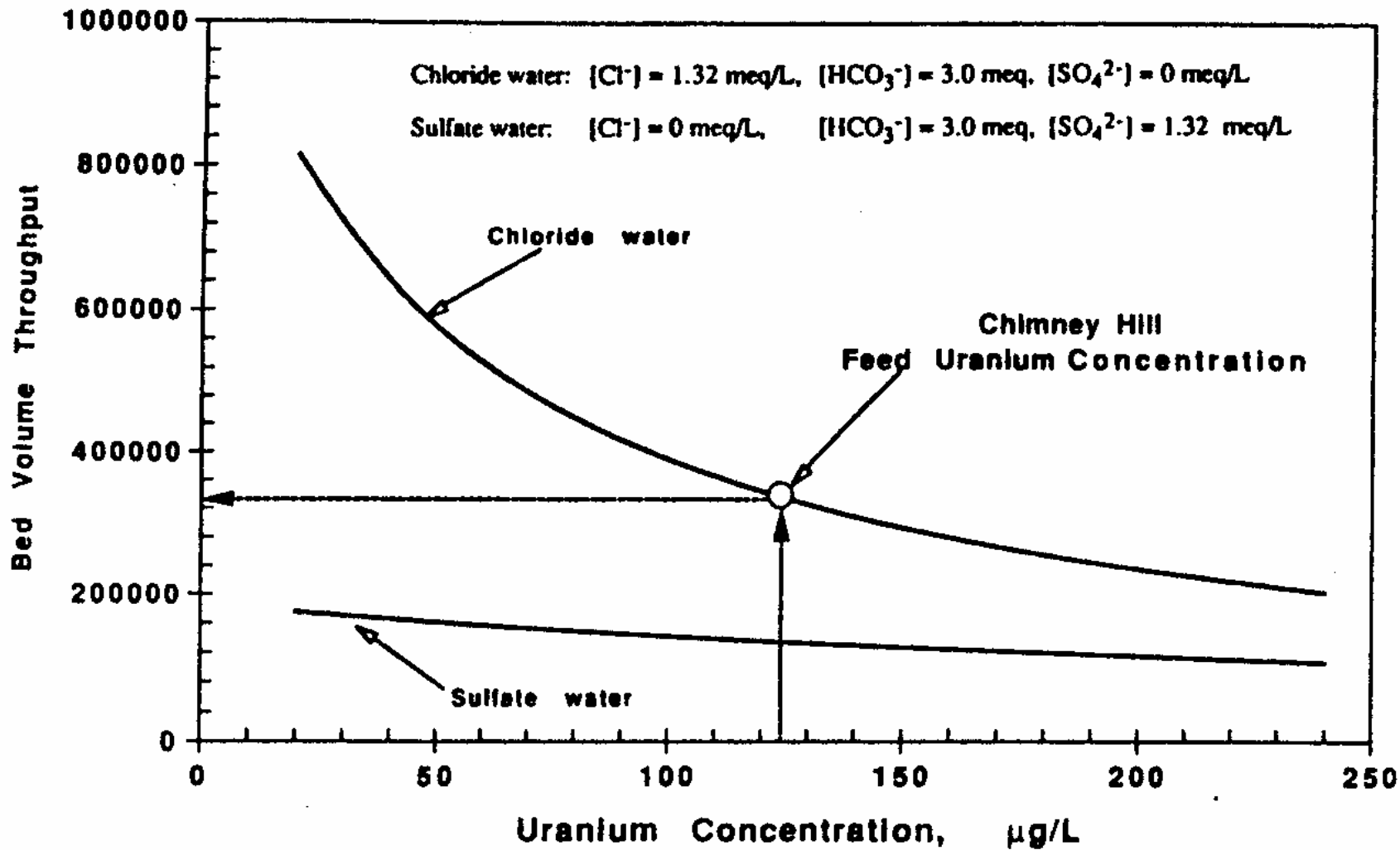
# Ion-Exchange Resins for Uranium Removal

<b>Designation</b>	<b>Resin Description</b>	<b>Ionic Form</b>	<b>Capacity meq/mL</b>
<b>Strong-Base Anion exchange resin for uranium removal Ionac A-642 Purolite A-500 Amberlite IRA 900</b>	<b>Type 1, macroporous, SBA resin, polystyrene-DVB matrix, <math>-\text{N}(\text{CH}_3)_3^+</math> exchange groups</b>	<b>Cl<sup>-</sup></b>	<b>1.0</b>



Effluent uranium levels during anion exchange with macroporous SBA resin at pH 8.

*If feed water contains 40 µg U/L, Waste brine contains ~80,000 pCi/L for a 30,000 BV run length.*



Effect of uranium, sulfate, and chloride concentrations on BV to uranium exhaustion.

# Processes for Radium Removal

<b>Treatment Method</b>	<b>Removal</b>	<b>Comment</b>
IX Softening (Na <sup>+</sup> , SAC)	>95%	Operate to hardness breakthrough, NaCl Regen.
Ba(Ra)SO <sub>4</sub> Precipitation	50-95%	Add BaCl <sub>2</sub> to feed water before filtration.
MnO <sub>2</sub> Adsorption	50-95%	Use preformed MnO <sub>2</sub> or MnO <sub>2</sub> -coated filter media.
RO	>99%	Effective but expensive

# Processes for Uranium Removal

<b>Treatment Method</b>	<b>Removal</b>	<b>Comment</b>
Coagulation w Fe/Al	50-90%	Effective at pH near 6 and 10
Lime Softening	80-99%	Higher pH = greater removal. Mg <sup>2+</sup> helps at pH > 10.6.
Anion Exchange	>95%	Regenerate with 2-4 M NaCl after 10,000-50,000 BV
RO	>99%	Effective but expensive

# Residuals

- The more effective the coagulant or adsorbent, the higher is the radioactivity in the residuals.

Ion Exchange Softening for Radium Removal	600 pCi/L spent brine 20 pCi/g dry resin
Coag-Filt w $\text{MnO}_2(\text{s})$ for Radium Removal	21,000 pCi/g dry $\text{MnO}_2(\text{s})$
Fe(III) Coag-Filtration for Uranium Removal	800 pCi/g $\text{Fe}(\text{OH})_3(\text{s})$
Anion Exchange for Uranium Removal	80,000 pCi/L spent brine (30,000 BV run length)