

TECHNOLOGIES

## MAY 2019 – MAY 2020 PERIODIC REVIEW REPORT

ARO Corporation Site Cheektowaga, New York Site # 915147

June 2020

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Prepared for:

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#### 2019-2020 ANNUAL SITE MANAGEMENT PERIODIC REVIEW REPORT

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## **ACRONYMS AND ABBREVIATIONS**

Arcadis	Arcadis of New York, Inc.
bgs	below ground surface
cfm	cubic feet per minute
cm/sec	centimeters per second
COC	constituent of concern
DCE	dichloroethene
EC/BSA	Erie County/Buffalo Sewer Authority
EDD	EQuIS Electronic Data Deliverable
gpm	gallons per minute
in.Hg	inches of mercury
lb	pounds
LPGAC	liquid-phase granular activated carbon
LRP	liquid ring pump
NYSDEC	New York State Department of Environmental Conservation
O&M	Operation and Maintenance
ORP	oxidation-reduction potential
PF	pneumatic fracturing
PRR	Periodic Review Report
PVC	polyvinyl chloride
TCE	trichloroethene
µg/m³	micrograms per cubic meter
µg/L	micrograms per liter
USEPA	United States Environmental Protection Agency
VC	vinyl chloride
VER	Vacuum-Enhanced Recovery
VOC	volatile organic compound

## **1 EXECUTIVE SUMMARY**

Arcadis of New York, Inc. (Arcadis), on behalf of Trane Technologies Company LLC (formerly Ingersoll Rand Company), has prepared this Annual Site Management Periodic Review Report (PRR) for the ARO Corporation Site (New York State Department of Environmental Conservation [NYSDEC] Site Code 915147) (referred to hereafter as the Site) located in Cheektowaga, Erie County, New York (Figure 1). This PRR covers the period from June 2019 through June 2020 (reporting period), as requested in a letter from NYSDEC dated April 10, 2020.

This PRR summarizes the operational and performance monitoring data generated during the 2019-2020 reporting period for the remedial program at the Site. The basis of this report is to satisfy the requirements set forth in the Site Management PRR request and provide the supporting documentation for the Institutional and Engineering Controls Certification (Appendix A).

In accordance with the Remedial Design/Remedial Action Work Plan (Geraghty & Miller 1997), a vacuumenhanced recovery (VER) system (Figure 2) was installed to recover chlorinated volatile organic compounds (VOCs) present in the dissolved, adsorbed, and vapor phases in the subsurface at the Site. The main constituents of concern (COCs) at the Site are trichloroethene (TCE) and dichloroethene (DCE). The system has been in operation for approximately 22 years.

Overall, the current remedial program has been effective in achieving the remedial goals at the Site by containing and eliminating off-site migration of contaminated soils and groundwater. During the reporting period, the system recovered 1,105,117 gallons of impacted groundwater. Total COC mass removal included approximately 0.32 kilogram (kg) (0.7 pounds [lb]) in the dissolved phase and 20.4 kg (45 lb) in the vapor phase. VOC concentrations in groundwater continue to improve in seven of the ten wells, with three wells exhibiting historically low concentrations in 2019. Three of the ten wells remain relatively stable with some variability occurring due to seasonal fluctuation, as compared to baseline conditions.

All the elements defined in the Operation and Maintenance (O&M) Plan were in compliance during the reporting period. The remedial system was operated continuously during the reporting period, except for noted routine and/or non-routine maintenance activities. No substantial changes were made regarding site management and remedial system operation during the reporting period.

In accordance with the NYSDEC 2018-2019 PRR acceptance letter, dated February 3, 2020, Arcadis will prepare a Well Decommissioning Work Plan to abandon historical wells MW, MWR, MW-5, MW-14, MW-14R, MW-17, MW-18, MW-27, and VEROW-2). This work plan will be submitted under separate cover for the Departments review.

The PRR is organized as follows:

- Section 2 provides a brief overview of the site location, physical description, and previous remedial enhancements.
- Section 3 describes the VER system layout and process.
- Section 4 discusses the system O&M and summarizes operation data.
- Section 5 provides a summary of the system performance evaluation and system analytical results.

- Section 6 summarizes the groundwater monitoring program and groundwater sampling results.
- Section 7 provides conclusions and 2020-2021 goals.
- Section 8 provides a list of references.

## **2 SITE OVERVIEW**

## 2.1 Site Location and Description

The ARO Corporation site is located on Broadway Street (Route 130) in the Town of Cheektowaga, Erie County, New York (Figure 1). The property consists of the former ARO Corporation parcel and two parcels located adjacent and west of the ARO parcel. The area surrounding the Site is zoned as light industrial/residential. The Site is listed in the Registry of Inactive Hazardous Waste Disposal Sites in New York State as Site Number 915147. The Site is designated as Class "4,", which means the Site was properly closed and requires continued management or continuation of O&M activities.

### 2.2 Background

The former ARO main facility building, which was demolished in December 1997, covered approximately 69,000 square feet of the property. The floor slab of the former main facility building was left in place and not demolished. A separate maintenance and storage building, approximately 4,800 square feet in size, was not demolished and is located south of the west side of the main facility building (Figure 2). The maintenance building currently houses the on-site VER system. Other property areas include a paved area north of the former main facility building, and a larger, paved parking lot area south of the former building. Areas south and west of the parking lot are open fields. The former Zydel properties included former residences and a garage that were demolished in late November 1998.

A storm water drainage ditch extends southward along the eastern property boundary and westward along the southern property boundary. Another drainage ditch begins at a backfilled culvert on the south side of the parking lot. Surface water runoff within this ditch flows south to the west-flowing portion of the storm water drainage ditch located along the perimeter of the property.

The original VER system was installed in 1998 and has been operational for 22-years. The vapor treatment system was taken offline in July 2000 after it was determined not to be required because the vapor phase concentrations had not exceeded Air Guide 1 levels during the operation of the remedial system during the first several years of operation.

Pneumatic fracturing (PF) was conducted at several select areas of the Site in 2004, 2006, and 2009. Pneumatic fracturing is a process by which air is injected at high pressures into the subsurface to create fractures in the geological formation to promote increased hydraulic and pneumatic conductivity, thereby improving the mass recovery potential for site recovery wells. Pneumatic fracturing was conducted at PF-1 through PF-4 in 2004, PF-5 through PF-9 in 2006, and PF-10 through PF-13 in 2009 (Figure 2).

As part of an overall remedial strategy to reduce the remedial lifecycle at the Site, seven former PF wells and one former monitoring well were converted to recovery wells in 2014 (Arcadis 2013]). The remedial goals for the enhancements were to increase the radius of influence of the existing system within the

source areas, thereby providing additional extraction of the higher concentration VOC mass from these impacted areas of the Site.

### 2.3 Site Geology and Hydrogeology

The subsurface conditions encountered at the Site consist of three primary units: fill material and/or native clay to 5 feet below ground surface (bgs), brown till from approximately 5 to 15 feet bgs, and gray till from approximately 15 to 25 feet bgs. The brown and gray till subsurface conditions encountered at the Site are consistent with a low permeability glacial till geologic formation. Hydraulic conductivities within the till are estimated to be in the range of 10<sup>-5</sup> centimeters per second (cm/sec) to 10<sup>-8</sup> cm/sec.

Shallow groundwater has been encountered at depths ranging from 1 to 5 feet bgs throughout the Site. Based on the configuration of the water table at the Site, the horizontal direction of groundwater flow is to the south. The horizontal gradients across the Site vary and are dependent on whether the VER system is operational.

## **3 VACUUM ENHANCED RECOVERY SYSTEM OVERVIEW**

The VER system currently comprises 19 recovery wells. The recovery well locations are shown on Figure 2.

The above grade process and treatment equipment include the following: a liquid ring pump (LRP), a knockout tank (i.e., air/water separator), and liquid phase treatment components. The system equipment and instrumentation are interlocked to a programmable logic controller, which regulates system operation in automatic mode and will activate a system shutdown and alarm callout in the event of a system malfunction. A system layout showing the location of recovery wells and the treatment system is provided on Figure 2.

Vacuum is applied to the recovery wells by the LRP unit via below-grade vacuum process piping. The LRP removes both groundwater and subsurface vapor (i.e., dual-phase) from the recovery wells. The LRP is similar to a conventional vacuum blower, except that it can generate much higher levels of vacuum [28 inches of mercury (in.Hg)].

The recovered groundwater and vapor from each recovery well are directed from a common manifold to the knockout tank. The knockout tank is designed to separate the liquid and vapor process streams from one another. Groundwater is transferred using progressive cavity transfer pumps through four bag filter vessels configured in series, which removes particulates larger than 25 microns in diameter. The final treatment for groundwater consists of two 1,000-lb liquid-phase granular activated carbon (LPGAC) vessels piped in series. The average and cumulative extracted groundwater flows are monitored, and data are logged via a flow transmitter and paddlewheel flow sensor. The extracted vapor-phase flows are monitored and recorded utilizing a hand-held anemometer that measures the velocity, which is then converted to a volumetric flow.

Downstream from the knockout tank, the vapor stream passes through a particulate filter, the LRP, and a secondary knockout tank prior to being released to the atmosphere.

The liquid-phase treatment vessels are equipped with a manifold that can be valved for series, parallel, or isolated operating configurations, allowing flexibility in treatment operation during non-routine maintenance activities. Sample collection valves and individual pressure indicators are located on the inlet and discharge sides of each vessel.

The LPGAC vessels are designed to remove VOCs from the liquid process stream prior to discharge. Treated groundwater is discharged to an on-site sanitary sewer connection under an industrial wastewater discharge permit. The vapor is vented directly to the atmosphere approximately 10 feet above the building roofline.

## **4 SYSTEM OPERATION AND MAINTENANCE**

The VER system operated continuously during the reporting period with only brief shutdown periods due to scheduled O&M activities, non-routine maintenance, and the occurrence of alarm conditions. A combination of recovery wells was operated during 2019 and the first part of 2020, ranging from seven to ten recovery wells operating at one time.

O&M site visits consist of system inspection, recording of operating parameters, influent and effluent system sampling, and investigation of any alarms that may have occurred. The operational data collected during each site visit, as well as maintenance related to each of the major system components (extraction system, liquid and vapor treatment) are discussed in the following subsections.

## 4.1 System O&M

The following O&M tasks were performed on the VER system (LRP, transfer pump, and related equipment):

- Checked and recorded overall system operation and alarm status;
- Recorded vacuum gauge readings at the knockout tank and LRP to confirm applied vacuum operational set points;
- Checked LRP seal oil level, filter pressure, and temperature to ensure that the LRP was operating within the allowable ranges as recommended by the manufacturer;
- Recorded total volume of groundwater recovered and average groundwater recovery flow rates;
- Recorded extracted air flow rate; and
- Recorded vacuum level readings at individual recovery well gauges (both at interior valve manifold and recovery wellhead locations).

#### 4.1.1 Vapor Extraction System O&M

The following O&M tasks were performed regarding the vapor-phase portion of the system:

- Recorded the post-LRP/inlet temperature of the secondary knockout tank
- Recorded the vapor flow rate using a handheld anemometer
- Inspected all pipes and fittings for potential leaks
- Collected effluent vapor samples for laboratory analysis.

The vapor sampling results are also used to estimate the VOC removal from the vapor extraction portion of the system. Vapor-phase mass removal estimates are summarized in Section 5.4.2.

#### 4.1.2 Liquid Treatment System O&M

The following O&M tasks were performed regarding the liquid-phase treatment portion of the system.

- Recorded pressure level readings at the inlet and outlet pressure gauges for each of the two LPGAC vessels.
- Recorded the pre- and post-sediment filter pressure readings.
- Replaced liquid-phase bag filters as needed.
- Inspected all pipes and fittings for potential leaks.
- Inspected liquid- and vapor- phase flow meters to ensure proper operation.
- Collected influent (pre-LPGAC vessel #1), midpoint (post-LPGAC vessel #1), and effluent (post-LPGAC vessel #2) system groundwater samples and submitted for laboratory analysis.
- Cleaned out knockout tank and y-strainer as needed.
- Maintained the LRP and progressive pumps.
- Cleaned and maintained flow meter to ensure continuous flow monitoring, as required by the Erie County/Buffalo Sewer Authority (EC/BSA) industrial wastewater discharge permit.

As outlined above, influent, midpoint, and effluent liquid samples are submitted for laboratory analysis on a quarterly basis. The analytical results are used to determine if the LPGAC media is spent; a condition that can be indicated by the breakthrough of VOCs downstream from the first and/or second LPGAC vessel. Pressure differentials across LPGAC vessels are also used to determine if head losses across vessels are high as a result of the carbon being spent due to adsorption sites being utilized or inorganic fouling (e.g., silt or scale). The system influent groundwater sampling results are used to estimate the VOC removal from the liquid extraction portion of the system. The system effluent groundwater sampling results are used to track the performance of the treatment system to meet the permit requirements set forth by the BSA. The BSA permit requires compliance sampling and reporting on a quarterly basis.

## 4.2 System Repairs and Non-Routine O&M

During the reporting period, the following system repairs and non-routine O&M activities were performed and remedial enhancements were implemented:

- During the week of June 10, 2019 several non-routine site/system maintenance activities were completed:
  - Redeveloped recovery wells RW-3, 3A, 10, 10A, 11, 11A, and 11B.
  - Redeveloped monitoring well MW-6.
  - Cleaned/redeveloped recovery piping between wells RW-3, 10, and 11 and the treatment system manifold.
  - o Replace several faulty treatment system valves/fittings.
  - Site mowing and vegetation control.

- A transfer pump motor fault alarm was received on August 16, 2019. The alarm was determined to be a tripped overload relay. The system was inspected, restarted, and resumed normal operation on August 16, 2019.
- During the week of October 28, 2019 several non-routine system maintenance activities were completed:
  - Replace clogged section of recovery wells RW-3 and RW-10/RW-10A piping near the well heads.
  - o Clean system manifold control valves.
  - Replace faulty manifold vacuum gauges.
  - o Replace cracked fitting on bag filter housing.
  - o Change out carbon in lag vessel and swap lead lag position.

## 4.3 Objectives of Monitoring

During operation of the VER system, various data were collected and analyzed to evaluate the overall performance and effectiveness of the system. This performance monitoring is intended to achieve the following objectives:

- Evaluate total VOC recovery in the liquid and vapor phases during the operational period.
- Evaluate performance of the groundwater treatment system.
- Determine if any modifications to the system are required to enhance and maximize system performance.
- Ultimately determine when remedial endpoints have been achieved.

Data generated from the system performance monitoring activities are outlined below.

## 4.4 System Operational Data

The VER system operational data are summarized in Table 1. These data include the applied vacuum, extracted vapor and groundwater flow rates, and extraction wellhead vacuums.

#### 4.4.1 Groundwater Recovery Rates

Total groundwater flow readings were taken from the totalizing flow meter installed on the liquid discharge of the VER system. The average system groundwater flow rates are included in Table 1. A cumulative total of 19,4344,916 gallons of groundwater has been recovered by the VER system as of May 1, 2020. A total of 1,105,117 gallons of water were treated by the VER system during the reporting period (Table 2). This total flow corresponds to an average recovery rate of approximately 2.1 gallons per minute (gpm) over the entire reporting period.

### 4.4.2 Applied Vacuum/Extracted Vapor Flow Rate

The observed applied vacuum at the system knockout tank generated by the LRP ranged from 11 in.Hg to 21 in.Hg during the reporting period. The extracted vapor flow rate ranged from about 59 to 110 cubic feet per minute (cfm) during the reporting period. The average system vapor flow rates are included in Table 1.

## **5 SYSTEM PERFORMANCE EVALUATION**

The following sections provide an evaluation of the remedial system performance monitoring data during the reporting period, and an overview compared to the baseline (1998) remedial system operation. The estimated annual and total mass removed by the VER system was calculated using the influent VOC sampling results, and system groundwater and vapor extraction flow rates.

## 5.1 System Liquid Phase

As outlined, groundwater samples were collected on a quarterly basis from the influent of the treatment system, the midpoint between the two LPGAC units, and the effluent (prior to discharging to the sewer under the EC/BSA industrial wastewater discharge permit). All samples were submitted to SGS North America Laboratories located in Dayton, New Jersey, for analysis. The system liquid-phase sampling laboratory analytical results have been submitted to NYSDEC's EIMS Administrator in the required EQuIS Electronic Data Deliverable (EDD) format.

#### 5.1.1 Liquid-Phase Influent Analytical Results

System influent liquid-phase (i.e., groundwater) samples were analyzed for VOCs using United States Environmental Protection Agency (USEPA) Method 8260. The influent sample concentrations were used to estimate the total VOC mass removal from the subsurface and to evaluate the relative changes in the mass removal rate over time. The mass removal estimate is generated using the quarterly influent sample analytical data and the cumulative groundwater flow totals.

Dissolved-phase concentrations of TCE, DCE, and vinyl chloride (VC) in the influent, midpoint, and effluent liquid samples are provided in Table 3. The quarterly influent concentrations of TCE, DCE (total), and VC in samples collected since the system startup (1998) through April 2020 are illustrated graphically on Figure 3.

Quarterly liquid-phase influent concentrations during the reporting period ranged from 41 to 83 micrograms per liter ( $\mu$ g/L) for TCE and 16 to 37  $\mu$ g/L for DCE. Influent concentrations vary widely based on which recovery wells are online at the time of the sampling and other factors such as extraction rates and groundwater yield/recharge conditions.

Quarterly system liquid-phase samples were collected from the mid-carbon location between the two LPGAC units and analyzed for VOCs using USEPA Method 8260. Liquid-phase midpoint samples were collected to monitor the performance of the lead LPGAC unit and to help determine when a carbon media change is warranted. As noted previously, dissolved-phase concentrations of TCE, DCE, and VC in the influent, midpoint, and effluent samples are provided in Table 3.

#### 5.1.2 Liquid Extraction Rates

As discussed in Section 4.4.1, the total recovered groundwater flows correspond to an average recovery rate of approximately 2.1 gpm over the reporting period. This is relatively consistent with the annual average groundwater recovery rates from 2009 through April 2020, which ranged from 1.5 to 2.8 gpm.

#### 5.1.3 Liquid-Phase Mass Removal

Influent groundwater sampling results were used to estimate VOC recovery rates. As shown in Table 2, influent VOC levels and groundwater recovery rates were used to calculate the estimated overall mass of VOCs recovered in the dissolved phase. A total estimated approximate mass of 0.32 kg (0.7 lb) of VOCs was recovered in the dissolved phase during the reporting period.

As the data in Table 2 and on Figure 3 indicate, the dissolved-phase mass recovery estimates ranged from 0.5 to 1.3 gram per day. The fluctuation in dissolved-phase VOC recovery at the time of sampling is due to variability in the influent mass concentrations in the extracted groundwater depending on which recovery wells are online, extraction rate, and precipitation recharge to the groundwater system.

#### 5.1.4 Effluent Treated Liquid-Phase Analytical Results

Pursuant to the effluent standards set forth by the EC/BSA Pollutant Discharge Elimination System Permit # 10-10-E1017, an effluent sampling event was conducted on a quarterly basis which consists of a 24hour composite sample (via an automatic sampler) for laboratory analysis of total extractable hydrocarbons and the collection of four grab samples over an 8-hour period for analysis of VOCs. Additionally, a quarterly effluent liquid-phase grab sample is collected and analyzed for VOCs. VOCs and total extractable hydrocarbons were analyzed using USEPA Methods 8260 and 1664, respectively.

During the reporting period, the monitoring parameters were either non-detect or reported at quantities below the permitted effluent limits. These system effluent results indicate that the LPGAC treatment system removed more than 99 percent of the VOCs in the extracted groundwater. The effluent sample results for TCE, DCE, and VC are provided in Table 3.

## 5.2 System Vapor Phase

Effluent vapor (i.e., soil gas) samples were collected on a quarterly basis from the vapor discharge side of the LRP and submitted for laboratory analysis of VOCs by Method AM 4.02 Chlorinated Hydrocarbons by Pace Analytical Services in Pittsburgh, Pennsylvania. As with the extracted groundwater sampling, the purpose of the vapor sampling is to estimate the total VOC mass removal from the subsurface, and to evaluate the relative changes in vapor-phase mass removal rate over time as a result of the system operation. The mass removal estimate is generated using the vapor sample analytical data and the air flow rate estimates recorded at the time of sampling. The system vapor sample laboratory analytical data have been submitted to NYSDEC's EIMS Administrator in the required EDD format.

#### 5.2.1 Vapor Phase Analytical Results

The quarterly vapor concentrations of TCE, DCE, and VC are presented in Table 4, and timeconcentration data collected since the system startup (1998) through April 2020 are depicted graphically on Figure 4. The two predominant compounds detected in the vapor samples have historically been TCE and DCE. During the reporting period, concentrations of TCE in the vapor samples ranged from 8,055 micrograms per cubic meter ( $\mu$ g/m<sup>3</sup>) to 19,332  $\mu$ g/m<sup>3</sup>. Vapor concentrations of DCE ranged from 2,139  $\mu$ g/m<sup>3</sup> to 4,754  $\mu$ g/m<sup>3</sup>. Vinyl chloride remained below the laboratory detection limits.

#### 5.2.2 Vapor Extraction Rates

As discussed in Section 4.4.2, the extracted vapor flow rate ranged from 59 to 110 cfm during the reporting period. It should be noted that the measured flow rate is solely from the recovery well network online during the sampling event and does not include any makeup (i.e., dilution) air.

#### 5.2.3 Vapor-Phase Mass Removal

Influent vapor sampling results and total vapor extraction flow rates were utilized to estimate the vaporphase VOC mass removal rate for –the reporting period. These data are presented in Table 5. As the data in Table 5 and on Figure 4 indicate, the vapor-phase mass removal rate ranged from 35 to 73 grams per day. As with dissolved-phase mass recovery, the fluctuation in the vapor-phase recovery rate can be attributed to variability in influent vapor mass concentrations due to recovery well configuration and precipitation recharge influences at the time of sample collection. A total estimated mass of 20.4 kg (45 lb) of VOCs was recovered in the vapor phase during the reporting period.

As expected, the mass transfer of VOCs from soil to vapor is predominantly limited to desorption and diffusion processes, as noted above for the dissolved phase. Therefore, mass removal rates in the vapor phase continue to decline over time as the Site is remediated.

## 5.3 Total Mass Removal Trend

The VER system has recovered a cumulative total of approximately 61 kg (134 pounds lb) and 595 kg (1,312 lb) of dissolved- and vapor-phase VOCs, respectively, during the period of operation from startup in 1998 through April 2020 (Table 6). The mass removal rate had generally declined for both the liquid- and vapor-phase VOC mass removed during each year of the operation from 1998 through 2003. As indicated in previous reports, the rate of recovery is expected to decrease as the mass removal becomes more dependent on desorption and diffusion processes rather than advective movement and capture of VOCs. However, the dissolved- and vapor-phase mass removal rates increased significantly following implementation of several pneumatic fracturing events at the Site in 2004 through 2009. This mass recovered is a direct indication that the pneumatic fracturing program was effective at increasing the advective movement and capture of VOCs, and substantially enhancing the efficiency of the remediation system. This was accomplished by further increasing the bulk permeability of the dense glacial till formation in each of the recovery well areas, thereby allowing additional VOC mass recovery via physical desorption and diffusion processes.

VOCs in the vapor phase accounted for greater than 90 percent of the total mass recovered to date. However, a percentage of the dissolved-phase mass is transferred to the vapor phase due to the nature of VER system operation via in situ stripping within the capillary fringe, recovery well, and through the extraction piping network. Thus, the vapor-phase influent data reflect, in part, the contribution of dissolved-phase VOCs in groundwater. As presented in Tables 2 and 5, the dissolved- and vapor-phase mass recovered during the reporting period was estimated at 0.32 and 20.4 kg, respectively. Figure 5 also depicts annual mass recovery through April 2020 for both the dissolved and vapor phases. This corresponds to a combined dissolved- and vapor-phase mass recovery of 20.7 kg (45.7 lb) during the reporting period.

## **6 GROUNDWATER MONITORING PROGRAM**

## 6.1 Water Level Conditions

Water level measurements were recorded in on-site monitoring wells during June and December 2019. These measurements were collected to monitor groundwater levels in response to operation of the VER system, which provides an indication of the hydraulic influence in the vicinity of the recovery wells under pumping conditions.

Water level data are summarized in Table 7, and the corresponding groundwater contour maps for June 11 and December 17, 2019 are presented on Figures 6 and 7, respectively. The contour map representing groundwater elevations for June 11, 2019 were with recovery wells RW-1A/B, RW-3, RW-4, RW-4A, RW-5, RW-7, and RW-9 operating. The contour map representing groundwater elevations for December 17, 2019 were with recovery wells RW-10A operating. The hydraulic radius of influence, which varies with each recovery well based on local hydrogeologic conditions, indicates that the system is maintaining hydraulic control of the groundwater in the vicinity of operating recovery wells.

## 6.2 Semi-Annual Groundwater Monitoring Program

Semi-annual groundwater monitoring activities were conducted in June and December 2019. Groundwater monitoring consisted of collecting groundwater samples from monitoring wells, former pneumatic fracturing locations, and recovery wells, as well as measuring water levels in monitoring wells to evaluate the hydraulic influence of the VER system. The VER system was operating online during the June and December 2019 sampling events. The following 10 wells were sampled to monitor groundwater concentrations during active remediation and evaluate the VER system effectiveness:

#### Monitoring Wells

- MW-2 (located adjacent to RW-8)
- MW-6 (adjacent to RW-1, RW-1A, and RW-1B)
- MW-11 (adjacent to RW-3 and RW-3A)
- MW-13 (adjacent to RW-3 and RW-3A)
- MW-20 (adjacent to RW-5)
- MW-22 (adjacent to RW-4 and RW-4A)
- MW-23 (adjacent to RW-6)
- MW-24 (adjacent to RW-7)

• MW-29 (adjacent to RW-9 and RW-9A)

**Recovery Well** 

• RW-11 (formerly MW-3).

All groundwater samples were collected and submitted for analysis of VOCs using USEPA Method 8260 at SGS North America Laboratories located in Dayton, New Jersey.

Concentrations of TCE, DCE, and VC for the 2019 groundwater samples are shown in Table 8. Historical concentration trends of TCE and DCE detected in each of the monitoring wells and select recovery wells are shown on Figures 8A, 8B, and 9. The groundwater laboratory analytical results have been submitted to NYSDEC's EIMS Administrator in the required EDD format.

## 6.3 Groundwater Sampling Results Summary

Both groundwater sampling events conducted during 2019 included collecting groundwater samples from the 10 wells to monitor VOC concentrations and trends and evaluate the performance of the VER system. TCE, DCE, and VC concentrations from the 2019 groundwater monitoring program are shown in Table 8. Historical TCE and DCE concentration trends in groundwater for monitoring and recovery wells are depicted on Figures 8A, 8B, and 9.

The depth to groundwater and the total depth of each well were used to determine the standing volume of groundwater in each monitoring well. Three well purge volumes were calculated for each well prior to sampling. Water quality parameters including temperature, pH, dissolved oxygen, specific conductance, oxidation-reduction potential, and turbidity were measured in the field and recorded on sampling logs the day of sampling (Appendix B). Generally, the water quality parameters remained relatively consistent as compared to historical values/ranges with the exception of turbidity. Turbidity values increased in a number of wells, most notably in MW-6 and MW-29.

The analytical results continue to show improvement in groundwater. VOC concentrations in several of the monitoring wells have declined one to two orders of magnitude since pneumatic fracturing was implemented at the Site. VOC concentrations in several site monitoring wells have fluctuated somewhat in response to changes in pumping cycles or seasonal water table fluctuations but have remained relatively stable.

The following highlights the groundwater analytical data for specific monitoring wells at the Site:

- MW-2: TCE concentrations have remained below the historical high concentrations observed in 2011. However, generally, these concentrations have remained relatively stable the last several years. DCE concentrations generally continue to decline since observing a historical high in 2015.
- MW-6: 2019 TCE concentrations continue to trend downward as compared to baseline values. This
  trend is mostly attributable to the conversion of PF wells to recovery wells (RW-1A/1B) in that area.
  DCE concentrations have remained relatively constant as compared to baseline values.
- MW-11: TCE and DCE concentrations continue to trend downward over the last several years, with historical low levels observed in December 2019.

- MW-13: Overall, TCE concentrations both remain relatively stable compared to historical concentrations. However, an increase in concentrations was observed in the December 2019. The increase in TCE concentrations may be attributable to the redevelopment/repair of RW-3/3A that were completed in 2019.
- MW-20: TCE and DCE concentrations continue to remain well below the previous 4-year average concentrations and two to three orders of magnitude below the baseline concentrations.
- MW-22: Both TCE and DCE concentrations were detected at historical low levels, as compared to the baseline, during the 2019 sampling events.
- MW-23: TCE and DCE concentrations both remain relatively stable compared to historical concentrations.
- MW-24: TCE and DCE concentrations both remain relatively stable compared to historical concentrations.
- MW-29: Both TCE and DCE concentrations were detected at historical low levels in 2019, as compared to the baseline and post-pneumatic fracturing events. Based on the 2019 sampling results, the DCE concentrations are three to four orders of magnitude less than the baseline monitoring well concentrations
- RW-11 (former MW-3): TCE and DCE concentrations continue to remain stable and within ranges established following the conversion of this well from a monitoring well to a recovery well. Based on the 2019 sampling results, the TCE concentrations are three orders of magnitude less than the baseline monitoring well concentrations.

## 7 CONCLUSIONS

The following sections summarize the overall system operation, remedial progress, and operating, maintenance, and monitoring goals for the next reporting period.

## 7.1 System Summary

The VER system has been effective at removing dissolved, adsorbed, and vapor-phase VOC mass. Since startup of the VER system, groundwater quality at the Site has improved substantially in most areas. The groundwater monitoring analytical results discussed in Section 6.3 are consistent with the decrease in mass removal estimates based on VER system influent groundwater and vapor-phase results presented in Section 5.4. As the available VOC mass decreases, as indicated by groundwater monitoring results, the VOC mass extracted by the VER system will decrease.

The effectiveness of the system is summarized below with the following performance metrics:

 Groundwater monitoring data have continued to indicate substantial improvement in groundwater quality in response to operation of the VER system and remedial enhancements implemented at the Site. This includes the reduction of VOC concentrations by several orders of magnitude at nine of the 15 wells historically monitored on site. These trends in VOC concentration reductions are depicted on Figures 8A, 8B, and 9.

- System dissolved-phase influent VOC concentrations decreased during the reporting period. This
  decrease in system influent VOC concentrations can be attributed to the areas being influenced by
  recovery wells and being remediated and mass removal becoming more dependent on diffusion and
  desorption processes. Therefore, mass removal rates in both the dissolved and vapor phase are
  declining over time as the Site is remediated.
- Performance monitoring data (i.e., groundwater drawdown and vapor concentrations) have indicated that the VER system has been able to dewater portions of the formation, thus allowing adsorbed VOC mass available below the groundwater table and within the capillary fringe for vapor extraction and in-situ stripping.
- The extent of the groundwater plume has remained stable although VOC concentrations have declined at several monitoring well locations due to operation of the VER system and enhanced VOC mass recovery created by the pneumatic fracturing program and expanded recovery well network. Groundwater concentration trends also indicate a cyclical, fluctuating pattern at some of the monitoring wells.
- Groundwater quality changes are expected to occur over a longer time frame due to the low
  permeability of the site geology. The advective movement and capture of dissolved-phase VOCs will
  remain an important mechanism in the mitigation and reduction of VOC impacts, but is expected to
  decline with continued pumping as VOC mass removal becomes more influenced by slower diffusion
  processes.
- The liquid-phase treatment system has been effective at removing over 99 percent of the dissolvedphase influent VOC mass recovered by the VER system.
- As of April 2020, the VER system has removed an estimated 595 kg (1,311 lb) of vapor-phase VOC mass and 61 kg (134 pounds lb) of dissolved-phase VOC mass.
- As of April 2020, the VER system has treated an estimated 19,434,916 gallons of groundwater.

## 7.2 Recommendations and Goals for the 2020-2021 Operation

System operation and performance monitoring will continue to focus on optimizing mass removal rates through cycled operation of recovery wells, evaluating individual recovery well mass removal rates, and continued O&M of the VER system equipment and components.

The goals for system operational activities during the next several months of operation in 2020 will be as follows:

- Redevelop monitoring wells, including MW-6, MW-13, MW-23, and MW-29.
- Redevelop recovery wells RW-1/1A/1B, RW-3/3A, and RW-4/4A.
- Perform individual recovery well pump tests to confirm liquid and vapor phase recovery rates.
- Measure water level at all monitoring wells to monitor hydraulic influence of the system.
- Collect quarterly influent samples to monitor the liquid- and vapor-phase treatment system for mass removal efficiency based on laboratory analysis of samples collected from the system influent.

- Continue operation of the system while performing the required vacuum adjustments at each of the recovery wells to optimize system performance and efficiency and maximize contaminant mass removal rates.
- Continue to collect groundwater samples on a semi-annual basis in accordance with the existing monitoring program. Collect groundwater samples from other selected monitoring wells and recovery wells to track changes in groundwater quality and support remedial decisions.
- Collect quarterly system effluent samples as required by the EC/BSA industrial wastewater discharge permit.
- Continue to monitor the LPGAC treatment system for VOC breakthrough based on laboratory analysis of samples collected from the system influent, midpoint, and effluent locations.
- Abandon historical/non-essential monitoring wells following receipt of NYSDEC approved work plan.

Based on the results of the 2019-2020 remedial program, including the field and laboratory data, the projected overall remedial strategy for the remainder of 2020 will remain unchanged.

#### 2019-2020 ANNUAL SITE MANAGEMENT PERIODIC REVIEW REPORT

## 8 REFERENCES

- NYSDEC. 2020. Acceptance Letter, 2018-2019 Periodic Review Report and IC/EC Certification, ARO Corporation, Site No.: 915147. February 3.
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- Arcadis. 2019. Site Management Periodic Review Report and IC/EC Certification Submittal, ARO Corporation, Cheektowaga, Erie County, Site No.: 915147. June 6.
- Arcadis. 2013. Supplemental Remedial Enhancement Work Plan, ARO Corporation Site, Cheektowaga, New York.
- NYSDEC. 2009. NYSDEC CP-43: Groundwater Monitoring Well Decommissioning Policy.
- Arcadis G&M, Inc. and GM Consulting Engineers, P.C. 1998. Engineering Report, Vacuum Enhanced Recovery System. ARO Corporation Site. Cheektowaga, New York.
- Arcadis G&M, Inc. and GM Consulting Engineers, P.C. 1998. Operation and Maintenance Plan, Vacuum Enhanced Recovery System. ARO Corporation Site. Cheektowaga, New York.
- Geraghty & Miller. 1997. Remedial Design/Remedial Action Work Plan, ARO Corporation Site, Cheektowaga, New York.

## TABLES



## Table 1VER System Operational Data 2019–2020ARO Corporation SiteCheektowaga, New YorkNYSDEC Site # 915147



#### Notes:

1. Recovery well statuses shown are only those present at the time of the monthly system sampling event. Recovery well configurations different than those shown may have occurred between monthly sampling events.

#### Definitions:

cfm - cubic feet per minute in.Hg - inches of mercury "--" - Indicates recovery well offline



# Table 2Dissolved Phase VOC Recovery 2019-2020ARO Corporation SiteCheektowaga, New YorkNYSDEC Site # 915147



Date	Dissolved Phase Influent VOC Concentrations (µg/L)		Total Cumulative	Monthly Reporting Period Flow	Estimated Mass Recovered Per <sup>(2)</sup> Reporting Period (kg)				Cumulative VOC Recovery (kg)	Cumulative Days Operating	Estimated VOC Recovery Rate Per Reporting Poriod (kg/day)	Estimated VOC <sup>(3)</sup> Mass Adsorbed Per Reporting	
	TCE	DCE (tot)	VC	- How (gai)	(L)	TCE	DCE (tot)	VC	Total	(1.9)	opolalig	Period (kg/day)	Period (%)
4/25/2019	38	37	0	18,329,799	773,138	0.029	0.026	0.000	0.055	6.11	0	0.0006	100.0
7/13/2019	41	16	0	18,566,179	894,793	0.035	0.024	0.000	0.059	6.17	79	0.0007	100.0
11/7/2019	43	23	0	18,803,245	897,390	0.038	0.017	0.000	0.055	6.22	196	0.0005	100.0
1/28/2020	63	29	0	19,083,037	1,059,125	0.056	0.027	0.000	0.083	6.30	278	0.0010	100.0
5/1/2020	83	37	0	19,434,916	1,332,003	0.084	0.038	0.000	0.122	6.43	372	0.0013	100.0
Groundwater Recovered			1 105 117	Total VOC	s Recover	ed April 20	19 - April	2020 (kg):	0.32			100.0	
	4/25/2019 - 5/1/2020 (gal)			1,103,117							-		

Average Groundwater Recovery Rate (gpm) 2.1

#### Notes:

1. Total cumulative flows indicated are estimated values based on flowmeter FQI-210.

2. Estimated mass recovered/discharged per reporting period calculated using influent/effluent water VOC concentrations and groundwater flow for that reporting period, respectively. VOC concentrations used for calculation are averages of those obtained from previous monthly sampling event and those obtained from current monthly sampling event.

3. Adsorption rates calculated using estimated VOC mass recovered and estimated VOC mass discharged per reporting period.

#### Definitions:

DCE (tot) - Dichloroethene (sum of 1,1-DCE, cis-1,2-DCE, and trans-1,2-DCE) gal - gallons gpm - gallons per minute kg - kilograms kg/day - kilograms per day L - Liters NS - Not Sampled TCE - Trichloroethene tot - total µg/L - micrograms per liter VC - Vinyl chloride VOC - Volatile Organic Compounds Table 3
Dissolved Phase System Influent TCE, DCE, and VC Concentrations
ARO Corporation Site
Cheektowaga, New York
NYSDEC Site # 915147

Sample Date	Sample Point	TCE (μg/L)	DCE (total) (µg/L)	VC (µg/L)
	Influent	40.9	15.7	ND
7/13/2019	Mid-Point	ND	21.2	ND
	Effluent	ND	ND	ND
	Influent	43.2	22.8	ND
11/7/2019	Mid-Point	13	6.8	ND
	Effluent	ND	ND	ND
	Influent	63.0	28.5	ND
1/28/2020	Mid-Point	8.3	4.1	ND
	Effluent	ND	ND	ND
	Influent	83.3	36.7	ND
5/1/2020	Mid-Point	78.6	34.0	ND
	Effluent	ND	ND	ND

#### Notes:

1. All concentrations in µg/L.

2. Samples analyzed using USEPA method 624.

#### Definitions:

DCE (total) - Dichloroethene (sum of 1,1-DCE, cis-1,2-DCE, and trans-1,2-DCE)

ND - Non-Detect, below the laboratory detection limits

TCE - Trichloroethene

VC - Vinyl Chloride

µg/L - micrograms per liter



Table 4 Vapor Phase System Effluent TCE, DCE, and VC Concentrations **ARO Corporation Site** Cheektowaga, New York **NYSDEC Site # 915147** 

Sample Date	т	CE	DCE	(total)	vc		
	ppmv	μg/m³	ppmv	μg/m³	ppmv	μg/m <sup>3</sup>	
7/13/2019	3.60	19,332	1.20	4,754	ND	ND	
11/7/2019	1.50	8,055	0.54	2,139	ND	ND	
1/28/2020	1.50	8,055	0.66	2,615	ND	ND	
5/1/2020	3.10	16,647	1.00	3,962	ND	ND	

#### Notes:

1. Samples analyzed by Pace Analytical using their in-house analytical method AM 4.02.

#### Definitions:

DCE (total) - Dichloroethene (sum of 1,1-DCE, cis-1,2-DCE, and trans-1,2-DCE)

 $\mu\text{g/m}^3$  - micrograms per cubic meter

ND - Non-Detect, below the laboratory detection limits

ppmv - parts per million by volume

TCE - Trichloroethene

VC - Vinyl Chloride

#### Table 5 Vapor Phase VOC Recovery 2019-2020 ARO Corporation Site Cheektowaga, New York NYSDEC Site # 915147



Date	Influ Conce	ent Vapor V entrations (p	OC <sup>(1)</sup> ppmv)	Influe Conce	ent Vapor V entrations (	/OC <sup>(2)</sup> μg/m <sup>3</sup> )	Influ Conc	ent Vapor V entrations (	ОС <sup>(3)</sup> [µg/L]	Vapor Extraction Flowrate (cfm)	Reporting <sup>(4)</sup> Period Volume of Air (L)	Mass Repo	Recovered orting Period	Per <sup>(2)</sup> i (kg)	Cumulat	ive Mass Re (kg)	ecovered	Estimated Cumulative VOC Recovery (kg)	2019-2020 Cumulative Operating Days	Estimated VOC Recovery Rate Per Reporting Period (kg/day)
4/25/2019	0.84	0.60	0.0	4 511	2 377	0.0	4.51	2.38	0.0	44	112 787 459	0.46	0.23	0.0	60.6	13.3	0.0	73.9	0	0.011
7/13/2019	3.6	1.20	0.0	19.332	4 754	0.0	19.33	4 75	0.0	110	355.673.825	4.24	1.27	0.0	64.8	14.6	0.0	79.4	79	0.070
11/7/2019	1.5	0.54	0.0	8,055	2,139	0.0	8.06	2.14	0.0	104	496,220,774	6.79	1.71	0.0	71.6	16.3	0.0	87.9	196	0.073
1/28/2020	1.5	0.66	0.0	8,055	2,615	0.0	8.06	2.61	0.0	82	274,210,099	2.21	0.65	0.0	73.8	17.0	0.0	90.8	278	0.035
5/1/2020	3.1	1.00	0.0	16,647	3,962	0.0	16.65	3.96	0.0	59	226,170,317	2.79	0.74	0.0	76.6	17.7	0.0	94.3	372	0.038
													Total VOC	s Recove	red Apr. 2	019 - Apr. 2	020 (kg):	20.4		

#### Notes:

1. Samples analyzed by Pace Analytical using their in-house analytical method AM 4.02 Vapors.

2. Vapor results were converted to μg/m<sup>3</sup> and μg/L using unit conversion factors, assuming a temperature of 25 C (+ 273.15 K), and gas constant, 0.08206 I\*atm/(mol\*K).

3. Estimated mass recovered per reporting period calculated based on monthly influent vapor concentrations and estimated volume of air treated for that reporting period. Influent vapor concentration used for calculation is average of influent vapor

concentrations obtained from current and previous monthly vapor sampling event.

4. Volumes of air treated are estimated values based on handheld anemometer readings.

#### Definitions:

cfm - cubic feet per minute DCE (total) - Dichloroethene (sum of 1,1-DCE, cis-1,2-DCE, and trans-1,2-DCE) kg - kilograms kg/day - kilograms per day L - Liters ppmv - parts per million by volume TCE - Trichloroethene tot - total µg/L - micrograms per liter µg/m<sup>3</sup> - micrograms per cubic meter VC - Vinyl chloride VOC - Volatile Organic Compounds

# Table 6Cumulative VOC RecoveryARO Corporation SiteCheektowaga, New YorkNYSDEC Site # 915147



	Dissolve	d Phase	Vapor	Phase		
Year(s)	Estimated Annual Dissolved Phase VOC Recovery (kg)	Cumulative VOC Recovery (kg)	Estimated Annual Vapor Phase VOC Recovery (kg)	Cumulative VOC Recovery (kg)		
1998-2000	12.2	12.2	22.4	22.4		
2001	0.38	12.6	10.8	33.2		
2002	0.77	13.4	5.4	38.6		
2003	0.74	14.1	3.8	42.4		
2004	0.64	14.8	5.6	48.0		
2005	1.63	16.4	16.8	64.8		
2006	2.19	18.6	31.9	96.7		
2007	5.25	23.8	50.6	147.3		
2008	8.35	32.2	60.7	208.0		
2009	8.12	40.3	130.3	338.3		
2010	1.19	41.5	33.7	372.0		
2011	4.79	46.3	47.4	419.4		
2012	2.89	49.2	31.7	451.1		
2013	0.89	50.1	21.8	472.9		
2014	4.66	54.7	27.4	500.3		
2015	2.02	56.8	17.2	517.5		
2016	0.76	57.5	19.9	537.5		
2017	1.04	58.6	21.9	559.4		
2018	1.91	60.5	11.2	570.5		
2019	0.49	60.9	17.7	588.2		
2020 (Through April)	0.21	61.2	6.4	594.6		
Cumulative VOCs Reco	overed through April 2020:	61.2		594.6		

#### Notes:

1. Due to error in the summary table, the cumulative liquid and vapor phase mass removal values reported for the 2017-2018 reporting period were incorrect. The values shown in the table above have been corrected.

#### Definitions:

kg - kilograms VOC - Volatile Organic Compounds

#### Table 7 Groundwater Elevation Data, June and December 2019 ARO Corporation Site Cheektowaga, New York NYSDEC Site # 915147



	Management and Destant	Da	ate	Date			
Well	Measuring Point Elevation	6/11/	/2019	12/17	/2019		
We in	(ft amsl)	DTW (ft)	GW Elevation	DTW (ft)	GW Elevation		
			(ft amsl)		(ft amsl)		
MW-1	104.12	3.03	101.09	3.32	100.80		
MW-2	101.33	5.25	96.08	3.79	97.54		
MW-4 <sup>(1)</sup>	103.52	4.29	99.23	4.25	99.27		
MW-4R	100.98	29.71	71.27	29.91	71.07		
MW-5 <sup>(1)</sup>	103.31	11.20	92.11	10.26	93.05		
MW-6	98.50	3.83	94.67	2.43	96.07		
MW-7 <sup>(1)</sup>	102.16	11.10	91.06	9.18	92.98		
MW-8	99.49	3.09	96.40	3.07	96.42		
MW-9	100.29	13.32	86.97	3.51	96.78		
MW-10R	98.94	0.10	98.84	0.33	98.61		
MW-11 <sup>(1)</sup>	99.82	9.81	90.01	10.04	89.78		
MW-13	99.86	11.20	88.66	11.61	88.25		
MW-14	103.14	5.93	97.21	6.07	97.07		
MW-14R	101.80	13.13	88.67	13.16	88.64		
MW-15	103.16	4.50	98.66	2.95	100.21		
MW-16	99.70	8.63	91.07	4.21	95.49		
MW-17	99.92	0.00	99.92	0.50	99.42		
MW-19	100.52	8.99	91.53	4.42	96.10		
MW-20	101.70	7.45	94.25	6.35	95.35		
MW-21	100.34	5.20	95.14	4.73	95.61		
MW-22	101.39	7.98	93.41	5.42	95.97		
MW-23	100.25	7.05	93.20	5.29	94.96		
MW-24	98.22	11.92	86.30	2.51	95.71		
MW-25	97.80	3.70	94.10	2.00	95.80		
MW-26	98.76	0.00	98.76	0.00	98.76		
MW-27	98.80	4.32	94.48	2.44	96.36		
MW-28	101.04	3.33	97.71	3.10	97.94		
MW-29	101.01	6.13	94.88	2.48	98.53		
OW-101	99.84	3.45	96.39	3.57	96.27		
OW-102	98.60	1.74	96.86	1.91	96.69		
VEROW-1	98.44	10.92	87.52	2.45	95.99		
VEROW-2	98.58	0.26	98.32	0.00	98.58		

#### Notes:

1. Monitoring wells MW-4, MW-5, MW-7, and MW-11 underwent repairs in September 2008 which altered their measuring points. This table uses the previous measuring point elevations, as the repairs did not result in significant elevation changes.

#### Definitions:

DTW - Depth To Water ft amsl - feet above mean sea level GW - Groundwater

# Table 82019 TCE, DCE, and VC Concentrations in GroundwaterARO Corporation SiteCheektowaga, New YorkNYSDEC Site # 915147

Well ID	Sample Date	TCE (μg/L)	DCE (total) (µg/L)	VC (μg/L)
	6/13/2019	28,000	5,853.7	ND
10100-2	12/18/2019	10,500	2,326.2	ND
	6/12/2019	1,290	1,383.9	26.3
MW-6	6/12/2019 (Duplicate)	1,160	1,212.5	23.0
	12/18/2019	441	1,340.6	36.9
M/M/ 11	6/12/2019	4,700	1,059.6	11.6
	12/18/2019	253	26.1	ND
	6/12/2019	61,600	10,965.2	ND
MW-13	12/18/2019	92,900	9,982.2	42.5J
	12/18/2019 (Duplicate)	76,200	8,920.6	59.8
M/M 20	6/13/2019	13.8	25.5	ND
10100-20	12/18/2019	64.9	219.53	4.0
M/M/ 22	6/13/2019	192	62.62	ND
	12/18/2019	56.8	15.2	ND
M\\/_23	6/13/2019	700	532.9	2.9
10100-25	12/18/2019	1,710	(13)-1(13)-1(13)-128,0005,853.7ND10,5002,326.2ND1,2901,383.926.31,1601,212.523.04411,340.636.94,7001,059.611.625326.1ND92,9009,982.242.5J76,2008,920.659.813.825.5ND64.9219.534.019262.62ND56.815.2ND700532.92.91,710642ND929486.712.5861249.14.6581136.2ND48.69.4ND2,280942.42082,940499.963.8	
NANA 24	6/12/2019	929	486.7	12.5
10100-24	12/18/2019	861	249.1	4.6
M/M/ 20	6/13/2019	581	136.2	ND
10100-29	12/18/2019	48.6	9.4	ND
P(N/11(M(N/2)))	6/13/2019	2,280	942.4	208
(1000-11)	12/18/2019	2,940	499.9	63.8

ARCADIS Design & Consultancy for natural and built assets

#### Notes:

1. All concentrations in micrograms per liter (µg/L).

#### **Definitions:**

DCE (total) - Dichloroethene (sum of 1,1-DCE, cis-1,2-DCE, and trans-1,2-DCE) J - Estimated value. ND - Non-Detect, below laboratory detection limits TCE - Trichloroethene

VC - Vinyl Chloride

## **FIGURES**





G:ACAD/PROJ/AY000220.0000/00300-FIG-1.dwg LAYOUT: 1 SAVED: 5/21/2019 3:11 PM ACADVER: 21.0S (LMS TECH) PAGESETUP: C-LA-PDF-GMS PLOTSTYLETABLE: PLTFULL.CTB PLOTTED: 5/22/2019 1:47 PM BY: MULLINS, JASMINE



SOURCE: RAY L. SONNENBERGER LAND SURVEYOR, 1	997					N
LEGEND					PROPERTY BOUNDARY	T
● <sup>MW-17</sup>	MONITORING WELL	▲ RW-2	RECOVERY WELL	w	WATER LINE	
⊕ <sup>OW−101</sup>	OBSERVATION WELL	₩ VEROW-2	MONITORING WELL	NG	NATURAL GAS LINE	
⊙ PF-3	PNEUMATIC FRACTURING WELL		RECOVERY SYSTEM TRENCH/PIPING		TREATMENT SYSTEM DISCHARGE LINE	
					BSA SANITARY SEWER LINE	

ARCADIS

FIGURE 2
















#### TRANE TECHNOLOGIES COMPANY LLC ARO CORPORATION SITE CHEEKTOWAGA, NEW YORK

#### GROUNDWATER CONTOUR MAP DECEMBER 17, 2019



FIGURE









- FORMER PNEUMATIC FRACTURING WELLS PF-1, PF-2, PF-4, PF-6, PF-8, PF-9, PF-10, PF-11 AND PF-13 CONVERTED TO RECOVERY WELLS, OCTOBER 2013. THESE WELLS HAVE BEEN RE-IDENTIFIED AS RW-1A (FORMER PF-1), RW-1B (FORMER PF-2), RW-10A (FORMER PF-4), RW-3A (FORMER PF-6), RW-9A (FORMER PF-4), RW-4A (FORMER PF-10), RW-11B (FORMER PF-12) AND RW-11A (FORMER PF-13).
- ANALYTICAL RESULTS OF GROUNDWATER SAMPLES COLLECTED FEBRUARY AND MARCH 1998 REPRESENTS BASELINE GROUNDWATER QUALITY CONDITIONS PRIOR TO START UP OF VER REMEDIAL SYSTEM ON MARCH 11, 1998.



TRANE TECHNOLOGIES COMPANY LLC ARO CORPORATION SITE CHEEKTOWAGA, NEW YORK

#### **HISTORICAL VOC CONCENTRATIONS IN GROUNDWATER IN SELECT WELLS**

ARCADIS

FIGURE 9

## **APPENDIX A**

Institutional Controls and Engineering Controls Certifications





#### Enclosure 2 NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL CONSERVATION Site Management Periodic Review Report Notice Institutional and Engineering Controls Certification Form



Sit	Site Details e No. 915147	Box 1	
Sit	e Name ARO Corporation		
Site Cit Co Site	e Address: 3695 Broadway Zip Code: 14227 y/Town: Cheektowaga unty: Erie e Acreage: <del>1.000</del> The three parcels listed below total 8.8 Acres		
Re	porting Period: May 14, 2019 to May 14, 2020		
		YES	NO
1.	Is the information above correct?		Х
	If NO, include handwritten above or on a separate sheet.		
2.	Has some or all of the site property been sold, subdivided, merged, or undergone a tax map amendment during this Reporting Period?		Х
3.	Has there been any change of use at the site during this Reporting Period (see 6NYCRR 375-1.11(d))?		Х
4.	Have any federal, state, and/or local permits (e.g., building, discharge) been issued for or at the property during this Reporting Period?		Х
	If you answered YES to questions 2 thru 4, include documentation or evidence that documentation has been previously submitted with this certification form.		
5.	Is the site currently undergoing development?		Х
		Box 2	
		YES	NO
6.	Is the current site use consistent with the use(s) listed below? Industrial	Х	
7.	Are all ICs/ECs in place and functioning as designed?	Х	
	IF THE ANSWER TO EITHER QUESTION 6 OR 7 IS NO, sign and date below a DO NOT COMPLETE THE REST OF THIS FORM. Otherwise continue.	nd	
AC	Corrective Measures Work Plan must be submitted along with this form to address th	iese issi	ues.
Sig	nature of Owner, Remedial Party or Designated Representative Date		

SITE NO. 915147	Box	τ 3							
Description of Instit	utional Controls								
Parcel	Owner Institutional Control								
103.17-1-17	Ingersoll-Rand Company								
	Trane Technologies Company LLC (formerly Ingersoll Rand Company)								
A long term Operation, Monitoring and Maintenance Plan is in place in accordance with the March 1995 Record of Decision (ROD). The OM and M Plan includes periodic sampling of the groundwater and monitoring of the Vacuum Enhanced Recovery System (Extraction System, Vapor Treatment System, and Liquid Treatment System).									
103.17-1-18		1							
	I rane Technologies Company LLC (formerly Ingersoll Rand Company)								
A long term Operation, Mor Record of Decision (ROD). monitoring of the Vacuum I Liquid Treatment System).	nitoring and Maintenance Plan is in place in accordance with the March 1995. The OM and M Plan includes periodic sampling of the groundwater and Enhanced Recovery System (Extraction System, Vapor Treatment System, a	5 and							
103.17-1-19	Ingersoll-Rand Company								
	Trane Technologies Company LLC (formerly Ingersoll Rand Company)								
A long term Operation, Mor Record of Decision (ROD). monitoring of the Vacuum I Liquid Treatment System).	nitoring and Maintenance Plan is in place in accordance with the March 1995. The OM and M Plan includes periodic sampling of the groundwater and Enhanced Recovery System (Extraction System, Vapor Treatment System, a	5 and							
	Box	<b>4</b>							
Description of Engir	neering Controls								
Parcel	Engineering Control								
103.17-1-17	Groundwater Treatment System Vapor Mitigation								
103.17-1-18	Groundwater Treatment System Vapor Mitigation								
103.17-1-19	Groundwater Treatment System Vapor Mitigation								

	Box 5
	Periodic Review Report (PRR) Certification Statements
1.	I certify by checking "YES" below that:
	a) the Periodic Review report and all attachments were prepared under the direction of, and reviewed by, the party making the certification;
	b) to the best of my knowledge and belief, the work and conclusions described in this certificatio are in accordance with the requirements of the site remedial program, and generally accepted engineering practices; and the information presented is accurate and competent.
	YES NO
	X 🗆
2.	If this site has an IC/EC Plan (or equivalent as required in the Decision Document), for each Institutional or Engineering control listed in Boxes 3 and/or 4, I certify by checking "YES" below that all of the following statements are true:
	(a) the Institutional Control and/or Engineering Control(s) employed at this site is unchanged since the date that the Control was put in-place, or was last approved by the Department;
	(b) nothing has occurred that would impair the ability of such Control, to protect public health an the environment;
	(c) access to the site will continue to be provided to the Department, to evaluate the remedy, including access to evaluate the continued maintenance of this Control;
	(d) nothing has occurred that would constitute a violation or failure to comply with the Site Management Plan for this Control; and
	(e) if a financial assurance mechanism is required by the oversight document for the site, the mechanism remains valid and sufficient for its intended purpose established in the document.
	YES NO
	X 🗆
	IF THE ANSWER TO QUESTION 2 IS NO, sign and date below and DO NOT COMPLETE THE REST OF THIS FORM. Otherwise continue.
	A Corrective Measures Work Plan must be submitted along with this form to address these issues.
	Signature of Owner, Remedial Party or Designated Representative Date

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	IC CERTIFICATIONS SITE NO. 915147								
		Box 6							
SITE OWNER OR DESIGNATED REPRESENTATIVE SIGNATURE I certify that all information and statements in Boxes 1,2, and 3 are true. I understand that a false statement made herein is punishable as a Class "A" misdemeanor, pursuant to Section 210.45 of the Penal Law.									
Todd Carignan	at 855 Route 146, Suite 21	0, Clifton Park, NY 12065 <sub>,</sub>							
print name	print business address								
am certifying asRemedial Party		(Owner or Remedial Party)							
for the Site named in the Site Details S Signature of Owner, Remedial Party, of Rendering Certification	Section of this form. or Designated Representative	5/29/2020 Date							

	IC/EC CERTIFICATIONS
Pr	rofessional Engineer Signature
l certify that all information in Boxes 4 punishable as a Class "A" misdemean	and 5 are true. I understand that a false statement made herein is nor, pursuant to Section 210.45 of the Penal Law.
Moh Mohiuddin	at 50 Millstone Rd, East Windsor, NJ 08520
print name	print business address
am certifying as a Professional Engine	eer for the
Signature of Professional Engineer, for Remedial Party, Rendering Certification	or the Owner or

## **APPENDIX B**

Groundwater Sampling and Purge Logs



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Water Level Record

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Page 1 of 2

HB

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Project	Ingersoll-ARO	*			Date 6/11/2019
		•			Technician JB/MK
Well (s)	Depth to Water (ft)	Total Depth	Time	MP (PVC)	Remarks Vacuum on/off
MW-1	3.03	28.48		VoloEMG.	44
MW-2	4.80	21.28			121D
MW-3					
MW-3R	24.20	44.14			HR
MW-4	4,74	18.90		1	SR
MW-4R 17 .	30 1 2971	32 91		1	48
MW-5	11.20	21. 87		1	SR
MW-6	ton DRY				00
MW-7	11.10	77.51			HR
MW-8	3.79	17.54			#B
MW-9	13.32	24.83			1.0
MW-10R	0.10	16.38			SR Sedinant
MW-11	6.08	1218			AGB
MW-13	6.22	23.41	-		SB
MW-14	5.93	23.20			HB
MW-14R	13.13	43,60			HB
MW-15	4.50			•	
MW-16	8.63	23.28			HB
MW-17	9,00	23,63			Above Top of les
MW-18	Obstruction				
MW-19	8.99	2005 245	_		\$B
MW-20	7.63	24.61			SB
MW-21	\$ 5.20	15.50			53
NW-22	9.62	20.89			SB
MW-23	10.02	19.48	J		HB .
MW-24	11.75	17.53			HB
MW-25	3.70	12.10			HB
MW-26	Suctare				
MW-27	4.32	16.915			SS HB
MW-28	3.33	18.84	200		HB X
MW-29	1248	18.32			SB
OW-101	3.45	6.20	× .		,
OW-102 🖕	174	4.64			/ <sub>e</sub>
OW-103		45004			Could not access
VEROW-1	10.92	1246			58
VEROW-2	0.26	13.70		<	ISB N

G:APROJECTUNGERSOLVARO/AY000220.0012/Water Level Round.ARO.XLS

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#### ARCADIS

#### Water Level Record

Project

Ingersoll-ARO

Date 6/11/2019 Technician JB/MK

	Well (s)	Depth to Water (ft)	Total Depth (ft)	Time	MP (PVC)	Remarks Vacuum on/off
	RW-1A/PF-1	13.58	19.43			·
	RW-1B/PF-2	13.53	13-531861			
	PF-3	9.91	19.00			58
	RW-10A/PF-4	12.00	19.28			HB
	PF-5	6.82	19.14			
	RW-3A/PF-6	5.50	18 68 6			UHB .
	PF-7		_			Stuch Closed
	RW-9A/PF-8	17.70	1924			SR
	PF-9	5.33	18.83			50
	RW-4A/PF-10	8.00	19.68			HB
	PF-11	10.41	17.61			
	RW-11B/PF-12	2 13.85	19.32			HB
	RW-11A/PF-13	11.84	19.32			HB
A	RW-11	17.43	2434			HIZ
	RW-1 Dry	# 1.98	H.08 19.12			
	RW-2 🗸	2.0	17.90		•	HB
	RW-3	4.88	19.10			
	RW-4	9.20	17.95			11-13
	RW-5	400834	16.31			On HB
	RW-6	19.97	20.75			00
	RW-7	13.19	18.50			HIS
	RW-8	2.70	19.63			53
	RW-9	18.67	19.48			HB
	RW-10	1153	22.19			1423
						2
					1	

Page 2 of 2

<b>A</b> Water		ingin & Commission 17 Alexand and 19 Reports						
Project	Ingersol Ran	d - ARO	Project No. <u>A</u>	1000 220.0	225-	Page	1 of	-
Site Loca	ation 3695 Broa	dway, Cheek	towaga, NY		Date	675-1		-
Site/Wel	INO. MW-2		Replicate I	No		11-5		
Weather	60	ram	Sampling	Time: Begin 132.	5 End	1400	-	
Evacuat	tion Data			Field Parameters		`		
Measuri	ng Point		тос	Color		x		
Sounder	d Well Depth (ft bmj	p)	21.17	Odor	Vov	2		
Depth to	Water (ft bmp)		5.25	Appearance				
Depth to	Packer (ft bmp)		-			11/	2V	3V
Water C	olumn in Well (ft)		13, 42	9	907	7.50	7.39	7.35
Casing I	Diameter		2	pH (s.u.)	-1.07	1.00		and the second
Gailons	in Well		2.5	Conductivity	285	9 80	6 79	0.73
Gallons	Pumped/Bailed		_	(mS/cm)	121	0,1/2		
Germala	Prior to Sampling			(pmnos/cm)	20.1			10 0
Sample	Setting (ft bmp)		_	Temperature (°C)	13.1	19.3	12.1	ld.1
Packer F	Pressure (psi)		_		A	0.67	045	0
Pumping	g Rate (ml/min)			DO (mg/L)	244	6.01	4.05	4/1
Evacuat	ion Method		Bailer	Turbidity (NTU)	1330/94	30	12.1	167
Samplin	g Method		Bailer	Time	1330	1355	14 25	1455
Purge Ti	ime	Begin	End	DTW (ft bmp)	5.25	9.40	13.40	13.00
•				ORP	<u>-13, 8</u>	01.5	106-4	64.
Remarks	s: Water Qu	ality Meter:	YST Po	DDS		_	_	
	System O	n/Off: 🕈	on			-		
	Initial Purg	je: 🛏				_		
Constitue	ents Sampled:	See COC	Samp	ling Personnel: JE	3/MK		8	-
	Well Casing	Volumes						
Gal./Ft.	$1^{1/4_{\rm W}} = 0.06$	2" = 0.16	3" = 0.37	4" = 0.65				
	1" <sup>2</sup> " = 0.09	2-1⁄2" = 0.26	3-½" = 0.50	6" = 1.47				-
bmp °C ft gpm mg/L	below measuring poi Degrees Celsius feet Gallons per minute Miligrams per liter	nt mS/cm s.u. NTU N/A COC	Milislemens per centin Standard units Nephelometric Turbidi Not Applicable Chain of Custody	neter VOC Vo umhos/cm Mi ty Units	blatile Organic ( icromhos per c	Compounds entimeter		17

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Water Project Site Loc Site/We	RC/ Sam cation ell No.	ADIS pling Lo ngersol Ra 3695 Bro MW-6	Dg nd - ARO hadway, Che	Project rektowaga, N	t No. <u><u>A</u> Y Replicate No Sampling Tin</u>	. <u>DP-</u> me: Begin _	07-	Date 201906 End	Page 6- 12 15-30	9 <u>101</u> -12-19 	ole Time
Evacua	tion Dat	ta				Field Paramo	eters	,	( <sup>(</sup> )		
Measuri Sounde Depth to	ing Point d Well D o Water (	t )epth (ft bm (ft bmp)	 	TOC 14.1. 3.8	¥ }	Color Odor Appearance		1	tone tone		21/
Depth to	o Packer	(ft bmp)		103	1				1V	2V	1720
Water C	Column ii	n Well (π)	-	2"		pH (s.u.)		7.45	7.52	1.47	1.20
Casing Gallons	Diamete in Well	r I Railed		1.65		Conductivity (mS/cm)		0.71	0.78	1.02	1.07
Gallons	Pumped			560	1	(µmhos/cr	m)				
Sample	Prior to Pump Ir Setting	ntake (ft bmp)				Temperature	(°C)	57.4	57.1	58.6	57.9
Dacket	Pressure	e (psi)		-				136	1 40	S.CC MA	3.25
Pumpin	a Rate (r	ml/min)		-		DO (mg/L)	,	6.20	6.00	Vain	>1100)
Evacual	tion Meth	nod		Bailer		Turbidity (NTL	J)	TYC	11000	1000	11.20
Samolin	a Metho	d		Bailer		Time	į	15:00	15:10	5.62	400
Purge T	ime		Begin 13	CO End	15:20	DTW (ft bmp) ORP		3.83 137.8	112.8	91.2	863
Remark	s:	Water Qu System O Initial Purg	ality Meter: n/Off: ge: 72	YST ON Turbid	Prop	0/15					
Constitu	ents San	npled:	See COC		Sampling	g Personnel:	JB/M	IK			
	114	Well Casing	Volumes	o# _ i	1 37	4" = 0.65					
Gal./Ft.	$1^{1/2} = 0.$ $1^{1/2} = 0.1$	06 09	2" = 0.16 2-½" = 0.26	3-½" =	0.50	6" = 1.47					
bmp °C ft gpm mg/L	below me Degrees feet Gallons p Miligrams	easuring poli Celsius per minute s per liter	nt mS/cm s.u. NTU N/A COC	Milisiemens Standard un Nephelomet Not Applical Chain of Cur	per centimete its ric Turbidity U ble stody	er VOC umhos/cm Inits	Volati Micro	ile Organic C mhos per ce	ompounds ntimeter		

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ARCADIS	Canadianay And M					
Water Sampling Log	Ar.	00-00-0-0-	770		an tott	
Project Ingersol Rand - A	RO Project No. /79	00020.002		- <sup>Pa</sup>	ge	-
Site Location 3695 Broadwa	y, Cheektowaga, NY		_ Date	6-15-1	9	-
Site/Well No. MW-11	Replicate No		_	aa		
Weather 75-8	Sampling Tir	me: Begin <u>/4/24</u>	End	1500		
Evacuation Data		Field Parameters				
Measuring Point	тос	Color	Clear			
Sounded Well Depth (ft bmp)	9 12.19	Odor	Nabe			
Depth to Water (ft bmp)	9.81	Appearance	- 1			
Depth to Packer (ft bmp)				.5	LO	1,5
Water Column in Well (ft)	3.10			1V	2V	3V
Cesing Diameter	2	pH (s.u.)	7.67	7,8	85	86
Gallons in Well	.496	Conductivity		55.0	0.00	SAA
Gallons Pumped/Bailed		(mS/cm) C	.453	0.382	0.396	, 009
Prior to Sampling	-	(µmhos/cm)				
Sample Pump Intake			IF Q	12/	17/6	7.5%
Setting (ft bmp)		Temperature (°C)	0.0	19.10	12.60	610
Packer Pressure (psi)			1.15.	0 03	746	6.31
Pumping Rate (ml/min)		DO (mg/L)	600	6.00	LICC IC	41.867
Evacuation Method	Bailer	Turbidity (NTU)	301	Ge. dd	784.00	1/150
Sampling Method	Bailer	Time	1435	1440	1445	1900
Purge Time Begin	1430 End 1700	DTW (ft bmp)	1004	10.24	0.01	222
		ORP	173.8	184: 1	2014	<u> </u>
Remarks: Water Quality M	leter. A Pro DOS				2	
System Ch/Off:						
Initial Purge:	Clear					
Constituents Sampled: See	COC Sampling	Personnel: JB/N	ЛК			
Well Casing Volum	nes 3" = 0.37	4" = 0.65			*	
Gal./FL $1^{3/2} = 0.09$ $2 \cdot \frac{1}{2}^{3/2} = 0.09$	= 0.26 3-1/2" = 0.50	6" = 1.47				
bmp     below measuring point       °C     Degrees Celsius       ft     feet       gpm     Gallons per minute       mg/L     Miligrams per liter	mS/cm Milisiemens per centimeter s.u. Standard units NTU Nephelometric Turbidity Un N/A. Not Applicable COC Chain of Custody	VOC Volat umhos/cm Micro	ile Organic Cc omhos per cen	mpounds timeter		ļ
		A Sampled	@ 1451			

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AR	RCADIS 📰	Consultancy Slamb Na					
Water	Sampling Log	A					
Project	Ingersol Rand - A	ARO Project No. 4	000220.0	25		a <u>1 of 1</u>	-
Site Loca	tion 3695 Broadwa	ay, Cheektowaga, NY		- Date	6-1d-1	1	-
Site/Well	No. MW-13	Replicate No	)		1 = 0 - 2		
Weather	75-80	Sampling Tin	me: Begin <u>1503</u>	End	1532	_	
Evacuati	ion Data		Field Parameters				
Measurin	na Paint	TOC	, Color	Clear			
Sounded	I Well Depth (ft bmp)	23.45	Odor	Nate			
Deoth to	Water (ft bmp)	11.20	Appearance				
Depth to	Packer (ft bmp)				2	4	6
Water C	olumn in Well (ft)	12.25			1V	2V	30
Casing [	Diameter	2"	р <b>Н (</b> s.u.)	7.87	7,73	1.97	1.0
Gallons i	in Well	196	Conductivity				DIP.
Gallons	Pumped/Bailed		(mS/cm)	0-425	0.641	0.651	2646
Gallorio	Prior to Sampling	•	(µmhos/cm)				
Sample	Pump Intake			14	10.6	n 5	21
	Setting (ft bmp)		Temperature (°C)	1-1-1-	1010	10 2	.90
Packer F	Pressure (psi)		<b>DO</b> (	ぐつ	5.02	4,24	3.66
Pumping	g Rate (ml/min)			N C	6202	11144	222584
Evacuat	ion Method	Bailer	Turbidity (NTU)	12.2	1502	1501	1528
Samplin	g Method	Bailer	Time	100	1013	15/0	17.31
Purge Ti	ime Beg	gin 120 End 1520	DTW (ft bmp)	11.00	910 7	01/6	201
		1200	ORP	18221	1218 1	1 diain	avan
		1540TO POI	DOG				
Remarks	s: Water Quality	Meter: 10 10 10	Pla			- 27	
	System On						
	Initial Purge:						
Constitu	ents Sampled: Se	e COC Samplir	ng Personnel: JB	MK			-
4	Mall Casing Vo						
Gal /Et	$1^{1/4_{w}} = 0.06$ 2"	= 0.16 3" = 0.37	4" = 0.65				
Guiste	1 <sup>1/2</sup> = 0.09 2-3	∕₂" = 0.26 3-½" = 0.50	6" = 1.47				
bmp ℃ ft	below measuring point Degrees Celsius feet	mS/cm Milisiemens per centimel s.u. Standard units NTU Nephelometric Turbidity	ter VOC Vo umhos/cm Mic Units	latile Organic cromhos per c	Compounds entimeter		
gpm	Gallons per minute	N/A Not Applicable COC Chain of Custody			1. 1	622	
mg/∟	milligrams per inter		i i i i i i i i i i i i i i i i i i i	Samo	td 0 1	000	
				v v and			
		2			-		

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Water Sampling Log	•	MA 220 0	ሥህ ቢ	Page	1 of (	
Project Ingersol Rand - ARO	Project No. /T 1.C		Date	6-13-1	9	
Site Location 3695 Broadway, Ch	neektowaga, NY	~				
Site/Well No. MW-20	Replicate No.		5 End	1135	-	
Weather <u>60</u> , ram	Sampling Time	e: Begin <u>Itot</u>				
Evacuation Data		Field Parameters	~ 1			
Measuring Point	тос	Color	_Clea	v		
Sounded Well Depth (ft bmp)	24.60	Odor	Non	8		
Depth to Water (ft bmp)	200 7.45	Appearance				
Depth to Packer (ft bmp)	_			1V	·2V	3V
Water Column in Well (ft)	17.15			7.32	7.40	7.43
Casing Diameter	2	pH (s.u.)	141		1.1-	
Gallons in Well	2.74	Conductivity	0701	0,738	0.746	0.748
Gallons Pumped/Bailed		(mS/cm)	UTICA			
Prior to Sampling		(µmnos/cm/				10.2
Sample Pump Intake Setting (ft bmp)	-	Temperature (°C)	12.0	10	10.0	10-5
Packer Pressure (psi)			11 50	4 -6	1134	4 64
Pumping Rate (ml/min)	_	DO (mg/L)	9.50	109	2.0	/14
Evacuation Method	Bailer	Turbidity (NTU)	62.00	JILL)	20.6	6-1175
Sampting Method	Bailer	Time	1100	10-00	1 00	12 91
Purge Time Begin	103_End_125	DTW (ft bmp)	195	10.15	174 0	1728
	iz Da Di	ORP .	]][,=]	] //· -	173.4	1 did
Remarks: Water Quality Meter	ar. TOL PIO DI	$\mathcal{N}$				
System On/Off: (	20					
Initial Purge:						
Constituents Sampled: See CO	C Sampling	Personnel: JB	MK			-
Well Casing Volumes	3" = 0.37	4" = 0.65				
Gal./Ft.       1 = 0.00       2 = 0.10 $1^{1/2_m} = 0.09$ $2 \cdot \frac{1}{2}^n = 0.09$	26 3-½" = 0.50	6* = 1.47	_			
bmp below measuring point mS °C Degrees Celsius s.u ft feet NT gpm Gallons per minute N// mg/L Milligrams per liter CO	<ul> <li>/cm Milisiemens per centimete</li> <li>Standard units</li> <li>Wephelometric Turbidity U</li> <li>Not Applicable</li> <li>Chain of Custody</li> </ul>	r VOC Vo umhos/cm Mit nits	latile Organic ( cromhos per c	Compounds entimeter	30	2 - Z <sup>a</sup> -

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ARCADIS				
Project Ingersol Rand - ARO Project No. A	(000200.00	25 F	age 1 of (	_
Site Location 3695 Broadway, Cheektowaga, NY		Date 6-1	3-19	-
Site Avell No. MA/-22 Replicate J	No.			
Weather $60^{\circ}$ fain Sampling	Time: Begin140	End 126		
Evacuation Data	Field Parameters			
Measuring Point TOC	Color	Clear		
Sounded Well Depth (ft bmp) 20.8(	Odor	hone		
Depth to Water (ft bmp) 7.98	Appearance			
Depth to Packer (ft bmp)				
Water Column in Well (ft) 12.9.8		1 1V	2V	3V
Casing Diameter	рН (s.u.)	7.34 7,3	1 7.26	7.39
Gallons in Well 2.06	Conductivity			(10.0
Gallons Pumped/Bailed	(mS/cm) ()	.889 0.83	4 0.845	0.848
Prior to Sampling	(µmhos/cm)			
Sample Pump Intake	Tomoaratura (°C)	T. 107	10.5	10.6
Setting (ft bmp)	Temperature ( O)	111 1 12 17		
Packer Pressure (psi)	DO (mg/L)	5.84 667	6.33	6.30
Pumping Rate (m/min)	Turbidity (NTII)	208 7 754	41 1444.91	232466
Evacuation Method Paristenic Pump	Time	1145 1151	11.58	120.5
Sampling Method Paristeric Pump	DTM (# hmp)	7.95 971	10.31	11.60
Purge Time Begin <u>170</u> End <u>170</u>	ORP	179.3 183,	191,7	1897
Remarks: Water Quality Meter: 457 Pro D	)5		1	,
System On/Off: On			*	
Initial Purge:				
Constituents Sampled: See COC Samp	ling Personnel: JB/	МК	<u></u>	-
Well Casing Volumes				
<b>Gal./Ft.</b> $1^{1/4} = 0.06$ $2^{*} = 0.16$ $3^{*} = 0.37$	4" = 0.65 6" = 1 47		•	
1 = 0.09       2-½* = 0.26       3-½* = 0.50         bmp       below measuring point       mS/cm       Millisiemens per centimes         °C       Degrees Cetsius       s.u.       Standard units         ft       feet       NTU       Nephelometric Turidities         gpm       Gallons per minute       N/A       Not Applicable         mg/L       Milligrams per liter       COC       Chain of Custody	eter VOC Vola umhos/cm Mic y Units	atile Organic Compounds romhos per centimeter		

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A/ Wate	RCADIS	Deservice-	<b></b> ,						
Project	Ingersol R	and - ARO	Project No	AYC	00220.00	025	Pag	181 of	-
Site Lo	cation 3695 Bi	roadway, Ci	heektowaga, NY			Date	6-13-19		
Site/W	ell No. MW-23		Rep	olicate No.					
Weath	er <u>60</u> °	rain	Sar	npling Time	: Begin 1030	O End	100	-	
Evacu	ation Data				Field Parameter	\$			
Moocu	ring Point		тос		Color	Clear			
Cound	nng r'oin. od Well Denth (ft bi		19.04		Odor	Nane			
Death	b Water (ft bmn)		7.05		Appearance	-			
Depth	to Packer (ft hmn)	8	15				2	4	ç
Weter		1	11 99			1	1V	2V	3V
vvalci ·					oH (s.u.)	8.03	7.63	7.48	7.33
Casing	Diameter		191		Conductivity				
Gallons		í <del></del>	1. 11		(mS/cm)	0.785	11.760	0.768	. 963
Gallons	S Pumped/Balled	-	•		(umhos/cm)	~			
Sample	Prior to Sampling	9	, a.	1	(p		11.05	100	110
Gampic	Setting (ft bmp)		_		Femperature (°C)	1280	11.0	10.3	/1.8
Packer	Pressure (psi)		_		·	10	10,	1	483
Pumpin	g Rate (ml/min)		_	(	)O (mg/L)	6.10	606	4.06	Ucal
Evacua	tion Method		Bailer	1	urbidity (NTU)	1.07	154.4	1304.79	756
Samolir	na Method		Bailer	1	īme	1036	1039	042	1050
Pume 7	'ime	Begin	End	[	)TW (ft bmp)	7.05	914	9.99	10.43
				C	)RP	164.4	122	157.5	160.3
Remark	s: Water Q	uality Meter	457 F	$\sim 0$	QS:				
	System C	Dn/Off:	0A						r.
	Initial Pu	rge:							
Constitu	ents Sampled:	See COC	;	Sampling P	ersonnel: JB/	/MK			
	Well Casir	ng Volumes			- 0.05				
Gal./Ft.	$1^{1/4\pi} = 0.06$ $1^{1/2\pi} = 0.09$	$2^{\circ} = 0.16$	3" = 0.37 6 3-14" = 0.5	4 0 6'	= 0.65 = 1.47				
bmp °C ft gpm mg/L	below measuring po Degrees Celsius feet Gallons per minute Miligrams per liter	int mS/c s.u. NTU N/A COC	om Millslemens per Standard units Nephelometric T Not Applicable Chain of Custody	centimeter urbidity Units	VOC Vol: umhos/cm Mic	atile Organic C cromhos per cer	ompounds ntimeter		
				\$-3	Sampter Co	1050			

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Mater Project	RCADIS Sampling	Log Rand - AF	20	_ Project No	<u>44</u>	000000.1	30	Date	Page 6-12-10	e1of	-
Site Loca	ation 3695 l	Broadway	, Chee	KTOWAGA, INT							
Site/Wel	No. <u>MW-2</u>	4		Replic	ate No.		40	- ILILIO	512		
Weather	75-1	30 0	Sunr	Sampl	ing Tim	ne: Begin 🛃	92		NE	-).	
Evacuat	ion Data			0		Field Paramet	ters				
A 10	- <del>2</del>			TOC		Color		Cear			
Measurin	ng Point			17.57		Odor		None			
Sounded	Well Depth (ft	omp)		100		Appearance		-			
Depth to	Water (ft bmp)			1100					t	2	3
Depth to	Packer (ft bmp)	)	_	515					1V	2V	3V
Water C	olumn in Well (f	t)		2:40		11 (2 41 )		7.44	7.45	7.36	1.3.3
Casing [	Diameter			-0		pH (s.u.)					
Gallons i	in Well			. 70	_	Conductivity	<i>r</i> .	G1/07	0.934	0.91	6.913
Gallons	Pumped/Bailed					(mS/cm)	, C				
	Prior to Sampli	ng		<u> </u>	_	(µmnos/cm	9				157
Sample I	Pump Intake					Temperature (°	C)	14.1	12.7	13.0	19.1
	Setting (ft bmp	) (			—	i on por a contra c			•		E 60
Packer F	Pressure (psi)				-	DQ (mg/L)		6.61	2.00	\$ 5.67	7.8.7
Pumping	g Rate (ml/min)	3			-	Turbidity (NTH)		315.64	17676	45.50	10.17
Evacuati	ion Method	9		Bailer	_		ilion	BUT	12531453	1059145	a 1512
Sampling	g Method	3		Bailer	-		<b>n</b> 1	1.00	3.75	13.96	15.38
Purge Ti	me	Begin		End 15	10	DTW (rt omp)		161 g	IGDE 5	2650	2267
			14	47 10	12	ORP		01.1		140001	<u>_Corow</u> _+
<b>D</b>	. Water	Quality M	eter:	PODT	48	JI Pro Pl	S				
Remarks	Si Eveter	CROff.	Oh	-							
	Initial F	ume'						- C.			
	Innuar	bigo.									
Constitue	ents Sampled:	See (	coc	Sa	mpling	Personnel:	JB/N	١K			
	Well Ca	sing Volum	ies			/= - 0 6F					
Gal./Ft.	$1^{1/4_{\rm H}} = 0.06$ $1^{1/2_{\rm H}} = 0.00$	2" = 0.	16	3" = 0.37 3.14" = 0.50		6" = 1.47					
	1 = 0.09	2-12	0.20	J=72 = 0.50		1000	Velat		amounde		Δ.
bmp °C	below measuring Degrees Celsius	point I	n\$/cm 3.U.	Millsiemens per cer Standard units	ntimeter	umhos/cm	Micro	omhos per ce	ntimeter		Υ.
ft	feet	1	UTU	Nephelometric Turt	idity Ur	hits					
gpm mg/L	Gallons per minut Miligrams per liter	e l		Chain of Custody							

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4

# Water Sampling Log

4

Project Ingersol Rand - AR	O Project No. <u>A4</u>	000,00,002	5 Pag	je1 of /		
Site Location 3695 Broadway,	Cheektowaga, NY		Date 6-12	- 19		
Site/Well No. MW-29	Replicate I	No				
Weather $70^{1}$	SUMP Sampling	Time: Begin 134	HG End 1415	-		
Evacuation Data		Field Parameters				
Measuring Point	тос	Color Clew				
Sounded Well Depth (ft bmp)	18.3	Odor	Nore			
Depth to Water (ft bmp)	6.13	Appearance	1			
Depth to Packer (ft bmp)						
Water Column in Well (ft)	12 17		I 1V	2V 3V		
Casing Diameter	0.	oH (s.u.)	7.75 7.67	7.48, 7.441		
Casing Diameter	<u>_</u>	Conductivity				
Gallons III Well		(mS/cm)	0 507 6.747	0,730 0,733		
Gallons Pumpeo/Balled	~	(IIIO/CIII)	0,00,02,111	1		
Sample Pump Intake		(prineareny)				
Setting (ft bmp)	_	Temperature (°C)	14.0 120	11.2 11.4		
Packer Pressure (psi)						
Pumping Rate (ml/min)		DO (mg/L)	8.0% 7.33	7.22 7.34		
Evacuation Method	Bailer	Turbidity (NTU)	634.1 670,4	841.6 216.0		
	Bailer	Time	1345 1350	1356 1400		
	1345 End 1400	DTW (ft bmp)	613 671	6.80 6.92		
Purge Timé Begin		ORP	2246 2151	2141 216-5		
Remarks: <u>Water Quality M</u> System On/Off:	Neter: 45I PD	OPS				
Initial Fulge.				<u> </u>		
Constituents Sampled: See	COC Samp	ling Personnel: JB	/MK			
Well Casing Volu	mes	4" = 0.65				
<b>Gal./Ft.</b> $1^{1/2*} = 0.06$ $2^* = 0.06$ $2^{-1/2*}$	= 0.26 3-1/2" = 0.50	6" = 1.47				
bmp below measuring point °C Degrees Celsius ft feet gpm Gallons per minute mg/L Miligrams per liter	mS/cm Milisiemens per centin s.u. Standard units NTU Nephelometric Turbidi N/A Not Applicable COC Chain of Custody	neter VOC Vol umhos/cm Mic ty Units	latile Organic Compounds cromhos per centimeter	5 5		

## ARCADIS

## Water Level Record

Project

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Ingersoll-ARO

Page 1 of 2 -

Date /2//7/19 Technician 57 /2 ŊΒ

Well (s)	Depth to Water (ft)	Total Depth (ft)	Time	MP (PVC)	Remarks Vacuum on/off
MW-1	3.32	28.48		1.7	
¥ MW-2 ✓	3.79	21.28	1150	~	
MW-3					
MW-3R		21.24			
MW-4	4,25	18.90	1230		
MW-4R	29.91	32.91	1231		
MW-5	10.26	24.87	1245	-	
MW-6 🗸	Z.43	14.14	1325		PFOA
MW-7	9.18	22.51		1	
MW-8	3.07	17.54	1208	1	
MW-9	3.51	24.83	12.00	~	
MW-10R	-0.33	16.38			Caston't arrit
MW-11 J	10.04	12.18 .	1300	~	
MW-13 🗸	11.61	23.41	1302	~	
MW-14	6.07	23.20	1240	$\sim$	
MW-14R	13.16	43.60		V	
MW-15	2.95				PFOA
MW-16	4.21	23.28		-	
MW-17	0.50	23.63	1315	/	water in well beer renoved
MW-18	Obstruction			<u> </u>	1
MW-19	4.42	24.50		V	the Thomas Mitel Hele
MW-20 9	6.35	24.61		V	
MW-21	4.73	15.50		V	
MW-22 🗸	5.42	20.89		1	
MW-23 🗸	5.29	19.48			
MW-24 🗸	2.51	17.53		V	
MW-25	2.00	12.10		V	
MW-26 1.00	above Tol in well box	John off			->
MW-27	2.44	16.15	1250	~	
MW-28	3.10	18.84	1155	5	
MW-29 🗸	2.48	18.32	1204	V	
OW-101	3.57	6.20	1304	$\checkmark$	
OW-102	1.91	4-64	1322	/	6
OW-103	-				Could not access
VEROW-1	2.45	12.46			
VEROW-2	water above TOL in -	13 70		_	->

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F

0.00 Well box, J-plug off

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#### Water Level Record

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Ingersoll-ARO

Well (s)	Depth to Water (ft)	Total Depth (ft)	Time	MP (PVC)	Remarks Vacuum on/off
RW-1A/PF-1	2.16	19.43			
RW-1B/PF-2	2.13	18.61			
PF-3	6.26	17.00			
RW-10A/PF-4	6.50	19.28			
PF-5	8.23	19.14			On
RW-3A/PF-6	7.99	18.88			
PF-7					On Carlant alles Lid.
RW-9A/PF-8	0.09	19.24			
PF-9	3.96	18.83			
RW-4A/PF-10	3.96	19.68			On
PF-11	2.53	17.61			
RW-1	2.00	19.32			
RW-2	1.98	19.32			on
RW-3	6.43	24.34			on
RW-4	14,40	19.12			on
RW-5	2.23	17.90			On
RW-6	2.45	19.10			
RW-7	2.60	17.95			
RW-8	2.21	16.31			
RW-9	4.27	20.75			
RW-10	6.50 5,72	18.50			on
RW-11 √	5.06	19.63			Change Nome on hell Lid
RW-11A/PF-13	4.60	19.48			-
RW-11B/PF-12	4.24	22.19			
			137		

2 of 2

Proj	ject	Ingersol Rand - A	RO Pro	ject No.	AY000220.0027	5	Pa	ge1 of	
Site	Location	Broadway, Che	eektowaga, NY			Date	12/18	119	
Site	Well No.	MW-2		Replicate	No.				
Wea	ather			Sampling	Time: Begin	End	+3:0	20 13	:45
Eva	cuation Da	ata			Field Parameter	\$			
Mea	suring Poir	nt	TOL		Color		Clar		
Sour	nded Well	Depth (ft bmp)	21.2	8	Odor		None	-	
Dept	h to Water	(ft bmp)	3.7	9	Appearance		·		
Dept	h to Packe	er (ft bmp)	_						
Wate	r Column	in Well (ft)	Z	49		1	1V	2V	3V
Casir	ng Diamete	эг	2"		pH (s.u.)	7.14	7.49	7.16	7.32
Galio	ns in Well		2.70	1	Conductivity				
Gallo	ns Pumpe	d/Bailed	<i>%</i>		(mS/cm)	0.793	0.759	.761	0.754
	Prior to	o Sampling			(µmhos/cm)				
Samp	le Pump li	ntake							25
	Setting (ft bmp)				Temperature (°C)	7.2	7,3	8.0	8.2
Packe	er Pressure	e (psi)				Sal	11 110	201	(1 10
Pump	ing Rate (I	ml/min)			DO (mg/L)	5.26	7.77	3.31	<u> 4,1C</u>
Evacu	ation Meth	nod .	Bailer	priping	Turbidity (NTU)	9.17	0,66	1.99	1.74
Samp	ling Metho	d ,	Bailer/	Ar: punp	Time	12:30	12:55	13:15	13:30
Purge	Time	Begin	End		DTW (ft bmp)				
					ORP	146,6	153,2	141.4	146.3
Berro	+	Water Quality Me	ater KSE	DSCPro					
Reina	цэ.	System Op/Off							
		Initial Purce:							
	3	nuar ruge.							
Constit	uents Sam	pled: See C	00	Samplin	g Personnel:	TA			
		Well Casing Volume	BS						
Gal/Ft.	$1^{1/4_{\pi}} = 0.0$	06 2" = 0.1	6 3ª =	0.37	4" = 0.65				
	1 "" = 0.0	99 2-½ <sup>e</sup> = (	0.26 3-½"	= 0.50	0 = 1.4/				
bmp ℃	below me Degrees (	asuring point m Celsius s.i	S/cm Milislemen u. Standard u	s per centimete Inits	r VOC Volat umhos/cm Micro	ile Organic Co mhos per cent	mpounds imeter		
ft com	feet Gallons n	er minute N/	TU Nephelom A Not Applica	etric Turbidily U able	nits				
ng/L	Miligrams	per liter CC	OC Chain of C	ustody					

Pr	Project Ingersol Rand - ARO Project No. AY000220.00225		5	Pa	age 1 of							
Sit	e Location	Broadv	vay, Cheek	towaga, NY					Date	12/18	119	
Sit	e/Well No.	MU	v-6		Replicate	No.	_					
We	ather	clea	. 24'		Sampling	Time: 1045	Begin	102	<u> </u>	a <u>1045</u>		
Eva	acuation D	ata				Fiel	ld Para	meters	l			
Mea	asuring Poi	int	_	TOC		Cole	or		Cloud	4		
Sou	Inded Well	Depth (ft b	mp)	14.14		Odo	r		Na	0		
Dep	th to Wate	r (ft bmp)	-	2.43		Арр	earance	<del>)</del>	shaft	ly tyrbit		
Dep	th to Packe	ər (ft bmp)							/	/		
Wat	er Column	in Well (ft)	-	11.71					1	1V	2V	3V
Casi	ing Diamet	er		2"		pH (s	s.u.)		7.55	7.22	7.23	7.11
Gallo	ons in Weil	1		1.87		Conc	Juctivity					
Galic	ons Pumpe	d/Bailed				(1	mS/cm)		447.5	787	932	1044
	Prior t	o Sampling				()	umhos/c	cm)				
Sam	ple Pump I	ntake										
	Setting (ft bmp)					Temperature (°C)7			7.7	9.4	8.6	9.7
Pack	er Pressure	e (psi)										
Pump	oing Rate (	ml/min)				DO (n	ng/L)		7.19	4.91	3.87	2.69
Evace	uation Meti	hod		Baili		Turbiç	Sity (NTI	J) ,	54	1131 AU	1264 AN	1498 10
Samp	ling Metho	d		Baile		Time			1020	1028	1035	1042
Purge	Time		Begin	End		DTW	(ft bmp)		2.78	2.80	2.82	
						ORP		1	123.3	125,0	124.7	120.0
				11 m -								
Rema	rks:	Water Qua	ality Meter:	YST .	USS P	0						
		System Or	ı/Off:									
	3	Initial Purg	e:									
Constit	uents Sam	pled:	See COC		Samplin	g Personr	nel:		57/JR			
	1	Well Casing	Volumes									
Gal./Ft.	$1^{1/4_n} = 0.0$	6 2	2" = 0.16	3" = 0.3	7	4" = 0.65	5					
	1 = 0.0	9 2	2-1/2" = 0.26	3-1/2" = 0	.50	6" = 1.47						
bmp °C	below me Degrees (	asuring point Celsius	mS/cm s.u.	Milisiemens pe Standard units	r centimete	r VOC umhi	; os/cm	Volatile Microm	Organic Cou hos per cent	mpounds imeter		
ft	feet Gallons or	er minute	NTU N/A	Nephelometric	Turbidity U	nits						
mg/L	Miligrams	per liter	COC	Chain of Custo	dy							

INYOSFP01\Data\APROJECTINGERSOLWRO\Field work\field forms\3 Volume Purge Water Sampling Log

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## ARCADIS

## Water Sampling Log

Project	Ingersol Rand - A	RO Proje	ct No	AY000220.0	0225		Pa	age 1 of		
Site Location	Broadway, Che	ektowaga, NY				Date	12/18	119		
Site/Well No.	MW-11		Replicate No.			-				
Weather	Clear 24	10	Sampling Time:	Begin (	7840	End	<u>Sinplu</u>	<u>L @</u> 1000		
Evacuation D	ata		1	Field Param	eters					
Measuring Poil	nt	TOC	(	Color		Cloudy	brown			_
Sounded Well	Depth (ft bmp)	12.18		Odor	-	nore				
Depth to Water	r (ft bmp)	10.04	<i>F</i>	ppearance	-	Turb	d			
Depth to Packe	er (ft bmp)				-					<del></del>
Water Column	in Well (ft)	2.14				I	1V	2V	3V	_
Casing Diamete	er	2"	p	H (s.u.)		7.01	8.34			
Gallons in Well		0.34	 C	onductivity						
Gallons Pumpe	d/Bailed			(mS/cm)		4.2	4.6			3
Prior t	o Sampling			(µmhos/cr	n)					5 6
Sample Pump I	ntake									8
Setting	g (ft bmp)		Te	emperature (	°C)	8.9	6.+			
Packer Pressure	e (psi)				_		2.00			
Pumping Rate (	mi/min) -		D	0 (mg/L)	_	+.24	9.72			
Evacuation Mether	hod	Beili	Tu	irbidity (NTU	) 28	sg7 au	4092 AU			
Sampling Metho	d _	Bailer	Ti	me	0	844	0855			
Purge Time	Begin_	0840 End	D1	TW (ft bmp)			11.81	DRY -	->	
			OF	RP	10	94.4	199.1			
								Blitten to	collect Sample	- <i>E 100</i> 0
Remarks:	Water Quality Me	ter: (SIII)	SS Pro							
	System On/Off:									
	Initial Purge:									
Constituents San	npled: See Co	oc	Sampling Per	sonnel:	ST/	JB				
f	Well Coston Volume				<u> </u>					
Gal./Ft 1 <sup>1/4</sup> = 0.	06 2" = 0.1	⊪s 6 3"=0.	.37 4" =	0.65						
$1^{1/2_m} = 0.0$	09 2-½" = (	).26 3-½" =	0.50 6" =	1.47						
bmp below me °C Degrees ft feet gpm Gallons p mg/L Miligrams	easuring point mi Celsius s.u Ni ver minute N/ s per liter CC	S/cm Millisiemens p J. Standard unli U Nephelometri A Not Applicabl DC Chain of Cust	per centimeter ls c Turbidity Units e ody	VOC umhos/cm	Volatile C Micromho	)rganic Co os per cent	mpounds limeter			

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Proje	ect	Ingersol Ran	d - ARO	Project No.	AY000220.002	5	Pa	age 1 of	
Site I	Location	Broadway	, Cheekto	waga, NY		Dat	e 12/1	8/19	
Site/	Vell No.	MW	-13	Replicat	No. DUP-DI-	20191218		•	
Weat	ther	Clear	24'	Samplin	g Time: Begin <u>()9</u> 0938	06 En	d <u>0938</u>	<u>.                                    </u>	
Evac	uation Dat	ta			Field Parameter	5			
Meas	uring Point	t	-	TOL	Color	NA			
Sound	ded Well D	epth (ft bmp	)	23.41	Odor				
Depth	to Water	(ft bmp)		11.61	Appearance	Stattly	tubid		
Depth	to Packer	(ft bmp)			_				
Water	Column ir	n Well (ft)		11.80	_	1	1V	2V	3V
Casing	g Diameter	r		2"	рН (s.u.) <sup>;</sup>	7.98	7.76	7.66	7.58
Gallon	is in Well			1.88	Conductivity				
Gallon	s Pumped	/Bailed			- (mS/cm)	361.8	654	697	700
	Prior to	Sampling			(µmhos/cm)				
Sampl	e Pump In	take							
	Setting	(ft bmp)			Temperature (°C)	11.0	12.8	12.5	13.0
Packer	r Pressure	(psi)		—					
Pumpi	ng Rate (m	nl/min)			DO (mg/L)	3.41	2.97	3.54	3.15
Evacua	ation Metho	bd		Baile	Turbidity (NTU)	103.2	2429 AU	5268 AU	3384 AV
Sampli	ng Method	I		Baile	Time	0907	0916	0925	0935
Purge 1	lime	В	egin <u>09</u>	06 End 0938	DTW (ft bmp)	16.44	18.08	19.22	20.58
					ORP	168.0	152.8	139.1	86.3
				1920 C					
Remark	(s: 1	Water Qualit	y Meter:	YSI DSS P	0				
	4	System On/C	Dff:						
	1	nitial Purge:							
Constitu	ients Sam	pled: <u>Se</u>	e COC	Sampl	ing Personnel:	T/JB			
	-1//	Veli Casing Vo	olumes		(II				
Gal./FL	$1^{1/2n} = 0.09$ $1^{1/2n} = 0.09$	5 2* 9 2-1	= 0.16 % = 0.26	3" = 0.37 3-½" = 0.50	4" = 0.05 6" = 1.47				
bmp °C fl gpm mg/L	below mea Degrees C feet Gations pe Miligrams (	elsuring point Celsius Priminute per liter	mS/cm s.u. NTU N/A COC	Milisiemens per centime Standard units Nephelometric Turbidity Not Applicable Chain of Custody	oter VOC Votati umhos/cm Micro Units	ile Organic C mhos per cer	ompounds ntimeter		

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Proje	ict	Ingersol Rand -	ARO	Projec	t No.	AY000220.0	0225	Pa	ge1 of	
Site I	ocation	Broadway, C	heektowa	ga, NY			Date	12/18/	19	
Site/	Vell No.	MW-	20		Replicate No	).				
Weat	lher				Sampling Ti	me: Begin	En	+ <u> 0:13</u>	5	
Evac	uation Da	ta				Field Param	eters			
Meas	uring Point	t		TOL		Color		Cher		
Soun	ded Well D	epth (ft bmp)	2	24.61	1	Odor		None		
Depth	to Water	(ft bmp)		6.35		Appearance				
Depth	to Packer	(ft bmp)		_						
Water	Column ir	n Well (ft)	/	8-210				1V	2V	3V
Casin	g Diamete	r		2"		pH (s.u.)	7.66	7.11	7.18	7.01
Gallor	ns in Well			2.92		Conductivity	A 4 7			
Gallor	s Pumped	/Bailed				(mS/cm)	5.34	0.822	0.836	0.840
	Prior to	Sampling		-		(µmhos/cr	n)			
Sampi	e Pump In	take								21
	Setting	(ft bmp)				Temperature (	°C) /./	10.0	9.5	1,6
Packe	r Pressure	(psi)					C.0201	1 20	20-	
Pumpi	ng Rate (n	nl/min)				DO (mg/L) 🔎	04 Eat	3.00	5.97	2.97
Evacu	ation Methe	od	B	nilv		Turbidity (NTU	) <u>20.4</u>	108	62 15.0	100
Sampl	ing Method	i	B	ailer		Time	9.38	9:46	9 5.5	10:05
Purge	Time	Beg	in	End		DTW (ft bmp)				
						ORP	165,3	161.4	154.0	148.0
Remar	ks: -	Water Quality System On/Off Initial Purge:	Meter:	YSI I	SI Pro					
Constitu	uents Sam	pled: See	COC		Sampling	Personnel:	JB			e.
Gal./Ft.	1 <sup>1/4</sup> * = 0.0 1 <sup>1/2</sup> * = 0.0	Well Casing Volu           6         2" =           9         2-½"	imes 0.16 = 0.26	3" = 0. 3-½" =	37 0.50	4" = 0.65 6" = 147				
bmp °C ft gpm mg/L	below mea Degrees C feet Gallons pe Miligrams	asuring point Detsius ar minute per liter	mS/cm M s.u. SI NTU Na N/A Na COC Cł	ilisiemens p andard unit sphelometri of Applicable nain of Cust	er centimeter s c Turbidity Uni a ody	VÓC umhos/cm i ts	Volatile Organic C Micromhos per cei	ompounds ntimeter	1	

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Proj	ect Ingerso	Rand - A	RO	Project No.		AY000220.0027	5	Pag	e 1 of	_
Site	Location Broa	idway, Che	ektowaga,	NY			Date	12/18/1	9	_
Site	Well NoM	W-22		Replic	cate No.					
Wea	ther	<u>r d. d</u>	20"+1	Samp	ling Tim	e: Begin	End	9:2:	٤	<i>a</i>
Evac	uation Data					Field Parameter	75			
Meas	suring Point		+	OL		Color	6	+ Bran	~	
Sour	ided Well Depth (f	t bmp)	20.89			Odor	/			
Dept	Depth to Water (ft bmp)		5.42			Appearance	Slipht Tulb			1
Deptł	Depth to Packer (ft bmp)							/		
Water Column in Well (ft)			.47			I	1V	2V	3V	
Casin	Casing Diameter			2"		pH (s.u.)	6.96	6.97	7.07	8,3
Gallons in Well		2.	48		Conductivity					
					(mS/cm)	0,992	0,925	0,902	4.0.683	
Prior to Sampling		~			(µmhos/cm)					
Samp	Sample Pump Intake						11			6.
Setting (ft bmp)						Temperature (°C)	6.3	4.9	7.5	0.5
Packe	Packer Pressure (psi)						212	3 11-	2	
Pumpi	ing Rate (ml/min)	-			-	DO (mg/L)	3,03	6.71	2.67	4,13
Evacu	ation Method	-	Bai	Ur/pr. pu	Y	Turbidity (NTU)	143	175	200	487.2
Sampl	ing Method	-	Bai	hrpp:pn	ne i	Time	1:57	1-2	9,12	9.17
Purge	Time	Begin_		End	'	DTW (ft bmp)	1.65	7.56	7.83	8.27
					(	ORP .	130	160	160	161.7
Remar	ks: Water (	Ouality Me	ter: Ys	TDCCP	50					
, contain	System	On/Off:	3							
	Initial P	urge:				·				
		- 197 - 194								
Constitu	uents Sampled:	See CO		San	pling Pe	ersonnel:		( Bray	Key-	
	Well Car	ing Volume			-					<i></i>
Gal./Ft.	1 <sup>1/4</sup> = 0.06	2" = 0.16	5	3" = 0.37	4"	= 0.65				
	$t^{1/2n} = 0.09$	2-1/2* = 0	.26 🦂 3	3-1/2" = 0.50	6"	= 1,47				
bmp	below measuring p	oint ms	5/cm Milisie	mens per cent	meter	VOC Volat	tite Organic Cor	npounds		
°C ft	Degrees Celsius	5.U NT	Stand: Nephe	ard units Iometric Turbid	lity Linits	umhos/cm Micro	omhos per cent	meter		
gpm	Gallons per minute	N/	Not Ap	plicable	aty on the					
mg/L	Miligrams per ilter	ÇC	Chain	of Custody						A.
					1.00					
IVNYOS	FP01\Data\APROJECT\IN	GERSOLIARÓI	Field worktfield h	orms\3 Volume Purg	e Water Sa	mpling Log				

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Pr	oject Ingen	sol Rand - ARC	D Project N	lo	AY000220.002	45	P	age 1 of				
Sit	te Location Bro	adway, Cheek	towaga, NY			Date	12/18	119				
Sit	e/Well No.	MW-23	Re	eplicate N	10		2					
We	eather		Sa	mpling T	ime: Begin <u>/2</u> [240	ce End	1240					
Ev	acuation Data				Field Paramete	9 <b>7</b> 5						
Me	asuring Point	_	TOC		Color	clear -	looting b	lack particles	to claudy			
Sou	inded Well Depth	(ft bmp)	19.48		Odor	Na	Na					
Dep	oth to Water (ft bm	p)	5.29		Appearance	Slight 1	turbol					
Dep	oth to Packer (ft bri	np)	<u> </u>			0						
Wat	ter Column in Well	(ft)	14.19			1	1V	2V	3V			
Cas	ing Diameter	-	2"		pH (s.u.)	7.24	7.18	7.15	7.27			
Gall	ons in Well		2.27		Conductivity	<u>//</u>						
Galle	ons Pumped/Baile	d			(mS/cm)	615,3	588.5	650.5	684.6			
	Prior to Samp	oling	-		(µmhos/cm)							
Şam	ple Pump Intake											
	Setting (ft bm	p)	**		Temperature (°C	) _7.9	3.8	9.3	9.3			
Pack	er Pressure (psi)							4.00				
Pump	oing Rate (ml/min)				DO (mg/L)	5.05	5.76	4.73	4.05			
Evac	uation Method		Baile		Turbidity (NTU)	18.1	98.3	100911	1221 AU			
Samp	ling Method		Baile		Time	1205	1210	1220	1235			
Purge	Time	Begin	20: End 12"	40	DTW (ft bmp)	6.11	8.16	8.22	8.31			
					ORP	14 9.6	142.0	137.0	149.5			
			Vcc ar	- 0								
Rema	rks: Water	Quality Meter:	IST DS.	S Pro			_					
	System	on/Off:	6.414 ····									
	Initial F	'urge:										
Constit	uents Sampled:	See COC	S	ampling	Personnel:	17/JB						
-	Well Cas	sing Volumes		-								
Gal.JFt.	$1^{1/4_{\rm H}} = 0.06$	2" = 0.16	3" = 0.37		4" = 0.65							
	1 <sup>1/2</sup> * = 0.09	2-1⁄2" = 0.26	3-1/2" = 0.50		6" = 1.47			_				
bmp	below measuring p	point mS/cm	Milisiemens per ce	entimeter	VOC Vola	itile Organic Co	npounds					
°C	Degrees Celsius	S.U.	Standard units	hidiby t lait	umhos/cm Micr	omhos per cent	Imeter					
gpm	Gallons per minute	N/A	Not Applicable	Didity Office	5							
mg/L	Miligrams per liter	COC	Chain of Custody									
				11								
WN YOS	FP01/DataMPROJECTVN	GERSOLVAROVField	vorkilieid forms\3 Volume P	urge Winter S	sampling Log							
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Water Sampling Log

Project	Ingersol Rand - Al	RO Project	t No	AY000220.0022	5	Pa	ge 1.of		
Site Location	Broadway, Che	ektowaga, NY			Date	 12/18/	19		
Site/Well No.	_MW-24	-	Replicate N	lo		<u> </u>			
Weather	SUMAY 24	4	Sampling Ti	ime: Begin <u>(/</u> 0 //ЧО	5 End	1140			
Evacuation Da	ta			Field Parameters	S				
Measuring Poin	t	TOL		Color	clear	to cloud	6		
Sounded Well	Depth (ft bmp)	17.53		Odor	N/a		8		
Depth to Water (ft bmp) 2.51				Appearance stightly function					
Depth to Packer	(ft bmp)				0 1				
Water Column i	n Well (ft)	15.02				1V	2V	3V	
Casing Diamete	r	Z"		рН (s.u.)	7.15	6.97	7.01	6.99	
Gallons in Well		2.4		Conductivity					
Gallons Pumper	l/Bailed			(mS/cm)	748	1024	1031	1014	
Prior to	Sampling	-		(µmhos/cm)					
Sample Pump In	ntake				Itte				
Setting	(ft bmp)			Temperature (°C)	10.1	9.9	11.3	12.3	
Packer Pressure	e (psi) -	—			40.51		1		
Pumping Rate (r	nt/min) -	_		DO (mg/L)	4.90	2.38	2.24	256	
Evacuation Meth	od -	Bailer		Turbidity (NTU)	18.5	79.8	82.5	1094	
Sampling Method	d -	Bailer		Time	1108	1115	1125	1137	
Purge Time	Begin_	1105_End_	1140	DTW (ft bmp)	3.78	5,60	7.98	11.75	
				ORP	126.9	123.2	121,1	121.7	
Remarks:	Water Quality Me System On/Off: Initial Purge:	ter: Y.SI	DSS P	стр					
Constituents Sam	pled: See Co	00	Sampling	Personnel:	Г/ ЈВ				
	Well Casing Volume	95 6 07 - 07	7	4" - 0.65					
Gal./Ft. $1^{1/2n} = 0.0$ $1^{1/2n} = 0.0$	)9 2-½"=() )9 2-½"=(	5 3 = 0.3 ).26 3-½° = (	97 0.50	4 = 0.65 6" = 1.47					
bmp below me °C Degrees f ft feet gpm Gallons p mg/L Miligrams	asuring point m Celsius s.t NT er minute N/ per liter CC	S/cm Milisiemens p u. Standard units FU Nephelometric A Not Applicable OC Chain of Custo	er centimeter s c Turbldity Un s ody	VOC Volat umhos/cm Micro lits	ile Organic Co mhos per cen	mpounds limeter			

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ARCADIS		13		7		3		
Water Sam	pling Log		and the second s	<u>i</u>		ALC: NO.		
Project Inc	ersol Rand - AR(	) Project No.	AV000000 000		_	*		
Site Location	Broadway, Chool		A1000220.002	25	- Pa	e 1.of		
- Site/Well No	MIAL - 2 A	lowaga, NT		Date	12/18	119		
Weather -	100-21	Sampling	Pino. Mime: Begin	End	11:0	0		
Evacuation Data			Field Parameter	rs	*			
Measuring Point		100	12 Color	10 B	11	_		
Sounded Well Dep	th (ft bmp)	\$18.32	Odor		Ulear	[		
Depth to Water (ft )	отр)	2.48	Appearance		10000			
Depth to Packer (ft	bmp)		- Production	0				
Water Column in W	/ell (ft)	15.84	5	1	1 1V	2V	3V	
Casing Diameter	_	2"	рН (s.u.)	7.90	2.38	7.35	7.37	,
Gallons in Well		2.51	Conductivity					
Gallons Pumped/Ba	iled		(mS/cm)	0.589	0.542.0	0.536	6.528	
Prior to Sa	mpling		(µmhos/cm)					
Sample Pump Intake Setting (ft b	e omp)		Temperature (°C)	5.9	7.7	7.7	8.2	
Packer Pressure (ps	i)						0	
Pumping Rate (ml/m	in)		DO (mg/L)	4.89	3.29	284	3,24	
Evacuation Method		Baili	Turbidity (NTU)	50.28	87.00	143	1/2-	
Sampling Method	-	Bail	Time	10:35	10:39	10:98	10 55	
Purge Time	Begin	End	DTW (ft bmp)	2.48	2.90	3.02	11051	2,91
			ORP	138.7	117.7	113.9	112.7	•
Remarks: Wat	er Quality Méter:	YSE DSS F	<u>م</u>	1				
Syst	tem On/Off:			l				
Initia	al Purge:			Ĩ				ū.
				1				
Constituents Sampled	See COC	Samplin	g Personnel:	v E				
Well (	Casing Volumes							
<b>Gal</b> $J$ <b>Ft</b> . $1^{372a} \approx 0.09$	2" = 0.16 2-½" = 0.26	3" = 0.37 3-½" = 0.50	4" = 0.65 6" = 1.47					
bmp below measurin	ng point mS/cm	Milisiemens per centimete	er VOC Volati	ile Organic Con	pounds			ŀ
°C Degrees Celsiu ft feet	S S.U. NTU	Standard units Nephelometric Turbidity II	umhos/cm Micro	mhos per centil	meter		.18 <sup>4</sup>	
gpm Gallons per min	ude N/A	Not Applicable					al a	
myre mingrams per in		Unain of Custody						

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Proj	ect	ingersol Rand -	ARO	Project No.	AY000220.0022	15	Pag	e 1 of		
Site	Location	Broadway, C	heektowaga, N	١Y	+1	Date	12/18	119	_	
Site	ite/Well No. RW-11			Replicate	Replicate No.				-	
Weather			Sampling	Sampling Time: Begin End End						
Evad	cuation Da	ita			Field Parameter	75				
Meas	suring Poin	ıt	10	L	Color	£	ter a	L+ Bra		
Sounded Well Depth (ft bmp) 19.63			3	Odor None						
Dept	h to Water	(ft bmp)	50	6/2.72	Appearance		Slightly	Tuble	1	
Depti	h to Packe	r (ft bmp)		/	-		/			
Wate	er Column i	n Well (ft)	14.5	7			1V	2V	3V	
Casir	og Diamete	r	4'	1	pH (s.u.)	721				
Gallo	ns in Well		9.4	7	Conductivity					
Gallo	ns Pumped	I/Bailed			(mS/cm)	0.775				
	Prior to	Sampling			(umhos/cm)					
Samp	ile Pump In	take			. ,					
	Setting	(ft bmp)			Temperature (°C)	7.5				
Packe	er Pressure	(psi)								
Pumpi	ing Rate (π	nl/min)			DO (mg/L)	4.45				
Evacu	ation Meth	od	Bayle		Turbidity (NTU)	55.3				
Sampl	ing Method	1	Baile		Time	13:20				
Purge	Time	Begir	I	End	DTW (ft bmp)	7.51				
					ORP	144.2				
Remar	ks:	Water Quality M System On/Off: Initial Purge:	leter: YS	L DSS F	174 SYSte,	27				
Constit	uents Sam	pled: See (	000	Samplin	ng Personnel:					
	14	Well Casing Volun	nes							
Gal./Ft.	$1^{1/2_{m}} = 0.0$	6 2" = 0. 9 2.14* -	.16 3"	= 0.37	4" = 0.65					
Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the second structure         Image: Provide the second structure       Image: Provide the second structure       Image: Provide the se										



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