ENGINEERING REPORT CONTAMINATED WELL WATER SUPPLY

OLIN CORPORATION NIAGARA FALLS, NEW YORK

APRIL 15, 1983

David L. Cummings Senior Specialist, Environmental Affairs

# TABLE OF CONTENTS

I.	INTR	CODUCTORY	1
II.	THE	INDUSTRY	2
	Α.	General Statement	2
	В.	Process Description	2
		1. General Description of Plant	2 4 7 8 9
	С.	Water Supply and Receiving Water	10
		<ol> <li>Water Supply</li></ol>	10 10 12 12
III.	DEVE	LOPMENT OF DESIGN CRITERIA	
	Α.	Industrial Waste Survey	14
	В.	Evaluation of Survey Results	14
	С.	Waste Characterization	22
	D.	Combination with Domestic Waste	24
	Ε.	Investigations of Treatment Methods	24
	F.	Alternative Proposals	26
	G.	Conclusions - 1980	26
IV.	DESI	GN CRITERIA - JULY 1, 1984 OBJECTIVES	
	Α.	Receiving Water	29
	В.	Abatement Plans	31
	APPE	NDIX I - Water Quality Standards	
	APPE	NDIX II - Analytical Data	
	APPE	NDIX III - Letter of March 16, 1981 - NYSDEC to Olin	
		NDIX IV - Pilot Column Study - Calgon Corp. NDIX V - Bioassay Data	

### I. INTRODUCTION

In late 1978, Olin Corporation found that the well water supply at its Niagara Falls plant was contaminated with low levels of organic compounds. Upon confirmation, through additional sampling and analysis, the situation was reported to the Niagara County Health Department and the New York State Department of Environmental Conservation (DEC). Because the mass of organics might be significant, Olin was requested to further investigate the situation and prepare an engineering report setting forth a proposed course of action to "eliminate such discharges to the greatest extent practicable".

The National Pollutant Discharge Elimination System (NPDES) permit (Permit Number NY 0001635) for the Niagara Falls plant had an expiration date of March 31, 1980 and application was made for a renewed permit under the State Pollutant Discharge Elimination System (SPDES). Preparation and submission of a preliminary engineering report on the contaminated water supply was made a condition of the draft SPDES permit.

The preliminary engineering report, submitted on October 10, 1980 included all available analytical data, reviewed potential abatement methods and provided initial, rough cost estimates for abatement. The conclusion of the report was that two wells should be pumped continuously. Such continued pumping would lead to stabilized performance with a steadily reduced organics output and would, over a period of time, cleanse the contaminated aquifer. The approach was approved by the DEC with a recommendation for continued investigation of abatement methods.

The concentrations of low level organics did reduce substantially; however, the receiving water quality considerations as developed by governmental agencies required reductions in a shorter period of time than was being accomplished in the pumping process.

The recently issued SPDES permit includes an abatement schedule for reduction of organic discharges to a maximum of 10 lb/day. The first step in that draft abatement schedule calls for submission of a preliminary engineering report by April 15, 1983. Submission of this report fulfills that permit condition.

# II. THE INDUSTRY

# A. General Statement

Historically, the Olin-Niagara Falls plant has been a basic producer of chlorine and caustic soda. Almost all chlorine (Cl<sub>2</sub>) is made by electrolysis, principally from sodium chloride (NaCl) brine, accounting for 95% of the production. The co-product is caustic soda. As early as 1789, Cl<sub>2</sub> produced from MnO<sub>2</sub> and HCl was bubbled into potash to produce potassium hypochlorite, KClO, and used to bleach textiles. The commercial production of Cl<sub>2</sub> by electrolysis, discovered by Cruickshank in 1800 and described in principle by Faraday in 1834, had to await the development of adequate electric power generation.

The first mercury cell to operate commercially started up July 4, 1895, in Saltville, Virginia. This was the Castner Rocking Cell, named for its inventor, Hamilton Y. Castner, who was born in Brooklyn but developed his cell in England in order to produce caustic soda for the manufacture of aluminum. Before the cell could be commercialized, the aluminum process for which it was designed became obsolete. Thomas Mathieson founded the Mathieson Alkali Works (a predecessor of the Olin Corporation) and built at Saltville a 1 ton/day chlorine caustic plant based on the Castner cell. It was soon discovered that more power than anticipated was required for operation, and the cells were moved to Niagara Falls to take advantage of the abundant, cheap power from a new hydroelectric plant. The new installation was designed for a production of approximately 30 tons/day. The cells were called "rocking cells" because a slow back-and-forth tilting motion was imparted to the cells to move the mercury from the electrolyzer to the decomposer and back again.

At about the time that Castner was developing his version of the rocking cell, Carl Kellner of Vienna made several important inventions in the field of mercury cells, among them the device of short-circuiting the soda cell. This principle is utilized in the amalgam decomposers of modern mercury cell installations.

Shortly thereafter Kellner designed a mercury cell featuring a long, slightly inclined trough down which mercury and salt brine flowed by gravity. The denuded mercury from the decomposer was returned to the inlet of the cell by a pump. This design, progressively improved, is the configuration of most modern mercury cells.

# B. <u>Process Description</u>

# 1. General Description and History of Plant

The Niagara plant began operation in November, 1897 under the name of Castner Electrolytic Company. Rated capacity for the one cell room containing 580 cells was 17.5 tons per day of chlorine and 19.5 tons of dry caustic soda. The gaseous chlorine was converted to bleaching powder in lead-lined chambers. In 1901, two additional cell rooms were built and in 1915 a half cell room was added making a total of 2030 Castner rocking cells. Liquid chlorine was produced for the first time in 1909.

Over a period of 60 years, there were few changes in the cell operations except that the electrolytic load was gradually increased to 1750 amperes and the rated daily production to 125.0 tons of chlorine and 139.0 tons of caustic soda.

Research on stationary mercury cells was carried out at Niagara by Olin and the first commercial installation was the E-4 cell, rated at 10,000 amps, at the Aluminum Company of Canada in Arvida, Quebec in 1948. The E-11 cell room at Niagara was put in operation in 1961 with 58 cells rated at 95,000 amperes and 186 tons of chlorine per day. The Castner cells were removed. A fifth rectifier was added in 1965 and production is now rated at 252 tons of chlorine per day and 277 tons of caustic soda per day with a load of 135,000 amperes. The power supply was changed from 25 cycle to 60 cycle at this time.

HTH® Dry Chlorinator (calcium hypochlorite) production was started on a small scale in 1927 and by 1945 had attained a rate of 6.0 tons per day. Production was increased in 1961 to 36 tons per day and now is rated at 60 tons per day. Hydrated HTH® has been produced since May, 1976.

Sodium chlorite production was started on a commercial scale in 1941 at a rate of 2000 lbs per day. The original process used calcium chlorate and muriatic acid for generation of chlorine dioxide and caustic and carbon black for reduction to chlorite. Sodium chlorate and sulfur dioxide were used for chlorine dioxide generation in 1951 and sodium peroxide reduction was started in 1957 with hydrogen peroxide and caustic substituted in 1972. Production capacity is now 16,000 lbs per day. This is the only sodium chlorite plant in the United States.

Sodium methylate production also started in 1941 using metallic sodium and methyl alcohol. Production was 1000 lbs per day using one vacuum dryer. As additional dryers were added, production increased to 10,000 lbs per day. The first amalgam reactor was installed in 1965 and metallic sodium was discontinued in 1966. The reactor was relocated to the cell room in 1968 and the second reactor was installed in 1973. Total reactor capacity is now 20,000 lbs/day and dryer capacity 13,000 lbs/day.

Niagara production items that were produced but have been tin tetrachloride in 1906, sulfur include, discontinued 1897-1945, 1908, bleaching powder monochloride in 1950-1956. trichlorobenzene hexachloride (BHC) and trichlorophenol 1954-1956, and GX (diglycollic dihydrizide) and Omset 1957-1959. The explosion of the BHC plant on August 6, 1956 marked the end of organic chemical production. In 1922, the first synthetic ammonia plant in North America was started with a capacity of one ton per day. This was enlarged to a capacity of 20 tons per day in 1926 and shutdown in 1962.

The production facilities are currently located on 22.161 acres on Buffalo Avenue in Niagara Falls, a portion of which is the original Castner Electrolytic Company site. The facilities consist of two (2) sites separated by a portion of the E. I. DuPont de Nemours Company. Plant 1 consists of the HTH® Dry Chlorinator production facility, administration offices and warehousing. Plant 2 consists of the chlorine/caustic soda, sodium methylate and sodium chlorite production facilities plus the powerhouse, maintenance facilities and additional warehousing.

# B. Production Processes

# Caustic Soda (Sodium Hydroxide) and Chlorine

Worldwide, slightly more than 50% of electrolytic Cl<sub>2</sub> production is by the mercury-cell process. In the United States, mercury cells account for about 30% of the production.

Most modern mercury cells are similar in appearance and construction. Modern cells may operate above 300,000 A and at a current density at the cathode of over 10,000 A/m<sup>2</sup>. Among the cells in operation in the United States are those by de Nora, Olin, Uhde, Solvay, and Krebs.

Production of Cl<sub>2</sub> by the mercury-cell process involves two cycles: the brine cycle and the mercury cycle. Brine is normally sodium chloride brine. The brine is partially depleted of its sodium chloride in the electrolyzer and must be fortified using a source of dry salt. The brine must be purified to ensure that harmful impurities from the salt do not build up and cause operating problems. The extent of the need for purification depends upon the impurities in the salt and the operating conditions which have been established.

The mercury cycle is part of the operation of the cell itself. Mercury flows by gravity in a thin layer along the bottom of the steel trough of the electrolyzer. Brine flows concurrently on top of the mercury. The amalgam, containing up to 0.3% sodium, is removed at the end of the cell. It then goes to the decomposer (or denuder) where it is reacted with water. Caustic soda is normally produced at a concentration of 50%. The denuded mercury is then collected in a sump where it is pumped back to begin its cycle over again.

Chlorine gas, saturated with water vapor and containing traces of organic impurities and hydrogen, collects in the cell chamber above the anodes. The chlorine gas goes from there to the drying and liquefaction part of the plant.

Where specific description or numbers are used in this article, they are based on the Olin E-510 cells as typical of most modern mercury cells.

The electrolyzer is a long rectangular steel chamber with rubber-lined sides, top, and end boxes. It is about 4 ft wide x 40 ft long. It is supported on adjustable, insulated structural pedestals along the length. The bottom has a pitch of about 10 mm/m. The cell itself is 8-10 inches deep. The cell cover can be lifted from the cell by a crane to permit renewal of the anodes and cleaning of the cells. When in place, a gas tight seal is made all around the edges with soft rubber gaskets and clamping devices.

The Olin cell uses metallic anodes. Flexible rubber seals and a flexible section in the anode bus permit a group of five anodes to be raised and lowered in a single operation. A recent development scans the voltage drop continuously over all the cells in a cell room and uses a computer program to adjust the anode/cathode gap for optimum performance.

The first step in processing gaseous chlorine is to cool it. This is done by direct contact in a packed tower or in a water-cooled titanium heat exchanger. A demister is then used to eliminate as much brine mist as possible. From the demister, the chlorine goes to the dryers. These are usually two-to-four packed towers over which sulfuric acid is pumped to contact the chlorine counter currently. Spent sulfuric acid is discharged at about 70% concentration. Chlorine gas is dried so that it contains 50 parts per million moisture or less.

The overhead gas is then compressed to the pressure at which it is liquefied. Dry air is usually added during liquefaction to replace the chlorine as it liquefies so as to maintain the gaseous mixture below 4% hydrogen. Non-condensable gases, principally air, hydrogen, and carbon dioxide, are purged from the condenser system. The vent or sniff gas may be variously treated in order to remove the chlorine. In the Niagara Falls plant, it is converted to sodium hypochlorite. Condensed chlorine is then transferred to storage tanks from which it may be loaded into transportation containers.

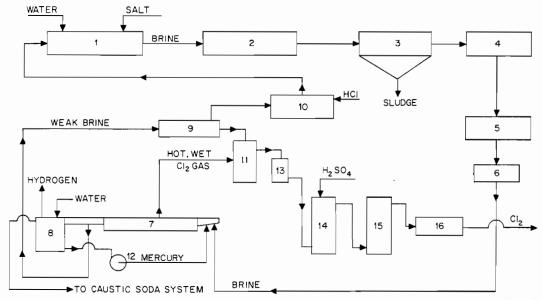


Fig. C-18. Simplified representation of materials flow in production of chlorine by mercury-cell process. (1) Salt dissolving, (2) brine treatment, (3) settling, (4) filtration, (5) brine storage, (6) heating, (7) electrolyzer, (8) decomposer, (9) dechlorination, (10) pH adjustment, (11) cooling, (12) mercury pump, (13) demisting, (14) drying, (15) scrubbing, (16) liquefaction.

Liquid chlorine is usually transferred by compressed air. Compressed air is dried in chlorine-producing plants to a dew point of -60°F or less. This is to prevent pickup of moisture in the transfer operation. Since pressures of 150 psig are not uncommon for transfer purposes, it is clear that tanks must be vented to permit the admission of fresh chlorine. These are vented normally to the plant sniff gas system. In some cases where high transfer rates are required, submerged pumps designed for this service can be used. This is commonly the case when transferring from storage tanks to barges.

# Calcium Hypochlorites

Bleaching powder (prepared by passing chlorine gas over slaked lime) was the first way that chlorine was made generally available commercially (the technique was patented in 1799). The product usually contained about 30% available chlorine. Although it was unstable and difficult to use, it was of enormous importance in bleaching of textiles and later for sanitizing.

Bleaching powder has largely been supplanted in the United States by an improved calcium hypochlorite product containing about 65% available chlorine. Several commercial routes are available for its production. In the HTH® Dry Chlorinator process, a caustic solution is chlorinated to form sodium hypochlorite which is then filtered. The solution is mixed with lime and enters a second chlorinator where a triple salt is formed. The solution is filtered to remove sodium chloride crystals and stored. The triple salt is filtered from the solution and mixed with chlorinated lime. The paste formed (high test hypochlorite) is filtered, pre-dried, pre-formed, granulated, dried, crushed, screened and packaged.

The largest use of the product is for swimming pool sanitation, but substantial quantities are used for water purification and algae control. Because of its relative stability, it is an ideal product as an emergency standby for chlorine. It is particularly useful for sanitation at times of floods or other disasters.

# Sodium Methylate

In the sodium methylate manufacturing operation, a sodium/mercury amalgam from the chlor-alkali cells is fed to a reactor along with methyl alcohol to form sodium methylate (NaOCH3). The denuded mercury is returned to the decomposers of the electrolyzing cells. The sodium methylate/methyl alcohol solution is passed through filters and pumped to storage. From storage, part of the solution enters dryers where powdered sodium methylate is produced. The methyl alcohol evaporated in the dryer is condensed and recycled for reuse in the reactor. The remaining solution is sold as such.

### Sodium Chlorite

In the sodium chlorite manufacturing operation, a sodium chlorate/sodium chloride solution, sulfuric acid, and a sulfur dioxide/air mixture are added to a generator vessel. The chlorine dioxide produced, along with some chlorine and sulfur dioxide gas leaving the generator, enters a reducer (absorber) along with hydrogen peroxide and caustic soda, where an aqueous sodium chlorite solution is formed. This solution is filtered to produce liquid product and also dried to produce solid sodium chlorite product.

# 3. Plant Operations

a. Finished Products - Rated Capacity

Liquid Chlorine - 284 tons/day Caustic Soda - 277 tons/day HTH® - 57.5 tons/day Sodium Chlorite - 5.95 tons/day Sodium Methylate - 5.25 tons/day

b. Principal Raw Materials

Sodium Chloride (Rock Salt) Sulfuric Acid Water Electricity

Lime Water

Methanol

Sodium Chlorate Hydrogen Peroxide Sulfur Dioxide Water

c. Shifts, Operating Hours, Number of Employees

Shifts - 3 Operating Hours - 24 hrs/day, 7 days/week Employees - 393 (total hourly and exempt)

d. Expansion - There are no current plans for expansion of operations at the Niagara Falls plant. Production of HTH® was temporarily shutdown due to business conditions on October 30, 1982. The shutdown is for an indefinite period with no estimate of a future startup date. This report is prepared with the understanding that the HTH® facility will operate in the future.

# Plant Description

a. Company

Olin Corporation Olin Chemicals Group 120 Long Ridge Road Stamford, Connecticut 06904

b. Plant Location

Olin Corporation Olin Chemicals Group Niagara Falls Plant 2400 Buffalo Avenue Niagara Falls, New York 14302

c. Mailing Address

Olin Corporation
Olin Chemicals Group
Niagara Falls Plant
P. O. Box 748
Niagara Falls, New York 14303

d. Name of Responsible Individuals

M. L. Norsworthy

Plant Manager P. O. Box 748

Niagara Falls, New York 14303

A. F. Kapteina

Environmental & Quality Assurance Mgr.

P. O. Box 748

Niagara Falls, New York 14303

D. L. Cummings

Senior Specialist, Environmental Affairs

P. O. Box 248

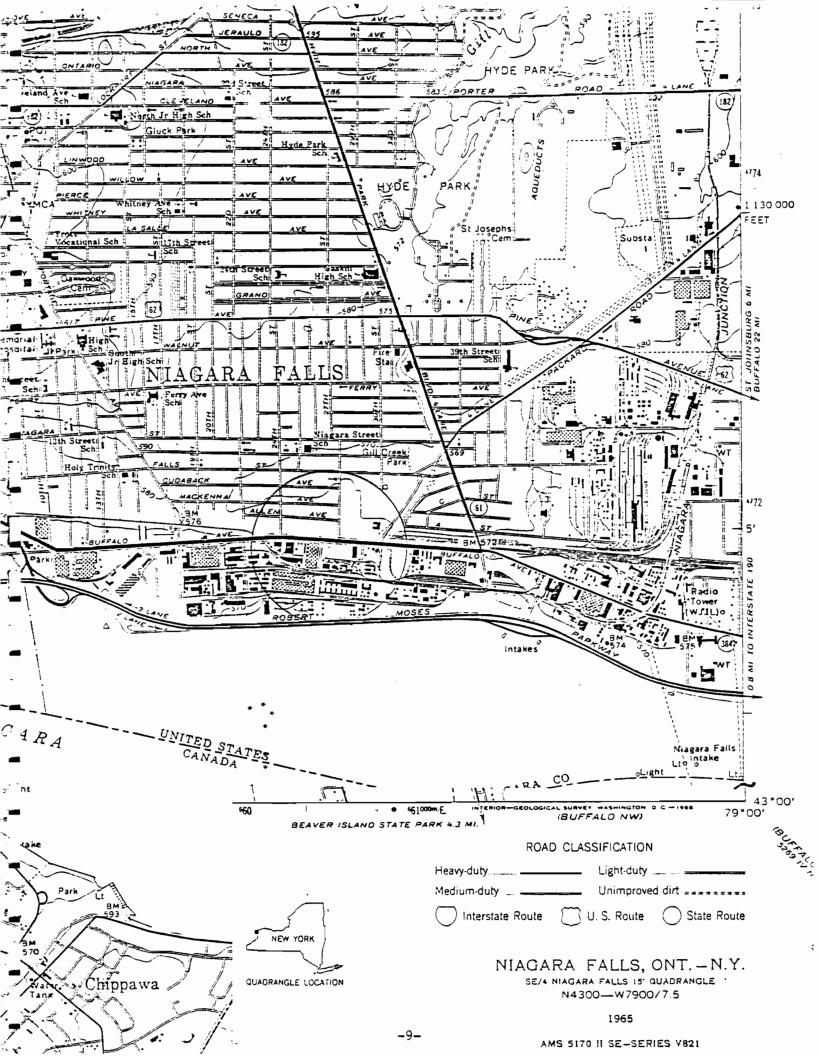
Charleston, Tennessee 37310

e. Map of Environment - Following Page.

U.S.G.S. Topographical Map. Niagara Falls, Ontario - New York, SE/4, Niagara Falls 15' Quadrangle, 1965.

f. Sewer Map and Process Connections - See enclosed Olin Drawing Numbers:

Number D-0000-840-10-2 Number D-1592-830-5-1 Number D-1592-830-5-2



# C. <u>Water Supply and Receiving Water</u>

# Water Supply

The Niagara Falls plant operates with three (3) sources of water supply. Since the primary use of water is for cooling and the heat load and temperature of the Niagara River water vary with the seasons, there is a seasonal variation in consumption figures:

Source	Flow (mgd)				
	Winter	Summer			
Niagara River	2.02-2.95 2.48 avg.	2.88-4.90 3.89 avg.	ام المراج		
Well Water	2.88-3.74 3.31 avg.	3.74-5.18 4.46 avg.	31000		
City Water (City of Niagara Falls)	0.43	0.43			

# 2. Water Quality Requirements

Among the several uses of raw water at the Niagara Falls plant (e.g., boiler feed water, product, cooling, etc.), cooling is by far the major usage of river and well water.

As noted previously, the plant can use in excess of 8 million gallons of water per day in the summer months. Ninety percent of this is for cooling purposes, mainly in "once-through" systems. In once-through systems, the initial temperature is of considerable importance. Generally, the lower the initial temperature of such a water, the more desirable it is as cooling water. Of similar importance is the consistency of temperature and the Olin process wells produce a supply at 53-55°F, summer and winter. The real value of the wells lies in the combination of low temperature and high volume.

Wells in an area about a half mile wide adjacent to the Niagara River above the falls have substantially higher yields than wells elsewhere in the area. The higher yields in this area are caused by two conditions: (1) the Lockport Dolomite is thickest in the area, and (2) more importantly, conditions are favorable for the infiltration of water from the Niagara River. The greatest thickness of the Lockport provides the maximum number of water-bearing zones to supply water to the wells. The Niagara River provides an unlimited source of recharge to the water-bearing zones.

Evidence that a substantial part of the water pumped is supplied by induced infiltration from the Niagara River is indicated by the high yields, which exceed 2000 gpm at some wells, and the chemical character of the water. The chemical composition of the water in well 304-901-6 (Olin) (which has been pumped at 2100 gpm) is more similar to Niagara River water than "typical" groundwater in the Lockport.<sup>2</sup>

The Niagara River water is returned via "clear water" sewers to the river after use. Important considerations with this supply are screening of debris, prevention of growth of aquatic organisms, fouling of conduits and heat exchangers. The major problem is lack of consistency in temperature. River water can actually be too cold in the winter months. Treatments for prevention of slime and scale must be inexpensive on a once-through system and substances cannot be added which would prove deleterious to its further uses or be in contravention of water quality or discharge standards.

In short, cooling waters should have appropriate initial temperatures and should not deposit scale, be corrosive, or encourage the growth of slimes. Among the constituents of natural water that may prove detrimental to its use for cooling purposes are hardness, suspended solids, dissolved gases, acids, and oil and slime-forming organisms. One of the most definitive lists of quality requirements for cooling waters gives the following recommended limiting concentrations:

Turbidity	50 mg/1
Hardness	50 mg/1
Iron	0.5  mg/1
Manganese	0.5  mg/l
Iron and manganese	0.5  mg/l

The Olin process wells provide a source of supply which is slightly harder than desired but in all other respects, is an ideal cooling water supply. No raw water treatment has been required for control (chemical addition or filtration) and the temperature is a uniform  $53-55^{\circ}F$ .

Johnston, <u>Groundwater in the Niagara Falls Area, New York</u>, NYS Conservation Department, Bulletin GS-53, (1964) p. 30.

# 3. Description of Production Wells

The Mathieson Chemical Company originally had one well at the Plant 1 site. The well was 18 inches in diameter, 125 feet deep, and was originally drilled in 1937. In a search for additional water in 1947, two additional wells were drilled approximately 50 feet west of the original No. 1 well. Also at this time, an 8 inch diameter test well was drilled between the two new wells (Number 2 and 3). Wells 2 and 3 (the wells in use at present) are 24 inches in diameter and 125 feet deep. In approximately this time period (1947), Olin discontinued use of the No. 1 well and later sold the property where the well was located to E. I. DuPont de Nemours Company. Plant records indicate that DuPont also had several wells on their property ranging in diameter from 6 to 24 inches in diameter and all approximately 125 feet deep. Field investigations carried out in 1948 concluded that "all the accessible DuPont and Mathieson operating and observation wells are cross connected either directly or indirectly" in the aquifer. Reports at the time also noted the consistent recording of crevices and broken limestone at the 45-50 foot level. was a major water bearing layer.

Repair and remedial work was performed on Olin wells 2 and 3 in late 1978. This included plugging the 8 inch test well with concrete to a depth of 38 feet and relining the two production wells with new steel casings. The casings were 16 inches in diameter and were grouted in place from the 38 foot level to the surface. Any contamination reaching the wells must be entering from below the 38 foot level.

# 4. Receiving Water

All process waters are discharged to the City of Niagara Falls Municipal Wastewater Treatment Facility (POTW). Process contaminated wastewaters are pretreated in one or more on-site pretreatment processes, as needed, prior to discharge to the POTW. The POTW is a physical/chemical treatment facility which is intended to utilize activated carbon filters for the removal of organic compounds prior to ultimate discharge to the Niagara River. Difficulties have been experienced with the carbon beds and they are currently out of service. However, they are scheduled for rehabilitation and reactivation in 1984.

The cooling water, or "clear water" sewers (SPDES discharges 002, 004 and 005) discharge directly to the City-owned diversion sewer on Buffalo Avenue. The Diversion Sewer receives other industrial treated and untreated wastewaters prior to discharge to the Niagara River. The Niagara River (NYS 0-158) is classified by the New York State Department of Environmental Conservation as Class A Special (International Boundary Waters).

Classifications and Standards of Quality and Purity (Parts 700, 701 and 702 of Title 6, Chapter X of the Codes, Rules and Regulations of the State of New York) provide the current State water quality standards. Applicable portions are enclosed as Appendix I.

The NYSDEC has proposed additional water quality standards which provide for specific concentration limitations on a variety of organic compounds. (Proposed revisions to Parts 701 and 702, December, 1978). These proposed standards were remanded by the Commissioner of Environmental Conservation and have not been reproposed or promulgated to date.

The USEPA has promulgated water quality criteria¹ for most of the 127 priority pollutants. These criteria were not promulgated as fixed limitations or standards. Rather, they were provided by the USEPA as guidelines to the states and other standard settling authorities. The criteria promulgated in November 1980 replaced the criteria for the same pollutants previously published in the "Red Book".²

The United States of America entered into an agreement with the government of Canada in 1972 on Great Lakes Water Quality (GLWQA). The agreement was reaffirmed and expanded in 1978 (Appendix I) and is currently in effect. No clear definition has been made within the USA regarding enforcement power for the 1978 agreement and no specific regulations have been promulgated which specifically address the agreement. The agreement was signed by Ms. Barbara Blum, Deputy Administrator of the USEPA. The USEPA has promulgated various regulations regarding water quality primarily under the Clean Water Act (CWA). It must be presumed that the EPA, in addressing its responsibility for assuring "clean water", believes that its promulgated regulations satisfy the obligations of the GLWQA.

The NYSDEC has no regulations which specifically address the GLWQA. Again, the NYECL and NYCRR sections on water quality must address the issues of the GLWQA. NYS is prohibited from attempting to enforce the GLWQA without have NYS promulgated statutes and regulations.

The GLWQA is in existence, however, it is not currently enforceable per se. It is only through existing NYS and US statutes and regulations that its objectives can be obtained.

Since the Niagara River is a drinking water supply, USEPA primary drinking water standards and NYS Health Department drinking water standards would apply and are enclosed in Appendix I.

<sup>&</sup>lt;sup>1</sup> 45 FR 231, November 28, 1980.

Quality Criteria for Water

# III. DEVELOPMENT OF DESIGN CRITERIA

# A. Industrial Waste Survey

In 1978, Olin Chemical Group, on the recommendation and direction of the Environmental Affairs Department, carried out a program of characterization of all Chemicals Group plant discharges. Each discharge was analyzed for the U. S. Environmental Protection Agency list of 129 priority pollutants. Preliminary results for the Niagara Falls plant surprisingly showed the presence of a series of organic compounds. The contaminants were totally unexpected as the identified chemicals were not and, for the most part, had not been used or produced at the plant.

An immediate check of Niagara River water supply showed some contamination by several of the compounds in question but not at levels sufficient to account for the discharge levels detected. Process well water was subsequently sampled and was found to be the source. The total of the organics concentrations was 3.132 ppm. Further analyses were performed to confirm the initial results (see Appendix II for analytical data).

The first three sampling results showed a general downward trend  $(11/1/78,\ 3/5/79,\$ and 5/27/79). The next sampling (6/27/79) showed a substantial increase in organics concentration, to 41.173 ppm. A sampling program was instituted which resulted in approximately monthly samples during the period of June, 1979 through March, 1980. Weekly samples were collected and analyzed from March, 1980 to the present.

### B. Evaluation of Survey Results

The significant compounds identified in the analytical program were not used or produced by Olin. Several chlorinated benzene compounds were produced by Olin at the Plant 2 site in the period from 1950-1956, but the compounds identified in the well water were generally chlorinated methanes, ethanes, and ethenes.

Comparison of the organic compounds found in the production wells (125 ft. deep) versus the compounds found near Gill Creek (monitoring wells 7.2 to 18 ft. deep) reveals that the character of the two conditions are completely different. It can further be shown (2) that the primary source of water for the deep production wells is infiltration from the Niagara River.  $^{1}$ 

Two apparently separate natural hydrologic system exist at the Niagara Falls plant. The <u>soil-water system</u> is the water in the lower part of the soil/fill (5 to 10 feet thick) and uppermost, fractured part of the bedrock (1 to 5 feet thick); this water probably moves slowly eastward to Gill Creek and south toward the Niagara River.

Johnston, R. H., Groundwater in the Niagara Falls Area, New York, p. 30.

The ground water system is the water in the limestone-dolomite bedrock (Lockport Formation) underlying the fill. The base of the formation is about 140 feet below the surface. Water in the bedrock moves mostly through solution-widened horizontal openings (bedding-joints or bedding planes), although some water moves through more or less If no water were being pumped in the Buffalo vertical fractures. Avenue industrial area, water would probably move slowly from the Niagara River above the falls to the outcrop of the formation in the Niagara Gorge below the falls. Because of relatively large pumping rates, especially at Olin, the movement of water is locally reversed. The heavy pumping has already served to further induce infiltration from the Niagara River into the bedrock near the plant; in fact, most of the water being pumped from the Olin wells comes fairly directly from the River. Water levels in the bedrock away from pumping centers is probably slightly below the river stage, and near the wells the levels are drawn down, as low as 50 feet below the surface at Olin.

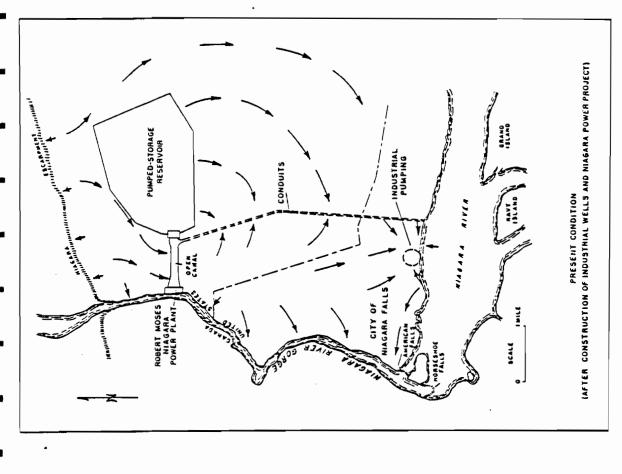
The two water systems are apparently separated by at least 15 to 20 feet of hard, impermeable bedrock except that vertical fractures, or joints do occur at irregular spacing in the bedrock.

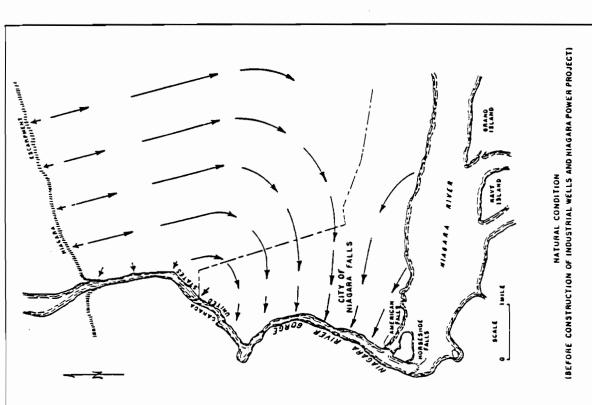
Infiltration from the river can occur where pumping has lowered groundwater levels below river level to such an extent that a hydraulic gradient is created between the river and the wells. The amount of the infiltration depends on the gradient and the nature of the hydraulic connection between the river and Lockport. The hydraulic connection is controlled by the character of the river bottom. Throughout most of its length in the Niagara Falls area, the bottom of the river is covered by a layer of unconsolidated deposits including both till and clay and silt. This layer was found to be from 10 to 20 feet thick in the vicinity of the Niagara Falls water-system intake. In the section of the river occupied by rapids, extending a half mile or more above the falls, the bottom has been scoured clean by the river. Where the layer of unconsolidated deposits is present, its low permeability greatly retards infiltration. Where the layer is thin or absent, infiltration can readily occur. '

Analysis of the potential sources of the identified pollutants in Olin well water revealed that >98% were product, by-product, or raw material for chlorinated solvents manufacture (see following pages). Manufacture of chlorinated solvents has never been an Olin activity. Further, methanol was identified in the well water and it also was produced by some chlorinated solvent manufacturers.

Greater than 95% of the compounds identified were characterized as volatile and the analysis program was modified after the first few samplings to reflect this fact. Analyses after May, 1979 were generally for volatile organics only, i.e., Volatile Organics Analysis or VOA as described in the USEPA Priority Pollutant Analysis protocol.

/ <u>Ibid. p. 30</u>





Inferred direction of ground-water movement in the upper water-bearing zones of the Lockport Dolomite in the vicinity of Niagara Falls.

From Johnston, Ground Water in the Niagara Falls Area, New York, NYS Conservation Department, p. 54, Bulletin GW-53 (1964).

The analytical data has shown a continual overall drop in concentration since the monitoring program began. A plot of the 12-month rolling average of total organics concentration versus time (p. 18) clearly exhibits the downward trends in organics concentration. There have been several temporary increases in concentration that are related to well pumping variations, soil retention characteristics, and/or seasonal variations. These temporary increases in concentration have also decreased in intensity with continual pumping. Actual plots of organics concentration versus time are also provided on page 19.

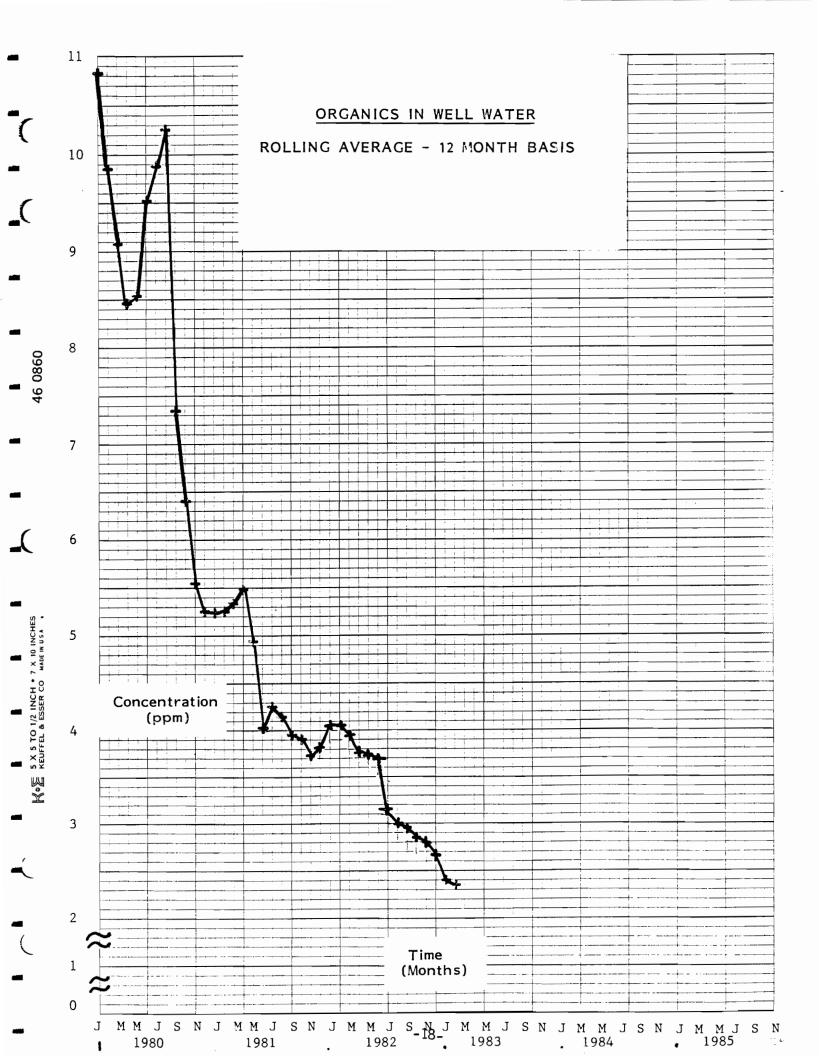
It has been previously shown (Engineering Report - Contaminated Well Water Supply - October 2, 1980) that an average of >98% of the detected compounds are found in the VOA analysis fraction. Further, it has been shown that the top five compounds found in any given sample consists of nine compounds. Considerations of potential treatment specifications concentrated on these nine compounds.

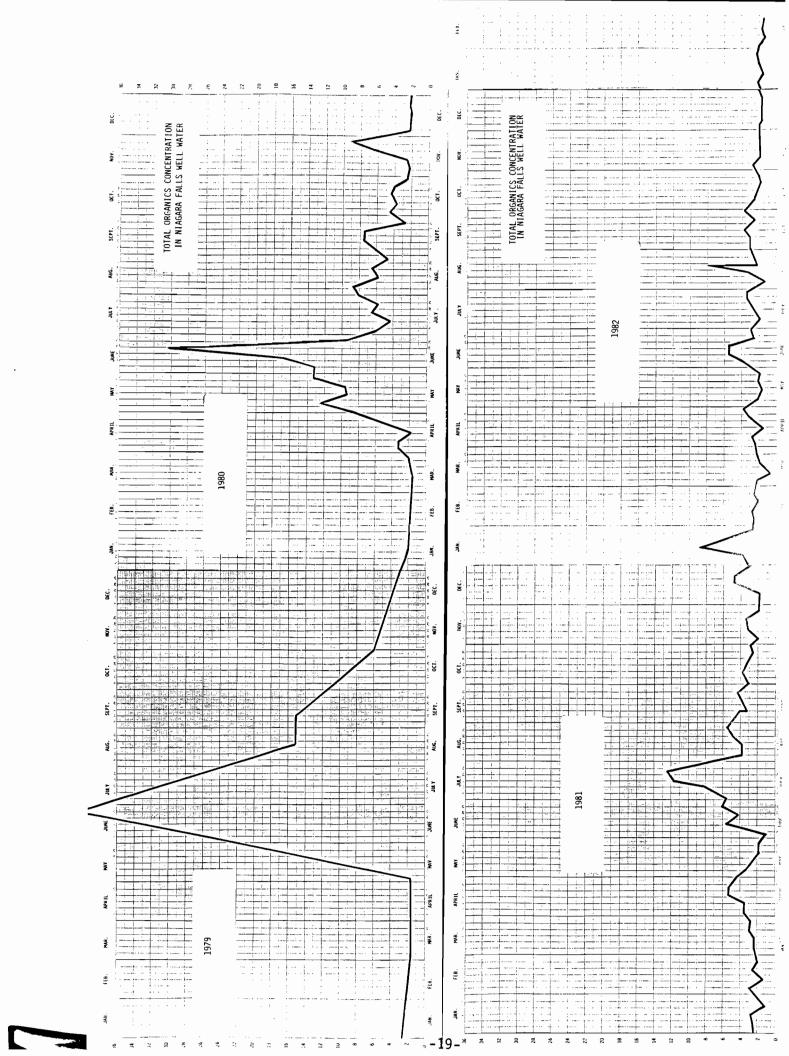
# AVERAGE ORGANIC CONCENTRATIONS PROCESS WELL WATER - PAST 12 MONTHS (3/82 - 2/83)

#### AVERAGE CONCENTRATION

	COMPOUND	<u>(ppb)-Overall</u>	(ppb)-2 North	Wells South	(ppb)-1 North	Well South	
1.	Carbon Tetrachloride	54	31	93	46	25	
2.	Chloroform	270	399	184	210	190	
3.	Dichloroethenes	≦148	166	150	133	114	
4.	Methylene Chloride	≦ 66	≦ 16	≦ 1	0	0	
5.	1,1,2,2-Tetrachloroethane	118	123	136	97	72	
6.	Tetrachloroethene	938	1091	1084	787	748	
7.	Trichloroethene	1063	1249	1119	797	614	
8.	Vinyl Chloride	21	≦ 16	<u>≤ 18</u>	5	<u>≤ 12</u>	
	TOTAL OF TOP NINE	2678	≦3091	<b>≦2785</b>	2070	≦1775	

It was also observed that in general the north well yielded higher concentrations of organics than did the south well. This observation held true with one well and two well operation.





# SUMMARY OF ORGANIC CONTAMINANTS (Total Number of Analyses - 276) (Total Number of Complete Characterizations - 7) (Data Through February 1983)

COMPOUND	NUMBER OF TIMES DETECTED/276	NUMBER OF TIMES DETECTED/7	MAXIMUM VALUE (ppb)	CHLORINATED SOLVENT MANUFACTURE(6)	OLIN USAGE
1,1,2,2-Tetrachloroethane Tetrachloroethene Trichloroethene Dichloroethenes Chloroform	260 285 265 269 283	   	26887 16000 14000 2006 1400	Known Intermediate Known Product/By-Prod Known Product Known Product/By-Prod Known Product	
Carbon Tetrachloride Methylene Chloride Methanol Vinyl Chloride 1,1,1-Trichloroethane	282 108 1(5) 227 202	  	1200 670 485 440 140	Known Co-Product Known Product/By-Product Known Product Believed By-Product Believed By-Product	(2) JCt (3)
1,1,2-Trichloroethane Hexachloroethane Trichlorofluoromethene Monochlorobenzene Tetrachlorobutadiene	106 (4(7) 46	7   2	53 29.6 27 24 22.2	Believed By-Product Known to be Present Known Intermediate	(2)
Benzene Ethylbenzene Dioctylphthalate Hexachloro-1,3,-butadiene Pentachlorobutadiene	33 2 	1 2 6 2	19 18 18 16 13.4	(5) Believed By-Product Known to be Present	(2)
Dichloroethane Pentachloroethane Diisooctylphthalate Trichlorobenzene Phenanthrene/Anthracene	8    	3 3 6 3	10 8.6 5.9 5	(5)	. (2)
Pyrene BHC (hexachlorocyclohexane) Toluene Dioctyladipate Dichlorobenzenes	  4 	5 5  2 2	1.21 1.8 1.7	(5)	(2) (4)
Fluoranthene Hexachlorobenzene	=======================================	5 1	1	Believed By-Product	(4)

<sup>(1)</sup> (2) (3) (4) (5) (6) (7)

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

Known to have been used; small, non-production quantity.
Used or produced in quantity at Plant 2 site.
Used in quantity, past and present, at Plant 2 site.
Potential by-product, Plant 2 site.
Presence of both phthalates and adipates at least partially due to contamination in analysis.
Non-Olin processes

Non-Olin processes.
Compound from 4/7/82 sample identified as dichlorodifluoromethane.

# SUMMARY OF ORGANIC CONTAMINANTS - PAST 12 MONTHS (Total Number of Analyses - 93)

(Data March 1982-February 1983)

COMPOUND	NUMBER OF TIMES DETECTED/93	MAXIMUM VALUE (ppb)	CHLORINATED SOLVENT OLIN MANUFACTURE(4) USAGE
Trichloroethene	93	4000	Known Product
Tetrachloroethene	93	3900	Known Product/By-Product (1)
Chloroform	93	810	Known Product
1,1,2,2-Tetrachloroethane	93	560	Known Intermediate (1)
Dichloroethenes	93	≤ 460	Known Product/By-Product
Carbon Tetrachloride	92	440	Known Co-Product (2)
Methylene Chloride	9	330	Known Product/By-Product
Vinyl Chloride	65	210	Believed By-Product
Trichlorofluoromethene	1(5) 7	27	
Monochlorobenzene	7	24	
1,1,1-Trichloroethane	57	24	Believed By-Product
Ethylbenzene	14	18	(2)
Benzene 1,1,2-Trichloroethane	14 34	14 11	Believed By-Product (2)
1,1,2-11 1011101 0e chane	<b>J</b> ¬	11	believed by alloudet

Known to have been used; small, non-production quantity.

Used or produced in quantity at Plant 2 site. (2)

(4) Non-Olin processes.

Compounds detected on one occasion only and not quantitated or quantitated at NOTE: <1 ppb have been omitted.

DLC/vrp 4/11/83

Compound from 4/7/82 sample identified as dichlorodifluoromethane. (5)

# C. Waste Characterization

### 1. Standards

The USEPA has proposed but not yet promulgated BAT effluent guidelines for the organic contaminants in question. BAT effluent guidelines cannot be applied to the Olin cooling water effluent. BAT guidelines apply to the process discharges only. Consequently, the only standards which apply are receiving water quality criteria and drinking water standards (See Appendix I). Except for two (2) compounds, the receiving water standards are written in general terms. The characterization of the discharge streams must be examined from the point of view of their effect on the receiving water and its usage.

# 2. Concentrations

The maximum and average concentrations of the major compounds as determined over the past year have been utilized to calculate equivalent concentrations in the diversion sewer and in the Niagara River (assuming zero background).

BASIS - 4.46 mgd well water output (2 wells)

- 80 mgd Diversion Sewer Flow (including 60 mgd from POTW)
- 32,313.6 mgd Minimum River Flow (50,000 cfs) - Average and Maximum Organic Concentrations

CONCENTRATION (ppb)
(March 1982-February 1983 Data)

	COMPOUND	IN WELL WATER			IN DIVERSION SEWER		RA R
		avg.	max.	avg.	max.	avg.	max.
1.	Carbon Tetrachloride	54	440	3	24	0.007	0.061
2.	Chloroform	270	810	15	45	0.037	0.111
3.	Dichloroethenes	≦148	460	8	26	0.020	0.064
4.	Methylene Chloride	≨ 66	330	4	18	0.009	0.045
5.	1,1,2,2-Tetrachloroethene	118	560	7	31	0.017	0.077
6.	Tetrachloroethene	938	3900	52	217	0.130	0.538
7.	Trichloroethene	1063	4000	59	223	0.147	0.552
8.	Vinyl Chloride	<b>≤</b> 21	210	1	12	0.003	0.029

<sup>&</sup>lt;sup>1</sup> 45 FR 144 Thurs, July 24, 1980, p. 49465

The most definitive applicable standard is the 0.10 mg/l trihalomethane drinking water supply limit. The average of chloroform discharges would contribute to the Niagara River 0.000037 mg/l (0.037 ppb) or approximately 1/2800th of the limit. The maximum chloroform level would be equivalent to ppb or approximately 1/1000th of the drinking water standard. Chloroform levels in the river, when compared to the drinking water standard, should present no threat to human health. It also should be considered that the 50000 cfs Niagara River flow used in the calculation only exists from the upstream power intakes to the power plant discharges below the falls. There is substantially more dilution below the power plant discharges. In addition, the calculation assumes 100% of the discharge goes to the diversion sewer (i.e., no flow to the POTW) and there are no losses of organics due to volatilization. This is certainly conservative since both assumptions are not completely correct. Discharges to the POTW are 8-10% and losses due to volatilization of organics could be 20% or greater.

noted highest organic concentration in the The past year (trichloroethylene) would be equivalent to 0.55 ppb in the Niagara River. The USEPA water quality criteria listed 45,000 ppb as the appropriate level for protection of aquatic life. Similarly, for those other compounds for which the USEPA and the NYSDEC proposed water quality criteria.

	LEVEL IN	CENTRATION NIAGARA RIVER Part 700;NYCRR) (ppb)	USEPA WATER QUALITY CRITERIA FOR PROTECTION OF AQUATIC LIFE(ppb)	NYS PROPOSED WATER QUALITY STANDARDS (ppb)
1. Carl	oon Tetrachloride	0.061	32,200	5.0
2. Ch1	oroform	0.111	28,900	10
3. Dicl	nloroethenes	0.064	11,600	
4. Meti	nylene Chloride	0.045	11,000*	
5. 1,1	,2,2-Tetrachloroethane	e 0.077	9,320/2,400	
6. Tet	rachloroethene	0.538	5,280/840	
7. Tric	chloroethene	0.552	45,000	10
8. Ving	/l Chloride	0.029	NA	

Halomethanes would include some other compounds but not carbon tetrachloride or chloroform.

It can be concluded, therefore, that based on the EPA and NYSDEC Water Quality Criteria, there is no threat to aquatic life posed by the continued discharge of the compounds in question. In fact, the average well water concentration meets the USEPA water quality criteria for all but as pumped from the well with no river dilution.

As additional support for this conclusion, bioassays on the discharge streams and the raw well water have shown that the streams are not acutely toxic under 24-hour static bioassay conditions. Olin carried out tests on the streams in August 1981 (Appendix V) with fathead minnow (Pimephales promelas) as the test species. All of the minnows were alive at the end of the 24-hour test period. The NYSDEC carried out additional tests (Appendix V) in October 1981 with both fathead minnows and Daphnia magna. As with the Olin tests, there were no fatalities at the end of the 24-hour period.

# D. Combination with Domestic Waste

One concept for treatment to remove organics is to discharge all well water to the POTW. The Niagara Falls POTW is a physical/chemical facility which is equipped with activated carbon adsorption for the removal of organic compounds. The carbon beds are not expected to be operational until 1984. The Olin plant has a contractual discharge limit of 770,000 gpd to the city treatment facility. Current discharges average approximately 429,000 to 584,000 gpd leaving approximately 260,000 gpd available. Well water usage at full production ranges from 2.88-5.18 mgd.

An additional problem is that the POTW is already hydraulically overloaded. The plant was designed to process 48 mgd and is presently handling approximately 55 mgd. The excess hydraulic load is due to infiltration and excessive volume discharges by some participants. It is expected that when the POTW is fully operational and fully evaluated that an influent in excess of 48 mgd may be allowed. The timetable for such an upgrading is over two years away, however, leaving little possibility of raising the contractual limit. The treatability of the well water in the POTW activated carbon system has not been addressed.

# E. <u>Investigations of Treatment Methods</u>

Several observations are pertinent prior to any evaluation of specific treatment methods.

- 1. The well water contaminants are most concentrated at the source. The well water is distributed to two (2) plant sites and five (5) separate wastewater discharges. It is reasonable, therefore, to consider treatment only at the well head. Treatment at the discharge(s) is not practical. Costs for piping to segregate and return the well water to a common point for carbon treatment, have been estimated at \$760,000-1,064,000 (1980 dollars).
- 2. The usage of the well water is as cooling water. Any potential treatment method must maintain the water temperature as withdrawn from the ground. Methods such as steam stripping would be useless in processing cooling water.

Investigations of treatment methods and systems began with a literature search and a review of the accepted treatment methodologies for removal of organics from water. Six data bases were searched resulting in over 100 references. The literature search and review yielded six (6) accepted technologies for consideration. Specifically, these technologies were:

- 1. Steam stripping;
- 2. Oil-Water separation;
- Filtration (diatomaeous earth or dual media);
- 4. Biochemical oxidation;
- 5. Air stripping; and
- 6. Activated carbon adsorption Our investigative program concluded that carbon adsorption was the only technically feasible approach to treatment for this application. Detailed evaluations of activated carbon adsorption was carried out in several stages.
  - a) Theoretical Calculations - In 1980, the Olin Process Technology Group calculated the potential carbon usage and cost to reduce the organics to 15 ppb. A worst case assumption was made, i.e., 41 ppm organics in the well water supply, and an unreasonable carbon consumption figure of 530 tons/day resulted. An alternate calculation, with an objective of 98% removal of organics to approximately 100 ppb, resulted in a carbon replacement requirement of 5.30 tons/day with an estimated replacement cost of \$3.75-4.50 million per year (1980 dollars). Calculations were also carried out based on an assumed stabilized organic concentration of 2.0 ppm. This resulted in a carbon requirement of 26.5 tons/day to attain a 98% reduction in the organics levels. Carbon costs for the 98% reduction were estimated at \$2,000,000/year (1980 dollars). While this cost is substantially below the worst case estimates, it is still unreasonable economically.
  - b) Bench Scale Isotherm - Again in 1980, Calgon Corporation performed bench scale activated carbon isotherm studies on well water with approximately 2.0 ppm organics. Their results, based on total organic carbon (TOC) only, resulted in an estimated 0.4-1.6 tons of carbon consumption/day and a carbon replacement cost of \$450,000-600,000/(1980 dollars) year. This study reduced the TOC to a non-detectable level. The approved TOC analysis procedure is only recommended for levels greater than 1 mg/l. The isotherm study started with a sample level of 2 mg/l which was reduced to a non-detectable level. The total TOC level, however, is made up of eight specific compounds of interest which may be in the concentration of the low ppb range to several ppm (mg/l). The bench scale isotherm did not show the resultant (treated) levels of each compound nor did it truly show the resultant total organics level. The isotherm did show a technical potential for activated carbon adsorption treatment.

# F. Alternative Proposals

- 1. Mechanical Refrigeration Systems The process wells are an important and valuable resource as a constant temperature cooling water supply, and are essential to the operation of the Niagara Falls plant. However, an obvious alternative is to replace the wells with a mechanical refrigeration system and eliminate the discharge of organics. Olin Engineering reviewed this concept and estimated that appropriate mechanical equipment could be provided at a one-time capital cost of \$2.2 million with operating costs estimated at \$100,000/yr.
- 2. Selective Sealing - A potential method of reducing or eliminating the contamination from the withdrawn water is to partially seal the well shaft to exclude the contaminated groundwater. To be a viable consideration, the contaminated groundwater must be in a discrete and isolatable section and the remaining or unsealed portion of the draft must still produce sufficient water to be usable. Olin carried out tests on the wells which consisted of isolating successive sections of the well shaft and chemically characterizing the water pumped from each section. Briefly, results showed very little contamination in the south well with the north well pumping and relative by high contamination in the north well with the south well pumping. It has been calculated that a packer installed in the north well at the 50 foot level will reduce the organics concentration in the withdrawn water by 25-50% and available potential flow would reduce 10-20%. A temporary packer could be installed at the 50 foot level to test the Conditions could develop which would decrease the gain conclusion. from packer installation. Continued pumping could result in a drawing up the contaminated water to a higher level above the packer.

### G. Conclusions - 1980

1. Treatment (Activated Carbon Adsorption) - High capital cost, extremely high operating cost and questionable effectiveness and need.

A comparison of the estimated treatabilities with the concentrations actually found in the well water (for those compounds which coincide) reveals that only eight compounds would be expected to be reduced from their maximum concentration and five compounds would be reduced from their average concentrations. Actual pilot tests on well water could provide solid data, compound by compound.

2. <u>Mechanical Refrigeration</u> - High capital cost, high effectiveness, but questionable need.

Mechanical refrigeration is a proven, standard technology and discontinuing well usage would be 100% effective in preventing discharge of organic contamination to surface water. Continued pumping of the wells has the advantage in retarding or preventing the natural groundwater aquifer movement towards the Lower Niagara Gorge, it is minimizing the areal distribution of the contamination. In time, the contamination should be reduced or cleared completely, particularly if surficial sources are eliminated.

Loure

3. Reduce Well Water Demand to One Well Only - High capital cost, effective but questionable need.

A review of potential areas where the demand for well water could be reduced was undertaken. It was determined that the plant presently has the capability to operate at the full load with one well for 8-9 months of the year. Complete elimination of one well can only be accomplished with an as yet undefined reduction of plant production capacity during the summer months.

4. <u>Maintain Well Water Usage at Two Wells Year-Round</u> - Reasonable cost, and effective.

It can be seen from the data that consistency in organic concentration is maintained with either one or two wells. Slugs of organic concentrations can develop when a second well is activated after a period of shutdown.

It is believed that continuous two-well operation would contribute a lower mass of organics if the operation is allowed to stabilize. The effect of continuous pumping will be monitored over the next few months to confirm this concept. Two-well operation would expedite flushing of the aquifer.

Re-examination of the true conditions reveals that the existing situation is not as serious as is indicated by a superficial examination of the data. The organic concentrations are in the ppb/ppm ranges.

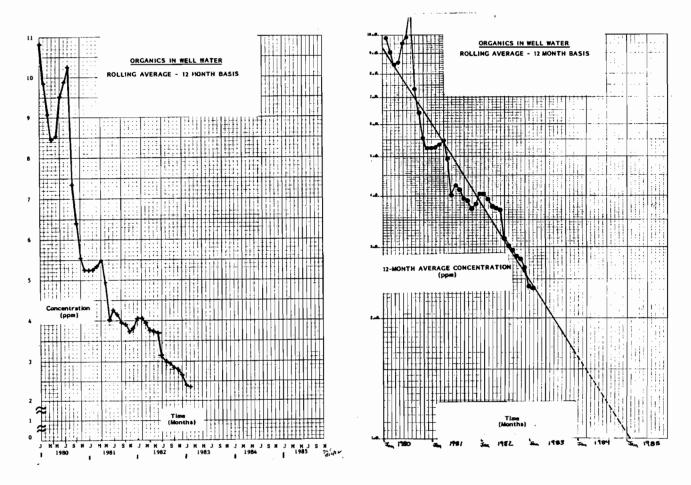
Levels of the various contaminants found in well water will not exceed any of the numerical standards listed when discharged into the Niagara The ambient river levels would not be sufficient to cause taste, odor or color problems or be injurious to aquatic life. It can also be seen in a review of the data that there is a trend toward lower concentrations during two-pump operations. It would seem reasonable that since the disposal operations which caused the problem have ceased, that the contaminant concentrations would have to continue to reduce over a period of time. Further, since remedial operations on the waste disposal areas presumed to be affecting the well water contaminant levels will be carried out, the reduction in concentrations should be accentuated. In approximately 8-10% of the well water flow is discharged to the POTW and by 1981, will be processed through an activated carbon system which will further reduce the organic loading on the Niagara River.

# H. Abatement Plans

In view of the 1980 conclusions above, Olin proposed to continue monitoring the well water supply on a monthly basis (VOA analyses) and perform a complete organic characterization on a semi-annual basis. These analyses were summarized and reported quarterly.

Continued pumping of the wells at the lower concentrations coupled with the remedial surficial action will result in flushing of the aquifer and a return in time to an uncontaminated state. If pumping is not continued, natural groundwater flow will carry the organics to the Lower Niagara Gorge where they would enter the river anyway. The DEC concurred with the continuous plan as noted in a comment letter dated March 16, 1981 (Appendix III).

The concept of continuous pumping has proven the theory of continued reductions in organics concentration. As shown in the figures below, the 12-month rolling average has dropped from 11.8 ppm in 1980 (based on very few analyses) to 2.4 ppm in February 1983 (based on approximately 52 samplings).



Olin continues to believe that continued pumping and completion of surficial remedial actions at contributing non-Olin hazardous waste disposal sites was and is the appropriate abatement plan. Several events of the past three years affect that belief, however, the events are beyond Olin's control and require that additional abatement efforts be carried out.

### IV. DESIGN CRITERIA - JULY 1, 1984 OBJECTIVES

# A. Receiving Water

Several events in 1981 served to focus additional attention on the Niagara River and the municipal and industrial discharges to the River. The intense public interest resulted in the establishment of policies and imposition of standards which were politically and sociologically based and have little or no scientific or technical basis and have no basis in law or regulation. The policies regarding ambient river water quality standards, mixing zones, and discharge allocations were first developed in the preparation of the SPDES discharge permit for the City of Niagara Falls POTW. Those policies and standards have been applied to other industrial dischargers even though some have been legally challenged and have not yet been established as valid criteria for setting SPDES permit limitations. Notable among these are:

- 1) Inappropriate legal and factual bases upon which effluent limitations have been set.
- 2) Failure to account for sampling, analytical and operating variability of laboratory analyses.
- 3) Using water quality criteria which are inappropriate for developing permit limits.
- 4) Relying on unpublished rules and regulations.
- 5) Reliance on data which was not available to the public.

The SPDES permit issued to Olin Corporation and effective March 1, 1983 utilized the above policies and standards in developing the effluent limitation of 10 lb/day of total organics. A successful legal challenge to the policies may result in a re-evaluation and reissuance of the Olin permit, however, the current requirement is 10 lb/day total organics. While the organics concentration in well water has been shown to be dropping, it appears, based on extrapolation of historical data, that natural reductions by mid-1984 will not be sufficient to meet the new permit requirement (i.e., at 4.46 mgd two-well output; concentration limited to 269 ppb and at 3 mgd one-well output; concentration limited to 400 ppb). It is apparent, therefore, that the original concepts of well water replacement through mechanical refrigeration or activated carbon must be reconsidered.

In early 1982, Calgon Corporation was engaged to carry out a feasibility study activated carbon adsorption treatment of well water to reduce the organics concentrations. The initial aspect of the Calgon work was a "mini-column" or Accelerated Column Test (ACT). The results of this study have been previously reported to the DEC $^2$ . Conclusions of the ACT test were as follows:

Petition for Public Hearing, November 3, 1982.

Letter to G. Pallante, NYSDEC; April 26, 1982; and letter to W. Loveridge, NYSDEC, March 6, 1982.

- 1. A discharge limit of 0.010 ppm for each Volatile Organic Compound (including methylene chloride) is not practical physically or economically. [1.45 truckloads of carbon per day; \$7,145,000/yr. in carbon costs]. Carbon treatment is not a viable option with such effluent limitations.
- 2. A discharge limit of 0.050 ppm for each compound is also totally infeasible. When methylene chloride breaks through the concentration rapidly rises to >0.060 ppm. Carbon regeneration rate and costs are approximately the same as for a 0.010 ppm limit.
- 3. An average discharge limit of 0.300 ppm total halogenated organics (THO) approaches more reasonable physical and economical consideration. [One truckload/5.7 days; \$862,000/yr]. Chloroform can be 1.5 to 2.0 times the 0.300 ppm test level at times and chloroform breakthrough can be closer to 0.500 ppm THO than 0.300 ppm THO.
- 4. A discharge limit of 0.500 ppm makes carbon adsorption somewhat more reasonable option for consideration. [One truckload carbon/8.3 days; \$591,000/yr carbon cost]. A discharge concentration of 0.500 ppm would be equivalent to 20.8 lb/day with two-well operation. Effluent concentrations are difficult to predict at this point particularly with the proposed start/stop method of operation. We would expect that with a 0.500 ppm THO limit, methylene chloride (0.042 ppm average when present) and chloroform (0.400 ppm average) would be discharged at their influent concentrations. Effluent could also contain small amounts of dichloroethylene, vinyl chloride, 1,1,1-Trichloroethane and carbon tetrachloride. All other compounds detected in well water should be retained on the bed at nearly 100% efficiency.

The ACT test was sufficiently encouraging to consider a field pilot study. Calgon Corporation provided the equipment and guidance for the study while Olin carried out the test. Test data was evaluated by Calgon and summarized in their report dated March 29, 1983 (Appendix IV). The pilot column study verified that a 10-minute contact time was sufficient to contain the mass of priority pollutant organics below a total discharge limit of 10 pounds per day at a well water flow rate of 5 mgd. With 6 adsorbers operating in parallel and a 7 day staggered start-up of each adsorber, 52 truckloads (1,040,000 pounds of activated carbon) would be required to treat 5 mgd per year. A proportionally lower carbon usage rate is required at lower flow rates.

Meeting the 10 lbs. organics/day effluent limitation via activated carbon will be extremely expensive. Operating cost for the 5 mgd/6 adsorber/52 truckload situation was projected at \$688,000 per year for carbon regeneration and service charges. Capital costs for a facility to house the equipment had been previously estimated in the range of \$570,000-870,000.

# B. Abatement Plans - 1983

Several aspects of the contaminated well water supply problem are unresolved to date. These are:

- a) Effect of the actual packer (selective sealing) and net reduction in organics levels attainable. Test results are very promising.
- b) Status of the temporary shutdown of the HTH® manufacturing facility and the degree of water treatment capability to be provided at this time.
- c) The effect of the recently discovered groundwater contamination on adjoining property.
- d) The degree of continued overall reductions in organics concentration through the next 15 months.

My / Paris

With the above points in mind:

- Olin will pursue installation of a temporary packer in the south well. It is presently estimated that this will reduce the organics contamination from the well water supply by 25-50%. As such, we expect the level of contamination to be approximately 1.2 ppm (based on a 12-month rolling average). At 1.2 ppm, 5 mgd would produce approximately 50 lbs. of organics/day. Reduction in well water consumption to 3.0 mgd would result in an organics load of 30 lbs/day.
- 2) Olin will continue to pump two wells with continued weekly monitoring of VOA concentrations. Monitoring will show any continued overall reductions in well water concentrations, the effect of the packer and the permanence of those effects (i.e., water from the deeper aquifer may be drawn up to the higher levels and/or the south well may pick up contamination and show a rise in organics level).
- Olin will implement a well water replacement project, i.e., cooling for the Frick Ammonia Compressors used in the liquification of chlorine. Currently, these compressors utilize recycled river water in winter and well water during the summer. A closed-loop cooling water system (cooling tower) will be installed to replace the river/well water system and will eliminate the consumption of approximately 0.7 mgd of well water.
- 4) Olin will continue to investigate an activated carbon adsorption system which will maintain net total organic discharge levels at ≤10 lbs/day. Currently, installation of six adsorbers to treat up to 5 mgd is envisioned. However, Olin is considering the four points noted above and may design a carbon adsorption system for a lower flow and/or lower organics concentration. Operation of the carbon adsorption system will be varied from 100% treatment to a fractional treatment/bypass system to maintain the ≤10 lbs/day discharge limitation as the concentration in the well water decreases.

We have the ability to utilize carbon adsorption equipment presently existing at another Olin facility. Design and construction would involve site preparation (maximum 3,750 ft²) and piping. We do not expect the design problems which could exist with a new facility or the delivery problems which might be expected with newly manufactured equipment. Consequently, we do not require the amount of time for these phases of the project as might typically be expected. We will also continue to investigate mechanical refrigeration for well water replacement and other options. We believe the projects necessary to meet the  $\leq 10$  lb/day limitation can be completed by the required July 1, 1984 date.

# REFERENCES

- Black, Hayse H., <u>Planning Industrial Waste Treatment</u>, NYS Department of Health, Division of <u>Pure Waters</u>, New York, 1968.
- Codes, Rules and Regulations of the State of New York, Chapter X, Title 6, Parts 700, 701 and 702.
- Considine, Douglas M. (Ed.); Chemical Process Technology Encyclopedia, New York, 1974, pp. 273-279.
- Cummings, D. L. and R. B. Dow; <u>Engineering Report Contaminated Well Water Supply</u>, October 2, 1980.
- Federal Register, Volume 40, Number 141, December 24, 1975 as amended through March 11, 1980.
- Federal Register, Volume 48, Number 55, March 21, 1983.
- Federal Register, Volume 45, Number 231, November 28, 1980.
- Johnston, Richard H., <u>Groundwater in the Niagara Falls Area, New York</u>, State of New York Conservation Department, Water Resources Commission, Bulletin GW-53, 1964.
- McKee, J. E. and H. W. Holf, (Eds.), <u>Water Quality Criteria</u>, State Water Control Board, State of California, Pub. 3-A, 1963, 94-8.
- New York State Sanitary Code, Chapter I, Part 5.
- Petition for Public Hearing, State Discharge Elimination System (SPDES) Permit NY0026336, November 3, 1982.
- "Pollutant Treatability: A Molecular Engineering Approach", Environmental Science and Technology, Volume 14, Number 1 (January, 1980), pp. 28-31.
- Quality Criteria for Water, USEPA (EPA-440/9-76-023) Washington, D.C., July 1976.
- Strier, Murray P., Treatability of Organic Priority Pollutants Part C Their Estimated (30 day average) Treated Effluent Concentrations By Means of a Molecular Engineering Approach, Office of Quality Review, Effluent Guidelines Division, USEPA, June, 1978.

# APPENDIX I

# APPLICABLE WATER QUALITY STANDARDS

- 1. NYS Classifications and Standards of Purity, Part 700, 701 and 702.
- 2. USEPA National Primary Drinking Water Standards, Part 141.
- 3. NYS Drinking Water Supplies, Part 5.
- 4. USEPA Water Quality Criteria, 45 FR 231, Friday, November 28, 1980, Selected Sections.
- 5. NYS Proposed Amendments to Parts 701 and 702.
- 6. Great Lakes Water Quality Agreement as amended in 1978, Selected Sections.

### PART 700 CHAPTER X OF TITLE 6

### OF THE STATE OF NEW YORK

### Section 700.1 Collection of Samples.

In making any tests of analytical determinations to determine compliance or non-compliance of sewage, industrial wastes or other waste discharges with established standards, samples shall be collected in such manner and at such locations as are approved by the commissioner. In approving such locations the commissioner shall be guided by the fact that:

- (a) there must be prompt mixing of the discharge with the receiving waters;
- (b) that the mixing will not interfere with biological communities to a degree which is damaging to the eco-system;
- (c) that the mixing will not diminish other beneficial uses disproportionately.

### PART 701

# CODES, RULES AND REGULATIONS OF THE STATE OF NEW YORK CLASSIFICATIONS AND STANDARDS OF QUALITY AND PURITY

701.2 Conditions applying to all classifications and standards. (a) In any case where the waters into which sewage, industrial wastes or other wastes effluents discharge are assigned a different classification than the waters into which such receiving waters flow, the standards applicable to the waters which receive such sewage or wastes effluents shall be supplemented by the following: "The quality of any waters receiving sewage, industrial wastes or other wastes discharges shall be such that no impairment to the best usage of waters in any other class shall occur by reason of such sewage, industrial wastes or other wastes discharges."

701.4 Classes and standards for fresh surface waters. The following items and specifications shall be the standards applicable to all New York fresh waters which are assigned the classification of AA, A, B, C, or D, in addition to the specific standards which are found in this section under the heading of each such classification.

### QUALITY STANDARDS FOR FRESH SURFACE WATERS

### <u>ITEMS</u> <u>SPECIFICATIONS</u>

- 1. Turbidity
- 2. Color
- 3. Suspended, colloidal or settleable solids.
- 4. Oil and floating substances.
- 5. Taste and odor-producing substances, toxic wastes and deleterious substances.
- 6. Thermal discharges.

- No increase except from natural souces that will cause a substantial visible contrast to natural conditions. In cases of naturally turbid waters, the contrast will be due to increased turbidity.
- None from man-made sources that will be detrimental to anticipated best usage of waters.
- None from sewage, industrial wastes of other wastes which will cause deposition or be deleterious for any best usage determined for the specific waters which are assigned to each class.
- No residue attributable to sewage, industrial wastes or other wastes nor visible oil film nor globules of grease.

None in amounts that will be injurious to fishlife or which in any manner shall adversely affect the flavor, color or odor thereof, or impair the waters for any best usage as determined for the specific waters which are assigned to each class.

(See Part 704 of this title).

### FART 702 SPECIAL CLASSIFICATIONS AND STANDARDS

Section 702.1 Class A - Special (International Boundary Waters).

(GREAT LAKES WATER QUALITY AGREEMENT OF 1972)

Best Usage of Waters. Source of water supply for drinking, culinary or food processing purposes, primary contact recreation and any other usages.

Conditions Related to Best Usage. The waters, if subjected to approved treatment, equal to coagulation, sedimentation, filtration and disinfection with additional treatment, if necessary, to reduce naturally present impurities, meet or will meet New York State Department of Health drinking water standards and are or will be considered safe and satisfactory for drinking water purposes.

### QUALITY STANDARDS FOR CLASS A-SPECIAL WATERS

(INTERNATIONAL BOUNDARY WATERS) ITEMS SPECIFICATIONS 1. Coliform The geometric mean of not less than five samples taken over not more than a thirty-day period should not exceed 1,000 per 100 ml total coliform nor 200 per 100 ml fecal coliform. 2. Dissolved Oxygen In the rivers and upper waters of the lakes not less than 6.0 mg/l at any time. In hypolimnetic waters, it should be not less than necessary for the support of fishlife, particularly cold water species. 3. Total Dissolved Solids Should not exceed 200 milligrams per liter. 4. pH Should not be outside the range of 6.7 to 8.5. 5. Iron Should not exceed 0.3 milligrams per liter as Fe. 6. Phosphorus Concentrations should be limited to the extent necessary to prevent nuisance growths of algae, weeds and slimes that are or may become injurious to any beneficial water use. 7. Radioactivity Should be kept at the lowest practicable levels and in any event should be controlled to the extent necessary to prevent harmful effects on health. 8. Taste and odor-producing None in amounts that will interfere with use

substances, toxic wastes and

deleterious substances

for primary contact recreation or that will be injurious to the growth and propagation of fish, or which in any manner shall adversely affect the flavor, color or odor thereof or impair the waters for any other best usage as determined for the specific waters which are assigned to this class.

Suspended, colloidal or settleable solids None from sewage, industrial wastes or other wastes which will cause deposition or be deleterious for any best usage determined for the specific waters which are assigned to this class.

10. Oil and floating substances

No residue attributable to sewage, industrial wastes or other wastes nor visible oil film nor globules of grease.

11. Thermal Discharges

(See Part 704 of this title).

To meet water quality objectives referred to in the "Great Lakes Water Quality Agreement of 1972," the standards listed above shall be subject to revision from time to time after further hearings on due notice.

NOTE: With reference to certain toxic substances affecting fishlife, the establishment of any single numerical standard for waters of New York State would be too restrictive. There are many waters, which because of poor buffering capacity and composition will require special study to determine safe concentrations of toxic substances. However, most of the non-trout waters near industrial areas in this State will have an alkalinity of 80 milligrams per liter or above. Without considering increased or decreased toxicity from possible combinations, the following may be considered as safe stream concentrations for certain substances to comply with the above standard for this type of water. Waters of lower alkalinity must be specifically considered since the toxic effect of most pollutants will be greatly increased.

Ammonia or Ammonium Compounds

Not greater than 2.0 milligrams per liter expressed as NH, at pH of 8.0 or above.

### TITLE 40, PART 141

### CODE OF FEDERAL REGULATIONS

### 141.2 Maximum contaminant levels for organic chemicals.

(141.12 revised by 44 FR 68641, November 29, 1979).

The following are the maximum contaminant levels for organic chemicals. The maximum contaminant levels for organic chemicals in paragraphs (a) and (b) of this section apply to all community water systems. Compliance with the maximum contaminant levels in paragraphs (a) and (b) is calculated pursuant to  $\S$  141.24. The maximum contaminant level for total trihalomethanes in paragraph (c) of this section applies only to community water systems which serve a population of 10,000 or more individuals and which add a disinfectant (oxidant) to the water in any part of the drinking water treatment process. Compliance with the maximum contaminant level for total trihalomethanes is calculated pursuant to  $\S$  141.30.

		LEVEL mg/1
(a)	Chlorinated hydrocarbons:	
	Endrin - (1,2,3,4,10,10-hexachloro-6,7-epoxy-1,4,4a,5,6,7,8,8a-octa-hydro-1,4,endo, endo-5,8 - dimethane naphthalene).	0.0002
	Lindane - (1,2,3,4,5,6-hexachloro-cyclohexane, gamma isomer).	0.004
	Methoxychlor - (1,1,1-Trichloro-2,2-bis(p-methoxyphenyl) ethane).	0.1
	Toxaphene - $(C_{10}H_{10}Cl_8$ -Technical chlorinated camphene, 67-79 percent chlorine.	0.005
(b)	Chlorophenoxys:	
	2,4-D, (2,4-Dichlorophenoxyacetic acid).	0.1
	2,4,5-TP Silvex (2,4,5-Trichloro-phenoxypropionic acid).	0.01

(c) Total trihalomethanes (the sum of the concentrations of bromodichloromethane, dibromochloromethane, tribromomethane (bromoform) and trichloromethane (chloroform)) 0.10 mg/1.

### CHAPTER I, PART 5

### NEW YORK STATE SANITARY CODE

### Part 5 - 1.52 Organic Chemicals.

Maximum contaminant levels; sampling and analytical requirements; notification (a) the following maximum contaminant levels.

# ORGANIC CHEMICAL (1) Chlorinated hydrocarbons: MAXIMUM CONTAMINANT LEVEL (milligrams per liter)

	Endrin (1,2,3,4,10,hexachloro- 6,7-epoxy-1,4,4a,5,6,7,8,8a-octa- hydro-1,4-3ndo, endo-5,8-dimethano		
	naphthalene	•	0.0002
	Lindane (1,2,3,4,5,6-hexachloro-cyclohexane, gamma isomer)		0.004
	Methoxychlor (1,1,1-Trichloro-2,2-bis p-methoxyphenyl ethane)	•	0.1
	Toxaphene (C <sub>10</sub> H <sub>10</sub> Cl <sub>8</sub> - Technical chlorinated camphene, 67-68 percent chlorine		0.005
(2)	Chlorophenoxys:		
	2,4-D (2,4-Dichloropheoxyacetic acid)	•	0.1
	2,4,5-TP Silvex (2,4,5-Trichloro-phenoxypropionic acid)		0.001

### Carbon Tetrachloride

### Freshwater Aquatic Life

The available date for carbon tetrachloride indicate that acute toxicity to freshwater aquatic life occurs at concentrations as low as 35,200 µg/l and would occur at lower concentrations among species that are more sensitive than those tested. No data are available concerning the chronic toxicity of carbon tetrachloride to sensitive freshwater aquatic life.

### Saltwater Aquatic Life

The available data for carbon tetrachloride indicate that acute toxicity to saltwater aquatic life occurs at concentrations as low as 50,000 µg/l and would occur at lower concentrations among species that are more sensitive that those tested. No data are available concerning the chronic toxicity of carbon tetrachloride to sensitive saltwater aquatic life.

### Chlorinated Ethanes

### Freshwater Aquatic Life

The available freshwater data for chlorinated ethanes indicate that toxicity increases greatly with increasing chlorination, and that acute toxicity occurs at concentrations as low as 118,000 µg/l for 1,2-dichloroethane 18.000 μg/l for two trichloroethanes. 9,320 µg/l for two tetrachloroethanes. 7.240 µg/l for pentachloroethane, and 980 µg/l for hexachloroethane. Chronic toxicity occurs at concentrations as low as 20,000 µg/l for 1,2-dichloroethane, 9,400 p.g/l for 1,1,2-trichloroethane, 2,400 µg/l for 1,1,2,2,-tetrachloroethane, 1,100  $\mu$ g/l for pentachloroethane, and 540  $\mu$ g/l for hexachloroethane. Acute and chronic toxicity would occur at lower concentrations among species that are more sensitive than those tested.

### Saltwater Aquatic Life

The available saltwater data for chlorinated ethanes indicate that loxicity increases greatly with increasing chlorination and that acute toxicity to fish and invertebrate species occurs at concentrations as low as 113,000 µg/l for 1,2-dichloroethane. 31,200 µg/l for 1,1,1-trichloroethane, 9,020 µg/l for 1,1,2,2-tetrachloroethane, 390 µg/l for pentachloroethane, and 940 μg/l for hexachloroethane. Chronic toxicity occurs at concentrations as low as 281 µg/l for pentachloroethane. Acute and chronic toxicity would occur at lower concentrations among species that are more sensitive than those tested.

### Chloroform

### Freshwater Aquatic Life

The available data for choloroform indicate that acute toxicity to freshwater aquatic life occurs at concentrations as low as 28,900 µg/l, and would occur at lower concentrations among species that are more sensitive than the three tested species. Twenty-seven-day LC50 values indicate that chronic toxicity occurs at concentrations as low as 1,240 µg/l, and could occur at lower concentrations among species or other life stages that are more sensitive than the earliest life cycle stage of the rainbow frout.

### Saltwaler Aquatic Life

The data base for saltwater species is limited to one test and no stafement can be made concerning acute or chronic toxicity.

### Dichloroethylenes

### Freshwater Aquatic Life

The available data for dichloroethylenes indicate that acute toxicity to freshwater aquatic life occurs at concentrations as low as 11.600 µg/l and would occur at lower concentrations among species that are more sensitive than those tested. No definitive data are available concerning the chronic toxicity of dichlorethylenes to sensitive freshwater aquatic life.

### Saltwater Aquatic Life

The available data for dichlorethylenes indicate that acute toxicity to saltwater aquatic life occurs at concentrations as low as 224,000 µg/l and would occur at lower concentrations among species that are more sensitive than those tested. No data are available concerning the chronic toxicity dichloroethylenes to sensitive saltwater aquatic life.

#### Halomethanes

### Freshwater Aquatic Life

The available data for halomethanes indicate that acute toxicity to freshwate aquatic life occurs at concentrations as low as 11,000 µg/l and would occur at lower concentrations among species that are more sensitive than those tested. No data are available concerning the chronic toxicity of halomethanes to sensitive freshwater aquatic life.

### Saltwater Aquatic Life

The available data for halomethenes indicate that acute and chronic toxicity to saltwater aquatic life occur at concentrations as low as 12,000 and 6,400 µg/l, respectively, and would occur at lower concentrations among species that are more sensitive than those tested. A decrease in algal cell numbers occurs at concentrations as low as 11.500 µg/l.

### Tetrachloroethylene

### Freshwater Aquatic Life

The available data for tetrachloroethylene indicate that acute and chronic toxicity to freshwater aquatic life occur at concentrations as low as 5,280 and 840 µg/l, respectively, and would occur at lower concentrations among species that are more sensitive than those tested.

### Saltwater Aquatic Life

The available data for tetrachloroethylene indicate that acute and chronic toxicity to saltwater aquatic life occur at concentrations low as 10,200 and 450 µg/l, respectively, and would occur at lower concentrations among species that are more sensitive than those tested.

#### Vinyl Chloride

### Freshwater Aquatic Life

No freshwater organisms have been tested with vinyl chloride and no statement can be made concerning acute or chronic toxicity.

### Saltwater Aquatic Life

No saltwater organisms have been tested with vinyl chloride and no statement can be made concerning acute or chronic toxicity.

### Human Health

For the maximum protection of human health from the potential carcinogenic effects due to exposure of vinyl chloride , through ingestion of contaminated water and contaminated aquatic organisms. the ambient water concentration should be zero based on the non-threshold assumption for this chemical. However, zero level may not be attainable at the present time. Therefore, the levels which may result in incremental increase of cancer risk over the lifetime are estimated at 10-5, 10-6, and 10-7. The corresponding criteria are 20 µg/l, 2.0  $\mu$ g/l, and .2  $\mu$ g/l, respectively. If the above estimates are made for consumption of aquatic organisms only. excluding consumption of water, the levels are 5,246  $\mu$ g/l, 525  $\mu$ g/l, and 52.5 μg/l, respectively. Other concentrations representing different risk levels may be calculated by use of the Guidelines. The risk estimate range is presented for information purposes and does not represent an Agency judgment on an "acceptable" risk level.

# EXCERPTS FROM THE GREAT LAKES WATER QUALITY AGREEMENT OF 1978

### ARTICLE II

### **PURPOSE**

Consistent with the provisions of this Agreement, it is the policy of the Parties that:

(a) The <u>discharge of toxic substances in toxic amounts</u> be prohibited and the <u>discharge</u> of any or all persistent toxic substances be virtually eliminated;

### ARTICLE VI

### PROGRAMS AND OTHER MEASURES

- 1. (b) Pollution from Industrial Sources. Programs for the abatement, control and prevention of pollution from industrial sources entering the Great Lakes System. These programs shall be completed and in operation as soon as practicable and in any case no later than December 31, 1983, and shall include:
  - (i) Establishment of waste treatment or control requirements expressed as effluent limitations (concentrations and/or loading limits for specific pollutants where possible) for all industrial plants, including power generating facilities, to provide levels of treatment or reduction or elimination of inputs of substances and effects consistent with the achievement of the General and Specific Objectives and other control requirements, taking into account the effects of waste from other sources;
  - (ii) Requirements for the substantial elimination of discharges into the Great Lakes System of persistent toxic substances;

### ANNEX 1

### SPECIFIC OBJECTIVES

### I. CHEMICAL

### A. Persistent Toxic Substances

- 1. Organic
  - (a) Pesticides

### Lindane

The concentration of lindane in water should not exceed 0.01 microgram per litre for the protection of aquatic life. The concentration

### Unspecified Organic Compounds

For other organic contaminants, for which Specific Objectives have not been defined, but which can be demonstrated to be persistent and are likely to be toxic, the concentrations of such compounds in water or aquatic organisms should be substantially absent, i.e., less than detection levels as determined by the best scientific methodology available.

### B. <u>Non-Persistent Toxic Substances</u>

- 1. Organic Substances
  - (b) Other Substances

<u>Unspecified Non-Persistent Toxic Substances and Complex Effluents</u>

Unspecified non-persistent toxic substances and complex effluents of municipal, industrial or other origin should not be present in concentrations which exceed 0.05 of the median lethal concentration in a 96-hour test for any sensitive local species to protect aquatic life.

(c) Substances entering the water as the result of human activity that cause tainting of edible aquatic organisms should not be present in concentrations which will lower the acceptability of these organisms as determined by organoleptic tests.

### APPENDIX II

### ANALYTICAL DATA

When reviewing the following analytical data, the follow points must be kept in mind:

- 1. The first three (3) samples (11/1/78; 3/5/79; 5/27/79) were characterized completely. That is, each MS response was identified within the limits of the instrumentation.
- 2. The majority of the analyses are VOA or Volatile Organics Analysis, only. Consequently, some of the high boiling compounds such as flourene would not be detected.
- 3. Analyses from 1/9/80, 1/17/80, 2/12/80, and 3/12/80 were analyzed by two (2) laboratories. Data from the second laboratory is shown in parentheses. If two numbers do not appear for a given compound, that compound was not detected by one laboratory.
- 4. Samples from 4/15-17/80, 3/12/80 and 6/12/80 were performed by a third laboratory and included the USEPA list of 129 priority pollutants only. Samples from 4/15-17/80 and 3/12/80 were 72-hour composite samples.

TABLE I SCHMARY OF GROADIC ADALYSES ON VARIOUS SAMPLES (ppb)

-	11/1/78 WELL (Ipump)	3/5/79 WELL (1; ump)	WOLL	6/27/79 WELL (2pum.ps)	8/13/79 WELL (2pcmps)	WELL		10/31/79 WHLL eg/Zsaaple		(4) 9/80 (5) 1 WELLS (/2450ples).	1/17/50 (6) WELL (Ipump)	2/12/30 WELL (1; .mp)	3/12/80 WELL (1; ump)
COMPOUND				VOA	VOA	VOA	N	VЛA S	N	s	VOA S	VOA S	VOA N
*FHC(Hexachlerocyclohexane)		-	-	_	-			-		21) 0.7(1.2			-
** rbon Tetrachloride	33 426	19 191	12.8 174	225	98	22	15	54	41	45 140	65(4.3) 188	25(13)	20(17)
* loroform *butylphthalate	• x	0.6	-	362	276	103	165	102	365 0.2	0.2	100	281	97 (30 <b>0)</b>
*Dichloroethones	103	196	161	-	351.2	120	148	112	404	203	189 1	54.45(110)	145(113)
* 'ethylphthalate	x 1.7	x x	:	:	-	-	-	-	0.04	-	-	-	-
octyladipare *octylphthalate	1.2	_	-	-	-	-	<u>-</u>	-	:	-	-	-	:
*Fluoranthene	x	×	0.1	-	-	-	-	-	1	0.1	-	-	-
*Hexachloro-1,3-butadiene	8.1	-	×	-	-	-	-	-	14(-)	16(11	.) -	-	-
xachlorobutene	x 29,6	13.8	10.8	-	_	-	-	-	-	-		-	
xachloroethane rethylene Chloride	111	13.8	10.8	- 46	64	0.3	_ 12	~ по	8(x) 238	9(12 82	5) <b>-</b> 670	- 68	14(7.4)
*!!anochlorobenzene	×	-	-	1.5	1.4	-	2	2	0.9	0.1	0.2	-	0.5
Pentachlorobutadiene	13.4	-	x	-	-	-	-	-	-	-	-	-	-
entachlorobutene	×	-	-	-	-	-	-	-	-	-	-	-	-
Pontachloroethane	8.6 *	-	:	× -	-	-	-	-	4	2	-	•	-
*Phenathrene/Anthracene Phenylnaphthalene	x	-	-	-	-	-	-	-	-	-	-	-	-
yrene	×	x	0.1	-	-	-	-	-	2	0.3	-	-	-
Tetrachlorobutadiene	22.2		x	-				-		-	-	-	
*1,1,2,2-Tatrachloroethane *Tetrachloroethene	* 1147	37 6 <b>92</b>	410	268 <b>87</b> 7 <b>333</b>	10376 2535	5 <b>820</b> 6010	63 <b>73</b> 1 <b>287</b>	1134 1442	991	540	775/200\	-	-
oluene	x	-	1.8	0.9	0.3	-	-	-	991	340	375(280)	785(700)	877 (1000)
richlorobenzene	1.5		0.8		-		-		4	3	-	-	-
*1,1,1-Trichloroethane	7.5	0.5	1.2	17	11	-	4	\ <b>T</b>	.,				
,1,2-Trichloroethane	53	×	1.2	inter	8	-	-	М <b>D</b> —	11 3	2 1	-	5.3 1.4	(4.2)
,1,2-Trichloroethene	1164	431 0.3	464 0.6	6290	1616	3130	1403	2	1283	411	570(230)		732 (810)
Benzenedicarbexcylic Acid	-	*	-	11 -	-	-	- -	ND -	3 . -	0.6	2.5	2.0	0.2(3)
yclohexenol	-	×								_			
ichlorocyclohexane iisoctylphthalate	-	. *	-	-	-	-	-	-	-	-	<b>4</b> 1	-	-
Ethylphenol	-	5.9 *	-	-	-	-	-	-	0.6	0.3	<u>.</u>	_	
Heptanoic Acid	-	x	-	-	-	-	-	-	-	-	2 .	- '	-
examoic Acid	-	×	•							_	· ·		·
Tethylphenol *Phenol	-	x	-	-	-	-	-	<u>.</u> .	-	_	-	-	•
*2,4,6-Trichlorophenol		0.01 0.01	0.001	-	-	-	-	-	0.04	0.03	- '	-	-
imethoxymethane	-	-	x	-	-	-	-	-	-	-	-	-	- '
Methanol	(3)	(3)	485	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(2)	(5)	/3>
Acetone 1,1,1,2-Tetrachloroethane	-	-	-	×	-	-	-	-	(3)	(3)	(3)	(3)	( <u>\$</u> )
thylberzene	-	-	-	× –	-	-	-	<u> </u>	-	-	-	-	-
ichlorobenzenes	-	-	-	-	•	-	<b>Т</b>	0.4	1.2	0.21	-	-	-
Fluorene	-	-		-	_	-		-	0.4	0,08	-		
Hexachlorobenzene aphthalene	-	-	-	-	-	-	-	-	1	-	_	_	-
ichioroothane	-	-	-	-	-	-	-	-	0.1	-	, <del>-</del> ,	-	- '
hloroethane	-	-	-	-	-	-	-	-	-	:	1.1	0.15	-
Vinyl Chloride	-	-	-	-	-	-	-	-		<u>-</u>	•		(30)
-	3131.6 16	06 12 13	22 /25	-									
COP 5		06.12 17 96.3%	97.7%	173.4 99.9%	98.7 <b>%</b>	15209.3 99.8%	6101.7 A	BRATOV	2416.85	Average	2060.8 96.71	1950.30 98.22	1985.7 99.2%

OLC/cjb 4/3/80

2000 - 100 - 100 - 20,330

FUUTNOTES

\* Priority Pollutant

- Not Identified

x Identified But Not Quantified

(1) Sample from 6/27/79 through 10/31/79 analyzed for volatile components only.

(2) Presence of both Phthalates and Adipates is at least partially due to contamination in analysis.

(3) Procedure used would not detect methanol.

(4) Procedure identified priority pollutants only, specific VOA sample not collected.

(5) Numbers in parentheses indicated second source laboratory data, duplicate samples. (6) Converted to 1 well on the sample day.

## SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

COMPOUND	3/27/80 WELL (1pump) VOA S	4/3/80 WELL (1pump) VOA S	4/9/80 WELL (1pump) VOA S	4/16/80 WELL (1pump) VOA S	4/15-17/80(1) WELL (1pump) S
*BHC (Hexachlorocyclohexane)		_	_		
*Carbon Tetrachloride	29	35	34	220	12
*Chloroform	47	65	49	-	214
*Dibutylphthalate	-	-	-	-	-
*Dichloroethenes	≤141	≤221	≤190	152	122
*Diethylphthalate	-	-	-	-	-
Dioctyladipate *Dioctylphthalate	-	-	-	-	-
*Fluoranthene	_	-	-	_	-
*Hexachloro-1,3-butadiene	-	-	-	-	-
Hexachlorobutene	-	-	-	-	-
*Hexachloroethane	-	-	-	-	-
*Methylene Chloride	-	-	-	≤3	-
*Monochlorobenzene Pentachlorobutadiene	<b>-</b>	≤1	-	<u>≤1</u>	-
Pentachiorodutadiene				<u>-</u>	<del>-</del>
Pentachlorobutene Pentachloroethane	<del>-</del> -	- '	_	- x	-
*Phenathrene/Anthracene	-	_	_	-	<u>-</u>
Phenylnaphthalene		-	-	-	-
*Pyrene	<u>-</u>	-	-	-	-
Tetrachlorobutadiene	-	-	-	-	-
*1,1,2,2-Tetrachloroethane	-	-	-	-	
*Tetrachloroethene	1200	1500	1600	1500	782
*Toluene *Trichlorobenzene			_		-
- III Telizot o o cinicine					
*1,1,1-Trichloroethane					
*1,1,2-Trichloroethane	28	32	46	6.8	-
*1,1,2-Trichloroethene	890	1000	950	3.0	-
*Benzene	-	-	-	30	718
Benzenedicarboxcylic Acid		-	-	-	-
Cyclohexenol	-				<del></del>
Dichlorocyclohexane	-	-	-	-	-
*Diisoctylphthalate Ethylphenol	-	-	-	-	-
Heptanoic Acid	<b>-</b>	-	-	-	-
				<del>-</del>	<u> </u>
Hexanoic Acid Methylphenol	-	-	-	-	-
*Phenol	-	-	-	<u>-</u>	-
*2,4,6-Trichlorophenol	-	-	-	_	-
Dimethoxymethane	<u>-</u>				-
Methanol Acetone	(3)	(3)	(3)	(3)	(3)
1,1,1,2-Tetrachloroethane	<u>-</u>	-	-	-	-
Ethylbenzene	-	-	_	-	-
Dichlorobenzenes	-	-	-	-	-
Fluorene	_	-			
Hexachlorobenzene	-	-	-	-	:
Naphthalene Dickloroethane	-	-	-	-	-
Chloroethane	-	-	-	-	-
	<u>-</u>			-	-
Vinyl Chloride	280	440	440	15	-
	2615	3294	3310	1930.8	1848
	97.8%	97.9%	97.6%	99.3%	100.0%

<sup>(1)</sup> Mead Results; priority pollutants only

## TABLE III SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	5/1/80 WELL (1pump) VOA	5/8/80 WELL (1pump) VOA	5/12-14/80 () WELL (1pump) PP	) 5/15/80 WELL (1pump) VOA	5/21/80 WELL (1pump) VOA	WE (2p	8/80 LL Dumps) JOA
COMPOUND	S	N	Я	N	,у	Я	S
BHC (Hexachlorocyclohexane)	.:					-	
Carbon Tetrachloride	60 220	160 290	30 358	84 180	79 200	160 460	160 270
Dibutylphthalate	-	-	-	-	-	-	-/-
Dichloroethenes	≤150.5	201.2	. 351	130.7	140.6	222	≤270.
Diethylphthalate	-	-	<b>-</b>	-	-	-	•
Dioctyladipate Dioctylphthalate	_	-	18	_	_	-	_
Fluoranthene	-	-	-	-	-	-	-
Hexachloro-1,3-butadien	-	-	-	<u> </u>	-	-	
Hexachlorobutene Hexachloroethane	-	-	-	-	-	-	-
Methylene Chloride	×	x	16	≤5	×	-	_
Monochlorobenzene	-	-	-	-	-	-	-
Pentachlorobutadiene	•	-	-	-			
Pentachlorobutene	-	-	-	-	-	-	-
Pentachloroethane Phenathrene/Anthracene	-	-	-	-	-	-	-
Phenylnaphthalene	-	-	-	-	-	-	-
Pyrene	-		<u>-</u>	-		-	
Tetrachlorobutadiene	-	-	-	-	-	-	-
1,1,2,2-Tetrachloroethane Tetrachloroethene	4900	7700	764	5900	6000	9500	3200
Toluene	-	-	-	-	-	-	-
Trichlorobenzene	-	•	-	-	-	-	-
1,1,1-Trichloroethane	4.4	13	_	4.2	7.1	46	16
1,1,2-Trichloroethane	≤1	-	-	×	1.8	7.1	5.
1,1,2-Trichloroethene Benzene	3100	4000	670	3200 ×	3300	7000	3400
Benzenedicarboxcylic Acid	-	-	-	2	-	-	-
Cyclohexenol	_	-				-	
Dichlorocyclohexane	-	-	-	-	-	-	-
Diisoctylphthalate Ethylphenol	-	-	-	-	:	-	-
Heptanoic Acid	-	-	-	-	-	-	-
Hexanoic Acid	-	_	-	-	-	-	
Methylphenol Phenol	-	-	-	-	-	-	-
2,4,6-Trichlorophenol		_		=	-	-	-
Dimethoxymethane		-		-	-	-	-
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)
Acetone 1,1,1,2-Tetrachloroethane	Ξ	-	-	-	-	-	_
Ethylbenzene	-	-	-	-	-	-	-
Dichlorobenzenes						-	
Fluorene Hexachlorobenzene	-	-	-	-	-	-	-
Naphthalene	_	-	-	_	-	-	_
Dichloroethane Chloroethane	x -	-	-	x -	x -	×	:
Vinyl Chloride				12	12	 ≤5	
1,2-Dichloropropane	-	x	-	-	-	-	
	8435.9 99.9%	12364.2 99.9%	2207 98.5%	9515.9 99.8%	9740.5 99.8%		7327.1 99.6%
	99.92	44 47	UM 57				

<sup>(1)</sup> Mead Results; Priority Pollutants Only

## TABLE IV SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	6/5 WE (2pum	LL	, WE (2pu		WE (2pu	/80 (/) LL mps)	ม (2 <u>ว</u>	19/80 ELL cumps)
сомроило	7,	S	N	OA S	и	OA S	N	JOA S
*BHC (Hexachlorocyclohexane)	-		_	_				
*Carbon Tetrachloride	150	53	125	420	38-	90	200	1200
*Chloroform	420	67	380	160	593	294	710	490
*Dibutylphthalate *Dichloroethenes	222.9	≤36.5	222.1	- 69	2006	1154	342.6	163.9
*Diethylphthalate			<del>_</del>			-	-	
Dioctyladipate	-	-	-	-	-	-	-	-
*Dioctylphthalate	-	-	-	-	-	-	-	-
*Fluoranthene *Hexachloro-1,3-butadiene	-	-	-	-	-	-	-	-
Hexachlorobutene								
*Hexachloroethane	-	-	-	-		-	-	-
*Methylene Chloride	x	×	<u>≤</u> 5	6.4	163	94	95	52
*Monochlorobenzene	-	-	-	-	-	-	×	×
?entachlorobutadiene				-		<u> </u>		
Pentachlorobutene Pentachloroethane	-	-	-	-	-	-	-	-
*Phenathrene/Anthracene		-	-	-	-	-	-	-
Phenylanaphthalene	-	-	•	_	-	-		
*Pyrene		-	-	-	-	-	-	-
Tetrachlorobutadiene		-	-	-	_	_		
*1,1,2,2-Tetrachloroethane *Tetrachloroethene	690	190	440	1100		511	260	3900
*Toluene	11000	1300	10000	6700	1931	875	16000	15000
*Trichlorobenzene	-	-	-	-	-	-	Ξ	-
*1,1,1-Trichloroethane	- 53	2.9	35	44	39	54	77	140
*1,1,2-Trichloroethane	≤3 8400	x 1800	7000	6800	2446	1239	11 11000	14000
*1,1,2-Trichloroethene *Benzene	3400	1800	7000	-	12	1239	11000	14000
Benzenedicarboxcylic Acid	-	-	-	-	-	-	-	-
Cyclohexenol	-	•	-	-	-	-	-	_
Dichlorocyclohexane	-	-	-	-	-	-	-	-
*Diisoctylphthalate Ethylphenol	-	-	<b>-</b>	-	-	-	-	-
Heptanoic Acid	-	-	-	-	-	-	-	-
Hexanoic Acid	-	-	<u>-</u>	-	-	-	-	-
Methylphenol	-	-	-	-	-	-	-	-
*Phenol *2,4,6-Trichlorophenol	-	-	-	<del>-</del>	:	-	-	-
Dimethoxymethane	-	-	-	-	-	-	-	-
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)
Acetone 1,1,1,2-Tetrachloroethane	-	-	-	-	<u>-</u> .	-	-	-
Ethylbenzene	-	-	-	-	-	-	-	_
Dichlorobenzenes	-	-	-	-	-	-	-	- ,
Fluorene	-	-	-	-	-	-	-	-
Hexachlorobenzene	-	-	-	-	-	-	-	-
Naphthalene Dichloroethane	-	:	-	-	-	-	-	×
Chloroethane	-		-	-	-	-	-	- -
Vinyl Chloride Trichlorofluoromethane	-	32	47 -	7.7	116	86 11	x -	x -
	20938.9 99.0% 12210.15	3481.4 98.02 average	18211.8 98.32 16759.45	15307.1 99.2% average	7344 97.2 5877	4410 2 92.42 average	28695.6 98.73 31820.75	34945.9 99.02 average

<sup>(|)</sup> Mead Results; Priority Pollutants only.

in solver

## TABLE V SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	(2	26/80 ELL pumps) VOA	WE. (2 p	/80 LL umps)	(2	10/80 ELL pumps)
COMPOUND	<u>N</u>	S	N	OA S	N_	VOA S
*BHC (Hexachlorocycloehxane) *Carbon Tetrachloride *Chloroform *Dibutylphthalate *Dichloroethenes	160 480 —	960 340 ——————————————————————————————————	73 370 — 457.3	270 16 153	52 200	260 130
*Diethylphthalate Dioctyladipate *Dioctylphthalate *Fluoranthene *Hexachloro-1,3-butadiene		=		=======================================	660	742.7
Hexachlorobutene  *Hexachloroethane  *Methylene Chloride  *Monochlorobenzene  Pentachlorobutadiene	<u>x</u>	x ≤1	=	= -	=	
Pentachlorobutene Pentachloroethane *Phenathrene/Anthracene Phenylanaphthalene *Pyrene		-	=	=	=	
Tetrachlorobutadiene *1,1,2,2-Tetrachloroethane *Tetrachloroethene *Toluene *Trichlorobenzene	3000	5600	2700	2200	1800	1800
*1,1,1-Trichloroethane *1,1,2-Trichloroethane *1,1,2-Trichloroethane *Benzene Benzenedicarboxcylic Acid	3200	80 8.4 4000 x	21	27	17	27
Cyclohexenol Dichlorocyclohexane *Diishoctylphthalate Ethylphenol Heptanoic Acid	=	=		=	=	=
Hexanoic Acid Methylphenol *Phenol *2,4,6-Trichlorophenol Dimethoxymethane		=	=		=	
Methanol Acetone 1,1,1,2-Tetrachloroethane Ethylbenzene Dichlorobenzenes	(3)	(3)	(3)	(3)	(3)	(3)
Fluorene Hexachlorobenzene Naphthalene Dichloroethane Chloroethane	=	x	=		=======================================	=======================================
Vinyl Chloride Trichlorofluoromethane	280	200	43	310	120	24
	7821 <u>97.4%</u> 9505.2	11189.4 97.4% average	6364.3 98.6% 6120.2 a	5675.0 99.2% everage	4449 98.4% 4416.4	4383.7 98.8% average

## TABLE VI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	6621	average	5931.9	average	8234.5	average	8902.5	average	
TOTAL	6174 91.1 <b>2</b>	7068 97.6 <b>z</b>	7072 97.6%	4791.8 98.3%	7552 98.2%	8917 98.0%	6656 97.3%	11149 98.5%	
MIOI OPERZERE						-	-		
richlorofluoromehtane hlorobenzene	-	-	-	-	-	-	-	-	
inyl Chloride	82	64	29	21	78	78	100	60	
ichloroethane			-	-	-	-		-	
aphthalene	-	-	-	_	-	-	-	-	
luorene	-	-	-	-	•	-	-	-	
ichlorobenzenes	-	-	-	-	-	-	-	-	
thylbenzene	_	-	-	-	-	-	-	-	
,1,1,2-Tetrachloroethane		-		-	-		-	-	
[ethanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
,4,6-Trichlorophenol	-	-	-	-	-	-	-	-	
henol	-	-	-	-	-	-	-	-	
iisoctylphthalate	-	-	=	-	-	-	-	-	
enzen <b>e</b>	-		-		-	-	-		
.,1,2-Trichloroethene	2600	2900	2800	2100	3700	4000	2100	4800	
,1,2-Trichloroethane	-	-	-	-	-	-	-	-	
.,1,1-Trichloroethane	14	18	21	9.8	11	12	11	16	
richlorobenzene	-	-	_	_	-	-	_		
oluene	-	-		-		-	-	-	
etrachloroethene	2600	2800	3200	2000	3000	3800	3600	5300	
,1,2,2-Tetrachloroethane	180	540	170	210	130	360	140	150	
Tetrachlorobutadiene	-	-	-	-	-	-	_	-	
yrene	-	-	_	-	-	-	_	-	
henathrene/Anthracene		-			⁻,		-		
entachloroethane	· <b>-</b>	-	-	-	-		-	-	
entachlorobutadiene	-	<b>-</b> .	-	-	-	-	-	-	
fonochlorobenzene	-	-	-	-	-	-	-	-	
lethylene Chloride	-	8	-	-	-	-	-	-	
Hexachloroethane	-	_	_	_	-	-	_	-	
ruoranthene rexachloro-1,3-butadiene	_	-	-	-	_	-	-	_	
ioctylphthalate	-	-	-	-	-	_	-	-	
Dioctyladipate	<b>-</b>	-	-	-	-	-	-	-	
ichloroethenes	130	76	122	51	127	87	127	93	
ibutylphthalate	720	-	720	230		-	510	J10	
Thloroform	520	39 <b>0</b>	520	250	460	300	510	310	
HC (Hexachlorocyclohexane) Carbon Tetrachloride	48	280	210	150	46	280	- 6 <b>8</b>	420	
COMPOUND	N	s	N	s	N	s	N	s	
		VOA		VOA		VOA	\	VOA	
		umps)		umps)		umps)		oumps)	
		17/80 EL <b>L</b>		24/30 EL <b>L</b>		EL <b>L</b>		7/80 ÆL <b>L</b>	
•		17/80		24/80		31/80		7/80	

<sup>3)</sup> Procedure used will not detect methanol.

LC/cjb 2/4/80

MOTE: Compounds detected on one occasion only and not quantitated have been omitted.

## TABLE VII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	5940.5	average	6605.5	average	4973	average	6195.5	average	
TOTAL	4494 96.5 <b>%</b>	7387 97.7%	6360 97.8%	6851 98.7%	5037 97.8%	4909 97.8%	6411 94.4 <b>%</b>	5980 95.8%	
Chlorobenzene			6		4		3	· -	
Vinyl Chloride Trichlorofluoromethane	180	72 -	32	20	12	18	230	140	
Naphthalene Dichloroethane	-	-	-	-	-	-	-	-	
fluorene	-	-	-	-	-	-	-	-	
ichlorobenzenes	-	-	-	-	-	-	-	-	
Ethylbenzene				-					
1,1,1,2-Tetrachloroethane			-	-	-	-	-	-	
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
2,4,6-Trichlorophenol	-	-	-	_	-	_	-	-	
Phenol	-	-	-	-	_	-	-	-	
Diisoctylphthalate									
*1,1,2-Trichloroethene *Benzene	-	-	-	-	<u>≤</u> 3	-	-	-	
*1,1,2-Trichloroethane	2000	2800	2800	2800	2300	2100	2800	2600	
*1,1,1-Trichloroethane	14	15	10	-	-	-	-	-	
*Trichlorobenzene	<u>-</u>	- 15	10	15	15	13	11	10	
*Toluene				_					
*Tetrachloroethene	1800	3200	2500	3200	1900	2000	2300	2400	
*1,1,2,2-Tetrachloroethane	70	340	180	360	170	220 2000	160 2300	2400	
Tetrachlorobutadiene	-	<del>-</del>	-	-	-	-	160	170	
*Pyrene	-	-	-	-	-	-	-	-	
*Phenathrene/Anthracene	-	-				_			
Pentachloroethane	-			_	-	_	-	-	
Pentachlorobutadiene	-	-	-	-	-	-	-	-	
*Monochlorobenzene	-	-	-	-	-	-	-	-	
*Methylene Chloride	-	-	-	10	14	16	110	35	
~HEXACIIIOI OECIMARE									
*Hexachloro-1,8-butadiene *Hexachloroethage	_	-	_	_	-	-	-	-	
*Fluoranthene	-	_	-	-	-	-	-	-	
*Dioctylphthalate	<b>-</b>	-	-	_	_	-	-	-	
Diocytladipate	-	-	-	-	-	_	_	_	
*Dibutylphthalate *Dichloroethenes	77	80	158	70	81	62	180	65	
*Chloroform	200	J40 -	-	-	_		-	-	
*Carbon Tetrachloride	280	340	580	330	470	220	540	300	
*BHC (Hexachlorocyclohexane)	73	540	94	46	68	260	- 77	260	
COMPOUND	N	S	N	S	N	S	N	S	
	· -	VOA	,	VOA		VOA		VOA	
		umps)		umps)		umps)		umps)	
		ELL		ELL		ELL	พ	ELL	
	8/	14/80	8/	21/80	8/	28/80	9/	4/80	

<sup>(3)</sup> Procedure used will not detect methanol.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 12/4/80

## TABLE VIII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		/11/80 WELL pumps) VOA	ī	/18/80 /ELL pumps) VOA		/25/80 WELL pumps) VOA		.0/2/80 WELL Pumps) VOA
COMPOUND	N	S	N	S	N	s	N	S
*BHC (Hexachlorocyclohexane)	-	_	-					
*Carbon Tetrachloride	40	230	20	140	28	37	49	-
*Chloroform	160	110	160	120	290	110	280	110
*Dibutylphthalate	-	-	-	-			200	170
*Dichloroethenes	87	50	97	59	353	130	306	242
Dioctyladipate	-	-	_	-				
*Dioctylphthalate	-	-	-	-	-	-	_	_
*Fluoranthene	-	-	-	-	-	_	_	_
*Hexachloro-1,3-butadiene	-	-	-	-	-	_	_	_
*Hexachloroethane				-	-	-	_	-
*Methylene Chloride	41	12	42	12	22	8	22	10
*Monochlorobenzene	-	-	-	-	-	-		10
Pentachlorobutadiene	-	-	-	-	_	-	_	_
Pentachloroethane	-	-	-	-	-	_	_	_
*Phenathrene/Anthracene		-	-	-	-	-	-	-
*Pyrene	-	-	_					
Tetrachlorobutadiene	-	-	-	-	_	_	-	-
*1,1,2,2-Tetrachloroethane	32	60	34	56	62	63	35	58
*Tetrachloroethene	4800	5700	4900	5500	930	540	1300	1700
*Toluene		-	-	-	-	-	-	-
*Trichlorobenzene								
*1,1,1-Trichloroethane	8	9 -	7	8	16	7	26	-
*1,1,2-Trichloroethane	-	x	-	-	-	-	20	19
*1,1,2-Trichloroethene	1800	1900	1900	1900	1700	1000	2200	2000
*Benzene	-	_	-	-		1000	8	2000
				<u> </u>				
*Diisoctylphthalate	-	-	-	-	-	-	-	-
*Phenol	-	-	-	-	-	-	-	-
*2,4,6-Trichlorophenol	(2)	_	(2)	(2)	(2)	(2)	(2)	(2)
Methanol 1,1,2-Tetrachloroethane	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)
1,1,1,2-letrachioroethane								
Ethylbenzene	-	-	<b>-</b> .	-	-	-	-	-
Dichlorobenzenes	-	-	-	-	-	-	-	-
Fluorene	-	-	-	-	-	-	-	-
Naphthalene	-	-	-	-	-	-	-	-
Dichloroethane								-
Chloroethane	-	-	-	-	-	-	-	-
Vinyl Chloride	100	94	110	84	130	20	320	250
Trichlorofluoromethane	-	-	-	-	-	-	-	-
Chlorobenzene					3		2	1
				7070	2521	1015	4540	
#O# A T	7040	9145						
TOTAL	7068	8165	7272	7879	3534	1915	4548	4568
TOTAL	7068 98.3%	8165 98.4 <b>%</b>	99.1%	98.3%	3534 _96.4%	96.2 <b>7</b>	96.9%	95.5%

<sup>(3)</sup> Procedure used will not detect methanol.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 11/20/80

## TABLE IX SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

TOTAL	4050 96.9%	3714 94.5%	4292 96.8%	4669 93.9%	4730 96.2%	3286 96.6%	2123 97.0%	3034 97.1%	
Chlorobenzene	-	-	-	-	-	-	-	-	
Trichlorofluoromethane	-	-	_	-	_	-	-	-	
Vinyl Chloride	300	170	300	48	34	-	_	_	
Chloroethane	-	_	-	_	_	_	-	-	
Dichloroethane			-	-	-	-	-	-	
Naphthalene	-	-	-	-	-	-	-	-	
Fluorene	-	-	-	-	-	-	-	-	
Dichlorobenzenes	-	-	-	-	-	-	-	-	
Ethylbenzene	4	-	≰3	-	-	-	-	-	
~, ~, ~, ~ Testadintot decimant						_			
1,1,1,2-Tetrachloroethane	(3)	(3)	. (3)	(3)	(3)	(3)	(3)	(3)	
*2,4,6-frichtorophenoi Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
*Phenoi *2,4,6-Trichlorophenol	-	_	_	_	-	_	-	-	
*Diisoctylphthalate *Phenol	_	-	-	-	-	-		-	
*Benzene	-	-	10	-	≤10	-	-	-	
*1,1,2-Trichloroethane *1,1,2-Trichloroethane	1900	1800	2100	2100	2400	1600	1200	1700	
*1,1,1-Trichloroethane	-	-	-		-	<b>-</b>	-		
*Trichlorobenzene	21	19	21	24	4	<u>-</u> ≤4	-	<u>≤</u> 4	
hm.d.s.b.1ab.an.an.a		-		-		_			
Toluene	-	• -	-	-	-	-	-	-	
*Tetrachloroethene	1200	1200	1200	1400	1300	1100	630	1000	
*1,1,2,2-Tetrachloroethane	31	56	36	51	150	200	100	120	
Tetrachlorobutadiene	-	_	-	-	-	-	-	-	
*Pyrene	-	-	_	-	-	-	-	-	
rhenathrene/Anthracene									
Pentachioroethane Phenathrene/Anthracene	_	_	_	-	-	-	-	-	
Pentachloroethane	_	_	_	-	_	_	-	-	
Monochiorobenzene Pentachlorobutadiene	-	_	_	-	_	_	_	_	
Meinylene Chioride	30	-	-	-	-	, -	75	-	
Methylene Chloride	30	19	30	10	190	76	53	6	
*Hexachloroethane		-			-			-	
*Hexachloro-1,3-butadiene	-	-	-	-	-	-	-	-	
Fluoranthene	-	-	-	-	-	-	-	-	
Dioctylphthalate	-	-	-	-	-	-	-	-	
Dioctyladipate	-	-	-	-	-	-	-	-	
*Dichloroethenes	305	≤192	295	264	120	73	66	79	
*Chiorororm *Dibutylphthalate	220	-	-	-	-		-	,-	
Carbon Tetrachloride Chloroform	220	150	260	150	510	200	64	94	
*BHC (Hexachlorocyclohexane) *Carbon Tetrachloride	- 39	110	37	190	12	33	10	31	
					_	_	_		
COMPOUND	N	s	N	S	N	S	N	S	
		70A		OA		AON		70A	
		mps)		umps)	(2pt	umps)		mps)	
	WI	ELL.	WE	LL	WI	ELL	WI	29/80 <sup>(1)</sup> ELL	

<sup>(1)</sup> North well sampled 10/29/80; South well sampled 10/30/80.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 12/9/80

<sup>(3)</sup> Procedure used will not detect methanol.

## TABLE X SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

TOTAL	2850 95.6%	1892 93.2%	3639 96.32	1627 95.1%	7991 95.5%	4956 94.0%	11248 98.8%	6598.9 94.3%	
Chlorobenzene	-	-	-	_	-	-	-	-	
Trichlorofluoromethane	-	-	-	-	-	-	-	-	
Vinyl Chloride	23	32	-	-	44	330	48	110	
Chloroethane			_		_	_			
Dichloroethane	_	-	-	-			-		
Naphthalene	-	-	-	-	-	-	-	-	
Fluorene	-	-	-	-	-	-	-	-	
Dichlorobenzenes	-	-	-	-	-	-	-	-	
Ethylbenzene	-	_	-	-	_	_	-	-	
1,1,1,2-Tetrachloroethane	· <u>-</u>	· •	<u> </u>						
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
*2,4,6-Trichlorophenol	-	-	-	-	-	- (2)	-	-	
*Phenol	-	-		-	-	-	-	-	
*Diisoctylphthalate	-	-	-	-	-	-	-	-	
*Benzene							<u> </u>		
1,1,2-Trichloroethene	1100	640	1800	680	5100	2000	5100	2500	
1,1,2-Trichloroethane	-	-	-	-	19	-	-	-	
1,1,1-Trichloroethane	9	4	10	-	42	19	42	19	
Trichlorobenzene	-	_	_	-	-	_	-	-	
Toluene									
Tetrachloroethage	900	600	1100	530	3300	1700	3600	2400	
1,1,2,2-Tetrachloroethane	56	33	82	57	530	130	520	320	
Tetrachlorobutadiene	-	-	•	-	-	-	-	-	
Pyrene	-	-	-	-	-	-	-	-	
THEMSELLE CHE / AMERICACEME									_
Pentachloroethane Phenathrene/Anthracene	-	-	-	-	-	-	-	_	
Pentachlorobutadiene	-	-	Ξ	-	-	-	-	-	
Monochlorobenzene	•	-	-	-	-	-	-	-	
Methylene Chloride	400	340	93	29	160	17	42	35	
					162				
Hexachloroethane	-	-	-	-	-	-	-	-	
Hexachloro-1,3-butadiene	-	-	-	-	_	-	-	-	
Fluoranthene	-	_	_	-	-	-	-	-	
Dioctyladipate	-	_	_	-	_	_	-	-	
Dioctyladipate				_				_	
Dichloroethenes	92	63	130	100	456	220	456	394.8	
Dibutylphthalate	-	-	-	-		_	-	-	
Chloroform	240	120	380	180	1200	410	1300	610	
Carbon Tetrachloride	30	60	44	51	110	130	140	210	
*BHC (Hexachlorocyclohexane)	_	-	_	_	_	_	_	_	
COMPOUND	N	S	N	S	N	<u></u>	N	S	
		_		_				_	
	(2)	VOA.	(2)	VOA.	(2)	VOA	(2	VOA	
		VELL Dúmps)		ELL oumps)		VELL pumps)		WELL Dumps)	
		<i>₩</i> /80		13/80		/20/80		/26/80	

<sup>(1)</sup> North well sampled 10/29/80; South well sampled 10/30/80.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 1/9/81

<sup>(3)</sup> Procedure used will not detect methanol.

## TABLE XI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	₩Т (2pt	/4/80 ELL imps) /OA	WE (2pu	.0/80 TLL amps) 70A	W (2p	17/80 ELL umps) VOA	w) (2p)	23/80 ELL umps) VOA	W (2p	31/80 ELL umps) VOA	
COMPOUND	N	\$	N	\$	N	s	N	s	N .	<u>s</u>	
*BHC (Hexachlorocyclohexane)	-	_	_	-	_	-	-	-	-		
*Carbon Tetrachloride	31	33	28	42	29	33	25	32	31	26	
*Chloroform	390	170	370	160	350	130	430	140	390	120	
*Dibutylphthalate *Dichloroethenes	66	≤ 56	77	≤ 51	71	50	82	≤ 52	73	43	
Dioctyladipate				-	-	-	-	-	-	-	
*Dioctylphthalate	-	-	-	-	-	-	-	-	-	-	
*Fluoranthene	-	-	-	-	-	-	-	-	-	-	
*Hexachloro-1,3-butadiene *Hexachloroethane	-	-	-	-	-	_	-	-	-	-	
*Methylene Chloride	-		-	-	-	-	24	12	37	10	
*Monochlorobenzene	-	-	-	-	-	-	-	-	-	-	
Pentachlorobutadiene	-	-	-	-	-	-	-	-	-	-	
Pentachloroethane *Phenathrene/Anthracene	-	-	-	-	Ξ	-	-	-	-	-	
*Pyrene						-					
Tetrachlorobutadiene	-	-	-	-	-	-	•	-	-	-	
*1,1,2,2-Tetrachloroethane	180	90	160	79	130	62	240	58	200	50	
*Tetrachloroethene	910	570	960	620	1000	490	1000	470	970	420	
*Toluene				<b>-</b>						-	
*Trichlorobenzene	-	-	-	-	-	-	-	-		-	
*1,1,1-Trichloroethane	12	2	12	2	11	2	11	2	11	2	
*1,1,2-Trichloroethane *1,1,2-Trichloroethene	1500	560	1400	570	1400	480	1600	470	1600	400	
*Benzene	-	-	-	-	-	-	-	-	-		
*Diisoctylphthalate	-	-		-	_	-	-	-	_	-	
*Phenol	-	-	-	-	-	-	-	-	-	-	
*2,4,6-Trichlorophenol	(2)	(3)	(3)	(2)	(2)	(2)	(3)	(3)	(3)	(3)	
Methanol 1,1,1,2-Tetrachloroethane	(3)	(3)	(3) -	(3) -	(3) -	(3)	(3)	-	-	-	
Ethylbenzene	-		-			-	-	-	-		
Dichlorobenzene	-	-	-	-	-	-	-	-	-	-	
Fluorene Naphthalene	•	-	-	-	-	-	-	-	-	-	
Dichloroethane	-	-	-	-	-	-	-		-	-	
Chloroethane		-	•		-	-					
Vinyl Chloride	59	80	69	89	66	60	66	78	68	64	
Trichlorofluoromethane Chlorobenzene	-	-	-	-	-	-	-	-	-	-	
TOTAL Top 5	3148 96.82	1561 94.2%	3076 96.5%	1613 94.1%	3057 96.5%	1307 93.5%	3478 96.4 <b>z</b>	1314 92.5%	3380 95.6%	1135 92.9%	
	2354.5	average		average		average		average		average	

<sup>(3)</sup> Procedure used will not detect methanol.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 1/27/81

## TABLE XI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	WI (2pt	3/81 <sup>(1)</sup> ELL imps) VOA	WI (2pt	14/81 ELL imps) /OA	WI (2pt	21/81 <sup>(1)</sup> ELL umps) VOA	W] (2pt	28/81 ELL imps) JOA	
COMPOUND	N	S	N	S	Ŋ	S	N	S	
*BHC (Hexachlorocyclohexane)	_	_	-	_	-	-	_	-	
*Carbon Tetrachloride	30	20	36	43	2	20	32	30	
*Chloroform	60	200	530	190	300	100	160	120	
*Dibutylphthalate	-	-	-	-	-	-	-	-	
*Dichloroethenes	72	≤ 62	89	≤ 60	<u>≤</u> 42	≤ 42	63	37	
Dioctyladipate	-	-	-	-	-	-	-	-	
*Dioctylphthalate	-	-	-	_	-	-	-	-	
*Fluoranthene	-	-	-	-	-	-	-	-	
*Hexachloro-1,3-butadiene	-	-	-	-	-	-	-	-	
*Hexachloroethane	-	-	-		-	-	-	-	
*Methylene Chloride	-	-	-	-	-	-	-	-	
*Monochlorobenzene	-	-	-	-	-	-	-	-	•
Pentachlorobutadiene	-	-	-	-	-	-	-	-	
Pentachloroethane	-	-	-	-	-	-	-	-	
*Phenathrene/Anthracene	-	-	-	-	-	-	-	-	
*Pyrene	-	-	-	-	-	-	-	-	
Tetrachlorobutadiene	-	-	-	_	-			-	
*1,1,2,2-Terrachloroethane	200	50	170	51	80	40	83	17	
*Tetrachloroethane	1000	600	1800	570	200	400	1200	420	
*Toluene	-	_	-	-	-	-	-	-	Openio (° or
*Trichlorobenzene	-	-	-	-	-	-	-	-	
*1,1,1-Trichloroethane	8	2	12	2	2	-	14	2	
*1,1,2-Trichloroethane	-	-	-	-	-	-	-	-	
*1,1,2-Trichloroethene	2000	400	1300	440	400	300	1400	340	
*Benzene	-	-		_	. ~	-	-	-	
*Diisoctylphthalate	-	-	-	-	-	_	-	-	
*Phenol	-	-	-	-	-	-	-	-	
*2,4,6-Trichlorophenol	-	_	-	-	-	-	_	-	
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)		
1,1,1,2-Tetrachloroethane	-	-	-	-	-	-	-	-	
Ethylbenzene	-	-	-	-	-	-	-	-	
Dichlorobenzenes	-	-	-	-	-	-	-	-	
Fluorene	-	-	-	-	-	-	-	-	
Naphthalene	-	-	-	-	-	-	-	-	
Dichloroethane	-						-		
Chloroethane	- 80	200	- 120	180	- 10	- 80	- 76	120	
Vinyl Chloride Trichlorofluoromethane	80	<b>200</b>	120	190	10	80	/ <b>0</b>	130	
Chlorobenzene	-	-	-	-	-	-	-	<del>-</del>	
TOTAL	3450	1534	3757	1536	1036	982	3028	1098	
	97.2%	95.3%	96.4%	93.8%	98.6%	93.9%	96.4%	95.5%	

<sup>(1)</sup> Due to a computer malfunction, the original data from the analyses of the 1/18/81 and 1/21/81 samples was irretrievably lost. The original samples were reanalyzed but since the sample vials had headspace, the actual values may be somewhat greater than those reported. The values listed for these samples are reported with one significant figure to indicate a decreased level for confidence in their accuracy.

NGTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 3/24/31

<sup>(3)</sup> Procedure used will not detect methanol.

## TABLE XII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	W	(4/81 <sup>(1)</sup> VELL Oumps) VOA	2/11/81 WELL (2pumps) VOA	,	(18/81 VELL Dumps) VOA	,	/25/81 VELL Dumps) VOA
COMPOUND	И	S	N <sup>(2)</sup> S	N	s	N	S
*BHC (Hexachlorocyclohexane)	_		-	_		_	
*Carbon Tetrachloride	33	36	32	34	34	31	30
*Chloroform	230	150	160	430	160	160	370
*Dibutylphthalate	-	-	-	_	-	-	-
*Dichloroethenes	≤65	≤10	≤10	≤10	≤10	≤10	≤10
Dioctyladipate	-	-	-	-		-	_
*Dioctylphthalate	-	-	-	-	-	-	-
*Fluoranthene	-	-	-	-	-	-	-
*Hexachloro-1,3-butadiene	-	-	-	-	-	-	-
*Hexachloroethane	-	-	-	-	-	-	-
*Methylene Chloride	-		-	-	<b>≦</b> 5	6	-
*Monochlorobenzene	-	-	-	-	-	-	-
Pentachlorobutadiene	-	-	-	-	-	-	-
Pentachloroethane	-	-	-	-	-	-	-
*Phenoathrene/Anthracene	-	-	-	-	-	-	
*Pyrene	-	-	-	-	-	-	-
Tetrachlorobutadiene					-		-
*1,1,2,2-Tetrachloroethane	90	49	65	230	76	58	180
*Tetrachloroethane	610	490	480	860	490	490	870
*Toluene e	•	-	-		-		
*Trichlorobenzene	-	-	-	-	-	-	-
*l,l,l-Trichloroethane	≤ 5	≤ 5	<b>≤</b> 5	13	≤ 5	≤ 5	9.2
*1,1,2-Trichloroethane	-	-	-	-	-	-	-
*1,1,2-Trichloroethene	1100	460	520	1600	730	540	1300
*Benzene	-		-	-	-		
Diisoctylphthalate	-	-	-	-	-	-	-
Phenol	-	-	-	-	-	-	-
2,4,6-Trichlorophenol	-	-	-	-	-	-	
Methanol 1,1,1,2-Tetrachloroethane	(3)	(3)	(3)	(3)	(3)	(3)	(3)
1,1,1,2-letrachioroethane	-				-		
Ethylbenzene Dichlorobenzenes	-	-	<b>-</b>	-	-	-	-
Fluorene	-	-	-	-	-	-	-
Naphthalene	_	_	-	-	_	-	<u>-</u>
Dichloroethane	-	-		-	-	-	-
Chloroethane			-	-			
Vinyl Chloride	93	86	100	78	110	120	77
Trichlorofluoromethane	-	-	-	-	-	-	-
Chlorobenzene	-	-	-		-	_	-
TOTAL	2226	3512	1372	3272	1620	1420	2846.2
	95.4%	98.6%	96.6%	98.3%	96.7%	96.3%	98.3%
	2869						

<sup>(1)</sup> North well sampled 2/4/81; South well sampled 2/5/81; South well shutdown 2/4/81 through 9:30 a.m. on 2/5/81.

NOTE: Compounds detected on one occasion only and not quantitated have been omitted.

DLC/cjb 3/30/81

<sup>(2)</sup> Lost sample for North well - 2/11/81.

<sup>(3)</sup> Procedure used will not detect methanol.

## SUMMARY OF ORGANIC TABLE XIV ON VARIOUS SAMPLES (ppb)

	w (2p)	/5/81 <sup>(1)</sup> ELL umps) PP		/12/81 WELL pumps) VOA		WELL Pumps) VOA		3/25/81 <sup>(2)</sup> WELL <sup>2</sup> pumps) VOA
COMPOUND	N	s	N	S	N	s	N	s
*BHC (Hexachlorocyclohexane)	0.83	1.18	_		-			
*Carbon Tetrachloride	28	29	55	22	60	52	91	80
Chloroform	350	140	870	120	1010	350	1400	380
Dibutylphthalate	-	-	-	-	-	-	-	-
Dichloroethenes	<u>≤</u> 10	≤10		<b>≦</b> 5	_ ≤5	<b>≤</b> 5	30	≤10
Dioctyladipate	-	-	_	-				
Dioctylphthalate	-	-	-	-	-	_	-	-
Fluoranthene	-	-	-	-	-	-	-	_
Hexachloro-1,3-butadiene	13	10	-	-	<b>-</b> ·	-	-	-
Hexachloroethane	19	12		-		-	-	-
Methylene Chloride	3	11	_	7		7		7
Monochlorobenzene	-	-	. <b>-</b>	-	-	_		
Pentachlorobutadiene	-	-	-	-	-	-	-	-
Pentachloroethane	-	-	-	-	-		-	-
Phenoanthrene/Anthracene					<u>-</u>			-
Pyrene	-	-	-	_		_		
Tetrachlorobutadiene	-	-	-	-	-	-	-	_
1,1,2,2-Tetrachloroethane	190	82	320	38	720	130	490	200
Tetrachloroethene	940	540	1100	260	2000	570	1200	720
Toluene						-	-	-
Trichlorobenzene	5	≤ 5	-	_	_	_	_	
1,1,1-Trichloroethane	13	≤ 5	16	-	18	-	14	-
1,1,2-Trichloroethane		-	-	-	-	_	≤10	_
1,1,2-Trichloroethene	1400	530	1700	380	1700	700	1800	870
Benzene	<del>_</del>						-	-
Diisoctylphthalate	-	_ '	_	_	_	-	-	_
Phenol	-	-	-	-	-	-	-	-
2,4,6-Trichlorophenol	-	-		-	-	-	-	-
Methanol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)
1,1,1,2-Tetrachloroethane	<u>-</u>				-	-		-
Ethylbenzene	-	-	-	-	-	-	-	-
Dichlorobenzene	-	-	-	-	-	-	-	-
Fluorene	-	-	-	-	-	-	-	-
Naphthalene	-	-	-	-	-	-	-	-
Dichloroethane	<del>-</del>	<del>-</del> ·						•
Chloroethane	_	-	-	-	-	-	-	-
Vinyl Chloride	78	88	10	8	9	14	14	20
Trichlorofluoromethane	-	-	_	-	-	-	-	-
Chlorobenzene	<b>-</b>	-						
TOTAL	3049.83	1423.18	4091	840	5536	1828	5054	2287
	97.0%	97.0%	98.9%	97.6%	99.3%	98.6%	99.2%	98.4%
		average	2465.5	average	3682	average	3670.5	verage

<sup>(1)</sup> Priority Pollutant Analysis

NOTE: Compounds detected on one occasion only and not quatitated have been omitted.

DLC/cjb 5/12/81

<sup>(2)</sup> South well down 2:30 pm-7:30 pm, 3/24/81; North well down 4:30 pm-8:15 pm and 9:00 pm-10:45 pm on 3/25/81.

<sup>(3)</sup> Procedure used will not detect methanol.

TABLE XV
SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		4/1/81 WELL (2pumps) VOA .		4/9/81 WELL (2pumps) VOA		4/15/81 WELL (2pumps) VOA		4/22/81 WELL (2pumps) VOA		4/29/81 WELL (2pumps) VOA
COMPOUND	N	\$	1	N S	1	N S	1	s v	I	2 .
BHC (Hexachlorocyclohexane)	* 79		70	* * 0 51				* *		* *
Carbon Tetrachloride Chloroform	1000		590		86 1200		76 1200			
Dibutylphthalate	*	*	,	* *	•	* *	•	*	,	* *
Dichloroethenes	≤10	≤10	≤2:	1 ≤10	77	7 45	87	7 29	≤31	1 ≤34
Dioctyladipate	*		,		,				,	
Dioctylphthalate	*	*	,				•		,	
Fluoranthene Hexachloro-1,3-butadiene	*	*		* *	,		,		,	
Hexachloroethane	*	*	•		•	*	•		,	
Methylene Chloride	9	15		- <u>≤</u> 5					28	3 14
Monochlorobenzene	-	-			≤5		≤5	; <b>-</b>		
Pentachlorobutadiene	*			* *	*		*		,	
Pentachloroethane Phenoanthrene/Anthracene	*	*	,		*		*		,	
- rienoantiirele/Airtiiracelle	-				•					
Pyrene	*	*	,		*		*		,	
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane	360		260		440		360		260	
Tetrachloroethene	1400		1400		1500		1400		1200	
Toluene	-	-	•	-	•	-	•	-	•	-
Trichlorobenzene	*	*	*	*	*	*	*	*	*	*
1,1,1-Trichloroethane	16 ≤10	-	18 ≤10	•	27 11	19 11	24 21	15 ≤10	12 ≰10	16 11
1,1,2-Trichloroethane 1,1,2-Trichloroethene	1800	830	2700	990	3200	2300	3200	2100	2300	2500
Benzene	-	-	-	-	-	-	-		•	
Diisoctylphthalate	*	*	*	*	*	*	*	*	*	*
Pheno1_	*	*	*	*	*	*	*	*	*	*
2,4,6-Trichlorophenol	*	*	*	*	*	*	*	*	*	*
1,1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*	*	*
Ethylbenzene	_		_		_			_		
Dichlorobenzene	*	*	*	*	*	*	*	*	*	*
Fluorene	*	*	*	*	*	*	*	*	*	*
Naphthalene Dichloroethane	-	-	-	-	-	-	-	-	-	-
Chloroethane	_	_		_		_		_		
Vinyl Chloride	8	17	<u>∡</u> 5	<u>≤</u> 5	8	25	9	11	<u>≤</u> 5	12
Trichlorofluoromethane	•	-	-	-	-	-	-	-	-	-
TOTAL	4692	2324	5074	2091	6554	4210	6382	4205	4608	4927
	98.9%	98.2%	98.9%	99.0%	98.0%	97.6%	97.9%	98.4%	98.1%	98.2%
	3508	average	3582.5	average	5382	average	5293.5	average	4767.5	average

DLC/vrp 10/20/81

<sup>-</sup> Not Detected \* Procedure Used Will Not Detect

TABLE XVI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	. (	5/6/81 WELL 2pumps) VCA		5/13/81 WELL (2pumps) VOA		5/20/81 <sup>(1</sup> WELL (2pumps) VOA		/28/81 <sup>(2)</sup> WELL (2pumps) VOA	
COMPOUND	N	S	N	S	N	. S	N	S	
*BHC (Hexachlorocyclohexane	) -	- 36	43	120	34	100	80	- 84	
*Carbon Tetrachloride *Chloroform	480	340	560	130 320	500	260	380	170	
*Dibutylphthalate		340	500	320	300	200	300	1/0	
*Dichloroethenes	≤10	≤10	12	≤10	≤10	≤10	≤10	≤10	
Dioctyladipate	-	-	-	-		-	-	-	
*Dioctylphthalate	-		-	-	-	-	-	-	
*Fluoranthene	-	-	•	-	-	-	-	-	
*Hexachloro-1,3-butadiene *Hexachloroethane	:	-		-		:	-	·	
*Methylene Chloride	-	38	_	-	5ء	5	.≤5	_≤5	
*Monochlorobenzene Pentachlorobutadiene	-	<b>≤</b> 5	-	-		:	-	•	
Pentachloroethane		:	-	-			:		
*Phenoanthrene/Anthracene	-	-	-	-	-	-	-	-	
*Pyrene	-	-	-		-		-		
Tetrachlorobutadiene	220	200	420	260	240	220	220	200	
*1,1,2,2-Tetrachloroethane *Tetrachloroethene *Toluene	220 1100	300 1000	420 660 -	360 670 -	240 630 -	220 580 -	620	200 420 -	
*Trichlorobenzene *1,1,1-Trichloroethane	12	- 6	18	16	13	11	12	- 6	
*1,1,2-Trichloroethane	6	5≥	12	8	10	11 ≤5	6	≤5	
*1,1,2-Trichloroethene *Benzene	1500	1500	770	760 -	740	630 -	680 -	420 -	
*Diisoctylphthalate *Phenol		:	-	-	-	-	-	٠ -	
*2,4,6-Trichlorophenol				-	-	-	-	-	
Methonol 1,1,1,2-Tetrachloroethane	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
*Ethylbenzene	_								
*Dichlorobenzene	-	-	-	-		-	-	-	
*Fluorene	-	-	-	-	-	-	-	_	
*Naphthalene	-	-	-	-	-	-	-	-	
*Dichloroethane	-	-	•	<u> </u>	-	-	-	-	
*Chloroethane *Vinyl Chloride	- ≤5	25	17	17	13	22	- 25	- 25	
Trichlorofluoromethane	-	-		-	-	-	-	-	•
TOTAL	3356 99.0%	3265	2512	2291	1695	1843	2038	1345	
	3310.5	97.3% average	97.6% 2401.5	97.8% average	97.0% 1769	97.1% average	97.2% 1691.5	96.2% average	

<sup>(1)</sup> North well down for a time on 5/27/81

<sup>(2)</sup> North well sampled 7:00 A.M. on 5/28/81, south well down; south well on a 10:00 P.M. and sampled in evening.

<sup>(3)</sup> Procedure used will not detect methanol

TABLE XVII
SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES
(ppb)

		6/3/81 WELL (2pumps) VOA		6/12/81 WELL (2pumps) VOA		6/19/81 WELL (2pumps) VOA		6/25/81 WELL (2pumps) VOA	
COMPOUND	N	S	N	S	N	. \$	N	S	
*BHC (Hexachlorocyclohexane)	- <u>-</u>	.:		.:					
*Carbon Tetrachloride	29	53	41	69	54	78	43	160	
*Chloroform *Dibutylphthalate	390	190	710	240	730	280	730	480	
*Dichloroethenes	≤10	<u>≤</u> 10	≤10	-	<u>≤</u> 10	<u>≤</u> 10	<u>≤</u> 10	<u>&lt;</u> 10	
Dioctyladipate		_	_				-		
*Dioctylphthalate	-	-	-	-	-	-	-	-	
*Fluoranthene	-	-	-	-	-	-	-	-	
*Hexachloro-1,3-butadiene *Hexachloroethane	:	=	-	:		-	=	-	
*Methylene Chloride *Monochlorobenzene	18	18	-	-	15	16	42	29	_
Pentachlorobutadiene	<u>-</u> 5	_≤5	•	-	- :	-	-	-	
Pentachloroethane	-	-	-			-	-	-	
*Phenoanthrene/Anthracene	-	-	-	-	-	-	-	-	
*Pyrene	-	-	-				-	-	
Tetrachlorobutadiene	260	150	160		160		* 100	-	
*1,1,2,2-Tetrachloroethane *Tetrachloroethene	260 490	150 400	160 4000	110 1500	160 2100	110 1300	180 2300	350 2100	
*Toluene	-	+00	4000	1500	-	-	-	-	
*Trichlorobenzene *1,1,1-Trichloroethane	- 9	<b>-</b> ≤5		-	17	- :	12	19	
*1,1,2-Trichloroethane	≤10	ىن 10≥	-		≤10	_	≤10	≤10	
*1,1,2-Trichloroethene	520	400	2900	1300	2400	1200	2700	3000	
*Benzene	≤10	≤10	-	19	-		-	-	
*Diisoctylphthalate	-	-	-	-	-	-	-	-	
*Phenol *2,4,6-Trichlorophenol	-	-	:	-	-	:	-	-	
Methonol	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
1,1,1,2-Tetrachloroethane	-	-	-	-	-	-	-	-	
*Ethylbenzene	-	-	-	-	-	-	-	-	
*Dichlorobenzene *Fluorene	-		-		-	-	-	-	
*Naphthalene	-			-	-	-	:	-	
*Dichloroethane	-	•	10	-	-	-	-	-	
*Chloroethane *Vinyl Chloride	- 15	17		-		-	<i>-</i> :	-	
Trichlorofluoromethane	-	17	13	33	56	94	61	8 <b>9</b> -	
TOTAL Top 5 compounds	1766 95.6% 1517	1268 94.1% average	7844 99.6% 5557.5	3271 98.4% average	5552.5 98.1% 4320	3088 96.6% average	6088 98.1% 6167.5	6247 97.5% average	

<sup>(3)</sup> Procedure used will not detect methanol

DLC/vrp 10/22/81

TABLE XVIII
SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		7/1/81 WELL (2pumps) VOA -		7/10/81 WELL (2pumps) VOA		7/15/81 WELL (2pumps) VOA		7/22/81 WEĻL (2pumps) VOA		7/29/81 WELL (2pumps) VOA
COMPOUND	N	S	N	S	N	. \$	N	S	N	S
*BHC (Hexachlorocyclohexane)				_	_	-	-	-	_	
Carbon Tetrachloride	34	78	81	170	29	270	34	320	26	
*Chloroform	570	280	740	370	770	490	860	480	640	420
*Dibutylphthalate *Dichloroethenes		:	:	-	- ≤5	-	_ _<5	<u>-</u> _<5	:	-
Dioctyladipate	-			-	_		-			
*Dioctylphthalate	-	-	-	-	-	•	-	-	-	-
*Fluoranthene	-	-	-	-	-	-	-	-	-	-
*Hexachloro-1,3-butadiene *Hexachloroethane	-	:	-	-	-	-	-		-	-
*Methylene Chloride	-	-		-	-	-	-	-	-	-
*Monochlorobenzene Pentachlorobutadiene	-	-	-	-	-	-	-	-	-	-
Pentachloroethane	-	-	-	· -	•	•	-	-	-	-
*Phenoanthrene/Anthracene	-	-	-	-	:	-	-	:	-	-
Pyrene	-	-	-	-	-		_	-	-	-
Tetrachlorobutadiene			-						-	-
*1,1,2,2-Tetrachloroethane *Tetrachloroethene *Toluene	100 1800 -	170 2700	280 2800 -	510 3000 -	540 2800 -	1400 5900	290 2700	1700 7100 -	230 2400 -	560 3200 -
Trichlorobenzene				-		-	17	37	10	26
<pre>*1,1,1-Trichloroethane *1,1,2-Trichloroethane *1,1,2-Trichloroethane *Benzene</pre>	≤5 ≤10 2600 -	3100	3800 -	22 ∡10 4800 -	15 ≤10 4300 -	38 12 6900	10 4400	7100 7100	3400	∡10 5300
*Diisoctylphthalate	-	_		-	_		-			
Phenol	-	-	-	-	-	-	-	-	-	- :
*2,4,6-Trichlorophenol Methonol 1,1,1,2-Tetrachloroethane	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)
*Ethylbenzene	-	-		_		_	_		_	-
Dichlorobenzene	-	-	-	-	-	-	-	-	-	-
*Fluorene	-	-	-	-	-	-	-	- :	-	-
Naphthalene Dichloroethane	Ξ	:	-					:	-	-
*Chloroethane *Vinyl Chloride Trichlorofluoromethane	10	12	10	11	16	23	21	23	15	24
TOTAL	5134 99.5%	6348 99.7%	7228 99.7%	8838 99.5%	8485 99.5%	15033 99.8%	8377 99.4%	16777 99.5%	6721 99.6%	9750 99.4%

<sup>(3)</sup> Procedure used will not detect methanol

DLC/vrp 10/22/81

TABLE XIX SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		8/5/81 WELL (2pumps) VOA*		8/13/81 WELL (2pumps) VOA		8/19/81 WELL (2pumps) VOA		8/26/81 WELL (2pumps) VOA	
COMPOUND	N	S	N	S	N	. s	N	S	
*BHC (Hexachlorocyclohexane	) -				-			-	
*Carbon Tetrachloride	9		10		26		29	170	
*Chloroform	350	260	390	250	600	290	640	360	
*Dibutylphthalate *Dichloroethenes	≤5	:	-	-	-	-	<u>-</u> ≤5	:	
Dioctyladipate	٠.	_	-	-			-	· -	
*Dioctylphthalate	-	-	-	-	-	-	-	-	
*Fluoranthene	-	-	-	-	-	-	-	-	
*Hexachloro-1,3-butadiene *Hexachloroethane	-	-	-	:	-	-	-	:	
*Methylene Chloride	-	-	-	:	12	8	90	25	
*Monochlorobenzene Pentachlorobutadiene	-	_	_					-	
Pentachloroethane	_	_	_	_		_		_	
*Phenoanthrene/Anthracene	•	-	-	-	-	-	-	-	
*Pyrene	-	-	-		-	-	-	-	
Tetrachlorobutadiene	110	310	100	340	180	390	180	440	
*1,1,2,2-Tetrachloroethane *Tetrachloroethene *Toluene	1000		1100		1800	1800	1800	2500	
*Trichlorobenzene	-			_	-	_	-	_	
*1,1,1-Trichloroethane	-	18	-	18	-	14	-	20	
*1,1,2-Trichloroethane	1200	≤5 2100	1400	≤5 2100	2100	2400	2100	2600	
*1,1,2-Trichloroethene *Benzene	1300	-	1400	-	2100	-	-	-	
*Diisoctylphthalate	:	- :	:	-		:	-	:	
*Phenol *2,4,6-Trichlorophenol	_	-	_	-	-	_	-	_	
Methonol 1,1,1,2-Tetrachloroethane	(3)	(3)	(3)	(3)	(3)	(3)	(3)	(3)	
*Ethylbenzene		-		_	-	-	-	-	
*Dichlorobenzene	-	-	-	-	-	-	-	-	
*Fluorene *Naphthalene	-	-	- :		:	:	-	-	
*Dichloroethane		-		-	-	-	-	-	
*Chloroethane	-		- 6	11	15	- 19	- 18	- 27	
*Vinyl Chloride Trichlorofluoromethane	8	-	-	-		-	-		-
TOTAL Top 5 compounds	2782 99.5% 3811.5	4841 99.5% average	3006 99.5% 3870	4734 99.3% average	4738 99.3% 4882	5026 99.2% average	4862 98.9% 5504	6147 98.8% average	

<sup>(3)</sup> Procedure used will not detect methanol

DLC/vrp 10/22/81

TABLE XX SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		9/9/81 WELL 2pumps) VOA		9/10/81 WELL 2pumps) VOA		9/17/81 WELL (2pumps) VOA		9/24/81 WELL (2pumps) VOA
COMPOUND	N	, 8	N	S	N	S	N	S
BHC (Hexachlorocyclohexane Enterproform Dibutylphthalate	600	130 270	<10 490 *	69 200 *	≤10 470 *	59 240 *	≤10 630 *	240
Oichloroethenes	<u>≤</u> 170	98 ————	≤180	74 	<u>&lt;</u> 140	120	<u>&lt;</u> 230	110
Oioctyladipate Oioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane	* * *	* * *	.* * *	* * * *	*	* * *	* * *	* * * *
Methylene Chloride Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene	≤10 * *	*	- - * *	- - * *	- * *	- * *	- - * *	- - * *
Pyrene Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene	190 1400	240 1500	160 1100	250 1400	160 1100	590 1700	, 400 1400	
Trichlorobenzene 1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene	* ≤10 ≤10 1800	±10 ≤10 1800	* - ≤10 1400	* ≤10 ≤10 1400	* ≤10 1500	± 10 ±10 1700	±10 ≤10 1900	* ≤10 ≤10 1700
Diisoctylphthalate ?henol 2,4,6-Trichlorophenol Methonol 1,1,1,2-Tetrachloroethane	* * *	* * *	* * * * *	* * * * * *	* * * *	* * *	* * *	* * * *
Ethylbenzene Dichlorobenzene Fluorene Naphthalene Dichloroethane	* * * -	* *	- * * -	* * * -	* *	- * *	- * * -	*
Chloroethane Vinyl Chloride Trichlorofluoromethane	11	16	12	11	≤10 —	15	19	14
TOTAL Top 5 compounds	4211 98.8% 4142.5	4074 96.7% average	3362 99.0% 3393	3424 97.1% average	3410 99.1% 3932	4454 97.9% average	4619 98.9% 4305	3991 97.5% average

DLC/vrp 11/3/81

<sup>-</sup> Not detected \* Procedure will not detect

# TABLE XXII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

-		(	10/23/81 WELL 2pumps) VOA	10/29/8 WELL (1pump) VOA		11/ 4/81 WELL (1pump) VOA	11/11/81 WELL (1pump) VOA
-	COMPOUND	N	S	N(1)	S N	S(2) N	S(2)
	BHC (Hexachlorocyclohexane Carbon Tetrachloride Chloroform	34 400	* 36 150	3 22		* * 17 370	
-	Dibutylphthalate Dichloroethenes	120	77	9	4 81	140	
_	Diocty.ladipate Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene 'Hexachloroethane	* * * *	* * * *		* * * * * * * * * * * *	*	
-	Methylene Chloride Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene	- * *	- * *		 * * * *	- - *	
-	Pyrene Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene	92 1100	* 67 820	6			
-	Trichlorobenzene 1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene	± - ≤10 1600	920	1300	780	1200 -	
	Diisoctylphthalate Phenol 2,4,6-Trichlorophenol Methonol 1,1,1,2-Tetrachloroethane	*	* * *		* *	* * * *	
	Ethylbenzene Dichlorobenzene Fluorene Naphthalene Dichloroethane	*	- * * -	***	* *	- * * -	
	Chloroethane Vinyl Chloride Trichlorofluoromethane	≤10	11	12	*	22	
_	TOTAL Top 5 compounds	3366 98.4% 2723.5	2081 97.7% average	- 2831 N/A% 98.3% N/A average	100.0%	- N/A% 98.8% average N/A	N/A% average

DLC/vrp 12/23/81

<sup>-</sup> Not detected \* Procedure will not detect (1) Plant shutdown, North well down (2) South well down

NOTE: Compounds detected on one occasion only and not quatitated have been omitted.

## TABLE XXIII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		11/19/81 WELL 2pumps) VOA		11/25/81 WELL (1pump) VOA	(	2/2/81 WELL 1pump) VOA		.2/9/81 WELL 1pump) VOA
COMPOUND	N	s 	N	S <sub>1</sub>	N	\$ <sup>1</sup>	N	2,1
BHC (Hexachlorocyclohexane) Carbon Tetrachloride	* 16	*	*		*		*	
Chloroform	560	29 240	20 250		14 240		64 240	
Dibutylphthalate	*	*	*		*		*	
Dichloroethenes	180	88	83		79		92	
Dioctyladipate	*	*	*		*		*	_
Dioctylphthalate	*	*	*		*		*	
Fluoranthene Hexachloro-1,3-butadiene	*	*	*		*		*	
Hexachloroethane	*	*	*		*		*	
Methylene Chloride							12	
Monoch1orobenzene	-	-	-		_		-	
Pentachlorobutadiene	*	*	*		*		*	
Pentachloroethane Phenanthrene/Anthracene	*	*	*		*		*	
Pyrene	*	*	*		*		*	
Tetrachlorobutadiene	*	*	*		*		*	
1,1,2,2-Tetrachloroethane Tetrachloroethene	120 1400	1100	800		55 9 <b>00</b>		56 760	
Toluene	-	-	-		-		760	
Trichlorobenzene	*	*	*		*		*	
1.1.1-Trichloroethane	-	-	-		-		-	
1,1,2-Trichloroethane	1000	1100	-		740		-	
1,1,2-Trichloroethene Benzene	1800 -	1100	800		740 -		690 -	
- Dfisoctylphthalate	*	*	*		*		*	
Pheno1	*	*	*		*		*	
Methonol 1,1,1,2-Tetrachloroethane	*	*	*		*		*	
Dichlorobenzene	*	*	*		*		*	
Fluorene	*	*	*		*		*	
Dichloroethane	•	-	-		-		-	
Vinyl Chloride Trichlorofluoromethane	-	19	-		12		12	
TOTAL Top 5 compounds	4076 99.6%	2896 98.3%	2133 99.1%	- -%	2040 98.7%	- -%	1926 95.8%	-%
, sp o compounts		verage	N/A	average		verage		verage

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 1/22/82

<sup>-</sup> Not detected \* Procedure will not detect (1) South well down

### TABLE XXIV SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		12/16/81 12/23/81 12/30/81						1/6/82	
	ı	12/16/81 WELL (2pumps) VOA		WELL (2pumps) VOA		WELL (2pumps) VOA		WELL (2pumps) VOA	
COMPOUND	N	s	N	s	N	S	N	s	
BHC (Hexachlorocyclohexane)	*	*	*	*	*	*	*	*	
Carbon Tetrachloride	16	33	≤10	50	≤10		23	80	
Chloroform	740	370	680		310		350	280	
Dibutylphthalate	*	*	*	*	*		*	*	
Dichloroethenes	220	150	160	170	87	81	120	120	
Dioctyladipate	*	*	*	*	*	*	*	*	
Dioctylphthalate	*	*	*	*	*		*	*	
Fluoranthene	*	*	*	*	*		*	*	
Hexachloro-1,3-butadiene	*	*	*	*	*		*	*	
Hexachloroethane		•	•			*	*	•	
Methylene Chloride	-	-	≤10	17	-	-	-	•	
Monochlorobenzene	-	•	-	-	-	-	-	-	
Pentachlorobutadiene	*	*	*	*	*		*	*	
Pentachloroethane	*	*	*	*	*	*	*	*	
Phenanthrene/Anthracene		•	*	•	•		•		
Pyrene	*	*	*	*	*		*	*	
Tetrachlorobutadiene	*	*	*	*	*	•	*	*	
1,1,2,2-Tetrachloroethane	260	240	230	400	95		110	210	
Tetrachloroethene Toluene	2200	1200	1700	1300	1000	1600	1300	1800	
							<u> </u>		
Trichlorobenzene	*	*	*	*	*	*	* ≤10	*	
1,1,1-Trichloroethane 1,1,2-Trichloroethane	≤ <b>1</b> 0	-	≤10	· ≤10	-	-	≤10 ≤10	13 ≤10	
1,1,2-Trichloroethene	3100	1500	2600	2100	1400	1400	1300	1600	
Benzene	-	-	-	-	-	•	-	-	
Didagahulahthalata	•	*	*	*	*	*	*	*	
Diisoctylphthalate Phenol	*	*	*	*	*	*	*	*	
Methanol	*	. *	*	*	*	*	*	*	
1,1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*	
Dichlorobenzene	*	*	*	*	*	*	*	*	
Fluorene	*	*	*	*	*	*	*	*	
Dichloroethane	-	-	-	-	-	-	-	-	
Vinyl Chloride	10	19	≤10	14	≤10	11	≤10	13	
Trichlorofluoromethane	*	*	*	*	-	*	*	*	
TOTAL	6556	3512	5410	4421	2922	3438	3233	4126	
Top 5 compounds	99.4%	98.5%	99.3%	98.0%	99.3%	98.9%	98.4%	97.2%	
	5034	average	4915.5	average	3180	average	3679.5	average	

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 2/12/82

A Report Francis

-- ---

12 **- 32**917-5

---

<sup>-</sup> Not detected \* Procedure will not detect

# SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	1/13/82 WELL (1pump) VOA		1/20/82 WELL (1pump) VOA	1/27/82 WELL (1pump) VOA	2/3/82 WELL (1pump) VOA	
COMPOUND	N	s	N(1) S	<sub>N</sub> (1) s	N(1) S	
BHC (Hexachlorocyclohexane)	*	*	* 70	*	*	
Carbon Tetrachloride	64 9 <b>50</b>	140 290	70 270	31 190	≤10 220	
Dibutylphthalate	*	*	*	*	*	
Dichloroethenes	140	150	170	88	92	
Dioctyladipate	*	*	:	*	*	
Oioctylphthalate Fluoranthene	*	*	*		*	
Hexachloro-1,3-butadiene	*	*	*	*	*	
Hexachloroethane	*	*	*	*	*	
Methylene Chloride		•		-	-	
Monochlorobenzene Pentachlorobutadiene	:	:	:	:	:	
Pentach loroethane	*	*	*	*	- #	
Phenanthrene/Anthracene	*	*	*	*	*	
Pyrene	*	*	*	*	*	
Tetrachlorobutadiene	200	380	310	* 9 <b>2</b>	* 65	
1,1,2,2-Tetrachloroethane Tetrachloroethene	1500	6800	1900	1100	1100	
Toluene	•	•	•	•	•	
Trichlorobenzene	*	*	*	*	*	
1,1,1-Trichloroethane 1,1,2-Trichloroethane	:	26	18	<b>≤10</b>	:	
1,1,2-Trichloroethene	2200	4700	2800	1000	1000	
Benzene				<u> </u>	<u> </u>	
Diisoctylphthalate	*	*	*	*	*	
Phenol	*	*	*	*	*	
Methanol 1,1,1,2-Tetrachloroethane	*	*	*	*	*	
Dichlorobenzene	*			*		
Fluorene	*	*	*	*	*	
Dichloroethane Vinyl Chloride	≤10	19	19	12	13	
Trichlorofluoromethane	*	**	*		*	
TOTAL	5064	12,505	N/A 5557	N/A 2523	N/A 2500	
Top 5 compounds	98.5% 8784.5	98.5% average	% 98.1% N/A average	% 97.9% N/A average	% 99.1% N/A average	
	0/04.3	averaye	MA average	WA average	mn average	

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

<sup>-</sup> Not detected \* Procedure will not detect (1) North Well Down

### TABLE XXVI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	(PPD)				
	2/10/82 WELL (1pump) VOA	2/18/82 WELL (1pump) VOA	2/19/82 <sup>(2)</sup> WELL (1pump) VOA	2/24/82 WELL (1pump) VOA	
COMPOUND	N (1) S	N(1) S	N(1) S	N(1) S	
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dibutylphthalate Dichloroethenes	43 210	12 180	± ≤10 160	± ≤10 200	
	120	92	58	97	
Dioctyladipate Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane	* *	* * *	*	*	
Methylene Chloride Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene	:	- - - - - -	- - * *	≤10 - + +	
Pyrene Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethane Toluene	64 1200	57 1000	* 43 560	58 1100	
Trichlorobenzene 1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene	930	780	* - 540	810	
Difisoctylphthalate Phenol Methanol 1,1,2-Tetrachloroethane Dichlorobenzene	* * * *	* * * * * * * * * * * * * * * * * * * *	* * * *	* * *	
Fluorene Dichloroethane Vinyl Chloride Trichlorofluoromethane	*  \$10 *	* =- \$10 *	* ≤10 *	10	
TOTAL Top 5 compounds	N/A 2577 3 97.9% N/A average	N/A 21_1 % 99.0% N/A average	N/A 1381 2 98.6% N/A average	N/A 2295 % 98.7% N/A average	

<sup>-</sup> Not detected

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

OLC/vrp 3/25/82

<sup>\*</sup> Procedure will not detect

(1) North Well Down

(2) Confirmation sample for Calgon carbon study, sampled for THO and did not have zero head space, may have lost some volatiles.

#### TABLE XXVII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		3/4/82 WELL 1pump) VOA		3/9/82 WELL 1pump) VOA		3/18/82 WELL 1pump) VOA	(	3/24/82 WELL (1pump) VOA	3/31 WEL (1pc VOA	.L imp)
COMPOUND	N <sup>1</sup>	s s	N <sup>1</sup>	S	N <sup>1</sup>	S	N <sup>1</sup>	s	N1	s
BHC (Hexachlorocyclohexane)	*	*	*	*	*	*	*	*	*	*
Carbon Tetrachloride		19		. <del>.</del>		13		60		60
Chloroform		2 <b>90</b>		64 *		260 *	_	22 <b>0</b>	_	260
Dibutylphthalate Dichloroethenes	•	160	*	46	·	160	Î	150	-	170
Dioctyladipate	*	*	*	*	*	*	*	*	*	*
Dioctylphthalate	*	*	*	*	*	*	*	*	*	*
Fluoranthene Hexachloro-1,3-butadiene	*		*	*	*	*		*	*	. *
Hexachloroethane	*	*	*	*	*	*	*	*	*	*
Methylene Chloride		-		-		_				-
Monochlorobenzene		-		- *	*	:	_	Ξ	*	-
Pentachlorobutadiene Pentachloroethane	*	*	*	*	*	*	*		*	*
Phenanthrene/Anthracene	*	*	*	*	*	*	*	*	*	*
Pyrene	*	*	*	*	*	*	*	*	*	*
Tetrachlorobutadiene	*	*	*	*	*	* 71	*	* 53	*	* 84
1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene		93 820 -		150 190 -		71 770 -		960 -		980
Trichlorobenzene	*	*	*	*	*	*	*	*	*	*
1.1.1-Trichloroethane		-		-		-		-		-
1,1,2-Trichloroethane				-						
1,1,2-Trichloroethene Benzene		650 -		160		590 -		740		760 -
Diisoctylphthalate	*	*	*	*	*	*	*	*	*	*
Phenol	*	*	*	*	*	*	*	*	*	*
Methanol 1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*	*	*
Dichlorobenzene	*	*	*	*	*	*	*	*	*	*
Fluorene	*	*	*	*	*	*	*	*	*	*
Dichloroethane Vinyl Chloride		•		-		-		13		11
Trichlorofluoromethane Ethyl Benzene		:		18		:		-		-
TOTAL	N/A	2032	N/A	628	N/A	1864	N/A	2196	N/A	2325
Top 5 compounds	N/A	99.1% average	%	97.1% average	N/A	99.3% average	N/A	97.0% average	N/A	97.0% average

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 4/29/82

a galaria

يعرف المساء

----

- .--- . ·

<sup>-</sup> Not detected \* Procedure will not detect (1) North Well Down

#### TABLE XXVIII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		4/7/82 WELL 2 pumps) VOA		4/14/82 WELL 2 pumps) VOA		4/21/82 WELL 2 pumps) VOA		4/28/82 WELL (2 pumps VOA
COMPOUND	N	s	N	s	N	\$	N	S
BHC (Hexachlorocyclohexane)	*	*	*	*	*	*	*	*
Carbon Tetrachloride	40	40	2 <b>2</b>	22	42	42	47	49
hloroform	430	90	300	61	510	120	570	130
Dibutylphthalate Dichloroethenes	140	* 66	100	44	180	* 64	210	* 88
Tichtoroethenes	140			44	180		210	88
Dioctyladipate	*		*	*	*	*	*	*
Dioctylphthalate	*	*	*	*	*	*	*	*
luoranthene	*	*	*	*	*	*	*	*
Hexachloro-1,3-butadiene Hexachloroethane	*	*	*	*	*	*	*	*
Methylene Chloride								_
Monochlorobenzene	-	-	-	-	-	-	-	-
Pentachlorobutadiene	*	*	*	*	*	*	*	*
Pentachloroethane	*	*	*	*	*	*	*	*
Phenanthrene/Anthracene	*	*	*	*	*	*	*	*
yrene	*	*	*	*	*	*	*	*
「etrachlorobutadiene	*	. *	*	*	*	*	*	*
,1,2,2-Tetrachloroethane	120	52	88	45	130	82	170	72
[etrachloroethene [oluene	1300	730 -	750 -	450 -	1400	800	1900	920
Trichlorobenzene		*		*	*	*	*	•
1.1.1-Trichloroethane	-	-	-	-	-	-	-	
1,1,2-Trichloroethane	-	-	-	-	-	-	-	
1,1,2-Trichloroethene	1800	500	990	300	1800	540	2400	670
Benzene 	-					-	-	•
Diisoctylphthalate	*	*	*	*	*	*	*	
Phenol	*	*	*	*	*	*	*	*
Methanol	*	*	*	*	*	*	*	*
1,1,1,2-Tetrachloroethane Dichlorobenzene	*	*		*		*	*	•
Fluorene		*	*		*	*	*	*
Dichloroethane	-	-	-	-	-	-	-	
Vinyl Chloride	≤10	-	-	-	-	-	-	
Trichlorofluoromethane <sup>1</sup>		_	-	-	-	-	-	
	≤10							
TOTAL	3850	1478	2250	922	4062	1648	5297	1929
TOTAL		1478 97.3% average	2250 99.0% 1586	922 97.6% average	4062 99.0% 2855	1648 97.4% average	5297 99.1% 3613	1929 97.5% average

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 5/24/82

44.00

<sup>-</sup> Not detected
\* Procedure will not detect
1 Identified as dichlorodifluoromethane

#### TABLE XXIX SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	(1	/5/82 ⊮ELL pump) VOA		5/12/82 WELL I pump) VOA	(1	/19/82 ⊮ELL pump) √OA		5/26/82 WELL 1 pump) VOA
COMPOUND	N1	S	N1	s	N1	S	N1	S
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform	*	* 14 200	*	* 21 160	*	* 28 180	*	* 29 210
Dibutylphthalate Dichloroethenes	*	100	*	94	*	110	*	130
Dioctyladipate Dioctylphthalate	*	*	*	*	* *	*	*	*
Fluoranthene	*	* *	*	*	*	*	*	*
Hexachloro-1,3-butadiene Hexachloroethane	*	*	*	*	*	*	*	*
Methylene Chloride Monochlorobenzene	-	-	-	-	-	-	-	_
Pentachlorobutadiene	*	*	<del>-</del>	<del>-</del>	*	*	*	- *
Pentachloroethane	*	*	*	*	*	*	*	*
Phenanthrene/Anthracene		. *	*			*		*
Pyrene Tetrachlorobutadiene	*	*	*	*	*	*	*	*
1,1,2,2-Tetrachloroethane		100	-	50		51	•	45
Tetrachloroethene Toluene	-	1000	-	60 <b>0</b> -	-	850 -	-	640 -
Trichlorobenzene	*	*	*	*	*	*	*	*
1,1,1-Trichloroethane	-	-	-	-	-	-	-	-
1,1,2-Trichloroethane 1,1,2-Trichloroethene	-	630	-	590	-	650	-	700
Benzene	-	-	-	-	-	-	-	-
Diisoctylphthalate	*	*	*	*	*	*	*	*
Phenol Methanol	*	*	*	*	*	*	*	*
1,1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*
Dichlorobenzene	*	*	*	*	*	.*	*	*
Fluorene	*	*	*	* .	*	*	*	*
Dichloroethane Vinyl Chloride Trichlorofluoromethane	-	≤10 -	-	≤10 -	-	10	-	10
TOTAL Top 5 compounds	NA a	2054 98.8% verage	NÄ ä	1525 98.0% average	NA av	1879 98.0% verage	% NĀ a∙	1764 97.8% verage

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 6/21/82

40.40 40.5

The second section with the second

<sup>-</sup> Not detected \* Procedure will not detect <sup>1</sup> North well down

#### TABLE XXIX SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	(1	/5/82 /ELL pump) /OA	(1	/12/82 WELL pump) VOA	(1	19/82 (ELL pump) (OA		5/26/82 WELL 1 pump) VOA
COMPOUND	N1	s	N <sup>1</sup>	S	N <sup>1</sup>	s	N <sup>1</sup>	S
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dibutylphthalate Dichloroethenes	*	14 200 *	*	21 160 *	*	28 180 *	*	29 210 *
Dioctyladipate Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane	* * * *	* * * *	* * * *	* * * *	* * * *	* * * *	* * *	* * *
Methylene Chloride Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene	- * *	*	- * *	- * *	- * *	- * *	- * *	- * *
Pyrene Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene	*	100 1000	*	* 50 600	*	51 850	* *	* 45 640
Trichlorobenzene 1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene	• - -	630	* - -	* - 590	* - -	* - 650	* - -	* - 700
Diisoctylphthalate Phenol Methanol 1,1,2-Tetrachloroethane Dichlorobenzene  Fluorene	* * * * *	* * * * * * * * * * * * * * * * * * * *	*	* * * *	* * * * * * * * * * * * * * * * * * * *	* * * *	* * * * *	*
Dichloroethane Vinyl Chloride Trichlorofluoromethane	<u>•</u> ·	≤10 -	:	≤10 ————————————————————————————————————	:	10	:	10
TOTAL Top 5 compounds	NA a	2054 98.8% verage	n <mark>X</mark>	1525 98.0% average	% NA a	1879 98.0% verage	NA a	1764 97.8% average

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 6/21/82

-

<sup>-</sup> Not detected \* Procedure will not detect 1 North well down

### SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

	(2	2/82 /ELL pumps) /OA	(2	/9/82 √ELL pumps) √OA	(2	l6/82 √ELL pumps) /OA		/23/82 WELL 2 pumps) VOA		29/82 ⊮ELL pumps) VOA
COMPOUND	N	S	N	S	N	S	N	S	N .	S
HC (Hexachlorocyclohexane) arbon Tetrachloride	* 32	* 30	* 26	* 340	* 28	* 440	* 16	* 240	* 16	* 210
hloroform	620	300	810	720	790	580	390	310	390	270
ibutylphthalate ichloroethenes	* ≤450	120	350 350	* ≤290	* ≤460	* ≤160	<b>±</b> ≤210	<b>*</b> ≤290	<b>*</b> ≤22D	* ≤260
ioctyladipate	*	*	*	*	*	*	*	*	*	*
ioctylphthalate luoranthene	*	*	*	*	*	*	*	*	*	*
exachloro-1,3-butadiene exachloroethane	*	*	*	*	*	*	*	*	*	*
ethylene Chloride	-	-		-	-			≤10 ≤10	≤10 ≤10	≤10 ≤10
onochlorobenzene entachlorobutadiene	- *	*	*	<del>-</del>	*	* 710	710	* 710	*	±
entachloroethane	*	*	*	*	*	*	*	*	*	*
henanthrene/Anthracene	*	*	*	*	*					
yrene	*	*	*	*	*	*	*	*	*	*
etrachlorobutadiene ,1,2,2-Tetrachloroethane etrachloroethene oluene	240 1400	120 1000	190 1500	560 1500	170 1500	360 2000 -	142 760	22 540 -	35 780 -	190 1000 -
					•					
Trichlorobenzene 1,1,1-Trichloroethane	* 11	*	* ≤10	. *	* ≤10	* 20	* 10	* 24	10	*
1,1,2-Trichloroethane	10	-	-		-	≤10	-	≤10	-	- ≤10
1,1,2-Trichloroethene Benzene	1900	910 -	1700	2400 ≤10	1700	2200 ≤10	960 -	1300 ≤10	950 ≤10	1100 ≤10
Diisoctylphthalate	*	*	*	*	*	*	*	*	*	*
Phenol Methanol	*	*	*	*	*	*	*	*	*	- * *
1,1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*	*	*
Dichlorobenzene	*	*		*	*	*	*	*	*	*
Fluorene	*	*	*	*	*	*	*	*	*	*
Dichloroethane Vinyl Chloride	23	17	20	21	35	16	12	13	11	10
Trichlorofluoromethane		•		-	-	•		•	-	-
TOTAL Top 5 compounds	4686	2497	4606	5861	4693	5806	2410	2779	2442 97.3%	3090
Top 5 compounds	98.4% 3591.5	93.3% average	98.8%	94.5% average	98.4% 5249.5	96.1% average	98.0% 2594.5	96.4% average		96.1% average

<sup>-</sup> Not detected

<sup>\*</sup> Procedure will not detect

<sup>■</sup> NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

A sample for priority pollutant scan collected on 6/17/82 is not shown due to improper and incomplete analysis by the outside laboratory.

<sup>-</sup> OLC/vrp 8/27/82

# TABLE XXXI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

-		7/7/82 WELL Pumps) VOA		7/14/82 WELL 2 pumps) VOA	(	7/21/82 WELL 2 pumps) VOA		7/28/82 WELL (2 pumps) VOA
COMPOUND	N	S	N	\$	N	s	N	S
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dibutylphthalate Dichloroethenes	20 310 *	* 94 190 * ≤140	36 390 * ≤140	* 150 310 * ≤200	38 530 *	* 77 190 *	35 580 *	150 270 *
Dioctyladipate Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane	* * * *	* * * *	* * * *	* * *	* * *	* * * *	* * * *	* * * * *
Methylene Chloride Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene	- * *	- * *	≤10 * *	- * *	- * *	- * *	330 13 *	≤10 *
Pyrene Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene	96 500	140 690	180 650	200 1000	130 1200	240 1100	120 1100	* 180
Trichlorobenzene 1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene	* ≤10 ≤10 710	13 820	* 11 ≤10 820	* 24 ≤10 970	18 1200	* 14 ≤10 1100	18 1100	22
Diisoctylphthalate Phenol Methanol 1,1,1,2-Tetrachloroethane Dichlorobenzene	* * * *	* * * *	* * * * *	* * * *	* * * *	* * * *	* * * *	* * * * *
Fluorene Dichloroethane Vinyl Chloride Trichlorofluoromethane	* 19	21	23	18	* 19	* - 13	210	16
TOTAL Top 5 compounds	1776 96.7% 1942 a	2108 93.9% verage	2270 96.0% 2576	2882 93.0% average	3305 97.7% 3169.5	3034 96.2% average	3646 91.1% 3387	3128 93.7% average

NOTE: Compounds detected on one occasion only and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 3/27/82

<sup>-</sup> Not detected \* Procedure will not detect

### TABLE XXXII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		8/4/82 WELL 2 pumps) VOA	(	8/11/82 WELL 2 pumps) VOA		8/18/82 WELL 2 pumps) VOA		8/19/82 WELL (2 pumps) VOA	(	8/25/82 WELL 2 pumps) VOA
COMPOUND	N	\$	N	\$	N	S	N	\$	N	s s
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	* ≤10 160 46 *	42 120 84	23 380 110	67 110 26	* 87 680 ≤430	220 490 520	16 280 40	39 100 76	13 310 54	48 11 59
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	*	* * * -	* * *	*	* * *	*	* * *	* * *	* * *	: :
Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene Pyrene	*	*	:	*	14	≤10 * *	≤10 * * *	- * * *	10	* * * *
Tetrachiorobutadiene 1,1,2,2-Tetrachioroethane Tetrachioroethene Toluene Trichlorobenzene	96 280 -	200 620 -	76 1200	200 900 -	160 1900	450 3900 -	100 860	120 670	100 1100	150 770
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene Diisoctylphthalate	380	600	≤10 1400	≤10 ≤10 1100	12 11 2500 ≤10	≤10 ≤10 4000 ≤10	≤10 ≤10 1200 ≤10	≤10 690	≤10 ≤10 1400 ≤10	≤10 780
Methanol 1,1,1,2-Tetrachloroethane Dichlorobenzene Dichloroethane Vinyl Chloride	* * * ≤10	* * * ≤10	* * - 38	* * * *	* * * - ≤50	* * - 50	* * 18	* * * - ≤10	* * - 24	* * * - ≤10
Trichlorofluoromethane	-	-	-	-	•	-	-	-		•
TOTAL Top 5 compounds	982 98.0% 1329	1676 96.9% average	3237 97.8% 2830	2423 98.1% average	5854 98.3% 7737	9620 99.1% average	2554 97.1% 2134.5	1715 96.6% average	3041 97.5% 2489	1937 98.4% average

NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 10/27/82

<sup>-</sup> Not detected \* Procedure will not detect

### TABLE XXXIII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		9/1/82 WELL 2 pumps) VOA		9/8/82 WELL 2 pumps) VOA		/15/82 WELL 2 pumps) VOA		9/22/82 WELL (2 pumps) VOA		/29/82 WELL 2 pumps) VOA
COMPOUND	N	s	N	\$	N	\$	N	S	N	s
8HC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	14 250 35	80 160 100	42 400 ≤120	120 250 ≤150	31 530 ≤160	* 86 200 ≤200	23 440 ≤150	* 72 170 ≤180 *	36 410 ≤170	* 88 200 ≤210
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	* * * 41	* * * * 14	* * *	* * *	* * * 12	* * * * * -	*	* * * -	* * * 30	* * *
Monochiorobenzene Pentachiorobutadiene Pentachioroethane Phenanthrene/Anthracene Pyrene	14 * * * * *	*	* *	*	*	*	10	*	16 * *	* * *
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene Trichlorobenzene	150 1200	170 1200	99 1400 - *	140 860	59 1900	75 800 -	70 1200	70 730 -	120 2100	150 800
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene Diisoctylphthalate	≤10 ≤10 1100	≤10 1100	16 ≤10 1400 -	≤10 ≤10 880	12 2200 -	≤10 830	≤10 1300 ≤10	≤10 740 	17 2400 ≤10 *	12 ≤10 800
Methanol 1,1,1,2-Tetrachloroethane Dichlorobenzene Dichloroethane Vinyl Chloride	* * 17	* * *	* * *	* * - -	* * - 61	*	* *	* * -	*	* * *
Trichlorofluoromethane		-	-	-	-	•	•		-	-
TOTAL Top 5 compounds	2841 96.5% 2844.5	2848 95.9% average	3537 96.7% 2978.5	2420 98.8% average	4975 98.7% 3588	2201 99.1% average	3213 98.8% 2592.5	1972 99.0% average	5309 99.0% 3789.5	2270 98.6% average

NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 10/27/82

<sup>-</sup> Not detected \* Procedure will not detect

#### TABLE XXXIV SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		10/8/82 WELL (2 pumps) VOA		10/13/82 WELL (2 pumps) VOA		10/21/82 WELL (2 pumps) VOA		10/26/8 WELL (1 pump VOA
COMPOUND	. N	S	N	S	N	S	N	
BHC (Hexachlorocyclohexane)	*	*	*	*	*		*	
Carbon Tetrachloride	39 400	170	49		18		52	
Chloroform Dichloroethenes	400 ≤160	170 ≤370	.400 ≤160		310 ≤110		250 ≤130	
Dioctyladipate	*	*	*	* 2100	*	* *	* =130	
Dioctylphthalate	*	*	*	*	*	*	*	
Fluoranthene	*	*	*	*	*	*	*	
Hexachloro-1,3-butadiene	*	*	*	*	*	*	*	
Hexachloroethane Methylene Chloride	-	-	140	-	-	-	-	
icnochlorobenzene	17		24		≤10		≤10	
Pentachlorobutadiene	*	*	*	*	*	*	*	
Pentachloroethane	*	*	*	*	*	*	*	
Phenanthrene/Anthracene Pyrene	*	*	*	*	*	*	*	
Tetrachlorobutadiene	*	*	*	*	*	*	*	
1,1,2,2-Tetrachloroethane	160	150	130	130	130	120	120	
Tetrachloroethene	840	770	820	670	680	660	730	
Toluene Trichlorobenzene	*	*	*	*	*		*	
,1,1-Trichloroethane	15	10	21	13	≤10 ≤10		≤10 ≤10	
,1,2-Trichloroethane	≤10 050	≤10 800	10 880	≤10 650	≤10 740	≦10 580	≦10 750	
,1,2-Trichloroethene	950 ≤10	≥10	14	-	740	-	, 50	
enzene Hisoctylphthalate	*	*	*	*	*	*	*	*
lethanol	*	*	*	*	*	*	*	*
,1,1,2-Tetrachloroethane	*	*	*	*	*	*	*	*
Dichlorobenzene	*	*	*	*	*	<b>π</b>	*	*
Dichloroethane /inyl Chloride	-	-	Ξ	:	-	-		
Trichlorofluoromethane	-	-	-	-	-	-	-	
TOTAL	2601	2359 95.4%	2648 95.2%	1896 94.4%	2018 97.1%	1656 96.6%	2062 95.5%	N/A
Top 5 compounds	96.1% 2480	average	2272	average	1837	average	N/A	11//

OLC/vrp 11/30/82

<sup>-</sup> Not detected
\* Procedure will not detect

<sup>■</sup> NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

### TABLE YYXY SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (pob)

		11/4/32 WELL (1 oump) VOA		11/10/32 WELL (1 pump) VCA		11/17/82 WELL (1 pump) VOA		11/24/82 HELL (C summs) YOA
COMPOUND			į:	S	۸	s	X	\$
SHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	58 230 130		38 160 85	•	40 200 110		29 290 ≤130	* 54 130 ≤91 *
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	* * * * * * * * * * * * * * * * * * * *	* * *	* * * -	* * *	*	*	:	* * * * * *
Fonochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene Pyrene	- * *	* *	- * *	* * *	*	* *	*	· ·
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachlornethene Toluene Trichlorobenzene	140 980 -	*	74 720 -	*	56 720		46 800 -	73 650
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethane Benzene Diisoctylphthalate	≤10 1100	*	690 - *	*	≤10 - 650 -	*	≤10 730 -	≤10 580 -
Methanol 1.1.1.2-Tetrachloroethare Dichlorobenzene Dichloroethane Vinyl Chloride	* * * <100	:	* * * ≤100	:	* * * 20	:	* * - 14	26
Trichlorofluoromethane	•		-		-			•
TOTAL Top 5 compounds	42748 93.4% N/A	average	≤1867 94.0% N/A	average	≦1806 96.1% N/A	average	≤2049 97.4% 1831.5	≤1614 94.4 average

MOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 1/3/83

<sup>-</sup> Not detected \* Procedure will not detect

TABLE XXXVI SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		12/2/82 WELL Pumps) VOA		12/8/82 WELL 2 pumps) VOA		2/16/82 WELL 2 pumps) VOA		12/23/82 WELL 2 pumps) VOA		12/30/82 WELL (2 pumps) VOA
COMPOUND	N	s	N	s	N	s	N	s	N	s
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	* 34 350 ≤150	* 43 100 ≤81 *	23 250 41	64	36 240 110	66 44 ≤65	* 44 240 ≤90	* 38 41 ≤54	* 33 340 ≤180	* 21 47 ≤59
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	* * * * * * * * * * * * * * * * * * * *	* * *	•	* * * * -	*	* * *	* * *	* * *	*	* * *
Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene Pyrene	*	* * *	•	*	:	:	*	:	≤10 * * *	:
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene Trichlorobenzene	100 810	62 560 -	180 830	48 450	160 410	\$ 59 820	60 840	52 690	110 1100 -	27 310
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene Diisoctylphthalate	11 1000	≤10 - 440 - *	10 ≤10 740	540	430	≤10 710	≤10 ≤10 510	≤10 ≤10 520	≤10 ≤10 1200 -	≤10 ≤10 210
Methanol 1,1,1,2-Tetrachloroethane Dichlorobenzene Dichloroethane Vinyl Chloride	* * 15	* * * - 20	* * - 22	20	* * * ≤10	* * * - 25	* * 14	27	* * * - 13	* * * 25
Trichlorofluoromethane  TOTAL Top 5 compounds	2470 97.6% 1893	1316 94.4% average	2106 96.9% 1649	1192 97.23 average	1396 96.7% 1597.5	1799 95.6% average	1818 95.7% 1630	1442 94.1 average	3006 97.5% 1862.5	719 90.3% average

NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 1/31/83

<sup>-</sup> Not detected \* Procedure will not detect

#### TABLE XXXVII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		1/5/83 WELL pumps) VOA		/12/83 WELL pumps) VOA	1/	19/83 WELL pumps) VOA		/27/83 WELL Pumps) VOA
COMPOUND	N	S	N	\$	N	S	N	S
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	* 33 300 190 *	* 28 100 93 *	22 320 150	* 23 94 94	27 190 130	34 110 100	27 280 180	* 30 94 120 *
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	* * *	* * * -	* * * * *	* * * -	* * *	* * *	* * *	* * * -
Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene Pyrene	- * * *	- * * *	* * *	- * * *	- * *	* * *	- * * *	- * * *
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene Trichlorobenzene	140 920 -	* 46 940 - *	* 97 830 - *	* 50 320 - *	100 1100	* 38 540 - *	170 1400	54 560 -
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene Diisoctylphthalate	10 5.1 880 -	- 800 - *	11 6.7 1000	270	11 5-9 1200 -	9.2 - 450 -	11 6.5 1400	5.4 - 480 -
Methanol 1,1,2-Tetrachloroethane Dichlorobenzene Dichloroethane Vinyl Chloride	* * - 14	* * * 22	* * * -	* * *	* * *	* * - 19	* * * - 13	* * * - 22
Trichlorofluoromethane	-	-	-	-	-	-	-	-
TOTAL Top 5 compounds	2492.1 97.5% 2260.6	2029 97.5% average	2436.7 98.4% 1649.9	863 95.9% average	2763.9 98.4% 2032.1	1300.2 95.2% average	3487.5 98.4% 2426.45	1365.4 95.8 average

NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 3/15/83

<sup>-</sup> Not detected \* Procedure will not detect

# TABLE XXXVIII SUMMARY OF ORGANIC ANALYSES ON VARIOUS SAMPLES (ppb)

		2/2/83 WELL pump) VOA	(1 p	ELL	2/16 WE (1 pu VO	LL mp)	(1 p	3/83 ELL ump) OA
COMPOUND	N	S	N	S	N	\$	N 	S
BHC (Hexachlorocyclohexane) Carbon Tetrachloride Chloroform Dichloroethenes Dioctyladipate	*	27 180 130	*	20 140 69	*	27 160 140	*	* 26 150 100 *
Dioctylphthalate Fluoranthene Hexachloro-1,3-butadiene Hexachloroethane Methylene Chloride	* * * *	* * *	* * *	* * *	* * *	* * *	* * *	* * * *
Monochlorobenzene Pentachlorobutadiene Pentachloroethane Phenanthrene/Anthracene Pyrene	* * *	- * * *	* * * *	* * *	* * *	- * * *	* * *	- * * *
Tetrachlorobutadiene 1,1,2,2-Tetrachloroethane Tetrachloroethene Toluene Trichlorobenzene	*	* 81 870 - *	*	* 67 590 - *	*	* 69 710 - *	*	* 68 640 - *
1,1,1-Trichloroethane 1,1,2-Trichloroethane 1,1,2-Trichloroethene Benzene Diisoctylphthalate	*	6.3 820 *	*	500	*	580	*	490
Methanol 1,1,1,2-Tetrachloroethane Dichlorobenzene Dichloroethane Vinyl Chloride  Trichlorofluoromethane	* *	* * * 22	* * *	15	* *	* * - -	* *	* * * - -
TOTAL Top 5 compounds	N/A -	2136.3 97.4% average	N/A	1401 97.5% average	N/A a	1713 96.8% average	N/A	1491 97.1% average

 ${\tt NOTE:}$  Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

DLC/vrp 3/15/83

<sup>-</sup> Not detected \* Procedure will not detect

### New York State Department of Environmental Conservation 600 Delaware Avenue Buffalo, NY 14202



CERTIFIED MAIL

Robert F. Flacke Commissioner

March 16, 1981

bcc: D. L. Cummings

A. F. Kapteina M. L. Norsworthy

V. M. Norwood

M. B. Sokolowski

L. B. Tew Env. File

Mr. C.W. Newton Olin Chemical Corporation 2400 Buffalo Avenue Niagara Falls, NY 14302

Re: Olin Corporation SPDES #NY 0001635

Contaminated Well Water Supply - Report

December 1, 1980

Dear Mr. Newton:

This Department has reviewed Olin's submitted reports on the contaminated well water supply. The following comments are forwarded and additional information requested.

- A specific explanation as to the source or cause of this organic contamination in the groundwater supply wells is requested. This was noticeably absent in the report.
- The report references "remedial surficial action" which when supplemented with continued pumping of the wells will result in flushing of the aquifer. Detailed information is requested regarding specifics of such a program and its expected consequences.

The possibility of extending the well casings from their present 38 ft. level down to a 75-100 ft. depth should be considered as a means to exclude upper bedrock aquifer contamination from entering these wells.

Olin's December 1, 1980 Report entitled "Monitoring Study - Contaminated Well Water Supply" has shown that the groundwater wells as a cooling water source have been shown to contribute organic loadings to the River in the range of 250 lbs/day through the outfalls. The Clean Water Act specifies that BAT requirements must be met for all discharges to navigable waters by July 1, 1984. As such, two well operation can continue with monthly Volatile Organics Analysis monitoring and semi-annual complete organic characterization to assess the effectiveness of this pumping on decontamination of the bedrock aquifer. However, the company should proceed with an alternate design to meet BAT by 1984 if pumping does not exhibit sufficient flushing to decontaminate the cooling water. This contingency plan

..\_\_\_.,\_\_

should be drawn up to allow for review and subsequent completion of necessary construction by early 1984. A compliance schedule will be recommended for inclusion in the renewal permit which would require an Engineering Report by October 1982, Final Plans by February 1983 and Completion of Construction by June 1984.

If you should have any questions concerning the above, please contact Angelo Sarkees at 842-5826. A meeting between this office and Olin representatives would be appropriate subsequent to your review of this letter and submission of the requested information.

Very truly yours,

Robert G. Speed P.E.

Regional Engineer for Water Quality

AJS:dd

cc: Mr. Nadler, Attn: Mr. Pallante

NCHD

Mr. Adamczyk

CALGON CARBON CORPORATION PITTSBURGH, PENNSYLVANIA

CARBON APPLICATION REPORT

PILOT COLUMN STUDY

Prepared for Olin Corporation

Niagara Falls, New York

RV.

R. J. Beile

DATE:

#### INTRODUCTION

This report summarizes the pilot column study in which granular activated carbon was evaluated for treating up to five million gallons per day of contaminated well water at Olin Corporation, Niagara Falls Production Facility. The pilot column study was performed by Olin Corporation, as directed by Calgon Carbon Corporation, from October 5, 1982 to termination on January 31, 1983. Daily samples were collected by Olin from each of the four (4) carbon columns connected in series plus the influent well water supply. Selected samples were analyzed for five volatile compounds by gas chromatography. Samples were analyzed by RECRA Environmental Laboratories and these results were interpreted by Calgon in this report.

The primary objectives of this pilot column study was to verify the minicolumn test data developed previously by Calgon that a ten minute contact time is sufficient to contain the priority pollutant organics in the well water and project a carbon usage rate.

#### CONCLUSION

The pilot column study verified that a ten (10) minute contact time was sufficient to contain the mass of priority pollutant organics below a total discharge limit of ten (10) pounds per day at a well water flow rate of 5 mgd. With six (6) adsorbers operating in parallel and a seven (7) day staggerred start-up of each adsorber, 52 truckloads (1,040,000 pounds of activated carbon) would be required to treat 5 mgd per year. A proportionally lower carbon usage rate is required at lower flow rates.

#### RECOMMENDATION

It is recommended that six (6) adsorbers be connected in parallel to process this water at a flow rate of 5 mgd. These adsorbers should be staggered at a seven day interval in start-up so that only one vessel is replaced at a time.

It is recommended that chloroform be utilized as the operational control parameter to provide indications when to change the lead bed.

Also, since there was a solids build up on the first pilot column that resulted in increased pressure drops, it is recommended that this concern be further addressed prior to installing the full scale system.

#### DISCUSSION

#### Mini-Column Study

From February 22 to March 2, 1982 "Mini-Column Feasibility Testing" was performed to evaluate granular activated carbon for the treatment of five million gallons per day of contaminated well water at Olin Corporation,

Niagara Falls Production Facility. The mini-column test, is presently called "Accelerated Column Test" (ACT), can predict carbon requirement in a few days of laboratory analysis where normally months of field work are required. An ACT was performed on samples of well water at a flow rate of 279 gpm and a twenty (20) minute contact time. Results of this test yielded the run time at which various organic compounds in the well water broke through the carbon. Of the total organic loading, five (5) volatile organic compounds broke through the column in a simulated 125-day period. The twenty (20) minute contact time was shown to be conservative and a shorter time needed to be evaluated. Using these results, a pilot column study was designed which evaluated four different contact times at a flow rate of 579 gpm.

#### PILOT COLUMN OPERATION

The pilot column study was designed to determine the optimum contact time which would contain the wavefront. Four (4) five-inch (5") diameter columns, used in this study were connected in series. Ninteen (19) pounds of activated carbon was placed in each column to simulate a five (5) minute contact time per column at a flow rate of one (1) gallon per minute. Therefore, the effluent emitted from Column II would have a ten (10) minute contact time and Column IV a twenty (20) minute contact time.

Olin operated the pilot column system and adjusted the flow rate to maintain approximately 1 gpm through the columns. Samples of the influent (see Table 2) and the effluent (see Table 3 through 5) streams were collected by Olin personnel. These samples were then submitted to RECRA Environmental Laboratories for analysis and the data is tabulated in the attached tables. This data was then used to calculate the carbon requirement for the system.

#### ANALYTICAL RESULT

Table 1 presents a list of the organic priority pollutants present in the well water during the pilot column study. Over the duration of the study, seventeen (17) weekly samples of the well water were collected and analyzed for the volatile organic compound list in Table 1. The high, low, and average result of these analyses are presented in the table.

The pilot carbon study verified, as previously demonstrated by the ACT, that five volatile compounds were the only organics to break through the columns, these being methylene chloride ( $CH_2Cl_2$ ), chloroform ( $CHCl_3$ ), (1,1-and 1,2-) Dichloroethylene ( $C_2H_2Cl_2$ ), and carbon tetrachloride ( $CCl_4$ ). Table 2 presents the concentrations of these compounds in the influent to the first carbon column over the duration of the study while Tables 3 through 5 present the columns effluent concentrations. As can be seen, the influent is highly variable which in turn is reflected in the column effluents. Previously collected data has shown there are day-to-day and well-to-well fluctuations in the concentrations of total volatiles

A summation of the total effluent concentration from each column is presented in Tables 6 and 7. These results are translated into pounds of organics discharged versus actual operating time (or total gallons treated) in Figure 1.

#### TREATMENT SYSTEM

The proposed carbon treatment system to remove organics from Olin's contaminated well water is six (6) adsorbers with 20,000 pounds of granular activated carbon per adsorber that are connected in parallel. An influent header would distribute the untreated water to each adsorber. Each adsorber would begin treatment on a prearranged staggerred start-up so that only one carbon bed would require replacement at a time. The effluent from each adsorber would then be connected to a discharge header to feed the plant operation.

Effluent Total Volatile Organics (TVO), for a normal ten (10) minute contact time, are summarized in Table 6 (plotted in Figure 2) for the treatment of 833,333 gpd. With six (6) adsorbers connected in parallel, the system would treat 5 mgd.

Olin final SPDES permit limitations (effective July 1, 1984) will allow them to discharge up to ten (10) pounds/day total organic priority pollutants. However, because of the fluctuations in the data, Olin requested the system be designed with a 20% safety factor or to achieve a maximum eight (8) pound/day organic limit in the effluent stream.

Based on a seven (7) day staggered start of the adsorbers and 5 mgd for 365 days, Olin would require 52 carbon changes per normally operating year or 1,040,000 pounds of granular activated carbon. The sum of the projected effluent quality from each adsorber based on Figure 2 for a ten (10) minute contact time is 7.4 pounds of TVO per day.

Figure 3 shows a comparison of TVO and chloroform versus cumulative operating time. For the first 42 days of operation, chloroform approximately matches TVO; after 43 days, the increase in 1,2 dichloroethylene increases the slope of the TVO curve. Chloroform is a good indicator of carbon exhaustion and is recommended as the control parameter.

#### PRECIPITATE CONCERN

During the pilot column study a precipitate accumulated on the carbon in Column I which resulted in the column having to be backwashed. In a large scale system this solid buildup could increase the pressure drop to the point that frequent backwashing would be required to maintain a reasonable pressure drop through the system.

The normal analytical test for determining the precipitates characteristics are:

- Alkalinity (CaCO<sub>3</sub>)
  - A. Phenolphthalein
  - B. Total
  - C. Bicarbonate
  - D. Carbonate
- Hardness (CaCO<sub>3</sub>) (ETDA)
  - A. Ca
  - B. Mg
- 3. pH
- 4. Solids
  - A. Filterable, Dissolived-TDS
  - B. Non-filterable, Suspended-TSS
  - C. Total-TS
  - D. Settleable Volumetric
- 5. Sulfate (SO<sub>4</sub>)
- 6. Chloride (Cl-)

#### TABLE 1

# OLIN-NIAGARA FALLS PLANT PRIORITY POLLUTANTS PRESENT IN CARBON COLUMN INFLUENT (Samples only analyzed for volatile organics) 10/8/82 to 1/27/83

Concentration (ug/1)

BHC (Hexachlorocyclohexane)	*	*	*
Carbon Tetrachloride	58	18	35.4
Chloroform	400	160	279.4
Dichloroethenes	190	<b>≤ 41</b>	≤ 131.5
Dioctyladipate	*	*	*
Dioctylphthalate	*	*	*
Fluoranthene	*	*	*
Hexachloro-1,3-butadiene	*	*	*
Hexachloroethane	*	*	*
Methylene Chloride	140	N.D.	8.2
Monochlorobenzene	24	N.D.	≤ 4.2
Pentachlorobutadiene	*	*	*
Pentachloroethane	*	*	*
Phenanthrene/Anthracene	*	*	*
Pyrene	*	. *	*
Tetrachlorobutadiene	*	*	*
1,1,2,2-Tetrachloroethane	170	46	116.1
Tetrachloroethene	1400	410	854.7
Toluene	N.D.	N.D.	N.D.
Trichlorobenzene	*	*	*
1,1,1-Trichloroethane	21	N.D.	≤ 10
1,1,2-Trichloroethane	≤ 10	. N.D.	<b>≤</b> 6.0
1,1,2-Trichloroethene	1400	430	873.5
Benzene	14	N.D.	≤ 1.4
Diisoctylphthalate	*	*	*
Methanol	*	*	*
1,1,2-Tetrachloroethane	*	*	*
Dichlorobenzene	*	*	*
Dichloroethane	N.D.	N.D.	N.D.
Vinyl Chloride	22	N.D.	<b>≤ 13.8</b>
Trichlorofluoromethane	N.D.	N.D.	N.D.

#### N.D. Not detected

NOTE: Compounds detected and not quantitated or quantitated at <1 ppb have been omitted.

NOTE: Average values represent 17 sample results.

VDL/vrp 3/18/83

<sup>\*</sup> Volatile organic analysis will not detect this compound

TABLE 2 Olin - Niagara Falls Plant Pilot Carbon Study INFLUENT DATA  $(\mu g/1)$ 

RUN				DICHLORO	ETHYLENE		
DAYS	DATE	<u>CH<sub>2</sub>C1<sub>2</sub></u>	<u>CHC1</u> 3	1,1	1,2	<u>cc1</u> 4	TOTAL*
0 N	10/6 #1	280	450	<20	<20	<20	730.0
7 N	10/13	220	440	<20	<20	22	682.0
28	11/3	<b>33</b> 0	170	< 1	140	47	687.0
37	11/12	74	160	< 2	48	< 2	282.0
48	11/23	11	230	< 1	54	11	306.0
57	12/2	13	300	2.7	280	57	652.7
69	12/14	11	330	4.1	200	2.8	547.9
80(72)	12/25	48	350	<.5	110	25	533.0
85(77)	12/30	36	340	<.5	91	18	485.0

<sup>\*</sup> Total of indicated volatile organics

<sup>()</sup> Run days corrected for column down time

TABLE 3 Olin - Niagara Falls Plant Pilot Carbon Study METHYLENE CHLORIDE IN CARBON COLUMN EFFLUENTS ( $\mu g/1$ )

RUN			COLUMN	NUMBER	
DAYS	DATE	<u>I</u>	<u>II</u>	111	VI
0 13 4 5 6 7 8 10 11 13 15 17 19 12 22 32 32 33 34 44 45 47 48 51 55 57 58 63 64	10/6 10/7 10/9 10/10 10/11 10/12 10/13 10/14 10/16 10/17 5 AM 6 PM 10/19 10/23 10/25 10/27 10/28 10/29 10/31 11/2 11/4 11/5 11/7 11/8 11/9 11/12 11/15 11/17 11/18 11/20 11/22 11/23 11/26 11/28 12/1 12/2 12/3 12/5 12/8 12/9 12/14	<0.5 2.2 3.5 19.0 2.6 140 290 19 25 30 20 1.3 5.5 15 41 91 160 150 3.7 1.8 3.5 1.5 3.1	<pre></pre>	0.57 1.7 1.9 1.9 18 6.7 6.6 .75 12 11 4.5 6.9	39 5.0 6.5
69 80(72) 85(77) 91(83) 93(85)	12/25 12/30 1/5	4.6 47 99	230 39	59 85 64	<.5 <.5 39
95(87) 98(90) 103(95) 107(99) 113(105)	1/7 1/9 1/12 1/17 1/21 1/27		≤.5	31 39 24 42 31 12	11 29 2.4 51 ≤5

<sup>()</sup> Run days corrected for down time

TABLE 4
CHLOROFORM IN CARBON COLUMN EFFLUENTS
(µg/1)

RUN			COLUM	N NUMBER	
DAYS	DATE	Ī	<u>II</u>	III	IV
0 1 3 4 5 6 7 8 10	10/6 10/7 10/9 10/10 10/11 10/12 10/13 10/14 10/16 10/17 5 AM 6 PM	<.5 <.5 <.5 6.6 35 180 34 37 46	6.6 <.5 3.0 <20 <.5 <.5		
13 15 17 19 21	10/19 10/21 10/23 10/25 10/27	130 270 370 <.5 520 220	<.5 2.9 .9 6.6		
22 23 25 27 29 30	10/28 10/29 10/31 11/2 11/4 11/5	420 380 330 330	62 360 130 250		
32 33 34 37	11/7 11/8 11/9 11/12	390	280 350 370	3:0 35	
40 42 43 45	11/15 11/17 11/18 11/20	300	400 400 420	74 110	
47 48 51 53	11/22 11/23 11/26 11/28	330 260	400	250 160 190 230	
56 57 58 60 63	12/1 12/2 12/3 12/5 12/8		350 300	360	110
64 69 80(72) 85(77) 91(83) 93(85)	12/9 12/14 12/25 12/30 1/5	390 360 360	460 410 730	450 530 390 440 340 420	240 260 320 360
95(87) 98(90) 103(95) 107(99) 113(105)	1/9 1/12 1/17 1/21 1/27		410	450 340 500 490 700	340 400 440 550 660
() Run day	s corrected for do	wn time			

Olin - Niagara Falls Plant Pilot Carbon Study TABLE 5

EFFLUENT FROM CARBON COLUMNS IN µ9/1

CARBON TETRACHLORIDE COLUMN NUMBER I II III IV	ស ស ស	<.5 <.5	, 5 , 5 , 5	\$	<.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5	വവ		) •	71	2 <.5 10 7.1	<b>&gt;</b> 9.	24 <.5	31 <.5	1.0	2.7 <0.5	5.2 <0.5 <0.5	25 <b>&lt;0.5</b> 35 <b>&lt;0.5</b>	02
1,2 DICHLOROETHYLENE COLUMN NUMBER  I II III IV	, , , , , , , , , , , , , , , , , , ,	<.5 <.5	<.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5 <.5	\$	, , , , , ,			104 <.5		190 1.5 170 180		160 <.5	150 2.5	24 120 34	140	75 <0.5 <0.5	240 <b>&lt;0.5</b> 290 <b>&lt;3.4</b>	
1,1 DICHLOROETHYLENE COLUMN NUMBER I II III IV		;	.5	4 <10 <20 6 <10 <.	7 5 AM <.5 <. 6 PM <.5 <.	, , , 5 , 5	1,1	, 2, R		3.2 2.9	<b>\$</b>	6.6 <.	5.4	115 4.7 <1 17 4.7 <1 18 <0.5	720 .5 <0.5	.82	/28 5.4 <0.5 /1 2.4 <0.5	2.1
RAN DAYS DATE	0 10/6	101 101 101 101 101 101 101 101 101 101			ו/0נ וו		10, 10, 10,					32 11/7	37 11/19			֡֝֝֝֟֝֟֝֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝֟֝	53 11/2	12

TABLE 5 (CONTINUED)

EFFLUENT FROM CARBON COLUMNS IN µg/I

Щ	21	, E		×		×	×	×	×		,	×	·	×	×.
TETRACHLORIDE AN NUMBER	ΞĮ		<0.5	•	<0.5	3.2	<0.5	<0.5	=	<0.5	<.5 *	<b>.</b> 5	· · · · · · · · · · · · · · · · · · ·	5.	42
CARBON TETE	=					22	15	28				<b>~</b> .5			
CAI	  ⊷					, 5	28	31							
.NE	λĺ	<b>&lt;.</b> 5		<.5		<.5	<.5	<.5	<.5		<b>&lt;.</b> 5	<.5	33	22	81
,2 DICHLOROETHYLENE COLUMN NUMBER	III		9.3		22	63	0.5	0.5	39	79					320
2 DICH	=					250	28	140				93			
	<b>⊷</b> 1					190	9	110	-	-					
ENE	<u>  1</u>	<.5		<.5		<.5	<b>&lt;.</b> 5	<b>&lt;.</b> 5	<b>^.</b> 5		<b>^.</b> 5	<.5	<.5	<.5	<b>.</b> .5
المالح	III		<0.5		<0.5	5.3	<0.5	<0.5	<0.5	<0.5	<0.5	<0.5	<b>&lt;.</b> 5	<b>^.</b> 5	<b>~.</b> 5
COLUMN NUMBER	ΞĪ					9	<b>&lt;.</b> 5	<b>~.</b> 5				<b>&lt;.</b> 5			
-	⊷I					9	<b>~.</b> 5	·.5							
	DATE	12/3	12/5	12/8	12/9	12/14	12/25	12/30	1/5	1/1	1/9	1/12	1/17	1/21	1/27
RAN	DAYS	58	09	63	64	69	80(72)	85(77)	91 (83)	93(85)	95(87)	(06)86	103(95)	107 (99)	113(105)

() Run days corrected for down time

TABLE 6  $\label{eq:continuous} Olin - Niagara Falls Plant Pilot Carbon Study \\ SUMMATION OF TOTAL EFFLUENT FROM EACH COLUMN IN <math display="inline">_{\mu g}/1$ 

RUN DAYS	DATE	Ī	C O L U M N	<u>IV</u>
0 1 3 5 7 8 10	10/6 10/8 10/9 10/11 10/13 10/14 10/16 10/17	<.5 2.2 3.5 25.6 37.6 320.0 324.0 56.0		
13 15 17 19 21 22 23 25	10/19 10/21 10/23 10/25 10/27 10/28 10/29 10/31	71.0 160 290.0 397.0 5.5 639 429.5 621.9 667.2		
27 29 32 37 42 43 45 47 48	11/2 11/4 11/7 11/12 11/17 11/18 11/20 11/22 11/23	673.2 678.6 584.3 538.2 473.2 - - 512.3	36.7  75.9 111.9  268.0 166.7	
51 53 56 57 58 60 63 64 69	11/26 11/28 12/1 12/2 12/3 12/5 12/8 12/9 12/14	533.5 - - - - - - 590.6	196.6 234.2 372.0 - 410.3 - 476.5 608.4	149.0 135.0 246.5
80 (72) 85 (77) 91 (83) 93 (85) 95 (87) 98 (90) 103 (95) 107 (99) 113 (105)	12/25 12/30 1/5 1/7 1/9 1/12 1/17 1/21 1/27	535.0 600.0 - - - - - -	449.0 525.0 464.1 530.5 589.0 444.0 712.0 691.0	260.0 320.0 399.0 351.0 429.0 475.4 623.0 746.0

<sup>()</sup> Run days corrected for column down time.

TABLE 7 Olin - Niagara Falls Plant Pilot Carbon Study SUMMATION OF COLUMN 2 EFFLUENT DATA (10 Minute Contact Time)

1

ī

ī

ī

1

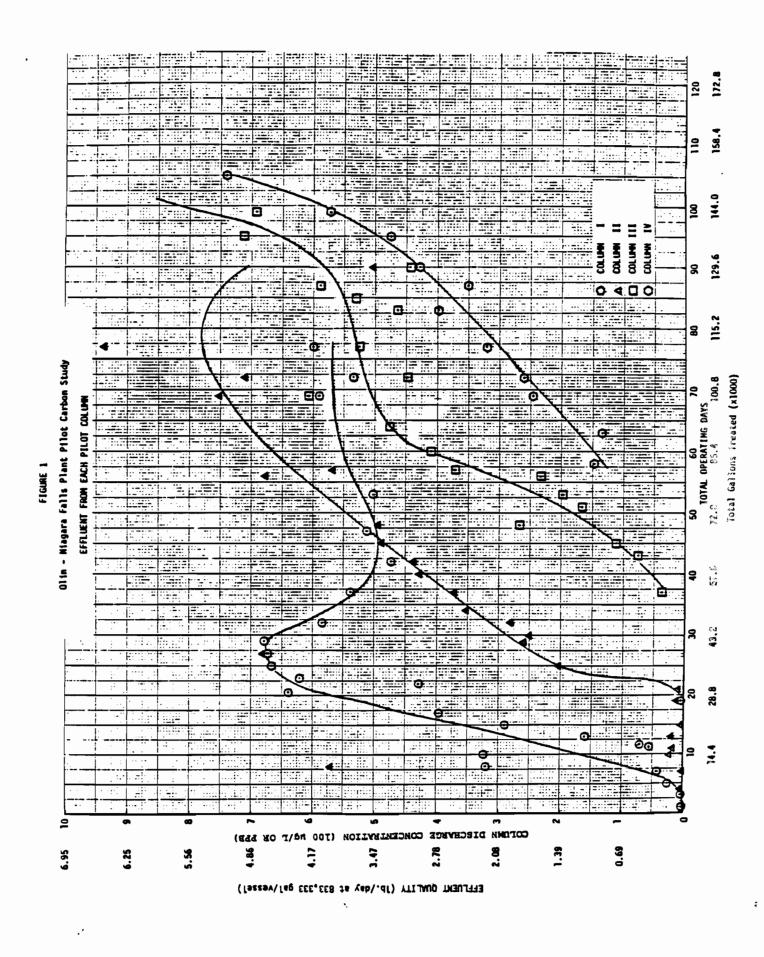
term term term, term, term, term, term, term, term,

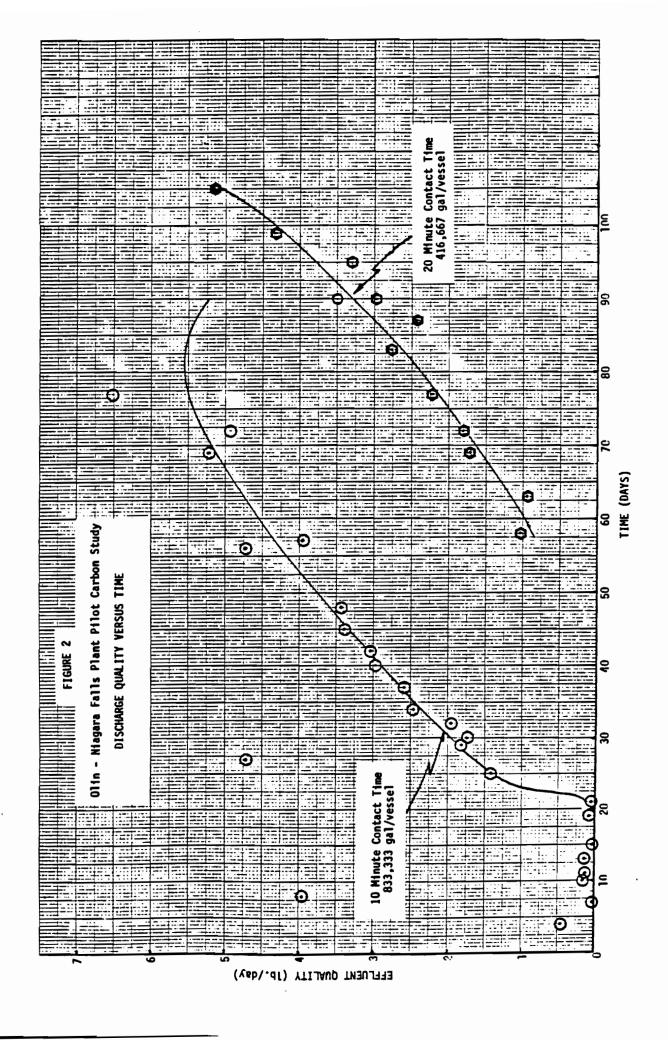
Persona, y

· ·

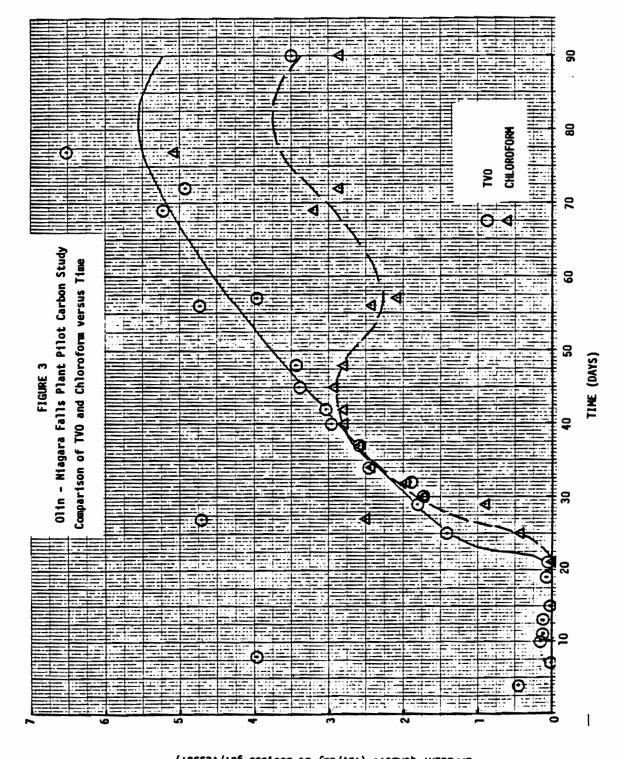
TOTAL * POUNDS/DAY TVO	0.46	0.02	0.17 0.13	0.14	0.09	1.41 4.72 1.81	1.74 1.95 2.45	2.58 2.97 3.04	3.39 3.43	3.95	4.93 6.51	3.49
T0TAL <u>u9/l</u>	9.9	3.0 3.0 570	24 18	20 6	13.4	203.5 680 260	280.6 353.2	370.9 428 436.9	488.2 494 678 6	568.1	710 937	503
CARBON TETRACHLORIDE µ9/l	.5	<.5 <.5 <20	, , , , , , , ,	, v , ;	, , 5.5	7.5 -1.	 	  	2.7 5.2	52 50 50 50 50 50 50 50 50 50 50 50 50 50	75 78 78	4.5
DICHLOROETHYLENE 1,1 1,2 19/! 19/!	۰ ت	<.5 <.5 <20	, , , , , ,	v v .	.5 .5	1.5		24 34 34	56 75 290	240	58 140	93
DICHLORO 1,1 Pg/L	.5	<.5 <.5 <20	ນ ຄ. ທ V . v	, , , , , ,	, s .5 .5	2.5 2.9	יא אי	, ^ <u>^</u>		2.1	, , ,	<.5
CHLOROFORM µ9/1	9.6	<.5 3.0 <20	v v v	2.5	9.9	62 360 130 250	280 320 320	370 400 400	420 400 350	300	410 730	410
METHYLENE CHLORIDE µ9/!	۰. ت	<.5 <.5 570	24 18 ^	20 3.1	4.4	140 130 130	1.2	.89 3.0 1.6	9.5 13 1.2		230 39	≤5.5 At 833.333 gal
DATE	10/ 6 10/ 7 10/ 9 10/10	10/12 10/13 10/14	10/16 10/17	10/19 10/21	10/25 10/27	10/31 11/2 11/4	7/11	11/12	11/20 11/23 12/1	12/ 2	12/25	1/12
RUN	0 - 6 4	9 / 8	9 [	13 15	19 21	25 25 30 30 30	325	3/ 40 42	45 48 56	57	80(72) 85(77)	_

\* At 833,333 gal. per adsorber and effluent concentration in  $\mu g/1$  () Run days corrected for column down time





EFFLUENT QUALITY (lb./day at 833,333 gal/vessel)





#### APPENDIX V

TO D. R. Vaughn

AT Charleston

DATE October 8, 1981

ΓROM

SUBJECT

J. W. O'Grady

AT Charleston

COPY TO D. L. Cummings

P. J. Craney

A. F. Kaptenia

M. L. Norsworthy

V. M. Norwood

M. S. Smithson

A. P. Szustak

New York State DEC Bioassay, October 5-6, 1981

On October 6, 1981, representatives from the NYSDEC were in the Niagara plant to sample the water sources and clear water outfalls. This was done as part of a larger state/federal project designed to assess the water quality of the Niagara River. While composite samples were being taken of the North and South wells, the river inlet and 1, 3, and 4 CW outfalls, grab samples were taken at all of the preceding, with the exception of the river inlet, for bioassay analysis. A bioassay was not run on the river water as the DEC feels it has ample testing information on this source showing that it is not acutely toxic.

The water for the bioassays was immediately transported to the State laboratory at Avon, New York (just south of Rochester) and a 24-hour static test was conducted. A 2-liter and two, 200 mil aliquots were taken from each sample. Five fathead minnows, Pinephales promelas, were placed in the 2-liter contained and 10 Daphnia magna, were placed in the 200 mil aliquots. The type and nature of the bioassay was a 24-hour static test which is an indicator of acute toxicity. At the end of the 24-hour cycle there were no fatalities. The results of this test by the State as well as our own test in August indicate there is no acute toxicity in either our water supplies or our clear water sewers.

The State will continue to test other industrial dischargers over the next 5 to 6 weeks and a report with all the results should be available in early December.

JWO/wr

# COMICON GEORGEO BECHING

Distribution TO

Various

DATE October 14, 1981

FROM

SUBJECT

J. W. O'Grady

Niagara Falls Bioassay

August 26-27, 1981

AT Charleston

COPY TO J. C. Brown

D. L. Cummings

P. J. Craney

A. F. Kapteina

M. L. Norsworthy

V. W. Norwood

M. S. Smithson

A. P. Szustak D. R. Vaughn

#### SUMMARY:

On August 26 and 27 two 24-hour static bioassays were conducted on influent and effluent water at the Niagara Falls plant. No mortality was exhibited in either of the tests.

TEST I - The first test was conducted on well water from both the North and South wells. All methods employed followed those discussed in EPA-600/4-78-012 (Methods for Measuring the Acute Toxicity of Effluent to Aquatic Organisms, Peltier 1978). The fathead minnow (Pimephales promelas) was the test species used. The we water was collected in four (4), five (5) gallon grabs. Two (2) each from each well. Each five (5) gallon grab was placed in a separate tank. Of the two (2) grabs from each well one was aerated and one was not. Ten (10) fish were placed in each chamber including two (2), five (5) gallon controls of city water.

TEST II - The second test was a crude screening test to obtain preliminary data from various water sources throughout the plant. Four (4), five (5) gallon grab samples were taken. One (1) each from 1CW, 3CW, 4CW and river influent. As in Test I a five (5) gallon control of city water was also used.

#### DISCUSSION:

Test organisms were purchased from a fish hatchery in Pennsylvania, treated for parasites and disease, and allowed to acclimate to laboratory conditions for two weeks prior to the tests. Average fish size was 4.5 cm, average weight .78 grams.

 $\overline{\text{TEST I}}$  - Two (2), five (5) gallon samples were taken from each well and placed in previously sterilized five (5) gallon aquariums. Temperature of the well water at the well head was 12°C. A heating coil was used to elevate the temperature to the 20-22°C range, as the fish were acclimated at 22°C. Prior to the start of the test each tank was tested for temperature and dissolved oxygen (D.O.).

	Temperature	D.O.
Control A	21.5°C	8.8
Control B	21.1°C	8.8
North Well A*	20.2°C	6.3
North Well B*	20.5°C	5.8
South Well A* South Well B*	20.2°C 20.5°C	6.0 6.5

<sup>\*</sup>Volatile Priority Pollutant Analyses ran on well water samples of the same date as the test water was taken (8/26/81) show levels of 4862  $\mu$ g/l in the North Well and 6147  $\mu$ g/l in the South Well.

To insure that there was enough oxygen and to avoid the possibility of its being a contributing factor to mortality, North Well tank B and South Well tank A were aerated for 10 minutes. Their D.O's were brought up to 7.6 and 7.5.

At the completion of Test I the temperature of all six (6) tanks was  $22.0^{\circ}$ C and the D.O. of each was:

Control A	7.3	North Well A	5.6	South Well A	6.4
Control B	7.2	North Well B	6.4	South Well B	5.7

All test organisms were alive at the end of 24 hours and Test I was terminated.

<u>TEST II</u> - One (1), five (5) gallon sample each of 1, 3 and 4CW effluent and river water influent as well as a five (5) gallon control were tested. The 1CW sample was heated to bring it up to  $22.0^{\circ}$ C and 3 and 4CW were cooled to bring them down to that range. The river water was  $22.0^{\circ}$ C at the sample point (the well house).

At the start of the test the following temperature and D. O. was recorded.

<u>Temperature</u>	<u>D.O.</u>
22.0°C	8.7
20.5°C	8.4
23.0°C	7.6
22.0°C	7.4
22.0°C	8.3
	20.5°C 23.0°C 22.0°C

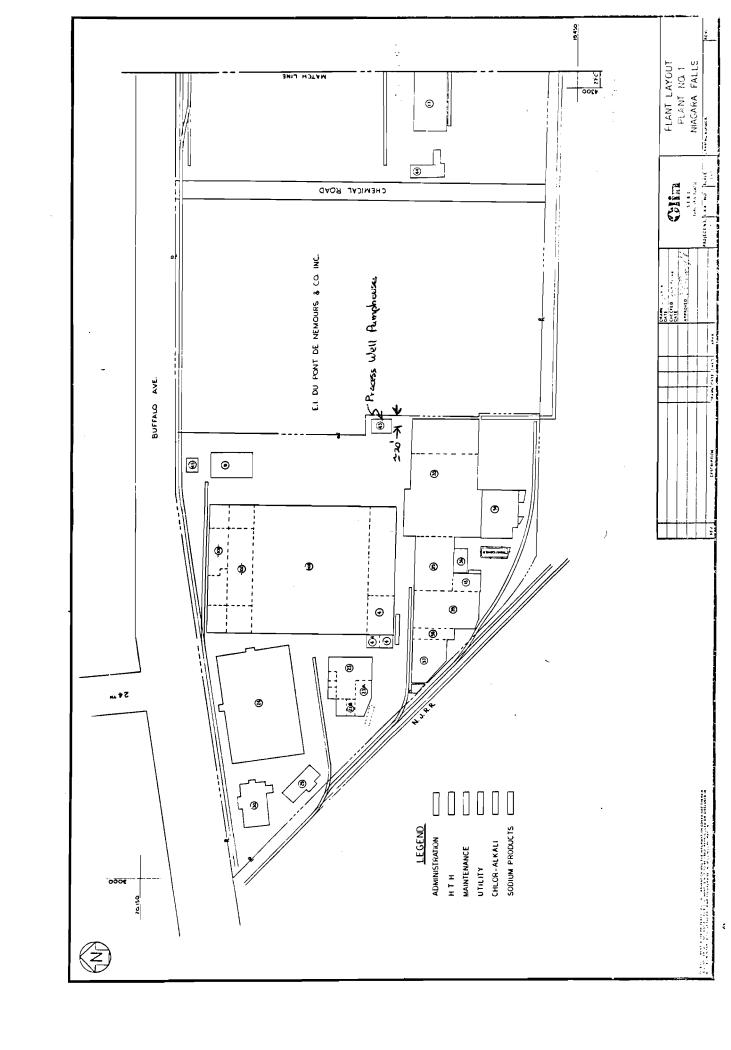
<sup>\*</sup>Volatile Priority Pollutant Analyses was run on 1CW grab as this outfall is primarily 100% well water. Data shows that the level was 3697  $\mu g/l$  on 8/27/81.

As in Test I, all organisms were alive at the end of the 24-hour testing period.

#### CONCLUSION:

Although the test serves as a preliminary indicator that the water at Niagara Falls is not acutely toxic a more vigorous long-term definitive test conducted over a 96-hour time period would confirm this.  $\Lambda$ 

JWO/vrp



\_

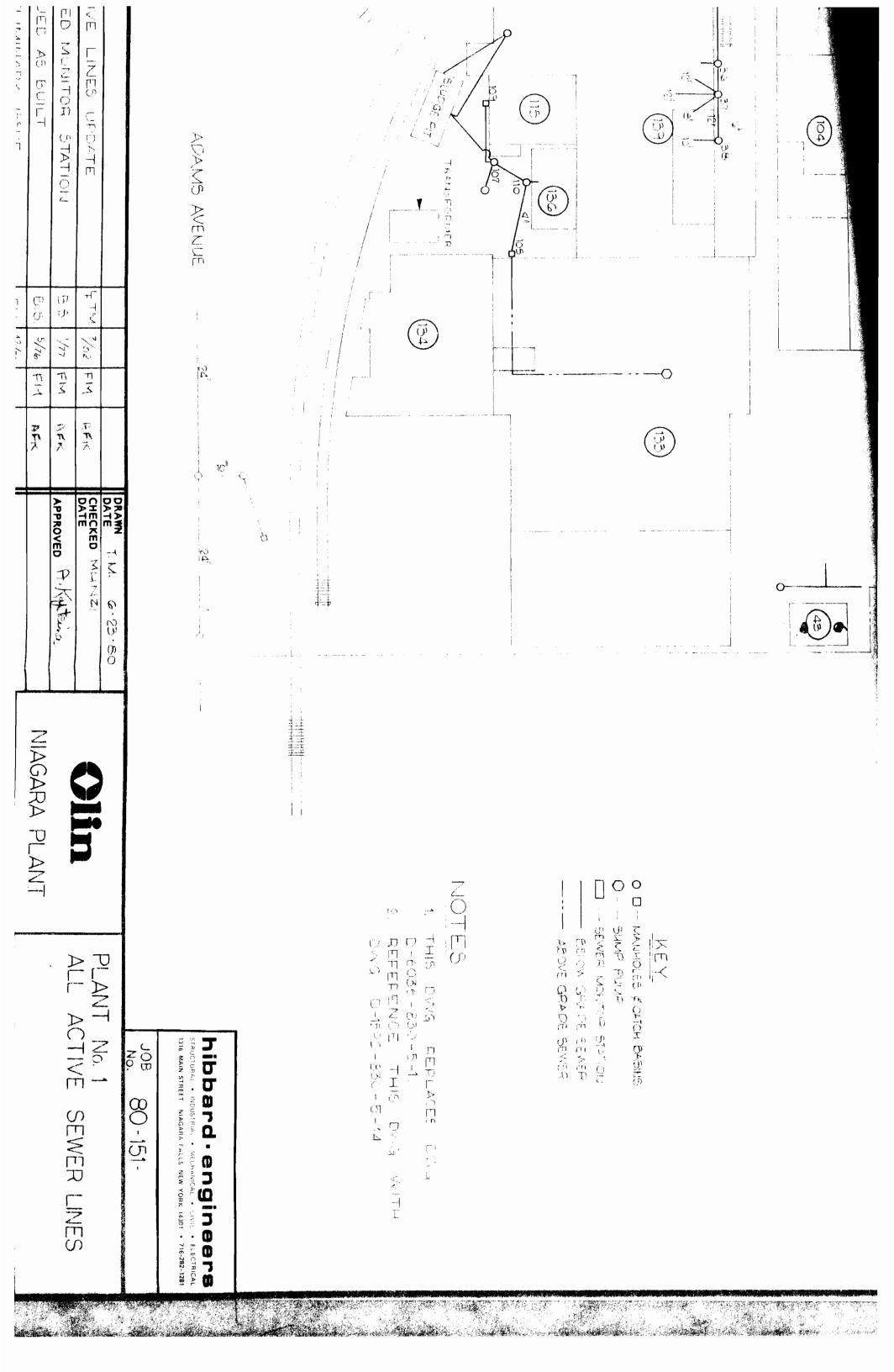
.

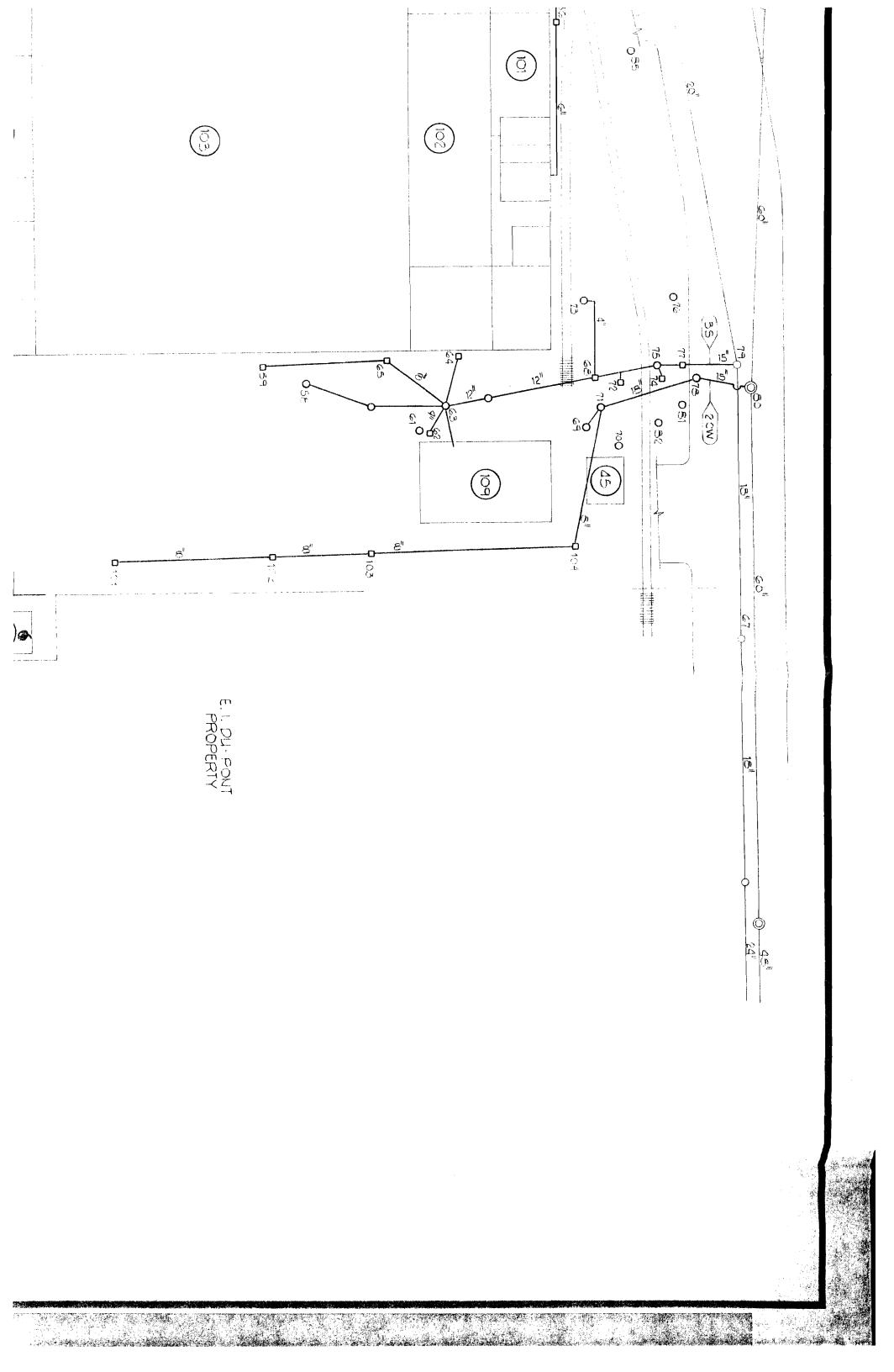
-

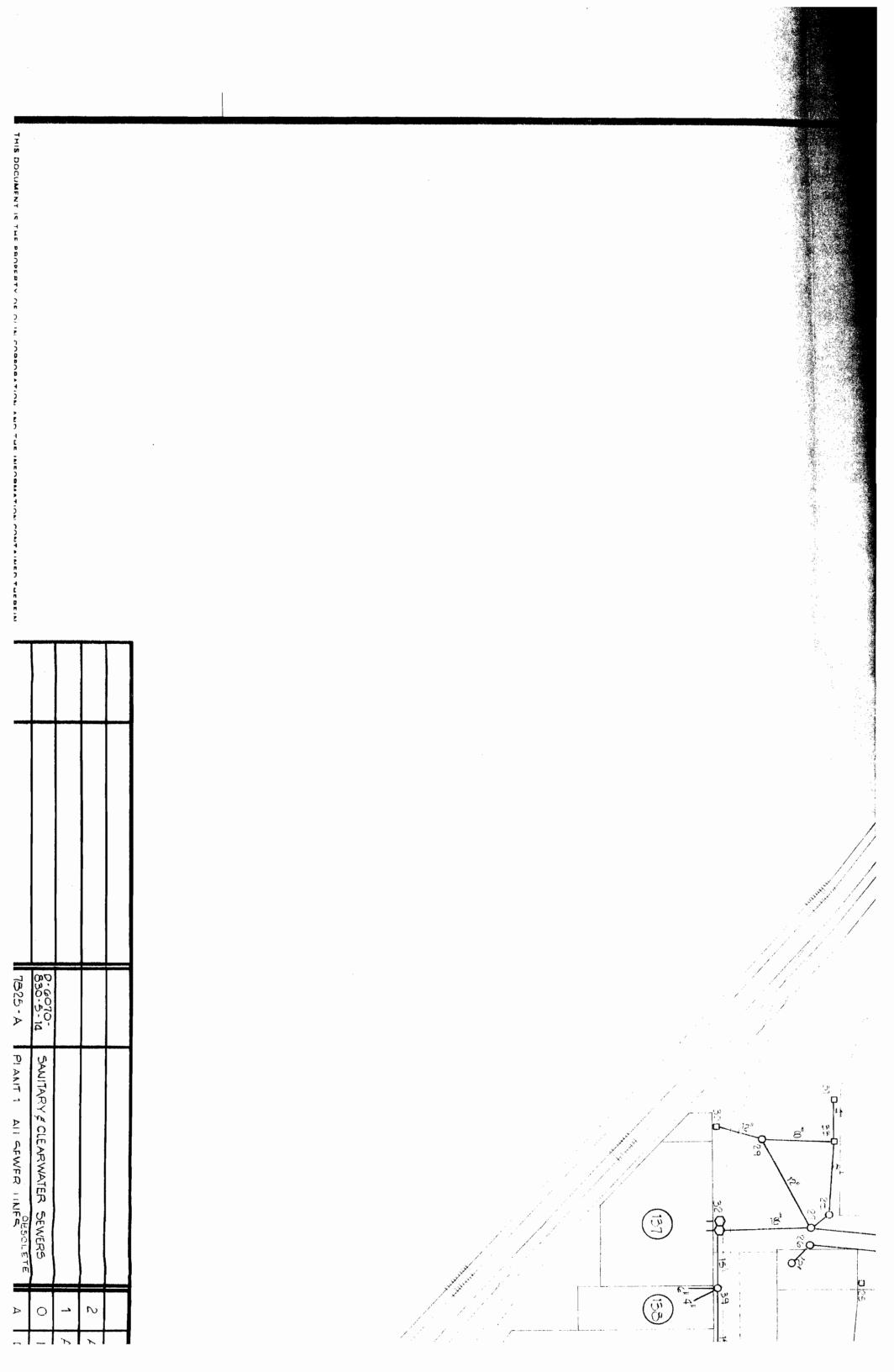
-

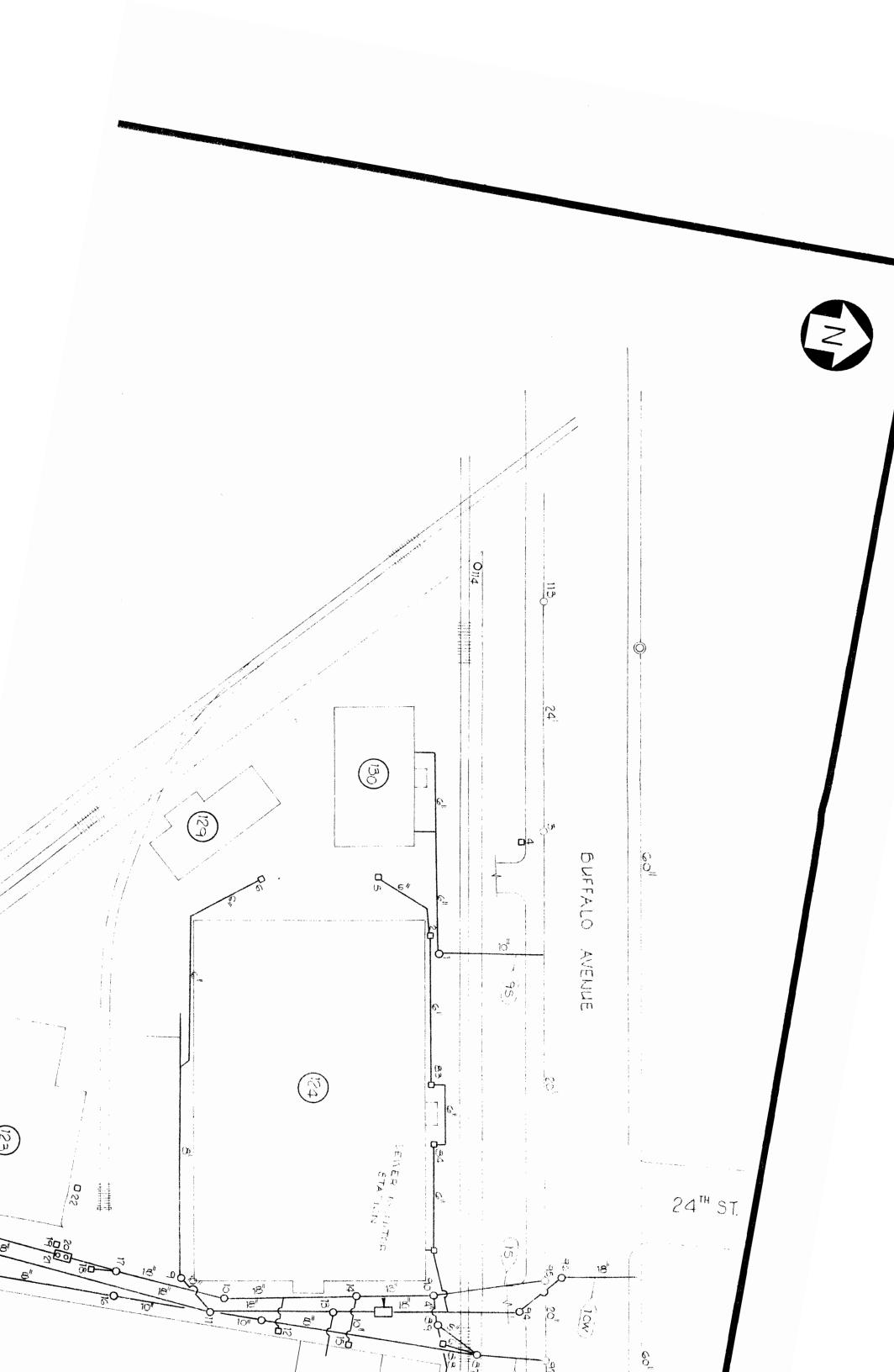
•

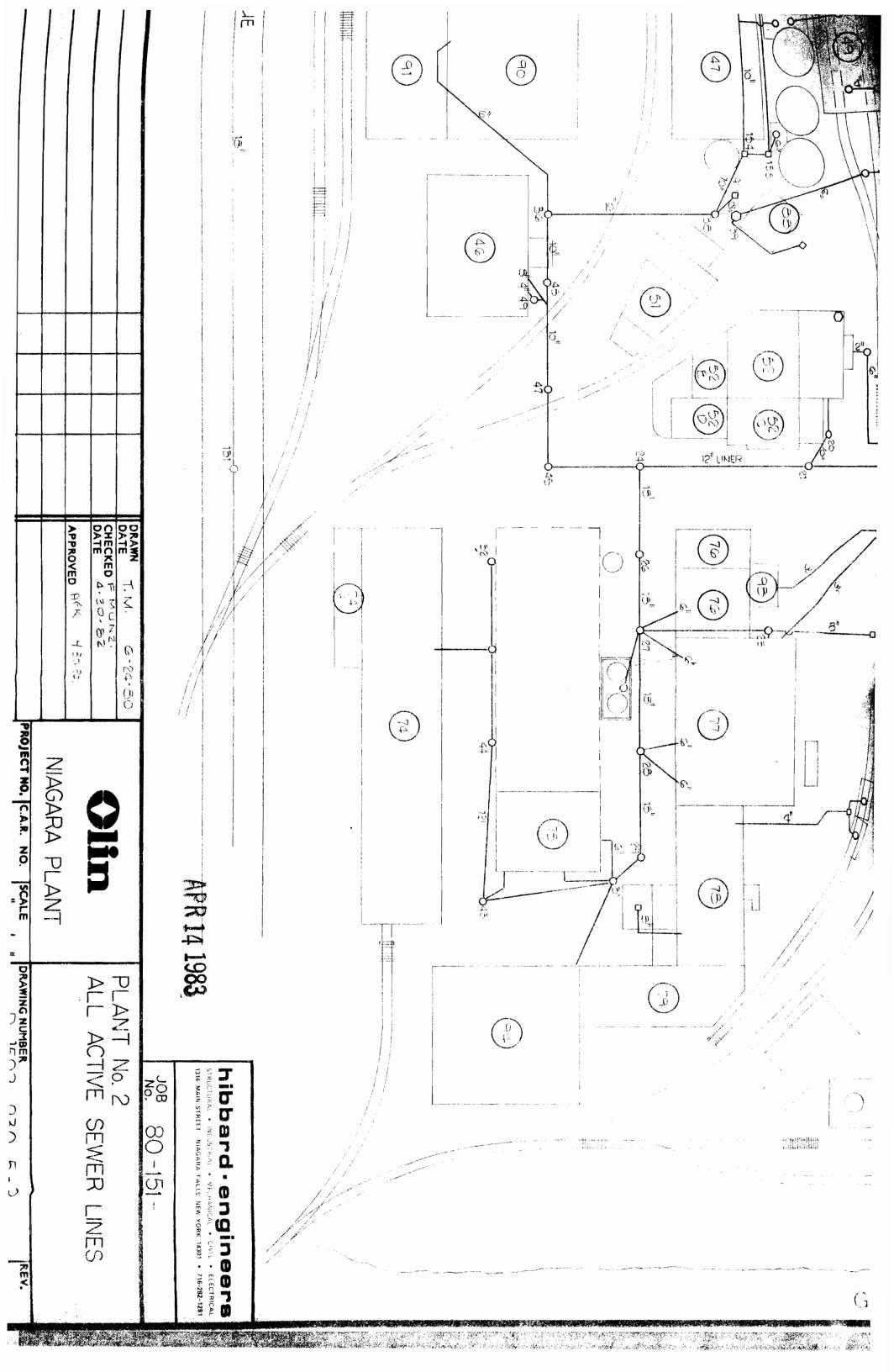
....

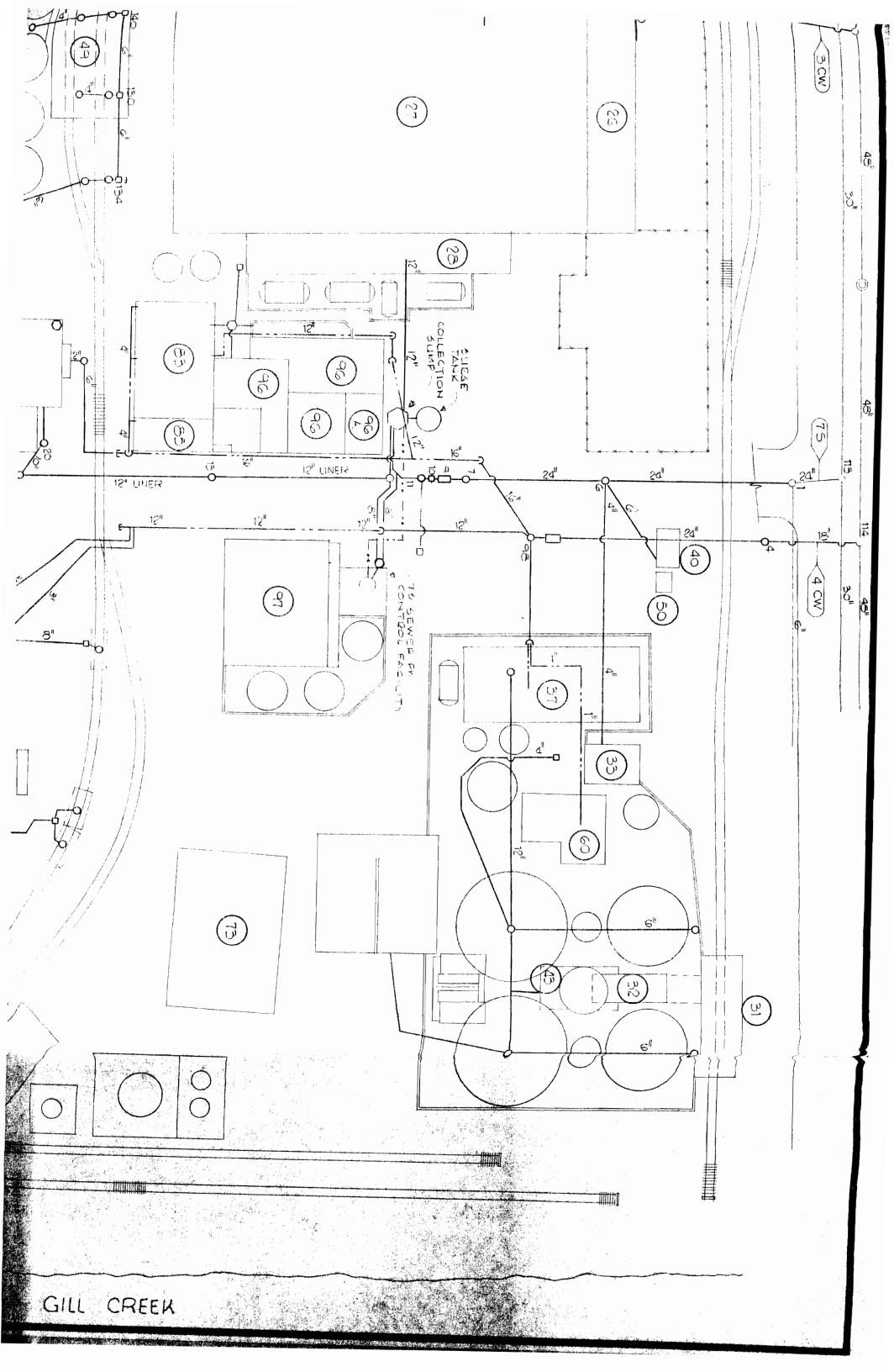


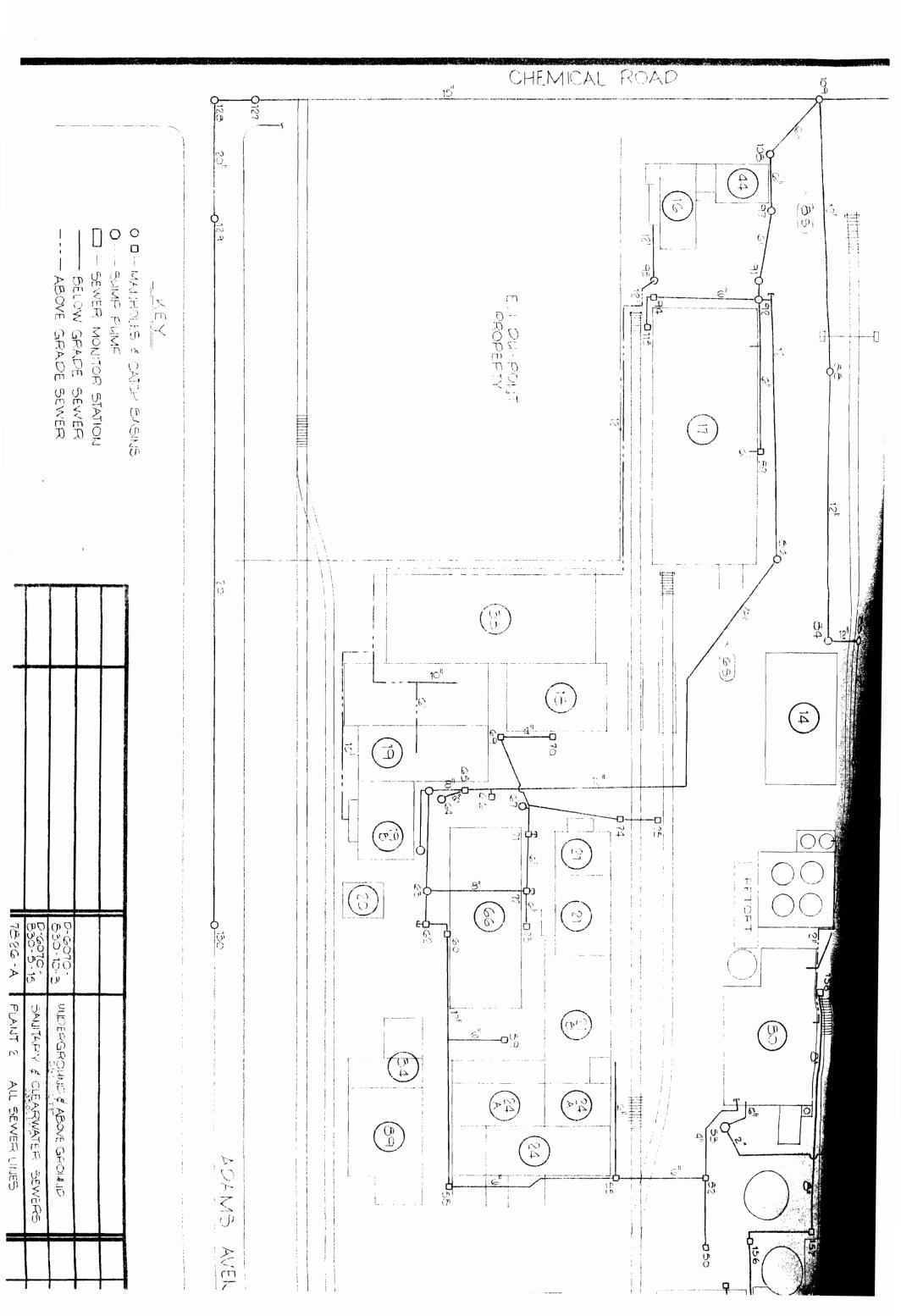












.

