

PURE WATLIS D.E.C. REG .#8

REPORT

ON

WASTEWATER DISCHARGE MODIFICATIONS PRESSWARE PLANT CORNING GLASS WORKS CORNING, NEW YORK OCTOBER, 1975

NOTE:

: Due to the proprietary nature of the contents of this report, Corning Glass Works requests that only authorized personnel be permitted to review this report and that every effort will be made to honor the confidential status of this information.

> Rumi N. Mazda Senior Engineer Facilities Design Department Facilities Engineering and Construction

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	NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL	CONSERVATION						
	APPLICATION FOR APPROVAL (AND/OR	OF PLANS						
FOR PER	MIT TO CONSTRUCT A WASTE D	ISPOSAL SYST	EM					
I. No st Applicant:	2. Location of Works (C, V, T): 3	. County	4. Entity or Area Served					
Pressware Plant Corning Glass Works	Steuben Street Corning, New York	Steuben	Pressware Plant					
i. Type of Ownership:								
Commercial Municipal Sewage Works X Industrial Private-Home	Corp. Private-Other Board of Education	Authority Federal State	Interstate International Indian Reservation					
5. Type & Nature of Construction:	Ilection System New Additions or Alterations	Treatment and/or New Additions or	Alterations					
7. Estimated Cost of Construction: Collecti	on System \$58,500 Tre	atment and/or Dispo	sal \$24,900					
Type of Waste: Sewage Industrial Other Specify Contact Cooling Water Specify								
Nome of Receiving Treatment Works: 10. Point of Discharge: Surface Water: Name of Watercourse_ Name of Watercourse_ Chemung River Closs_C								
Ground Water: I Is State or Federal Aid Applied For? Yes - Give Project Nome of Watercourse to which ground water is tributaryClass								
2. Name of Design Engineer: <u>G. J.</u> Address: <u>Corni</u>	Dudick ng Glass Works MP 50-3 Cor	N.Y. Stote Lic	hone No. <u>39776</u>					
3. Water Consumption (GPD): Present S	ee Appendix "B" thisFuture		_ Design Year					
4. Population Served: Present	Eport 500+ Future		Design Year					
5. Average Daily Flow for New or Existing Treatment Works (GPD): Presen	See Appendix "B" this Rep Future	ort.	_ Design Year					
6. Source of water supply (if private well; g	ive location; type; depth and character of soil)	17. Design E	17. Design Equivalent Population (BOD Basis):					
Combination of wells an supply.	N/A Ind ing wat	N/A Industrial contact cool- ing water supply.						
 Give number, character and distance of a treatment works 	ny buildings which may be affected by the prop	posed 19. Describe Disposal	19. Describe Proposed or Existing Storm Water Disposal:					
See Appendix "A" this r	To Che Outfai	To Chemung River through Outfall 002 (CGW #1)						
Additional information must be submitted	for private and institutional systems.							
20. Indicate on U.S.G.S. Topographic Map ex sources of water supply within 200' of th	act location of sewage treatment works and ad e proposed works. Give description of these so	jacent buildings. Sho ources and character	ow location of all wells or other of soil.					
For topographic map see buildings see Appendix below.	Appendix "E" this report. "A" this report. For char	For locat: acter of so	ion of wells and il see item 22					
 21. Stor- depth below existing ground surface of ch ground water is encountered 22. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 25 feet 22. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 23. Stor- depth below existing ground surface data (use additional sheet, if necessary) 24. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 25 feet 26. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 27. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 28. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 29. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 20. Describe soil at site of proposed works. Give design basis and observed soil percolational sheet, if necessary) 								
Ref: Same as item 22.	Ref: Same as item 22. test boring done by H. C. Nutting Company, Cincin Ohio. Report #B-16265jh dated July 20, 1966/							
2011. 5 (rev. 7, 68)			•					

NOTE: All applications must be accompanied by plans, specifications and completed Form San. 65 (appropriate portions). The submission must conform to a previously approved engineering report describing the system in detail. The plans must be stamped with the designing engineer's seal and must be of sufficient clarity and legibility to permit satisfactory microfilming. Only white prints will be accepted because of the difficulty of microfilming blue prints. There must be a blank area, at least 4" x 7", in the lower right corner of each sheet so that the approval stamp may be placed on the face of the plans.

Any deviation from the Department's standards for wastewater collection and treatment facilities must be explained in detail.

Approved plans are to be returned to:

X Applicant

If the application is signed by a person other than the applicant shown in Item 1, the application must be accompanied by a letter of authorization. Failure to comply with this provision may be grounds for the rejection of any submission.

Signatures and Official Titles:

John J. Chambers, Manager Environmental Control

Moiling Address: Corning Glass Works

Main Plant 8-4, Corning, New York 14830

Date of Application: October 1, 1975

REMARKS:

INTRODUCTION

The Pressware and Fallbrook Plants are currently operating under modified NPDES Permit No. NY0003981 effective August 29, 1975 and expiring on November 29, 1979. The Permit covers Pressware Outfalls 001 (CGW #1A), 002 (CGW #1), and 003 (CGW #2). (Outfall 003 (CGW #2) was formerly known as Fallbrook's Outfall.) The Schedule of Compliance calls for the submittal of final plans and specifications by October 1, 1975, with construction to begin by January 1, 1976; be completed by May 1, 1977, and operational levels to be achieved by July 1, 1977. This report and accompanying drawings comprise the final plans and specifications as mentioned above.

-1-

George Musick

SUMMARY

The following plant wastewater system is proposed. The start up of a new furnace Tank #52 with its related manufacturing processes, and the impending shutdown of an existing furnace Tank #48 are incorporated into the proposal.

All contact wastewater from Pressware's plant and compressor room will be transferred to the lagoons for oil and suspended solids reduction before being combined with Fallbrook plant's wastewater and on to Outfall 003 (CGW #2). All non-contact water and stormwater from Pressware's plant and compressor room will be combined and diverted to Outfall 002 (CGW #1). Under normal conditions, no wastewater is expected to be discharged through Outfall 001 (CGW #1A).

Flow monitoring and sampling will be done at the manholes on the river dyke just preceeding Outfalls 002 (CGW #1) and 003 (CGW #2).

DISCUSSION

I. SCOPE OF WORK (See drawing #11293-13251-WT1 and Appendix "B")

Contact water from Pressware Tanks #47, #51, and #52 will be rerouted through the two lagoons for oil and suspended solids reduction before discharging through Outfall 003 (CGW #2). In addition, contact water from Pressware's compressor house will also be diverted through the lagoons, as will Fallbrook's contact water from its washing operations. (The latter is routed through the waste treatment plant and will be treated with Oakite Defoament 5, when required, before discharging into the lagoons.)

Non-contact water and stormwater from the Pressware plant and compressor house will be segregated from the contact water, combined, and routed through Outfall 002 (CGW #1). Hence, no industrial wastewater is expected to flow through Outfall 001 (CGW #1A).

Flow rates and samples will be taken from Outfalls 002 (CGW #1) and 003 (CGW #2) and results reported as specified by the Permit.

II. BACKGROUND

An "Application for Approval of Plans and for Permit to Construct a Waste Disposal System" was filed on November 10, 1974 by Corning Glass Works with NYSDEC. The application was for the construction of a wastewater system for Tank #52 at the Pressware Plant. It was accompanied by a "Report on Industrial Wastewater - #52 Tank Expansion Pressware Plant" with drawings #11293-12141-BS6, -12071-C1, -12081-C2, and -12151-E1. The drawings detailed all the construction work to be done on the wastewater disposal system for Tank #52 and its manufacturing lines. The report discussed the existing status of Pressware's wastewater system, what the expected flows from Tank #52 and related areas were expected to be and a detailed description of Tank #52's proposed wastewater treatment system.

Pursuant to the Schedule of Compliance in the original EPA Permit No. NY0003981 issued to the Pressware Plant on October 23, 1974 and effective November 29, 1974 a "Preliminary Report on Wastewater - NPDES Compliance Pressware Plant" was submitted on March 3, 1975. This report outlined a tentative wastewater disposal system to bring all three Outfalls viz. Pressware's OO1 (CGW #1A), 002 (CGW #1), and Fallbrook Plant's OO1 (CGW #2) into compliance by November 29, 1976. Expected wastewater flows from both Pressware and Fallbrook plants were submitted, together with a proposed combined wastewater treatment system. Mention was made in the report, of Corning Glass Works' intent to propose to the EPA an NPDES permit modification to reassign Fallbrook's Outfall OO1 (CGW #2) as Pressware's Outfall 003 (CGW #2). The proposal for modification and time schedule for conformance were negotiated as indicated in the introduction.

III. DESCRIPTION OF WASTEWATER SYSTEM

A. <u>Outfall 001 (CGW #1A)</u>. (See drawings #11293-13251-WT1 and -13261-WT2.)

Currently about 511,000 GPD of wastewater comprising of approximately 2000 GPD of condensate and contact water, and roughly 509,000 GPD of non-contact cooling water, flows out of the Pressware Plant's compressor house to Outfall 001 (CGW #1A). The 2000 GPD of condensate and contact water will be collected in a new sump "B" and pumped in an overhead line leading to the main contact water line in Building #20. The remaining 509,000 GPD of non-contact cooling water will be rerouted through a new overhead line to the existing reclaim tank and eventually to Outfall 002 (CGW #1). An emergency overflow with a tee-type outlet from sump "B" will be connected to Outfall 001 (CGW #1A) to minimize loss of oil in the event that wastewater does overflow from the sump. However, under normal operating conditions no wastewater is expected to flow through Outfall 001 (CGW #1A).

B. <u>Outfall 002 (CGW #1)</u>. (See drawings #11293-13251-WT1 and -13271-WT3.)

A new overflow line from the existing reclaim tank will be connected to a new stormwater drain which will divert all non-contact water and stormwater around new sump "A" and discharge into the existing drainline leading to Outfall 002 (CGW #1). An emergency overflow from sump "A" will also be connected to this drainline. However, under normal operating conditions only stormwater and approximately 609,000 GPD of non-contact cooling water is expected to flow through Outfall 002 (CGW #1).

C. Outfall 003 (CGW #2). (See drawings 11293-13251-WT1, -13271-WT3, -12141-BS6, and -11851-BS31.)

The main contact water line in Building #20 will discharge all contact water from the compressor house and from Tanks #47 and #51 into new sump "A", from which it will be pumped through an overhead line to the lagoons. Contact water from Tank #52 will be pumped to the lagoons in the same overhead line. An oil skimmer will be mounted on each lagoon, accumulating skimmed oil in individual waste oil storage tanks for periodic removal by an approved hauler. (Northeast Oil Service of Syracuse for instance, will, under contract, periodically haul away the waste oil from the tanks.) Recommended API procedures for designing gravity type oil separators indicate the existing lagoons are adequately sized for this purpose (see Appendix "D").

D. Overflow Precautions

Even though there will be emergency overflows, from contact water sumps "A" and the one for Tank #52, connected directly to drainlines leading to Outfalls 002 (CGW #1) and 003 (CGW #2) sufficient precautions have been taken to prevent contact water from ever overflowing directly to these Outfalls without prior treatment. A pair of pumps will be installed in each sump with an alternator to evenly distribute the pumping load over both pumps. Each pump will be powered from separate transformers to minimize total breakdown from localized power failures. Three separate float switches will be installed in each sump to insure against switch failure. The high level switch will flash a warning light should the water approach the overflow level. In the event the water does overflow, the tee-type outlets will minimize any direct loss of accumulated oil from the sumps.

E. Flow Measurement and Sampling. (See drawing #11293-13281-WT4.)

Graduated weirs will be installed inside two manholes located on the river dyke, to measure wastewater flows for Outfalls 002 (CGW #1) and 003 (CGW #2). Outfall 001 (CGW #1A) will, ordinarily, have zero flow and therefore no weir is planned.

Grab and composite samples will be taken at these manholes consistent with the Permit requirements.

F. Defoamant Addition

Under normal operating conditions in the Fallbrook Plant approximately 10,500 GPD of contact water from its three washing operations is discharged to the waste treatment plant. Settleable solids are removed in the equalization tank and the old clarifier tank. However, soluble detergents remain in the effluent at times causing a foaming effect in the Chemung River. To minimize foaming it is proposed to add as needed Oakite Defoamant 5 directly into the equalization tank at a concentration of 120 mg/1 (based on a flow of 10,500 GPD). Therefore, the expected concentration of the defoamant at Outfall 003 (CGW #2) with an expected flow of 1,275,000 GPD is less than 1 mg/1.

The chemical composition of Oakite Defoamant 5 was submitted directly to Mr. J. F. Kelleher of N.Y.S.D.E.C., Albany by letter dated September 8, 1975 from Geogi St. John, Assistant Technical Information Administrator, Chemical Research Department, Oakite Products, Inc. This was submitted because the "Oakite" product was considered by them to be proprietary.

G. Lead Monitoring. (See Appendix C - Table I.)

The modified NPDES Permit No. NY0003981 stipulates the following limits for total Pb in mg/l for Outfall 003 (CGW #2).

From August 29, 1975 through June 30, 1977 --

Total Pb - Daily Average 0.43 mg/1

as monitored by a weekly composite sample.

From July 1, 1977 through November 29, 1979 --

Total Pb - Daily Average 0.1 mg/l - Daily Maximum 0.2 mg/l

as monitored by a monthly composite sample.

Table I (Appendix C) shows the total Pb concentrations in mg/l as monitored by weekly samples since December 4, 1974. Prior to July 17, 1975 the Fallbrook Plant was the sole contributor of wastewater to Outfall 003 (CGW #2). The average flow recorded during this period through Outfall 003 (CGW #2) was 344,000 GPD. From July 15, 1975 through September 16, 1975 Pressware's Tank #52 was also contributing wastewater to Outfall 003 (CGW #2). The average flow during this period was 544,000 GPD (see Appendix B).

The total Pb figures in Table I indicate occasional high levels in the months of July and August. However, the daily average total Pb concentrations for July and August are 0.263 mg/l and 0.193 mg/l respectively. Neither one of these values violate the interim daily average limit of 0.43 mg/l.

If these average daily Pb levels for the two months are extrapolated over the expected flow rate of 1,275,000 GPD from Outfall 003 (CGW #2) after July 1, 1977 the average daily Pb concentrations would be 0.071 mg/l and 0.082 mg/1. Neither one of these values would violate the final daily average limit of 0.1 mg/l. However, if individual daily values were extrapolated, as shown in Table I, then the 0.210 mg/l on July 9, 1975, and 0.239 mg/l on August 13, 1975 would constitute violations of the final daily maximum limit of 0.2 mg/l. Fortunately, the prompt analysis of samples by the Fallbrook laboratory have enabled the plant to pinpoint the exact reasons for the high total Pb values for the two dates in question. On July 9, 1975 the evaporative spray cooling tower walls were manually washed before tank start up and contaminated water inadvertently entered the Outfall. A similar incident with batch material hoppers took place on August 13, 1975. These occurrences will be controlled by strict housekeeping measures.

Based on past monitoring of flow and total Pb levels of wastewater in Outfall 003 (CGW #2) no future violations of either the interim or final limitations should occur.

/k





		EXPECTED		moment	EXPECTED	
	TOTAL PD	TOTAL Pb		TOTAL Pb	TOTAL Pb	
	(MG/L)	(MG/L)		(MG/L)	(MG/L)	
ï	AT AVERAGE	IN OUTFALL 003		AT AVERAGE	IN OUTFALL 003	
	F.LOW OF	AT FLOW		FLOW OF	AT FLOW	
DATE	0.344 MGPD	OF 1.275 MGPD	DATE	0.544 MGPD	OF 1.275 MGPD	
12/04/74	0.05	0 013	07/23/75	0.04	0.017	
12/12/74	0.06	0.016	07/30/75	0.07	0.030	
12/18/74	0.06	0.016	08/07/75	0.07	0.030	
01/02/75	0.04	0.011	08/13/75	0.56	0.239*	
01/10/75	0.31	0.021	08/20/75	0.06	0.026	
01/15/75	0.06	0.004	08/27/75	0.00	0.020	
01/30/75	0.05	0.013	09/03/75	0.13	0.055	
02/07/75	0.03	0.013	09/10/75	0.15	0.021	
02/11/75	0.04	0.011	09/16/75	0.03	0.030	
02/18/75	0.04	0.011	00/10/15	0.07	0.050	
02/10/75	0.04	0.011				
03/05/75	0.11	0.011				
03/14/75	0.11	0.034				
03/21/75	0.36	0.024				
03/25/75	0.33	0.089				
04/02/75	0.33	0.084				
04/10/75	0.31	0.059				
04/16/75	0.24	0.065				
04/23/75	0.11	0.030				
05/02/75	0.23	0.062				
05/08/75	0.12	0.032				
5/15/75	0.17	0.046				
105/22/75	0.13	0.035				
05/28/75	0.05	0.013	6			
06/04/75	0.05	0.013			7	
06/11/75	0.08	0.022				
06/17/75	0.04	0.011		. 6		
06/25/75	0.41	0,111				
07/02/75	0.14	0.038				
07/09/75	0.78	0.210*				
07/10/75	0.46	0.124				
07/17/75	0.09	0.124	1.			
0111113	0.05	0.121	S		14	

*Possible violations of final daily maximum limit of 0.2 mg/l.

APPENDIX "C" TABLE I - TOTAL Pb CONCEN-TRATIONS AT OUTFALL 003 (CGW #2)

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APPENDIX "D"

CALCULATIONS FOR A GRAVITY OIL SEPARATOR USING API DESIGN CRITERIA (1)

Wastewater Flow: 609,000 GPD = 57 CFM From Equation (7) Pg. 19, Rate of Rise $V_t = 0.0241$ (Sw-So)

Temp. ^OF at above flow (from Outfall CGW #1 data) = $67^{O}F$ From Fig. 2 Pg. 19. Specific gravity of wastewater, Sw = 0.997 From Fig. 3 Pg. 19. Absolute viscosity of oil, μ = 0.0103 From Manufacturer's Label, Specific gravity of oil, So = 0.882

 $V_{t} = \frac{0.0241 \ (0.977 - 0.882)}{0.0103}$

 $V_{t} = 0.269$

From Figure 4 Pg. 24. Since $V_t > 0.2$, Horizontal Velocity V_h = 3 Ft/Min. From Figure 4 Pg. 24. Theoretical cross sectional area A_c = 19 Ft.² From Figure 4 Pg. 24. Theoretical depth, d = 3.1 Ft.

Therefore, theoretical width, B = 19 = 6.1 Ft. 3.1

Theoretical ratio $\frac{V_h}{V_t} = \frac{3}{0.269} = 11.2$

From Figure 7. Pg. 25. Theorectical length, L = 54 Ft. Theoretical depth to width ratio $\frac{d}{b} = \frac{3 \cdot 1}{6 \cdot 1} = 0.508$

Dimensions of theoretical separator recommended by API are --

54 Ft. long X 6.1 Ft. wide X 3.1 Ft. depth (liquid)

Dimensions of each existing lagoons at Pressware Plant 100' long X 30' wide X 7' depth (liquid)

Both lagoons will be used in series.

(1) REF: API manual on disposal of Refinery Wastes - Vol. I, 7th Ed. Chapter 2.



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